

Department of Energy

Sandia National Laboratories

X, 162 P.

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NTIS price codes Printed copy: A16 Microfiche copy: A01

SAND94-2525 Unlimited Release Printed January 1995

Distribution Category UC-1301

RESULTS OF MOLTEN SALT PANEL AND COMPONENT EXPERIMENTS FOR SOLAR CENTRAL RECEIVERS: COLD FILL, FREEZE/THAW, THERMAL CYCLING AND SHOCK, AND INSTRUMENTATION TESTS

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Abstract

Experiments have been conducted with a molten salt loop at Sandia National Laboratories in Albuquerque, NM to resolve issues associated with the operation of the 10MW_e Solar Two Central Receiver Power Plant located near Barstow, CA. The salt loop contained two receiver panels, components such as flanges and a check valve, vortex shedding and ultrasonic flow meters, and an impedance pressure transducer. Tests were conducted on procedures for filling and thawing a panel, and assessing components and instrumentation in a molten salt environment. Four categories of experiments were conducted: 1) cold filling procedures, 2) freeze/thaw procedures, 3) component tests, and 4) instrumentation tests. Cold-panel and -piping fill experiments are described, in which the panels and piping were preheated to temperatures below the salt freezing point prior to initiating flow, to determine the feasibility of cold filling the receiver and piping. The transient thermal response was measured, and heat transfer coefficients and transient stresses were calculated from the data. Analysis is presented which quantifies the thermal stresses in a pipe undergoing thermal shock. In addition, penetration depths were calculated to determine the distances salt could flow in cold pipes prior to freezing shut and validated with panel tests. Freeze/thaw experiments were conducted with the panels, in which the salt was intentionally allowed to freeze in the receiver tubes, then thawed with heliostat beams to assess permanent deformation in the tubes, and to develop procedures to thaw a panel so minimal damage occurs. Slow thermal cycling tests were conducted to measure both how well various designs of flanges (e.g., tapered flanges or clamp type flanges) hold a seal under thermal conditions typical of nightly shut down, and the practicality of using these flanges on high maintenance components. In addition, the flanges were thermally shocked to simulate cold starting the system. Instrumentation such as vortex shedding and ultrasonic flow meters were tested alongside each other, and compared with flow measurements from calibration tanks in the flow loop.

ACKNOWLEDGMENT

We would like to acknowledge the following for their contribution to the molten salt panel and component experiments:

Greg Kolb Scott Rawlinson Craig Tyner -Roy Tucker John Kelton Darrell Johnson Clifford Hilliard Albert Mitchusson.

We would also like to thank Ann Van Arsdall for providing helpful suggestions to the report and acknowledge Tech Reps for formatting the manuscript.

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Nomenclature

Bi = Biot number

- $Cp_s = specific heat of solid$
- Cp_m = specific heat of liquid
- D = diameter of pipe
- E = modulus of elasticity
- Fo = Fourier number
- h = heat transfer coefficient
- $h_f = heat of fusion$
- k = thermal conductivity of pipe (Eq. 5)
- L = wall thickness
- Nu = Nusselt number
- Pr = Prandtl number
- r = radial coordinate of pipe
- $\mathbf{r}_i = \text{inner radius of pipe}$
- $\mathbf{r}_{o} =$ outer radius of pipe
- r^{*} = nondimensional pipe radius
- R = radial coordinate of inner radius of pipe
- R_o = radial coordinate of frozen layer
- Re = Reynolds number
- T = temperature
- $T_f =$ freezing point
- T_i = initial wall temperature
- T_0 = inlet liquid temperature
- $T_w =$ wall temperature
- T_{∞} = fluid temperature
- \mathbf{x}^{*} = nondimensional distance from insulated surface
- z = distance to freeze closed
- α = thermal diffusivity (Eq. 3) or coefficient of thermal expansion (Eq. 9)
- α_m = thermal diffusivity of liquid
- α_s = thermal diffusivity of solid
- $\delta = 1 r_i^{\bullet} =$ nondimensional wall thickness
- λ_n = characteristic values of transient conduction equation
- γ = parameter measuring the relative importance of sensible to latent heat, assumed to be 0.7 (water)
- θ^* = nondimensional temperature
- θ_0^* = nondimensional temperature at the insulated surface
- σ_0 = circumferential stress
- σ_r = radial stress
- σ_z = axial stress
- σ^* = nondimensional thermal stress
- v = Poisson's ratio

Executive Summary

This report summarizes experiments we conducted with a molten salt flow loop, located at the Central Receiver Test Facility at Sandia National Laboratories in Albuquerque, New Mexico, under the US DOE Central Receiver Development Program. Experiments were conducted to test hardware and instrumentation in a molten salt environment and to develop procedures that support the design and operation Solar Two. Solar Two is a 10 MW_e Solar Central Receiver Pilot plant in Daggett, California, which is undergoing retrofit with a receiver and storage system which use molten salt as the heat transfer fluid. The major conclusions and recommendations from our experiments with the molten salt loop are summarized below.

Cold Fill Tests

We successfully showed that molten salt can flow through ambient temperature piping without freezing shut provided the flow rate is high enough. These results were scaled to the riser and down comer of the Solar Two and a 100 MW_e molten salt power plant using a correlation. These large diameter pipes should not freeze closed during the cold filling procedure (e.g., at morning startup). The thermal stresses during this thermal shock were calculated to be lower than the material's endurance limit for vertical runs of the piping. We recommend testing the cold filling method in the riser and downcomer of Solar Two and if it proves favorable, implemented as a mode of operation in commercial plants to reduced parasitic power consumption and increase availability.

We found every region of the receiver does not have to be above the salt freezing point before flow is initiated. The minimum temperature to avoid freezing during startup for the Solar Two receiver is estimated to be 200°F (93°C). We found the best method for preheating a panel was to use moving heliostats to avoid hot or cold spots.

Freeze/Thaw Tests

A receiver panel which becomes frozen with salt could require hours to thaw and could damage the tubes. We measured permanent strains as high as 4% after two freeze/thaw cycles. Monitoring the temperatures during the thawing process was also difficult with a limited number of thermocouples, but an infrared camera would simplify the monitoring.

Component Tests

We found that check valves work well in a molten salt environment after repeated pressure cycling and recommend their use. Flanges held up well to slow thermal cycling and to thermal shocking without major failures. All the flanges tested, though, began to leak slowly. Flanges should be minimized in a molten salt loop. Hot torquing the flanges, periodically, may help reduce the leaks.

Instrumentation Tests

Vortex shedding flow meters worked exceedingly well with molten salt and are the preferred flow meter for this application. Overall flow rate uncertainties of less than $\pm 5\%$ can be obtained with a proper calibration. The impedance-type pressure transducer we tested was responsive and performed well. It could replace hard to find NaK filled pressure transducers. The impedance type is relatively expensive, though.

I. Background

In a molten salt central receiver power plant, the parasitic electrical power consumption can be a significant percentage of the total power production if it is not properly managed. Good management also involves careful assessment of operating strategies to minimize the parasities. Since the nitrate salt, which serves as the heat transfer medium between the receiver and the steam generator, has a freezing point of 430°F (221°C), the associated piping, valves, instrumentation, and tanks must be kept above this temperature (typically at 550°F, 288°C) to assure the salt will not freeze. During inclement weather and during the night the plant does not operate, but the heat trace is kept energized to maintain the temperature of the empty lines at 550°F (288°C). This operating strategy is not an economically advantageous method of conditioning a highly cyclic power plant. One strategy of reducing the nightly parasitic power consumption is to turn off the heat trace at night, allowing the piping to cool down to ambient, then fill the piping cold at start up the next morning.

There has been very little data collected on cold starting the receiver and piping at temperatures below the molten salt freezing point. The Molten Salt Electric Experiment receiver in the external configuration was cold started at temperatures below the freezing point. In one of three cases, the receiver partially froze [1]. No detailed analysis was done on the transient freezing phenomenon. In this report we describe experiments where we cold started receiver panels and piping.

Due to the nitrate salt's high freezing point and the fact that the salt expands upon melting, we were concern with the damage that could occur in receiver tubes if the salt were to freeze in the receiver and then thaw out. This situation could occur during shut down of the receiver. If one of the drain valves failed to open and went undetected during the drain process, molten salt would be trapped in the associated panel, and the salt would subsequently freeze. Upon thawing, the expanding salt could damage the tube. In previous experiments, detailed assessments of the freezing and thawing of the panel tubes were not conducted. The Martin Marietta molten salt receiver became frozen with salt and was successfully thawed, though no data on tube deformation was available.

Three molten salt receivers and large-scale pump and valve loops have been tested at Sandia National Laboratories to determine the viability of molten salt as a heat transport fluid and storage medium for central receiver solar power plants. The Category B receiver was a 5 MWt cavity molten nitrate salt receiver. The testing of this receiver in 1988 [2] showed the feasibility of fabricating and operating a molten salt receiver consisting of serpentine flow panels. However, there are some components and instrumentation that need further evaluation.

Check valves have not previously been used in molten salt. Check valves are required when pumps are connected in series to a common manifold, or to the base of a riser to prevent back spin and damage to a pump during a sudden shut off of one pump while the others are flowing. Experiments with flanges in the Pump and Valve Loop show that they were a significant source of leaks.

The purpose of the current molten salt experiments is to verify the operation and reliability of components, instrumentation, and procedures proposed for implementation in the Solar Two project. Many of the components have been proven in a molten salt environment, but additional information is required. Other components were not tested sufficiently or at all in previous molten

salt experiments. The goal of these tests was to reduce uncertainties concerning the performance of untested components and operating procedures (e.g., cold filling the receiver or piping, and thawing a frozen panel.)

We conducted these tests to address concerns by the Solar Two Technical Advisory Committee - a committee of utilities, industries, the U.S. Department of Energy, and Sandia National Laboratories overseeing the technical issue of the Solar Two Project. The technical needs and concerns were prioritized, and a test program was developed. Consequently, some issues, such as thermal cycling of full scale valves, could not be implemented. However, this test program did address all the high priority issues.

II. System Description

The experiments were conducted with an existing molten salt loop initially built for a direct absorption receiver [3]. It was modified to accommodate two wing panels (fabricated by Foster Wheeler Corporation) removed from a salt-in-tube receiver (the Category B receiver) to evaluate a cold receiver startup procedure and conduct freeze/thaw experiments. Each panel consists of two serpentine flow passes which have six 1 inch (2.5 cm) OD 304 stainless steel tubes with 0.065 inch (1.65 mm) thick walls. The two passes are connected to a common 6 inch (15 cm) diameter manifold (schedule 80 piping) at the top of the panel. Each panel vent connects to a common 1 inch vent line, in which a hand valve is located to vary the venting flow rate. The experiment was located at the base of the Solar Tower at the National Solar Thermal Test Facility in Albuquerque, NM. Figure 1 is a schematic of the system and the wing panels. Figure 2 is a photograph of the panels and flow loop.

In this flow loop, salt is pumped from the salt sump, through the components, then either returned to the sump or diverted up the riser. At the top of the riser is the pressurized accumulator (surge) tank. The flow goes through the down comer, and can either be diverted to the panel or a manifold. The outlet of the panel flows into the manifold. The manifold drains into two calibration tanks. Flow from the calibration tanks returns to the sump. The pump can flow salt at 100 gallons per minute (380 liters/min) through the 2 inch (5.1 cm) piping.

We added flanges, a check valve, flow meters, and pressure transducers to test their performance. Three types of flanges were tested: 1) clamped, compressive metal-seal type flanges made by Reflange (R-CON) and by Grayloc, 2) bolted, compressive metal-seal flanges (E-CON) also made by Reflange, and 3) a standard ANSI ring-joint flange. The check valve, manufactured by Reflange (V-CON), was a spring-loaded, swing-type check valve. Two types of flow meters were tested: 1) vortex shedding flow meters made by Engineering Measurements Company, and 2) ultrasonic flow meters (wetted type and clamp on type transducers) manufactured by Panametrics. In addition, we installed pieces of performed fiberglass insulation to determine their viability as another insulation material. This insulation is easier to install than the wool blanket or calcium silicate insulation previously used. Its upper temperature limit is approximately 850°F. Table 1 lists the components we tested.

Although we were not able operate the flow loop at the pressures expected to be encountered in the cold side of a typical molten salt system, we were able to simulate operational and thermal cycling expected on the cold side of the system where the thermal ramp rates and stresses are typical of nightly conditioning. The ramp rates on the hot side of a molten salt system (down stream of a receiver) are very difficult to simulate with the existing loop, and therefore were not simulated with this test setup.



Figure 1. Flow schematic of the system (a) and a wing panel front (b) and side view (c).



Figure 2. Photographs of molten salt panels (a and b) and flow loop test section (c) at the base of the Central Receiver Test Facility at Sandia National Laboratories.

Component or instrumentation	Туре	Size	Manufacturer
Flange	Clamped, compressive metal seal type	2 inch and two 4 inch	Reflange (R-CON) and Grayloc (2 inch)
Flange	Bolted, compressive metal seal type	6 inch	Reflange (R-CON)
Flange	ANSI ring type flange	4 inch	standard
Check valve	Spring loaded swing	3 inch	Reflange (V-CON)
Flow meter	Vortex shedding	2 inch	Engineering Measurements Co.
Flow meter	Ultrasonic - wetted transducer	2 inch	Panametrics
Flow meter	Ultrasonic - clamp on transducer	any sized pipe up to 10 feet dia.	Panametrics
Pressure	High temperature Impedance	0-250 psi range	Kaman
transducer			

Table 1. Components and instrumentation tested in molten salt loop.

III. Test Results

Cold Fill Tests

Cold filling involves flowing molten salt through piping or the receiver when all or part is below the salt freezing point. Cold filling has several advantages in the operation of a plant that experiences cyclic operation. If the molten salt can flow through parts of the system which are below the freezing point, parasitics could be reduced, since the heat trace would not have to be used on those lines. In addition, the operation of the plant could be more flexible if the plant could be brought on line faster by not having to wait for the heat trace to heat the lines to operating temperatures resulting in increased availability. Also, during morning startup, it is difficult to uniformly preheat the entire receiver. Some spots will experience much more heating than others due to non-uniform flux profiles from heliostats. This is a particular concern for the east side of a cylindrical receiver during morning start up. Localized convection will add to the problem. A roving aiming strategy, where the heliostat aim points are periodically changed, could provide more uniform heating of the receiver panels, thus avoiding severe hot or cold spots. Also, if the receiver can be filled with molten salt when areas of the receiver are below the salt freezing point, the receiver start up procedure would be much simpler, and could occur sooner. These strategies will boost performance and reduce operating expenses, resulting in lower energy costs. There are two major concerns with cold filling components and piping: freezing of the flowing salt, and transient thermal stresses.

We conducted cold fill experiments on the panels and on a section of piping. We measured the thermal response as the panel or piping underwent the rapid change in temperature, and estimated the heat transfer coefficients during this transition. We also derived expressions describing the transient stresses a pipe or tube will experience during a thermal shock. Using a correlation which describes the penetration distance of a liquid as a function of the fluid properties and flow conditions, we estimated the distance salt could flow through cold piping before freezing shut.

Results of Cold Fill Panel, Manifold, and Piping Tests. We conducted tests varying the initial panel temperature to determine whether salt could flow through all four passes of the panel before freezing shut. The flow velocity was approximately the same for each test, 2 ft/s (0.6 m/s). The purposes of these tests were to 1) determine if salt flow could be established in "cold" manifolds, panels, and piping, 2) measure the thermal responses of the tubes and manifolds undergoing thermal shock, and 3) estimate the corresponding stresses in the materials.

We conducted a series of tests trying lower and lower panel preheat temperatures ranging from 550 °F (288°C) to ambient before initiating salt flow. Next, we tried flowing salt through cold (near ambient) manifolds (heat trace off) with the panels preheated to 550°F. Then we tried flowing through cold manifolds and cold panels. Each scenario was repeated several times.

We found we were able to consistently flow through ambient temperature manifolds and panels without freezing salt or blocking tubes. In our test loop, we were able to fill the panels only in a serpentine fashion. To prevent entrapment of air, we had to fill the panel slowly (~ 2 ft/s, 0.6 m/s). Figure 3 shows the temperature response of the tubes and upper manifold as they are filled with 550°F (288°C) salt. The receiver tubes were initially at 50°F (10°C). The header was

Temperatures During Cold Fill



Figure 3. Temperature response of the cold receiver tubes and upper header as they are filled with 550°F (288°C) salt.

initially hotter than the panels, since an adjacent heat trace zone conducted heat to the header. The header and first pass receiver tubes experienced the greatest thermal shock. As the salt continued through the other passes, the temperature of the initial slug of salt decreased, resulting in the deposition of a frozen layer of salt on the tube wall, which reduced the shock, then melted away. This can be inferred from the change in slope of the fourth pass tube temperature and the upper header temperature. Figure 4 shows the temperature ramp rates of first, second, third, and fourth pass tubes. Note how the third and fourth passes show lower peak ramp rates. A frozen layer of salt is likely responsible for the reduced peak ramp rates, since as the initial slug of salt comes in contact with the cold tube surface, a frozen layer develops which limits the rate at which the temperature can rise, and provides some thermal capacitance. The outside tube temperature corresponding to the peak ramp rate in the fourth pass is approximately 395°F (202°C).

A thermal analysis was conducted on a receiver tube and header during this thermal shock, and is described in the Thermal Analysis section. The estimated heat transfer coefficients were calculated. In addition, calculations on the penetration depths—the distance a fluid flows through cold piping before freezing shut— are also discussed in the Calculation of Penetration Distances section.

Ramp Rates



Figure 4. Temperature ramp rates of first, second, third, and fourth pass tubes.

The stresses in the receiver tube were calculated using the heat transfer coefficients obtained from the experiment. A stress model is described in the Transient Stress Analysis section. Stresses in the tube-to-header junction are more complicated, and are dictated by the temperature gradients at the transition.

In addition to cold filling the panels and manifolds, we conducted similar tests on a section of piping. We turned off the heat trace to a section of piping and let it cool to ambient, then initiated salt flow to determine its thermal response and estimate heat transfer coefficients and stresses. We measured the thermal response of an insulated 40 foot $(12 \text{ m}) \log_2 2 \text{ inch} (5.1 \text{ cm})$ diameter 316 SS, schedule 40 pipe undergoing thermal shock. The piping was part of the riser. We turned off the heat trace, and allowed it to cool to ambient. When the piping was cold (at ambient), we pumped salt through it at approximately 9.5 ft/s (2.9 m/s) and measured the temperature outside of the pipe. Figure 5 is a plot of the outside wall temperature as a function of time. With this data, we calculated the heat transfer coefficient at the inner wall using a first eigenvalue approximation to an analytical solution of plane wall conduction. These procedures are discussed in the next section.



Figure 5. Outside wall temperature as a function of time of a 2 inch schedule 40 pipe undergoing thermal shock. The symbols are actual data points. The solid line is a fit of the data using the thermal model for Bi = 0.444.

Thermal Analysis During Cold Fill. In the cold-fill experiment on the panel, manifolds, and piping, we measured the outside wall temperatures as they are thermally shocked. From that data we wanted to obtain the inside wall temperature and the average heat transfer coefficient. The heat transfer coefficient allowed us to calculate the stresses developing in the wall of the pipe or tube as it rapidly heats up.

Assuming that the tube or pipe wall can be approximated as a plane wall, we can use an analytical solution to estimate the inside wall temperature and heat transfer coefficient. Since the receiver tube and piping have relatively thin walls, the plane wall assumption is a good approximation. In our tests, the outside of the pipe, manifolds, and the receiver tubes were insulated. (In actuality, only half of the receiver tube is insulated and the other side is exposed, but this should have minor bearing on the result, since initially the outside natural convective heat transfer to the air is relatively small, and the time scales are short for thermal shock.)

The solution to the energy equation for a plane wall suddenly subjected to a convection boundary condition describes the temperature distribution in the wall as a function of time [4]. Its form is:

$$\theta^*(x^*,t^*) = \frac{T(x,t) - T_{\infty}}{T_t - T_{\infty}} = \sum_{n=1}^{\infty} C_n \exp(-\lambda_n F_0) \cos(\lambda_n x^*)$$
(1)

where the coefficient C_n :

$$C_n = \frac{4\sin(\lambda_n)}{2\lambda_n + \sin(2\lambda_n)},$$
(2)

Fo (the Fourier number) is the nondimensional time and x^* is referenced from the insulated surface:

$$Fo = \frac{\alpha t}{L^2}, \ x^* = \frac{x}{L}.$$
(3, 4)

The discrete characteristic values (eigenvalues) of λ_n are the positive roots of the transcendental equation:

$$\lambda_n \tan(\lambda_n) = Bi = \frac{hL}{k}.$$
(5)

The length, L, is half the thickness of the plane wall since convection occurs on both faces, but in the case of a pipe or tube wall it is equal to the wall thickness, since one face has convection and the other is insulated. Note the midplane of a plane wall behaves like an insulated surface. The infinite series solution can be approximated by the first term in the series for values of $Fo \ge 0.2$. The solution becomes:

$$\theta^* = C_1 \exp(-\lambda_1^2 F o) \cos(\lambda_1 x^*)$$
or
(6)

$$\theta^* = \theta_o^* \cos(\lambda_1 x^*) \tag{7}$$

where θ_o^* is the temperature at the midplane, $x^*=0$ (the insulated boundary, in our case the outside tube wall). The coefficients C_1 and λ_1 are determined from the equations 2 and 5. Since we measured the outside wall temperature (insulated surface) as a function of time and we knew the approximate salt bulk-fluid-temperature ('initial salt temperature), we calculated measured values for θ_o^* and Fo. By iterating on λ_1 until the calculated value of θ_o^* converged on the measured value of θ_o^* , we obtained the Biot number, Bi. From the Biot number we obtained the heat transfer coefficient.

The average heat transfer coefficients determined during the thermal shock for each pass, for the upper header, and for a 2 inch pipe are shown in Table 2. The solid line in Figure 5 is a fit of the data to the model for a constant heat transfer coefficient. Note that initially the temperature changes gradually (the first three data points). In order to get a good fit of the data with the model, the initial starting time of the model had to be adjusted, since the actual heat transfer coefficient is not constant with time. Assuming a constant heat transfer coefficient will yield higher stresses than one which gradually increases to its final value, and thus will be conservative. Stress analyses for an insulated circular pipe undergoing thermal shock are discussed in the next section.

For heat transfer in fully developed pipe flow when applied to freezing with turbulent flow, the following correlation has been suggested to estimate heat transfer coefficients between the fluid and the frozen layer [5]:

$$Nu = 0.0155 \ Rc^{0.83} Pr^{0.5} (R_{e}/R)^{0.83}$$
(8)

Location	Approx. Velocity m/s	Bi (from data using the model)	h (from Bi) W/m ² K
2" sch40 Pipe	2.9	0.444	1700
6" sch80 Header	0.11	0.881	1200
First Pass Tube	0.67	0.296	2700
Second Pass Tube	0.67	0.243	2200
Third Pass Tube	0.67	0.124	1100
Fourth Pass Tube	0.67	0.114	1000

Table 2. Biot numbers and heat transfer coefficients during cold fill experiments.

where R_o is the inner pipe radius and R is the radial coordinate of the frozen layer. This correlation is applicable beyond the thermal entrance length (approximately 10 tube diameters), and provides a conservative estimate of the heat transfer to the pipe, since the frozen layer will act as an insulator.

It should be noted that the heat transfer that occurs when the receiver is under high flux is quite different for a cold start scenario. A description of the heat transfer under high flux is presented in Appendix C.

Transient Stress Analysis of Piping and Tubes Undergoing Thermal Shock - **Nondimensional Analysis.** The stress calculations are important in determining the material behavior in a severe transient condition. For an insulated pipe, we can use the temperature distribution from the thermal analysis to calculate the circumferential, radial, and axial stresses. These thermal stresses should be superimposed on existing pipe loads due to structural factors. If the temperature is a function of the radial component only, then each component of stress is [6,11]:

$$\sigma_{\theta}(r) = \frac{E\alpha}{(1-\nu)r^2} \left(\frac{r^2 + r_i^2}{r_o^2 - r_i^2} \int_{r_i}^{r_o} T(r)rdr + \int_{r_i}^{r} T(r)rdr - T(r)r^2 \right)$$
(9)

$$\sigma_{r}(r) = \frac{E\alpha}{(1-\nu)r^{2}} \left(\frac{r^{2} - r_{i}^{2}}{r_{o}^{2} - r_{i}^{2}} \int_{r_{i}}^{r_{o}} T(r)rdr - \int_{r_{i}}^{r} T(r)rdr \right)$$
(10)

$$\sigma_{z}(r) = \frac{E\alpha}{(1-\nu)} \left(\frac{2}{r_{o}^{2} - r_{i}^{2}} \int_{r_{i}}^{r_{o}} T(r) r dr - T(r) \right)$$
(11)

The temperature profile at a given time, Fo, can be found from Equation 7:

$$T(r) = \theta^{\bullet}_{o}(T_{i} - T_{\infty}) \cos(\lambda_{i} x^{\bullet}) + T_{\infty}$$
(12)

The nondimensional length x^* is referenced from the insulated surface (the outside radius) and can be transformed into the nondimensional radial coordinates, $r^*=r/r_0$ and $r^*_i=r_i/r_0$, from:

$$x^{*}=(1-r^{*})/(1-r^{*})=(1-r^{*})/\delta.$$

In carrying out the integration, the stress components can be expressed in a nondimensional thermal stress format:

$$\sigma^*(r^*) = \frac{\sigma(r)(1-\nu)}{E\alpha(T_i - T_{\alpha})}$$
(13)

Which for the three stress components are:

$$\sigma_{\theta}^{*}(r^{*}) = \frac{r^{*2} + r_{i}^{*2}}{1 - r_{i}^{*2}} \frac{\partial_{\alpha}^{*}}{r^{*2}} \left\{ \frac{\partial_{\lambda_{1}^{2}}^{2}}{\lambda_{1}^{2}} \left\{ 1 - \cos(\lambda_{1}) \right\} + \frac{\delta r_{i}^{*}}{\lambda_{1}} \sin(\lambda_{1}) \right\} + \frac{\delta^{2} \partial_{\alpha}^{*}}{\lambda_{1}^{2} r^{*2}} \left\{ \cos(A) - \cos(\lambda_{1}) \right\}$$

$$\left. - \frac{\partial \partial_{\alpha}}{\lambda_{1} r^{*2}} \left\{ r^{*} \sin(A) - r_{i}^{*} \sin(\lambda_{1}) \right\} - \partial_{\alpha}^{*} \cos(A) \right\}$$

$$\sigma_{r}^{*}(r^{*}) = \frac{r^{*2} - r_{i}^{*2}}{1 - r_{i}^{*2}} \frac{\partial_{\alpha}^{*}}{r^{*2}} \left\{ \frac{\partial^{2}}{\lambda_{1}^{2}} \left[1 - \cos(\lambda_{1}) \right] + \frac{\partial r_{i}^{*}}{\lambda_{1}} \sin(\lambda_{1}) \right\}$$

$$\left. - \frac{\partial^{2} \partial_{\alpha}}{\lambda_{1}^{2} r^{*2}} \left\{ \cos(A) - \cos(\lambda_{1}) \right\} + \frac{\delta r_{i}^{*}}{\lambda_{1}} \sin(\lambda_{1}) \right\}$$

$$\left. + \frac{\partial \partial_{\alpha}}{\lambda_{1} r^{*2}} \left\{ r^{*} \sin(A) - r_{i}^{*} \sin(\lambda_{1}) \right\}$$

$$\left. + \frac{\partial \partial_{\alpha}}{\lambda_{1} r^{*2}} \left\{ r^{*} \sin(A) - r_{i}^{*} \sin(\lambda_{1}) \right\}$$

$$\left. - \frac{\partial_{\alpha}}{\partial c} \cos(A) \right\}$$

$$(17)$$

$$A = \frac{\lambda_1}{\delta} (1 - r^*) \tag{17}$$

The characteristic value, λ_1 , is found from the solution to Equation 5 and is a function of the Biot number, Bi, which indicates the relative importance of surface heat transfer to conduction. Equations 14 to 16 are valid for $Fo \ge 0.2$. For smaller times (Fo <0.2), several terms in the series in Equation 1 must be used to calculate the temperature distribution. The temperature distribution is then used in Equations 9-11 to calculate the stresses. These equations can be used to calculate the transient stresses as a function of the Biot number and the pipe geometry. Figures 6, 7, and 8 show the nondimensional circumferential, radial, and axial thermal stresses as function of the nondimensional radius for several times (Fo) for a specific geometry. Note that in Figure 6 a skin stress develops at the inner surface. When the pipe is cold relative to the fluid—"up shock"—the stresses at the inner surface are compressive and tensile on the outer surface during the thermal shock. When it is hot relative to the fluid—"down shock"—the stresses are tensile on the inner surface. Figure 9 shows the effect of the Biot number on the stress distribution for a specific time. Figure 10 shows the nondimensional thermal (circumferential or axial) stress at the inner surface of the pipe as a function of time (Fo) for several Biot numbers using 30 terms of the series in Equation 1. When the heat transfer coefficient is large relative to the pipe thermal conductivity (large Bi numbers), there will be significant temperature gradients across the pipe wall and larger thermal stresses will develop during a thermal shock. At small Biot numbers, conductivity dominates relative to surface heat transfer and there are small thermal gradients across the wall

Circum. Stress vs Radius



Figure 6. Nondimensional circumferential thermal stresses in pipe undergoing thermal shock as function of the nondimensional radius for several times (Fo) using thirty terms in of the nondimensional temperature equation (Eq. 1) for $r_i/r_o=0.8$ and Bi=100.



Radial Stress

Figure 7. Nondimensional radial thermal stresses in pipe undergoing thermal shock as function of the nondimensional radius for several times (Fo) using thirty terms in of the nondimensional temperature equation (Eq. 1) for $r_i/r_o = 0.8$ and Bi=100.

Axial Stress



Figure 8. Nondimensional axial thermal stresses in pipe undergoing thermal shock as function of the nondimensional radius for several times (Fo) using thirty terms in the nondimensional transient temperature equation (Eq. 1) for $r_i/r_o = 0.8$ and Bi=100.



Effect of Bi

Figure 9. Effect of the Biot number on the nondimensional circumferential thermal stress distribution for a specific time (Fo=0.2) and $r_i/r_o = 0.8$.

Stress vs Time (Fo)



Figure 10. Nondimensional thermal (circumferential or axial) stress at the inner surface of the pipe undergoing thermal shock as a function of time (Fo) for several Biot numbers using 30 terms of the series in the nondimensional transient temperature equation (Eq. 1) for $r_i/r_o=0.8$.

resulting in small thermal stresses. The stresses build with time, reaching a peak, then finally drop as the wall reaches a uniform temperature. Each curve has a maximum thermal stress. These maximum stresses are shown in Figure 11 as a function of the Biot number. Figure 12 shows the time (Fo) when the maximum stress occurs as a function of Biot number.

From the data we gathered during the shock tests, we determined the Biot numbers are relatively small. We used these Biot numbers to calculate the stresses in piping or tubes we thermally shocked: a 2-inch schedule 40 316SS pipe, a 6-in schedule 40 304SS header and a 1-inch 0.065 inch wall 304SS receiver tube. Table 3 shows the maximum equivalent stress based on the maximum energy distortion theory of failure [7], sometimes referred to as the von Mises stress, for each case. In each case the stresses were calculated to be lower than the endurance limit of the material ($\sigma_e \approx 270$ MPa for stainless steel [8]) for these tests indicating that for the test conditions the piping itself can handle these stresses over the life of the system. It is likely these stresses are conservative, since the heat transfer coefficients are not constant, but gradually increase to the equilibrium value.

Maximum Stress vs Bi



Figure 11. The maximum nondimensional thermal stress as a function of the Biot number for a pipe undergoing thermal shock for $r_i/r_o = 0.8$. These are the maxima of Figure 10.

Time When Max. Stress Occurs



Figure 12. The time (Fo) when the maximum thermal stress occurs as a function of the Biot number.

Table 3. Calculated Maximum Stresses at the Inner Wall of Piping or Tubes Initially at 25°C Undergoing Thermal Shock with Molten Salt at 290°C based on the Biot Numbers from Experiments.

Pipe or Tube Size	$\sigma_{Equivalent}$, MPa
1 inch receiver tube, 0.065 inch wall, 304 SS	-100
2 inch schedule 40, 316 SS	-140
6 inch schedule 80 header, 304 SS	-240

Using Equation 9, a conservative estimate of the peak circumferential stresses at the inner surface of a pipe or tube can be calculated as a function of salt velocity. Plots of these relations are shown in Figures 13 and 14 for 6 inch and 16 inch piping proposed for handling molten salt in the Solar Two and Commercial scale systems, respectively. There is a critical velocity at which the stresses exceed the endurance limit of the material. These velocities are listed in Table 4 for several pipe schedules and materials proposed for handling molten salt. Carbon steel is able to handle thermal stresses better than stainless steel, because carbon steel has a much lower coefficient of thermal expansion, even though its endurance limit is lower.

Thermal Stresses in 6" Pipe (Stainless Steel)



Figure 13. Maximum stress at the inside wall as a function of velocity for 6 inch piping.

Thermal Stresses in Stainless Steel 16 inch Pipe



Figure 14. Maximum stress at the inside wall as a function of velocity for 16 inch piping.

Pipe Size	Schedule	Material	Maximum Velocity, m/s
6 inch	80	Stainless 316	0.9
6 inch	80	Carbon	3.7
6 inch	40	Stainless 316	1.5
6 inch	40	Carbon	6.3
6 inch	10	Stainless 316	3.8
16 inch	80	Carbon	1.9
16 inch	40	Carbon	3.7
16 inch	10	Carbon	12.2
16 inch	10	Stainless 316	5.7

Table 4.Maximum Velocities During Cold Fill Where Maximum Thermal Stresses are Below
Endurance Limit of the Material for $T_{wall} = 25^{\circ}C$ and $T_{salt} = 288^{\circ}C$.

Even though the stresses in the walls of piping or tubes were low when thermally shocked in our tests, high stresses could develop where there are large loads already existing in the piping due to structural considerations, where there is a sudden change in wall thickness, or where there is abrupt changes in contour resulting stress concentrations. It should be noted this analysis applies only to vertical runs of piping or tubes where the temperature gradient is a function of the radial coordinate. In horizontal pipes, the leading edge of the fluid could have a sloped profile resulting in circumferential temperature gradient, in addition to the radial gradient. This would result in stress condition. Most of the piping in the risers and downcomers of molten-salt central-receiver solar power plants is in vertical runs.

For a receiver illuminated with high flux, the stresses are quite different from the stresses during thermal shock. In addition to a through-wall stress, there is a front-to-back tube stress. Appendix D shows the strain equations applicable to receiver tubes under high flux.

Calculations of Penetration Distances - Transient Freezing in Pipes. Another issue pertaining to cold starting piping is how far the molten salt can flow through a cold pipe before freezing shut. This length is known as the penetration distance. There are several models which describe transient freezing in pipes, but one model correlates data from several experiments and a variety of fluids into a single equation that describes the penetration depth as a function of the fluid properties, the Reynolds number, the wall temperature, and fluid temperature [9]. The correlation, Equation 18, describes the axial distance a fluid will flow through a cold pipe whose temperature is held below the fluid's freezing point before the pipe freezes shut. The wall temperature is held constant.

$$\frac{z}{D} = 0.23 \operatorname{Pr}^{1/2} \operatorname{Re}^{3/4} (\alpha_m / \alpha_s)^{1/9} [h_f / (Cp_s(T_f - T_w))]^{1/3} [1 + \gamma Cp_m(T_o - T_f) / h_f]$$
(18)

The penetration depths were calculated for molten salt properties at several pipe diameters and flow velocities. These results are shown in Table 5 and in Figure 15. For large diameter piping, such as used with the riser or downcomer in the Solar Two central receiver power plant, we could theoretically flow through hundreds or thousands of feet of piping. In a commercial scale plant, we may be able to flow through *miles* of cold piping. We expect these values to be conservative, since the correlation was developed for a constant wall temperature.

Diameter	Flow Velocity	Salt Inlet Temperature	Penetration Depth
0.75 in	3 m/s (9.8 ft/s)	288°C (550°F)	39 m (129 ft)
0.75	1 m/s (3.3 ft/s)	288°C (550°F)	17 m (57 ft)
0.75	l m/s	371°C (700°F)	27 m (87 ft)
1.5 in	3 m/s	288°C (550°F)	132 m (435 ft)
1.5	l m/s	288°C (550°F)	58 m (191 ft)
1.5	l m/s	371°C (700°F)	90 m (294 ft)
6 in	3 m/s	288°C (550°F)	1498 m (4920 ft)
6	l m/s	288°C (550°F)	657 m (2160 ft)
16 in	3 m/s	288°C (550°F)	8340 m (27400 ft)
16	l m/s	288°C (550°F)	3660 m (12000 ft)

Table 5. Penetration depths for molten salt for various pipe diameters, velocities, and salt inlet temperatures for a wall temperature $T_w = 68^{\circ}F$ (20°C).

For the panel experiments described previously, we were able to flow through four passes and the associated headers and jumper tubes all at ambient temperature with a salt velocity of 2 ft/s (0.6 m/s). The total length of tubing is about 60 feet (18 m). The correlation predicts the fluid should freeze in about 50 feet (15 m). This means we were probably on the border of freezing.

Penetration Depths vs Salt Flow Rate



Figure 15. The penetration depths for several pipe diameters as a function flow velocity.

In addition, we were able to flow through over 155 feet (47 m) of ambient temperature ($<100^{\circ}$ F) 2 in piping without freezing the pipe shut. The correlation predicted we would be able flow at least twice that distance. It should be noted that the correlation was developed for piping that was submerged in a bath of fluid to hold the pipe outer surface at a constant temperature. In the cold fill tests described in the previous section, the piping or receiver tubing was not held at a constant temperature, but allowed to heat up. The correlation may be conservative, because an insulated pipe has a finite heat capacitance.

When tried filling the panels at lower velocities (0.4 m/s), we were not able to flow through all the passes. We detected salt in the second and part of the third pass, but it is unclearly whether the flow stopped in third pass due to freezing, or a systematic problem. The correlation predicted we should have frozen in the third pass. Unfortunately, we could not the verify the accuracy of the correlation very well with the panels, because they are connected with a common vent line which allows the flow to bypass the second and third pass and enter the fourth pass. We postulate that when the flow through the tubes in the second and third pass becomes restricted due to a buildup of a frozen layer of salt, the preferential path of least resistance is the bypass line. This could effectively cut off the venting of air through the second and third passes, resulting the panel becoming air bound.

In a report on the Molten Salt Electric Experiment of a receiver in the external configuration [1], experiments are described in which the receiver was started cold in a flood fill mode (all the panels in a receiver are filled from the bottom up). In two cases they succeeded in filling the panel, but in one case they froze part of it. For this case, the correlation predicts that salt would have barely made it through the 11.5 foot (3.5 m) high panel, which is consistent with the results.

The data are summarized in Table 6. (The flow rate was not given in the report, but was calculated from information about the system. The fact that third test in the series has a higher penetration distance than the second one may be attributed the uncertainty in the flow assumption and average panel temperature measurement.)

Table 6.Results for cold start experiments with the MSEE external receiver along with the
correlation results. The panel height is 11.5 feet (3.5 m), tube diameter 0.62 inches
(1.6 cm), salt flow rate approximately 0.4 ft/s (0.1 m/s).

Wall Temp	Salt Temp	Penetration Distance	MSEE Result
325°F (163°C)	700°F (371°C)	19.0 ft (5.8 m)	Fill OK
240°F (116°C)	650°F (343°C)	13.6 ft (4.2 m)	Fill OK
210°F (99°C)	700°F (371°C)	14.7 ft (4.5 m)	Partially frozen panel

For the Solar Two receiver designed by Rockwell, in order to prevent freezing, the receiver panels should be heated (with heliostats) to temperatures above 200°F (93°C) with headers and jumper tubes preheated with heat trace to the salt temperature, assuming the panels are flood filled at the design flow rate. The panels should be heated to at least 390°F (199°C) with jumper tubes initially at ambient temperature. These results are shown in Table 7.

Table 7.Estimated penetration depths for Rockwell's Solar Two receiver. Panel height is
approximately 21 feet (6.4 m), jumper tube length: approximately 10 ft (3.0 m), tube
inside diameter: 0.7145 inches (1.81 cm), salt velocity during flood fill: 0.87 ft/s
(0.27 m/s).

Tube Temp	Penetration depth
10°F (-12°C)	18.35 ft (5.6 m)
100°F (38°C)	19.9 ft (6.1 m)
200°F (93°C)	22.4 ft (6.8 m)
400°F (204°C)	44.3 ft (13.5 m)

Summary of Cold Fill Tests

The following conclusions can be made about the cold fill tests:

- Cold filling the panel and/or manifolds is feasible. In normal operation it would not be necessary to cold fill the panel. As a minimum, our results show that the entire panel does not have to be above the salt freezing temperature before salt flow is established.
- Results from the stress analysis show that the stresses in the header and receiver tubes were below the endurance limit during a thermal shock. Analysis should be done for a particular design of the tube-to-header junction and transitions in piping cross section to make sure there are not any localized stress concentrations, and to estimate the life based on fatigue of these areas.
- The best combination of reduced parasitics and increased availability might be partial preheating (c.g., preheating to 300°F).

- We recommend that even if the piping is cold started, valves, flanges, and instrumentation should be kept near the salt temperature to minimize reliability issues that could arise if these components were thermally stressed.
- Our experience has shown that the most successful method for uniformly preheating the panels is to use a roving aiming pattern where the heliostat aim points change every few seconds to avoid localized under- and overheating.
- Although our results show that we can successfully flow through cold piping and tubes, care must be taken to avoid freezing of salt past slow leaking valves in unheated piping.

Freeze/Thaw Experiments

In a molten salt receiver, there are multiple drain valves. During the nightly shut down of the receiver, a drain valve might fail to actuate. If a valve fails to actuate once in a thousand times, a receiver—which has 14 drain valves—will fail to drain approximately once every two and a half months. That does not necessarily mean a panel will freeze that often. Only if this failure is not detected in time and corrective action (such as manually opening the valve) is not taken will the salt trapped in the associated panels freeze. Since the volume of salt increase when it goes from the solid to the liquid state for a fixed mass, damage can occur to the panel if the salt is thawed in a section of tubing or piping which is constrained at both ends.

The objectives of these tests were to determine the procedure required to thaw a receiver panel if it became frozen with salt, and to determine what amount of damage were done to the receiver tubes during the thawing process. A total of five freeze/thaw cycles were conducted. Prior to installation of the panels, all the tubes' outside diameters were measured at various locations along its length, so we could determine the permanent strain induced during the freeze/thaw tests. The freeze/thaw test procedures we used are described below.

First, we established flow in all tubes of the panels to allow the panels to reach thermal equilibrium. After flowing salt through the panels for several minutes, we shut off all drain and outlet valves to prevent salt from draining out of the panel. We then allowed the panels to cool so their temperatures dropped below salt the freezing point. Figure 16 shows panel and header temperatures as they cool. Note how the slopes of the curves change at the salt freezing temperature is maintained above 460°F (238°C) by heat trace. The panels cooled to the salt's freezing point only 25 minutes after the pump stopped in the shielded environment of the solar tower. An exposed external central receiver (e.g., the Solar Two receiver) will cool much faster.

After the average panel temperature was less than $280^{\circ}F$ ($138^{\circ}C$), we opened the drain and panel outlet valves to empty the lower header of salt. Heat trace was kept on in the headers and on the jumper tubes to maintain the temperature above the freezing point. Once the headers had drained, we initiated thawing with heliostats. The only way for salt to leave the panel as it thaws is through the drain. Therefore, we started thawing from the bottom by putting on one heliostat and allowing it to heat that area of the panel to > $500^{\circ}F$ ($260^{\circ}C$). We continued to add heliostats, one at a time above the previous one, raising the panel temperature. One test was interrupted by weather and had to be continued the next sunny day. Once all thermocouple readings on the panel were above the salt freezing point, we tried to establish flow through the panel. On the first attempt, we were





Figure 16. Temperatures receiver panels and header as they cool when filled with molten salt which freezes in the panel at approximately 430°F (221°C).

unable to flow though the majority of the panel because there were sections of tubes under the insulation where the heat trace could not heat it up enough, and we could not heat it with solar. In these regions we had to rely on conduction to melt the salt. Once we achieved flow through part of the panel we continued to flow salt, which helped thaw the frozen areas. After several hours we were able clear all tubes.

After two freeze/thaw cycles we measured the tube diameters. Plots of the permanent (plastic) strain as a function of the panel height are shown in Figure 17 for the east panel and 18 for the west panel. There did not seem to be any pattern to the damage. The maximum permanent strain induced in the tubes was over 4%. Figures 19 and 20 show the plastic permanent strain as a function of the horizontal location (tube number). The values of tube deformations are also shown in Table 8. Tubes 3, 4, and 5 in the east panel have much lower permanent strains than the other tubes in the panel. The west panel does not show this behavior. These results indicate the freezing phenomenon is complex, and requires further study.

Some observations and conclusions can be made regarding these tests:

- Thawing a frozen panel can require several hours, and could result in significant down time.
- The major problem with thawing the panel was a lack of sufficient heat under the insulation, particularly in the upper header where beneficial natural convection within the header oven cavity is not significant. It may be necessary to install additional heat trace in the regions where the insulation meets the panel to assure those areas can heat up to above the salt melting point.

East Panel Deformation



Figure 17. Permanent strain induced in the east panel tubes as a function of the panel height after two freeze/thaw cycles.



West Panel Deformation

Figure 18. Permanent strain induced in the west panel tubes as a function of the panel height after two freeze/thaw cycles.

Side View: East Panel Deform.



Figure 19. Permanent strain as a function of the width (tube number) for the cast panel.

Side View: West Panel Deformation



Figure 20. Permanent strain as a function of the width (tube number) for the west panel.
Table 8. Pre- and Post-Measurements of Tube Diameters in East and West Panel after 2 Freeze/Thaw Cycles.

Molten Salt Panel Deformation Measurements Pretest Measurements: 02/02/93

Post Measurements	02/07/94-02/08/94

bottom	tation lo	dist fro bottom	E1	El	Doffer. El	Pre E2 Inches	Post E2	Differ. E2 ≪	Pre E3 inches	Post E3	Differ E3	Pre E4	Post E4	Differ. E4	Pre E5	Post (E5 I	Differ. ES	Pre E6	Post Dif	ler. Pre E7	Post E7	Differ. E7	Pre E8	Post E E8 E	Differ Eð	Pre E9	Post Diffe	r Pre E10	E 10	E10	Pre E11	Post E11	Differ. E11	Pre Po E12 E1	st Difter 2 E12
0 0.051 0.102 0.152 0.203 0.254	1 2 3 4 5 6	0 2 4 6 8 10	0.997 0.999 0.997 0.997 1.000	1 013	1 <u>401</u> 2.608	0.997 0.999 0.998 0.999 0.999	1.026	2.806	0.999 0.998 0.999 0.999 0.999	1.010	1.101	1.001 0.999 0.997 1.002 1.000	<u>v Autiliza </u> 	/0 	1.000 1.000 0.999 0.999 0.998	1.000	0.100	1.002 0.999 1.003 1.003 1.003	1 11C3 70	1.0 1.0 1.0 0.9 1.0	14 13 00 00 00 00 00		0.998 0.998 0.999 0.999 0.999	withers 7	~ 	0.998 0.998 0.997 0.998 0.998 0.998	0.999 0.2	0.9 0.9 01 0.9 0.9 0.9	98 97 97 98 97 97 99 99	<u>1998</u> 0. <u>10</u>	0.998 0.999 0.999 0.999 0.999	1 0.999	0.100	1.000 1.000 1 0.999 1 0.997 0.996	0001 0.000
0 305 0.356 0.406 0.864 1.321 1 727 2 235 2 692 3.15 3.2	7 8 9 10 11 12 13 14 15 16	12 14 16 <u>34</u> 52 68 88 106 124 126	0.999 0.997 1.001 1.001 1.000 0.999 0.999 0.999 1.001	1.030 1.033 1.035 1.024 1.026 1.018	3 310 3 197 3 397 2 400 2 703 2 004 1.698	1.001 0.999 1.001 1.001 1.001 0.999 0.999 0.998 1.000	1.031 1.041 1.028 1.015 1.015 1.014	3 203 3 996 2 800 1 399 1 602 1 502 0 500	1 000 1 001 0 999 0 997 0 998 0 997 0 999 1 000 0 999	1 012 1 008 1 009 1 005 1 005 1 005 1 009 1 002	1.099 0.901 1.204 0.701 0.802 1.001 0.300	1 000 1 000 1 000 0 998 1 001 1 000 1 000 0 998 0 998	1.005 1.006 1.009 1.007 1.010 1.010	0.500 0.600 1.102 0.599 0.700 1.000	1.002 1.001 0.999 1.000 1.001 0.999 1.001 1.001 1.001	1.012 1.009 1.010 1.009 1.009 1.009 1.000 1.000	1.099 1.001 1.000 0.799 0.300 0.100 -0.100	1.002 1.002 1.002 1.000 0.996 1.000 1.000 1.000 1.000	1.006 0. 1.005 0. 1.012 1. 1.020 2. 1.004 0. 1.005 0. 1.005 0.	1.0 399 0.9 299 1.0 200 1.0 410 1.0 400 1.0 500 0.9 0.9 400 0.9	03 09 1.019 01 1.019 02 1.029 01 1.019 01 1.019 01 1.019 01 1.019 01 1.019 01 1.019 01 1.019 01 1.019 02 1.039 08 1.019	9 2.002 9 1.798 5 2.295 9 1.798 8 1.698 2 3.511 9 2.104	1 000 0 999 0 997 0 999 0 996 0 998 1 000 0 997 0 998	1.010 1.010 1.026 1.010 1.022 1.023	1.101 1.304 2.703 1.406 2.405 2.300 2.004	1.001 0.998 0.997 1.001 1.001 1.000 0.997 0.999 1.001	1 020 2.2 1 020 2.3 1 029 2.7 1 020 1.8 1 034 3.4 1 024 2.7	1.0 04 1.0 07 0.9 97 0.9 98 0.9 98 0.9 08 0.9 08 0.9 08 0.9 08 0.9 08 0.9 08 0.9	02 01 1.0 97 97 1.0 98 1.0 98 1.0 98 1.0 98 1.0 98 1.0 97 96 1.0	218 1.69 228 3.10 232 3.40 238 4.00 235 3.70 239 4.31	0.998 0.998 1.000 9.0.997 7.1.000 8.0.997 7.0.996 7.0.998 7.0.998 7.0.998	1.032 1.017 1.022 1.030 1.030	3.511 1.700 2.508 3.414 3.607	0.999 0.997 1 0.996 1 0.999 1 0.999 1 1.007 1 1.005 1 1.005 1 1.005 1	029 3.21 031 3.51 028 2.90 025 2.60 031 2.38 040 3.48
3.251 3.302 3.353 3.404 3.454 3.505 3.556	17 18 19 20 21 22 23	128 130 132 134 136 138 140	1.000 1.001 1.001 1.002 1.002	1.017	1_497	1.000 1.000 0.999 0.999 0.998	1.019	2.002	0.999 0.998 1.000 1.001 1.000 0.999	1 000	-0.100 0.779	0.998 0.997 0.998 1.000 0.996 0.999	1.000	0.000	1.001 1.000 1.001 0.999 0.999	1.005	0 601	1.001 1.001 1.000 0.998 0.999	1.003 0	0.9 1.0 501 0.9 1.0 764 1.0	288 200 200 200 1 022 200 201 1 022	5 2 603	1.000 0.999 0.997 0.997 0.997	1.025	2.808	1.001 1.000 0.999 1.000 0.998	1.032 3.2	0.9 0.9 0.9 0.9 0.9 0.9 0.9 58 0.9	99 97 98 99 1.0 97 97 97 97 97	35 3.60	0.998 1.000 4 1.00 1.000 4 0.998	1.026	2.498	1.007 1.006 1.006 1.006 1.003	033 2.68
Std Dev Max Min			0 002 1 002 0 997	0 007 1 035 1 013	0.749 3.397 1.401	0.001 1.001 0.997	0.011 1.041 1.005	1.083 3.996 0.500	0.001 1.001 0.997	0.004	0 427 1 204 -0 100	0.002	0 004 1 010 0 998	0.404 1.102 0.000	0.001 1.002 0.998	0 005 1 012 1 000	0.484	0.002 1.003 0.996	0.006 0 1.020 2 1.003 0	722 0.0 410 1.0 299 0.9	4 0.00 4 1.03	5 0.598 2 3.511 8 1.698	0.001	0.007	0.660 2.808 1.101	0.002	0.010 0.9 1.034 3.4 0.999 0.2	37 0.0 00 1.0 01 0.9	01 0 0 02 1 0 96 0 9	014 1 40 039 4 31 098 0 10	9 0.001 7 1.001 0 0.996	0.012	1.257 3.607 0.100	0.004: 0 1.008: 1 0.996: 1	.014 1.29 .042 3.51 .000 0.00
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dist froi bottom meters 0 0 051 0 102 0 152 0 203 0 254 0 305 0 366 0 406 0 864 1 321 1 727 2 235 2 692 3 15 3 32 3 25	Station: 1 2 3 4 5 6 7 8 9 10 11 12 3 4 5 6 7 8 9 10 11 12 3 14 15 16 7 18	dist fro boltom inches 0 2 4 4 6 6 8 8 8 10 12 14 16 34 12 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	Pre W1 inchess 1.001 1.001 1.000 0.998 1.000 1.001 1.002 1.002 1.001 1.002 1.001 1.002 1.001 1.002 1.001	Post Wi inches 1.004 1.023 1.019 1.021 1.019 1.021 1.019 1.019 1.019 1.019 1.021 1.019 1.021 1.019 1.021 1.019 1.024 1.027	Dit 1 0.2 1900 1.2004 1.2004 1.2004 1.2004 1.2000 1.200	Pre, in W2 inches 1,000 1,000 1,000 0,999 1,000 0,999 1,000 0,998 1,001 0,999 1,001	Post, in W2 inches 0.999 1.001 0.998 1.001 1.016	Diff. % W2 % 0.000 0.100 -0.100 3.303 2.104 1.702	Pre. in W3 inches 0.999 1.000 1.000 1.000 1.000 0.999 0.999 0.999 0.999 0.999 0.999 1.001 1.000 1.000	Post, in W3 inches 0.999 1.002 1.014 1.014 1.017 1.020 1.018 1.019	Diff, % W3 % 0.100 0.200 1.705 2.108 0.801 2.108 1.902 1.798	Pre, in W4 inches 0.997 0.998 0.999 0.999 0.999 0.999 0.999 0.998 0.999 0.999 0.998 0.999 0.999 0.999 0.999 0.999 1.001 1.002 0.999 1.001 1.000 0.999	Post. in W4 inches 1.008 1.008 1.008 1.015 1.015 1.011 1.010 1.019 1.019 1.017	Diff. % W4 % 0.901 0.901 1.606 1.703 1.404 0.897 1.605 1.805 1.598	Pre. in W5 inches 1.000 1.000 1.001 1.001 1.001 1.001 1.005 0.999 0.997 1.005 0.999 1.005 0.999 1.005 0.999 1.002 1.002 1.002	Post, int W5 inches 1002 1002 1003 1014 1014 1013 1013 1013 1013	Diff. % W5 % -0.100 0.200 0.799 1.705 1.493 1.493 1.401 1.493 2.104 2.295	Pre_in W6 inches i 1.003 1.003 1.001 1.000 1.002 1.002 1.002 0.999 1.000 0.999 1.000 0.985 1.001 0.998 1.000 0.998 1.000 0.998 1.001 1.012 1.012 1.015	Dost in Diff VE We we We nches % 1.002 0 1.002 0 1.002 0 1.002 0 1.002 0 1.002 0 1.003 1 1.013 1 1.014 1 1.019 2 1.023 2	% Pre. W7 incht incht 1.0 100 1.0 100 1.0 700 1.0 100 1.0 703 0.9 300 0.9 303 0.9 505 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0	n. Post. i W7 s. inches 20 1.000 22.1.000 0.1.01 22.1.000 0.1.01 22.1.001 22.1.001 22.1.001 22.1.001 22.1.001 23.1.001 2	in Diff, % W7 W7 1% 3 0.200 0.200 0.1200 0.1200 0.1200 0.1200 0.1200 0.100 0.100 0.200 0.100 0.200 0.000 0.200 0.200 0.200 0.200 0.200 0.0000 0.000000 0.00000 0.0000 0.0000 0.0000	Pre, in W8 inches 0.993 0.993 0.997 1.001 0.994 0.997 0.996 1.000 1.001 0.999 0.997 1.004 0.999	Post, int W8 V inches 1 1.000 1.002 1.006 1.010 1.010 1.010 1.005 0.999 0.999 1.017	0.705 0.906 0.906 0.903 1.000 0.400 0.201 0.201 0.201	Pre. in W9 inches 0.996 1.000 0.998 1.000 1.000 1.000 0.998 1.000 0.998 1.000 0.998 1.000 0.999 0.999 0.999 0.999 0.999 1.000	Post. in Diff. W9 W9 inches % 1.004 0.3 1.020 2.0 1.020 2.0 1.021 2.2 1.021 2.3 1.015 1.5 0.999 0.0 1.000 0.1 1.000 0.5 -	Pre. W10 inchi inchi 00 9 00 10 10 10 100 100 100 100 100 100 100 100 100 100 100 100 00 100 100 100 100 100 100 100	in Posi W10 is inch 99 00 1 0 03 1 0 04 1 0 05 05 03 1 0 05 01 1 0 02 1 0 01 1 0 00 1 0 01 1 0 00 0 0 00 1 0 00 0 0 00 0 0 0 0 0 0 0 0 0 0	L in Diff. 9 W 10 es % 1 1 10 335 3 19 25 2 09 27 2 39 34 3 19 19 1 22 004 0.20 01 0.00 997 0.10 004 0.40 	6 Pre. in W11 inches 1.000 0.999 0.1.000 2.1.000 1.000 2.1.000 1.000 0.1.000 0.1.000 0.0.999 0.1.000 0.0.999	Post. in mches 1.004 1.019 1.019 1.036 1.028 1.028 1.028 1.029 1.030 1.030 1.016 1.029 1.030 1.016 1.029 1.030	Diff. % W11 % 0.300 1.102 1.798 3.187 2.697 2.797 2.897 1.600 0.300 0.800	Pre. in Po W12 W wrches inches 0.998 0 0.998 0 0.998 0 0.998 0 0.998 0 0.998 1 0.999 - 0.999 - 0.999 - 0.999 - 0.999 - 0.999 - 0.999 - 0.999 1 0.999 1 0.999 1 0.997 1 0.997 1 0.997 1 0.997 1 0.997 1 0.998 1 0.998 1 0.998 1 0.998 1 0.998 1 0.998 1 0.998 1 0.998 1	st. (10)11, 9 12 W12 (12) W12
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- Although we had over 41 thermocouples on the 24 receiver tubes and 4 headers, we were unable to determine where the blockages were. Even when all the thermocouples indicated that the temperatures were above the salt melting point, we still had plugs of salt. In the Solar Two and commercial receivers there will be even less instrumentation. If a panel becomes frozen, temporary thermocouples should be installed to monitor the panel temperatures more thoroughly. They could be mounted on the outside of the tubes. Another option is to monitor the temperatures with an IR camera.
- The heat trace should be designed to heat the headers and jumper tubes above 500°F within 10 hours when they are *full* of salt.

Component Tests

The main objectives of the component tests were to test unproven hardware and determine how well they perform in a molten salt environment, and to reduce uncertainties of the performance of untested components and operating procedures. Many of the flanges were tested in a molten salt environment, but additional information is required. Check valves were not tested previously in molten salt. The component tests were broken down into three areas: 1) check valve cycling, 2) slow thermal cycling of flanges, and 3) thermal shocking of flanges.

Check valves are needed at the pump outlet to prevent damage to the pump from the static "head" of salt when the pump stops, or to prevent pressure surges caused by redundant pumps on a common header when one pump stops. Serious damage to the pump can result if it is not protected from the strong inertial forces of the salt coming from the other pump and from the salt head in the riser.

It is desirable to use flanges that facilitate service of certain high maintenance components in molten salt loops. The flanges used in the molten salt pump and valve test loops were a constant source of salt leaks. The purpose of these tests was to test various other designs of flanges (e.g., tapered flanges or clamp type flanges) to measure how well they held a seal under thermal cycling, and to determine if it is practical to use flanges around the high maintenance components. We tested five flanges: a 2 inch Grayloc, two 4 inch R-CONs, a 6 inch E-CON, and a 4 inch ANSI ring type.

Check Valve Cycling. The purpose of the experiments with the check valve were to test their operation in a molten salt environment and to determine how to drain the salt from the check valve. A 3 inch spring loaded swing check valve was tested in a section of piping between flanges in the loop. Although we could not simulate the pressures expected to be encountered in cold side of a molten salt loop, we did simulate the flow velocities and the temperature cycles on the cold loop.

Figure 21 is a photograph of the check valve we tested (V-CON model manufactured by Reflange, Inc.). A drain hole was drilled in the flapper to allow a short section of piping downstream of the check valve to drain.



Figure 21. Photograph of the 3 inch check valve (V-CON model manufactured by Reflange, Inc.) tested in the salt loop.

In these tests we pressure cycled the check valve by flowing salt at the maximum flow rate - approximately 100 gallons/min (380 l/min) and establishing pressure in the accumulator to 30 psi, then shutting a bypass valve (FCV 720) and turning off the pump. Shutting the valve before turning off the pump caused a momentary spike in the pressure, but assured the check valve would receive positive pressure on the downstream side of the flapper. We monitored the pressure decay in the accumulator tank. After waiting approximately 30 minutes to allow the pump motor to cool, we repeated the cycling. Figure 22 shows the pressure and flow as a function of time for several cycles. There were no problems with its operation after over 300 cycles (approximately 1 year of operation). The flapper was inspected after the 300 cycles, and found to be in good condition with no signs of wear.

Slow Thermal Cycling of Flanges. Flanges in a molten salt environment have been known to leak significantly after being thermally cycled [12]. It is desirable to use flanges to facilitate service of high maintenance components, such as the pumps, in molten salt loops. The flanges used in the molten salt pump and valve experiments were a constant source of salt leaks. We tested various flanges to determine how well they hold a seal under the slow thermal cycling expected during nightly shut down of the plant followed by morning preheat with heat trace. We slow cycled four flanges: a Grayloc 2 inch with clamp type connectors, two 4 inch R-CON flanges with clamp type connectors manufactured by Reflange. The Reflange flanges have a unique metal gasket that is radially compressed (elastically) when the two faces are brought together, providing a tight seal.

Checkvalve Cycling



Figure 22. Pressure and flow as a function of time during a typical check valve cycle.

In these tests we simulated the nightly shut down and cooling of the components (assuming the heat trace were turned off) by using a fan and removing some of the insulation to enhance the cooling and match the temperature profiles we had expected to see in service at Solar Two. We cycled between 200 and 500°F. Each cycle took between six and eight hours. Figure 23 shows a typical slow thermal cycle. After approximately 180 slow thermal cycles, one of the 4 inch flanges started leaking very slightly. (We realized the torque on the bolts for the first 180 cycles was lower than the recommended value for the size of bolts we were using, and may have resulted in a less than optimum compression on the gasket.) We inspected all the flanges (we disassembled the two 4 inch flanges) and noticed they had all leaked to some extent, except the bolted 6 inch E-CON which showed no visible signs of salt. The bolted flange may provide a more uniform compression on the faces of the flange and gasket as compared to the clamp type flanges. See Figure 24. Since the salt is very wetting, it tends to get into cracks and seeps past gaskets, soaking and degrading the insulation. The continuous thermal cycling adds to its migration. Even though the flanges leaked a small amount (approximately 1 drop per hour), they would not likely fail catastrophically, since the gaskets are metal.

We retorqued the bolts to their recommended torque and continued the slow thermal cycling for an additional 120 cycles (a total of 300 cycles -- approximately one year of service) without any failures.



Figure 23. Typical slow thermal cycle of flanges simulating nightly cool down of components followed by slow heatup with heat trace.



a)



b)

Figure 24. Schematic of a) ECON and b) RCON flanges.

Thermal Shocking of Flanges. The most severe thermal cycling a flange could experience in a molten salt system would be a thermal shock where the flange is at one temperature and it is suddenly subjected to salt at a different temperature. This situation could occur in one of two ways: 1) when the salt temperature at the outlet of the receiver suddenly drops due to a cloud transient, or 2) at startup if the flanges were at a temperature below the salt temperature. In the first case, the salt temperature transient could be from 1050 to 550° F (566 to 288° C) in approximately five minutes. In the second case, the flange could be as cold as ambient with the salt at approximately 550° F (288° C). This situation could arise if the parasitic power consumption were being minimized at nightly shut down by turning off the heat trace followed by cold filling of the piping. In our test loop we only simulated the second thermal shock case, since it would be very difficult to simulate the transient salt temperature at the receiver outlet. We conducted these tests at two initial flange temperatures either: 300° F or ambient (~ 100° F) with the salt at 550° F.

Prior to the start of the thermal shock tests we installed a 4 inch ring-type flange to test alongside the other flanges. In these tests we allowed the flanges to cool for several hours or overnight by lowering set point temperature of the heat trace or by turning off the heat trace completely. After the flanges had cooled to the desired temperature, we shock them by pumping 550°F salt through them. Figure 25 shows a typical temperature profile of the flanges and check valve during a shock.



Thermal Shock of Components

Figure 25. Typical temperature transient of the flanges during a shock.

After 25 cycles at 300°F, we inspected the flanges. There did not appear to be any visible breaches of integrity. We continued the thermal shocks with the flanges at ambient temperature. The flanges experienced 146 shocks without failure, although the flanges continued to leak at a very slight rate. After all these thermal shocks, none of the flanges failed catastrophically. With continuous operation and exposure to pressurized salt, all except one of the flanges showed only minor leaking (wetting between the interfaces of the flange faces or actually dripping of salt at a rate of approximately one drop per hour). The exception is the Grayloc flange which leaked significantly, enough to form a stalagmite of salt on the floor. Leaks over a long period of time can soak the insulation and increase the thermal losses. Exposure of salt to heat trace can also cause an electrical short in the heat trace.

A finite element analysis was done on the 6 inch E-CON flange to determine the stresses that developed in this flange undergoing thermal shock with salt a 550°F and the flange either initially at 77°F (25° C) or at 300°F (149°C). The details of this analysis are included in the appendix. There were two areas of concern in the flange where the stresses reached a maximum: 1) at the interface of the two flange faces at the outer most radius, and 2) on the inner surface of the flange adjacent to the gasket. The stresses developed at the interface between the two flange faces during either initial condition (77 or 300°F) were highly localized and were in excess of the yield for the material, but a chamfer exists at this location. The actual stress should be much lower with the chamfer, so that region is not a concern. On the other hand, the stresses in second region are in excess of the yield when the flange is shocked from an initial temperature of 77°F (25°C) but not in excess when shocked at 300°F (149°C). Based on this analysis, we recommend that flanges are preheated at least to 300°F (149°C) prior to initiating salt flow.

These flanges are an improvement over the flanges used in the pump and valve test loops which were raised-faced flanges with a Flexitalic type gasket. Those flanges tended to leak severely under cyclic conditions.

Our observations and recommendations regarding these flanges are:

- The flanges held up remarkably well to the conditions to which we subjected them. There were no severe failures. The majority of the salt leaks were very slight.
- Flanges should be minimized in a salt system. They should be used only for removal of high maintenance equipment such as the pumps, if at all. All welded construction is preferred, especially on hot loops.
- If the piping is cold started, the flanges should be preheated to at least 300°F (149°C) prior to flowing salt through them.
- The flanges tend to seal better if they are not thermally cycled.
- Hot retorquing the bolts periodically may reduce the leaks.
- Heat trace zones should be designed so that flanges and valves are not part of the same heat trace circuit as the rest of the riser or down comer, so that cold starting the rest of the piping can be done.

Instrumentation Tests: Flowmeters and Pressure Transducer

Flowmeters. Flowmeters were a considerable source of problems in previous molten salt experiments [2]. For example, the Category B receiver used venturi type flowmeters with differential pressure transducers using silicone oil as an intermediate fluid to measure flow. The

pressure transducers had problems with silicone oil volatilizing at the cold salt temperature. In addition, venturi flowmeters only have a range of about 4:1. Because of the limited range and silicone oil problems, we investigated other designs of flow meters that could be more reliable, provide higher accuracy, and have a greater range.

We chose to test two types of flowmeters: vortex shedding and ultrasonic. These flowmeters were selected because they are common, commercially available products which can withstand the temperatures we expected to encounter in the cold side of a salt system. The vortex shedding flowmeter has wedge in the flow field and senses oscillations of the vortices which are shed from the wedge. The frequency of the oscillations is proportional to the flow rate. The ultrasonic flowmeter sends a sound wave through the moving fluid from one transducer to the other, with and against the flow. It measures the time difference between the traverses. We tested two types of ultrasonic flowmeters: a wetted type where the transducers actually send the sound wave directly into the fluid, and a clamp-on type where the transducers simply mount on the outside of the pipe and propagate the sound wave through the pipe wall. The vortex shedding flowmeter we tested was manufactured by Engineering Measurement Company, and the ultrasonics by Panametrics. Both have temperature limitations and are only rated for the cold side of a molten salt system. The ultrasonic flowmeters were calibrated with water at the factory prior to installation in the salt loop. The vortex shedding flowmeters had been calibrated under the Direct Absorption Receiver Program.

We have operated the flowmeters since the beginning of this test program. The first clamp-on transducers were not made for the cold salt temperatures and their bodies (made of a "high" temperature phenolic material) melted. The manufacturer replaced them with all metal transducers. We also experienced some problems with the cables to the wetted transducers. Once we worked through the bugs in the hardware and programming, the ultrasonic flow meters worked reasonably well. The clamp-on flowmeter uses a petroleum couplant between the transducer and the pipe wall which allows the sound wave to penetrate through the pipe and into the fluid. After approximately a week or two of intermittent service at the cold salt temperatures (above 500°F), the couplant dried out and caused inaccuracies in its readings. A new application of couplant restored the contact between the transducer and the pipe wall.

A comparison between the flowmeters is shown in Figure 26 during a varying flow condition. The vortex shedding responds much faster and stabilizes better to changes in flow rate. For control purposes, the vortex shedding would be the preferred flowmeter. The ultrasonic flowmeter took some time to tune and to get operating properly, partly due to the faulty cable. By changing the parameters (such as the number of samples it averages for a reading) in the software of the electronics for the ultrasonic flowmeters, we were able to change its response.



Figure 26. Response of vortex and ultrasonic flowmeters during a varying flow condition.

The flowmeters were compared with calibration tanks in the salt loop. Since the volumes of the calibration tanks are essentially constant with time, and the accuracy of the bubbler level measurement devices is good (\pm 3.8%), we chose to compare the flowmeters with the calibration tank flow.

The uncertainty of the flow measurement has two components: the bias (also called systematic) errors and the random errors [10]. The bias errors affect each measurement the same amount (at a given condition) and represent the offset from the "true" value. Random errors are the errors that change in a random fashion with repeated measurement. The random errors are not correlated with each other, and their limit can be measured if several data points are taken. Since the true bias and random errors are not known, their estimates are approximated by limits of each. The bias limit equals the square root of the sum of squares of each elemental bias limit (b_i):

$$\mathbf{B} = [\Sigma \mathbf{b}_i^2]^{1/2} \tag{19}$$

The random limit equals:

$$S = \left(\frac{t_{95}S_x}{\sqrt{N}}\right) \tag{20}$$

where t_{95} is the Student's t statistic at 95% confidence, S_x is the standard deviation of the data set, and N is the number of data points [10]. For the root-sum-square uncertainty model, the uncertainty is found by combining the bias and random limits as follows:

$$U_{RSS} = \pm \left[B^2 + S^2 \right]^{1/2}$$
(21)

This model provides an interval around the test average that will contain the true value $\approx 95\%$ of the time. In the flow tests, the flowmeter readings were compared with a reference—the calibration tanks. The bias errors relative to the reference can be measured. However, the reference (the calibration tanks) also has bias errors which we could not measure.

Table 9 lists each bias error source and estimated magnitude for the calibration tank flow measurement. The calibration tanks use bubblers to sense level. The amount of time to fill between two levels in each tank is measured and the flow rate calculated. Since the volumes of calibration tanks were not measured when the Panel Research Experiment was fabricated, exact volumes are not known. However, the dimensions were determined from drawings of the tanks. The volume was calculated, accounting for an overflow standpipe. Even if the tanks have significant amounts of eccentricity (5% change in the diameter) causing the tank to become elliptical, the volume of each is not significantly affected (it changes by less than 0.5%). Other bias sources of errors are thermal expansion of the tank volume between ambient and 550°F, salt density variations due to temperature, and the bubbler calibration.

 Table 9. Bias Limit Sources for Calibration Tank Flow Measurement.

Error Source	Magnitude
1. Tank Eccentricity (tank cross section is elliptical:	0.5%
minor axis is 95% tank radius, major axis 105% radius).	
2. Tank Thermal Expansion (change in tank volume from ambient to 550°F).	1.5%
3. Salt Property Variations (change in density and thus level between 550 and 650°F).	1.8%
4. Bubbler Calibration (approximately 0.5 inch in 18 inches).	<u>3.0%</u>
Total Bias Limit Calibration Tank Flow (Root Sum Square)	3.8%

The flowmeters were compared with the calibration tanks at several flow rates. Starting at 100% flow, we allowed the flow to stabilize, then closed the drain valves to the calibration tanks. The bubblers measured the level in each tank as a function of time. The elapsed time for the salt to fill the tank between the lower and upper level settings is measured in each tank to calculate the flowrate. The total flowrate is the sum of the two calibration tank flows.

Figure 27 shows the results of the comparison of the flowmeters against the calibration tank flowrate. Each data point represents the average of several readings during the calibration run. Figure 28 shows the measured bias errors (relative to the calibration tank flowrate) for each flowmeter as a function of flow. The bias errors represent the systematic errors in the measurements. Note how the bias errors are a function of the flow rate. The implication of this dependency is that calibration constant for each flow meter is off by a fixed percentage. The random errors are shown in Figure 29. The random errors were calculated from the data using Equation 20. The random errors are quite small, indicating the flowmeters give consistent readings over the range of the flows tested. The root-sum-square uncertainties, U_{RSS} , for each flow meter as a function of flow rate are shown in Table 10. The U_{RSS} accounts for the bias errors of the reference source—the calibration tanks.

Flowmeter Calibration



Figure 27. Comparison of the vortex and ultrasonic flowmeters against the calibration tank flowrate.

Bias Errors for Flowmeters



Figure 28. Measured bias errors (relative to the calibration tank flowrate) for each flowmeter as a function of flow.

Random Errors for Flowmeters



Figure 29. Measured random errors for each flowmeter as a function of flow.

Flowrate, L/min	Vortex, FT-720	Wetted Ultrasonic, PF-001	Clamp-on Ultrasonic, PF-002	Vortex, FT-730	Vortex, FT-800
102.6	± 9.8%	± 3.9%	± 8.5%	± 9.9%	± 5.3%
155.4	11.6	4.2	12.8	11.6	7.3
197.4	12.6	4.6	13.0	12.5	8.5
244.6	15.1	6.4	13.3	15.6	

Table 10. Root-sum-square Uncertainty (U_{RSS}) for Each Flowmeter.

The large uncertainties observed are primarily due to the large bias errors. By periodically calibrating the flowmeters against a calibrated reference (such as calibration tanks or the cold surge tank of receiver with a *calibrated* bubbler - this is important), the majority of bias error limits can be calibrated out resulting in a root-sum-square uncertainty with a magnitude of the uncertainty equal to the calibrated reference. Overall uncertainties (U_{RSS}) of less than ±5% can be obtained with these flowmeters. The random error limits were much smaller and did not contribute significantly to the overall uncertainty under steady conditions.

Other observations and recommendations regarding flowmeters:

• The vortex shedding flowmeter worked exceedingly well (very reliable) in the molten salt environment and should be used whenever possible. The ultrasonic flowmeters were less reliable.

- It is essential that provisions to calibrate the flowmeters in situ are designed into a molten salt system (e.g., <u>calibrated</u> level indicators in the cold tanks).
- For calibration purposes, the tank volume should be measured before installation and the bubbler must be calibrated.
- The clamp-on ultrasonic flowmeters are useful for temporarily (< 1 week) measuring flow in areas where there is no flow measurement or to verify flow measurement of an existing flowmeter and where the effort or expense and down time does not justify installation of a welded in flowmeter. During the check out phase of the receiver and salt system or during performance monitoring may be the time when clamp-on ultrasonic flowmeters could be useful on a very temporary basis or as a temporary backup if one of the permanent flowmeters were to fail and the plant was ready to run.
- The flow rate only needs to be measured on the cold side. There should be no need to measure flow on the hot side.

Pressure Transducer. We have tested an impedance-type pressure transducer and a NaK-filled pressure transducer in the salt loop to determine how well they work in molten salt. The silicone oil used in pressure transducers in previous molten salt tests tended to volatilize. The NaK-filled pressure transducers made by Taylor worked well in the pump and valve loop once snubbers were used to eliminate pressure pulsations which fatigued the membrane. Unfortunately, NaK-filled pressure transducers are difficult to find anymore. The impedance-type pressure transducer we tested in our loop is made by Kaman, and is good for temperatures up to 1200°F. It senses small displacements in its membrane and correlates them to pressure transducers in our system, the impedance-type pressure transducer was calibrated at the factory at 550, 750, and 1050°F. The impedance-type pressure transducer in our loop experienced the same thermal cycling and shock as the flanges, and did not fail or give erroneous readings. The pressure measurement in Figure 22 was from the impedance-type pressure transducer.

Comments regarding pressure transducers:

- The impedance-type pressure transducers work well but are expensive (~\$5k each).
- NaK-filled pressure transducers are hard to find.
- To keep instrumentation costs down, minimize the number of salt pressure measurements needed.
- The pressure transducers should be oriented so the salt can drain from them. Experience from previous molten salt experiments has shown, that if salt is allowed to freeze on the membrane, then thawed, the thawing process causes the membrane to rupture.

IV. Ongoing and Further Research

The work conducted so far has answered many of the questions regarding how far salt can flow through cold pipes during a cold fill scenario and the thermal stresses that develop when components and piping are thermally shocked, and some of the effects of freezing and thawing. We have also tested instrumentation that are an improvement over previous instruments. Ongoing and further research is directed towards understanding the freeze/thaw phenomenon, validating transient freezing models, and testing improved components and instrumentation. A description of each of these follows.

Simple Element Freeze/Thaw Tests (Ongoing)

A two-chamber oven was built to investigate the salt freeze/thaw phenomenon in typical receiver tubes. The purpose of the simple-element freeze/thaw experiments is to quantitatively measure in a controlled setup the permanent deformation inflicted to samples of receiver tubes undergoing freezing and thawing. When nitrate salt changes from the solid to the liquid phase the volume increases, causing an expansion of a given mass of salt. During the expansion process, the tube material can yield resulting in a plastic deformation of the tube material. In these tests, several receiver tubes of various diameters and wall thicknesses filled with nitrate salt undergo several freeze/thaw cycles to measure the deformation of tubes. Preliminary results indicate under the most severe case (freezing the lower half of a tube, then freezing the upper half, followed by thawing the lower part with a stop in the upper half to prevent sliding of the solid salt) the tubes will rupture after 12 cycles.

Ball Valves Test

Ball valves are desirable for use as drain and fill valves because they are relatively compact and in the fully opened position the flow restriction is small relative to other types of valves, such as globe valves. We have pressure cycled a 2 inch Mogas ball valve to assess its functionality and leak rate in a molten salt environment. The valve was closed and pressurized to 60 psi (410 kPa) for five minutes followed by flow for five minutes. After each 50 cycles, the leak rate was measured with the valve in the closed position and pressure on the valve. The amount of salt that leaks by was measured every 0.5 hour. After 300 cycles the leak rate was measured to be approximately 15 grams of salt per half hour.

Transient Freezing Experiments

The correlation for transient freezing in pipes used to calculate penetration depths is based on experiments where the pipe wall is cooled externally to maintain a constant wall temperature. In reality, pipes have a finite heat capacitance. The effects of the pipe heat capacitance on the penetration depths for molten salt penetration depths is an area that could be investigated further.

Impedance Heating System

For long runs of piping, impedance heating could have advantages over mineral insulated (MI) cable. With impedance heating, the pipe wall becomes the heater by passing a low A-C voltage (<80 volts) through it. One lead of the electrical cables is connected to the electrical midpoint of the pipe, and the other is divided in two, with each of these connected to an end of the pipe that is to be heated. The cables run on the outside of the pipe and are easy to access. We plan to test an impedance heating system in our salt loop.

Multiport Valve

A multiport valve allows flow from one line to be distributed to several lines. It has a single actuator to control the valve. A multiport valve could be used in place of several drain and fill valves, thus reducing the complexity associated with controlling and maintaining several valves. Although this valve is not a commercial product, a small company in Colorado (TedCo) has designed such a valve for molten salt applications. This type of valve should be investigated further.

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Appendix A. Finite Element Analysis of Flange Undergoing Thermal Shock

The following is memo written by Scott Rawlinson describing a finite element analysis of an ECON type 6 inch flange undergoing thermal shock at two different initial conditions: 25 and 149° C.

Sandia National Laboratories

Albuquerque, New Mexico 87185-1127

date: July 27, 1994

to: Jim Pacheco, MS-0703 Org. 6216

from: Scott Rawlinson, MS-1127 Org. 6215 5-3137

subject: Finite Element Results for Salt Flange

To ensure the reliability of some aspects of Solar Two, you are concerned about stresses in several critical components, one of which is the flange coupling. As an alternate method of thermal conditioning at night, some of the salt line may be drained and allowed to cool. At startup these lines will be at ambient temperature or they will be preheated to a temperature below the salt freezing point and will undergo a significant thermal shock. The purpose of this memo is to document the finite element analysis (FEA) results on the flanges undergoing thermal shock that will be used in these molten salt loops.

I used the COSMOS/M finite element program to model the pipe flange. This program can be used on a PC and according to a survey done by our analysis group about three years ago, is one of the better FEA programs. The program has been continuously updated and improved since that time. I used the latest version, 1.70. The developers of this code, Structural Research and Analysis Corporation (SRAC), verify its results using numerous test case models.

The system being modeled is two E-CON flanges that are bolted together at 45 degree intervals. A step is machined into each of the mating flanges. A gasket is placed in this notch that is formed from these steps. The model was developed to determine: (1) stresses at steady-state conditions; (2) stresses that would occur if 290 °C salt suddenly flowed through this pipe connection without any heat trace (at ambient temperature); and (3) stresses that would occur if 290 °C salt suddenly flowed through this pipe connection after the flanges are preheated to 149 °C (300 °F). Therefore a transient solution is required for (2) and (3).

The envelope of the FEA model was developed from the sketch you supplied, using data from Reflange. Several iterations of the model were developed. The first model was developed in an older version, 1.65A. Then the newer version arrived, and although it did not contain any changes that should affect this particular model, I developed the model in the newer version. In addition, after knowing what loading would occur, I decided that gap elements should be placed between the flange and the gasket. Otherwise, the gasket would appear to be part of the flange, adding to its strength -- this would not be realistic. Only the results using the gap elements, separating the gasket from the flanges, will be presented.

A summary of the parameters in the FEA model is given below:

- Element type (for flanges and gasket): 4-node planar, "PLANE2D", axisymmetric
- Average element size: 2-mm
- Element type (gap between flange and gasket): 2-node "GAP"
- Force/pressure boundary conditions: 28,300 N at bolt hole location
- Flux/Temperature boundary conditions:
 - Convection along entire length of inner pipe
 - Convection coeff = $550 \text{ W/m}^2\text{-K}$
 - Bulk fluid temp: 290 °C
- Displacement boundary conditions: Zero displacement in y direction at midpoint of gasket
- Flange material properties (SS316) [1,2]:
 - Modutus of elasticity: 193 GPa
 - Poisson's ratio: 0.3
 - Coefficient of thermal expansion: 17.5×10^{-6} m/m-K
 - Density: 8000 kg/m³
 - Specific Heat at Constant Pressure: 505 J/kg-K
 - Thermal conductivity: 15.6 W/m-K
- Gasket material properties (17-4PH) [3]:
 - Modulus of elasticity: 193 GPa
 - Poisson's ratio: 0.3
 - Coefficient of thermal expansion: 12.1×10^{-6} m/m-K
 - Density: 7832 kg/m³
 - Specific Heat at Constant Pressure: 505 J/kg-K
 - Thermal conductivity: 12.1 W/m-K

Note: Material properties were taken as constant and were calculated at the average between an ambient temperature of 25 °C and the operating temperature of 290 °C.

The boundary conditions stated above require some explanation. Since the pipe flange is modeled axisymmetically, the proper bolt load must be calculated. COSMOS/M assumes axisymmetric problems are based on one radian. Therefore the proper bolt load is:

$$F = F_b \frac{\# bolts}{2\pi}$$

The force in the bolt was given as 4000-5000 lb. from Bob Lathan at Reflange, Inc.. I used 5000 lb. = 22,242N, or an equivalent load of about 28,300N, using the above equation.

When I first developed the thermal model, I placed 290 °C boundary conditions (salt temperature) along the inside of the pipe. The resultant stresses were extremely high in this region. However, I realized that was not the proper boundary condition. The inside of the pipe will not instantaneously reach 290 °C -- it will reach that temperature much more slowly through the boundary layer. Therefore I re-analyzed the problem using convective boundary conditions.

1.

The correlation I used to determine the convection coefficient is based on turbulent flow in circular tubes and is given as [4]:

$$\overline{h} = .023 \frac{k}{D} \operatorname{Re}_{D}^{4/5} \operatorname{Pr}^{0.3}$$
for
$$0.7 \le \operatorname{Pr} \le 160$$
ReD \ge 10,000
L/D \ge 60
where
$$k = \text{thermal conductivity}$$
D = pipe diameter
L = pipe length
RcD = Reynolds number
Pr = Prandtl number

Using your stated flowrate of 100 gpm and using the properties of salt at 290 °C from [5], I calculated a convection coefficient of 552 W/m²-K \cong 550 W/m²-K (the above assumptions were met). This number is very close to your calculated valve based on experimental results from the smaller pipe flange at time \ge 90 seconds.

Since the problem is transient in nature, a timestep is needed. The critical timestep is calculated as (information supplied by SRAC):

$$\Delta t_{cr} \leq \frac{2}{1 - 2\theta} \frac{\Delta x^2 \rho c_p}{k}$$

where $\Delta x = \text{smallest mesh size}$ $\rho = \text{density}$ $c_p = \text{specific heat at constant pressure}$ $\theta = \text{stability parameter}$

Using the values of material properties and stability factor to give the smallest possible stable timestep, I calculated a critical timestep of 0.86 seconds. I used a 0.5 second timestep in the analysis.

My assumptions in the analysis were as follows:

- (1) Constant material properties (linear problem)
- (2) Constant convection coefficient
- (3) No external thermal losses (insulated)
- (4) Bolt load does not change with time or temperature

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- (5) No friction at gasket/flange interface (it will become apparent later that this value is irrelevant)
- (6) Flowrate = 100 gpm

Steady-State Results (Ambient Temperature):

The results of the steady-state analysis for 25 °C are shown in Figures 1a through 1d. All stresses discussed below are Von-Mises stresses, a common stress criterion used to predict failure. Figure 1a illustrates the model's element mesh, force, and displacement boundary conditions. Two areas, regions A and B are also illustrated -- these will be referred to later. Figures 1b and 1c are exaggerated displacement plots. The pipe flanges tend to be clamped together due to the bolt loads. This plot appears to show that the gasket is separating from the lower pipe flange. However, remember that this is an exaggerated plot on a scale on the order of several hundred. I was concerned that the apparent non-symmetry indicated a problem, so I consulted personnel at SRAC -- they said that sometimes this happens in a deformed plot when the displacements are very small, resulting in a very distorted plot with the huge scale factor. This is what happened in this case. In fact, he checked the entire model and found no problems. Figure 1d is a Von-Mises stress plot of the center of the bolted connection. The maximum stress is 175 MPa, and occurs where the two flange bodies contact due to the bolt forces (region A). This stress is well below the yield point of SS316 at ambient temperature.

Transient Results for No Preheat:

Next, the convective boundary condition was applied along the inside of the pipe wall. Since the temperature distribution changes with time, the resultant stresses will also change. I examined the results at t = 0.5, 1, 5, 10, 20, 30, 60, 120, 180, and 240 seconds. To observe how the stress patterns develop with time, I included the results at t = 0.5, 5, 10, 30, 60, 120, and 240 seconds in Figures 2 through 8.

The maximum stress occurs at the same location as the steady-state results, but is higher due to the additive effect of the temperature or convective boundary conditions. Because the pipe is being heated from the inside of the pipe, this inner region expands faster than the outer region, which tends to compress the contact line even greater than with only bolt loads.

The following table summarizes the stresses in the two areas of concern:

Time (seconds)	Von-Mises Stress, Region A (MPa)	Corresponding Temperature, Region A (°C)	Yield Strength, Region A (MPa)	Von-Mises Stress, Region B (MPa)	Corresponding Temperature, Region B (°C)	Yield Strength, Region B (MPa)
0.0	175	25	240	35	25	240
0.5	180	25	240	90	37	240
1.0	171	25	240	90	44	240
5.0	178	25	240	142	69	240
10.0	214	25	240	172	81	240
20.0	279	25	240	196	98	240
30.0	341	25	240	239	107	240
60.0	527	25	240	265	128	240
120.0	537	50	240	323	161	240
180.0	542	58	240	325	178	240
240.0	547	67	240	328	187	240

Table I - FEA Results for Case Without F	Preheat
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These results at the contact point (region A) indicate that the yield strength is easily exceeded. However, I asked if this was actually chamfered at this point. It turns out that it is, which would eliminate this high stress point. More of a concern is the stresses along the inner pipe adjacent to the gasket. For times > 30 seconds, stresses exceed the yield point in this region (the yield point is constant from 25-200 °C). Based on this, it is apparent that local yielding may occur if you thermally shock this bolted connection.

Notice that maximum stresses are nearly level at 240 seconds. As the temperature distribution evens out, the stresses will decrease and eventually return to the stresses with bolt loading only (since the expansion will be equal throughout the flange assembly). Therefore, the stresses at t= 240 seconds are about as high as can be expected.

Finally, I looked at any gap that may occur between the flange and gasket surfaces. There is a slight gap at t=240 seconds but is nearly undetectable -- less than $\cong 0.1$ -mm. Because of the effect of the bolt force and thermal loading, the gasket is never compressed. Any stresses in the gasket are only due to the thermal gradient. Because the gasket is never constrained, the coefficient of friction used is not relevant.

Transient Results with Preheat:

I re-ran the model assuming the entire flange was preheated to a uniform temperature of 149 °C (300 °F). I examined the results at t = 0.5, 30, 60, 120, 180, and 240 seconds. The results are displayed in Figures 9 through 14. The following table summarizes the Von-Mises stresses in regions A and B.

Time (seconds)	Von-Mises Stress, Region A (MPa)	Corresponding Temperature, Region A (°C)	Yield Strength, Region A (MPa)	Von-Mises Stress, Region B (MPa)	Corresponding Temperature, Region B (°C)	Yield Strength, Region B (MPa)
0.5	177	150	240	18	150	240
30.0	266	150	240	133	.193	240
60.0	361	150	240	145	204	240
120.0	454	162	240	182	221	≅ 240
180.0	495	170	240	198	230	≅ 240
240.0	504	180	240	202	235	≅ 2 40

Table I - FEA	Results for	or Case	Without	Preheat to	149 °C
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As with the case with no preheat, the highest stresses occurred at the point of contact between the two flange bodies. Again, this point was ignored because there is actually a chamfer at this location. The other area of concern, region B, has much more acceptable stresses. A maximum Von-Mises stress of 202 MPa occurs at t=240 seconds. The corresponding temperature at that point and time is approximately 235 °C. The yield strength of SS316 at this temperature point is nearly 240 MPa, therefore the stress level is acceptable. Note that as with the case with no preheat, the stresses have very nearly peaked and would begin to decrease with time to the levels of that in the steady-state condition.

Conclusions:

Based on these results of this model, it appears that local yielding may occur (without preheat) along the inner pipe adjacent to the gasket. It is possible that a full 3-D model may indicate otherwise, but it is not likely since the region in question is far from the bolts. Therefore, it is not recommended that this flange connection be thermally shocked from ambient conditions. However if heat trace is used to preheat the flanges to 149 °C (300 °F), the stresses would remain below the yield point of the material..

References:

- 1. American Society for Metals, Engineering Properties of Steel, pp. 292-296, ASM, 1982.
- 2. Incropera, F. P., and DeWitt, D.P., <u>Fundamentals of Heat Transfer</u>, p765, Wiley, New York, 1981.
- 3. Kattus, J.R., <u>Aerospace Structural Metals Handbook</u>, code 1501, March, 1978.
- 4. Incropera, F. P., and DeWitt, D.P., <u>Fundamentals of Heat Transfer</u>, p406-407, Wiley, New York, 1981.
- 5. Smith, David C., Chavez, James M., <u>Final Report on Phase I Testing of a Molten Salt Cavity</u> <u>Receiver, Vol II - The Main Report</u>, Table 2-II, p 2-4, SAND 87-2290, May 1992.

Attachments with all copies: Figures 1 through 14

Copy to: Chuck Lopez, SCE Bill Gould, Bechtel Alex Zavoico, Bechtel Dick Holl, Jenna Baskets Bob Lathan, Reflange Mark Marko, Rockwell Tom Tracey, Ted Co.

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 File K.3, 6215




















































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Appendix B. Fabrication of Heat Trace Circuits

The heat trace for large systems is usually designed by the supplier. Each zone is sized based on the heating load and the piping diagrams. The length and power rating of a heat trace cable are sized based on the power required to maintain a pipe at given temperature and the power supply voltage. For a given voltage and heat trace cable length, the MI cable resistance density can be selected to provided the desired power. As a rule of thumb, we try to limit the power wattage density to less than 50 W/ft of MI cable length. Figures B-1 through B-4 are photographs of heat trace installed on a section of piping, a valve body, the header of a receiver panel, and above the jumper tubes in a receiver panel.

To maintain the integrity of the electrical circuit, only, tube benders should be used to bend the heat trace cable. See Figure B-5. After the heat trace is installed, it is covered with metal foil to prevent insulation from getting between the heater and the pipe causing the heater to overheat. The metal foil also helps to direct the radiant heat from the heat trace to the pipe or component. The metal foil can either be wrapped around the pipe and heat trace or tack welded over the heat trace to the pipe.

A critical area in heat trace circuit fabrication is the hot to cold junction. This junction makes a transition from the power lead (copper cable) to the heater (NiCr cable). Most of the failures of heat trace circuits can be attributed to a failure at the hot to cold junction. Below is an outline of the fabrication of hot-to-cold junctions.

- 1. First, a splice is drilled out to fit over the MI cable. See Figure B-6.
- 2. Cut the MI cable by scoring it three times, but not cutting it all the way through because it may cause a short of the conductor wire. Snap off the cut piece.
- 3. Remove 3/8 inch of the sheath to expose the inner wire of the MI cable. Peel the sheath to expose the Magnesium Oxide (MgO) and conductor wire (Figure B-7.)
- 4. File the inner conductor wire flat. Everything must be kept clean to make sure the silver solder adheres. Clean with emery cloth (Figure B-8).
- 5. Test (Meger Test) the insulation quality of each MgO MI cable by measuring the resistance between the conductor and the sheath. The resistance should be at least 5 M Ω preferably 20 M Ω .
- 6. Clean everything that has to be brazed: the conductors and sheath.
- 7. Check the splice and stress fitting for fit.
- 8. Slip the stress fitting and splice over the MI cable.
- 9. Put flux on the conductor of the cold lead (copper wire) to help the brazing process.
- 10. Put solder on with a torch.
- 11. Check the resistance again to make sure there are no shorts.
- 12. Line up the hot (NiCr) and cold (Cu) leads (Figure B-9).
- 13. Melt the solder from the cold (Cu) side and let it flow towards the hot (NiCr) side.
- 14. Remove flux residue with pliers. Check integrity of joint. Buff with emery cloth.
- 15. Check resistance again for shorts.
- 16. Clean any outgassing of flux residue on the surface of the MgO by taking out the top surface of the MgO. The MgO is very hydroscopic.
- 17. Slide the splice over the junction until the junction can be seen through the breather hole.



Figure B-1. Heat trace installed on 2 inch pipe before metal foil was installed. It is snaked to allow for thermal expansion.



Figure B-2. Heat trace installed on valve body prior to being covered with metal foil.



Figure B-3. Heat trace on receiver panel header with metal foil covering the cable.



Figure B-4. Heat trace on jumper tubes in receiver panel.



Figure B-5. Tube bender used for bending MI cable.



Figure B-6. Splice is drilled to fit over MI cable.



Figure B-7. Sheath is peeled away to expose magnesium oxide (MO) and the conductor wire.



Figure B-8. The conductor wire must be cleaned so the silver solder will adhere.



Figure B-9. The heater wire - NiCr, (on the left) and cold lead - Cu (on the right) are lined up.

- 18. Braze the heater side of the splice to the sheath first. Don't have both sides of the MI cable clamped tight otherwise stress will build in the joint. Allow the junction to grow. Braze the hot side by first heating the splice because it has more thermal mass than the sheath, then heating the surrounding cable to bring all parts to temperature at once. Flow solder around the splice. Repeat for cold side (Figure B-10).
- 19. Check resistance again.
- 20. Use a screw to cap off the breather hole in the slice by first putting a kink in the threads two or three threads up to prevent the screw from going in too far and screwing it in the breather hole. Clip of the screw flush with the surface of the splice. File it down. Use a round tail file to make groves in splice for solder to adhere.
- 22. Flux area. Seal vent hole with solder.
- 22. Use a wet rag (Figure B-11) to determine if junction is sealed by measuring resistance. If water penetrated the seal, the resistance would decrease.

Don'ts with Heat Trace:

- 1. Don't weld near heat trace. Weld splatter could burn a hole in the sheath.
- 2. Don't hammer heat trace to fit it in tight spots (Figure B-12).
- 3. Don't use pliers or files to bend the MI cable (Figures B-13 and B-14). Use a tube bender (Figure B-5).



Figure B-10. The spice is brazed to the cable sheath.



Figure B-11. Use a wet rag to determine if the junction is sealed.



Figure B-12. Do not hammer heat trace.



Figure B-13. Do not use pliers to bend heat trace.



Figure B-14. Do not use a file on the heat trace sheath.

Appendix C. Heat Transfer Coefficient for Circumferentially Varying Heat Flux

The impetus behind establishing a method to estimate accurately heat transfer coefficients is so that the flux limitations on receiver tubes can be set using thermal fatigue data based on the maximum temperature the tube material will experience during normal operation. Since the receiver tubes in a central receiver are heated on one side and insulated on the other, asymmetric heating will affect the heat transfer and thus the tube-temperature distribution. In the Handbook of Heat Transfer Fundamentals there is a description of the effects of circumferentially varying heat flux distribution on the Nusselt number (the nondimensional heat transfer coefficient, Nu=hD/k) for a specific flux distribution, but not a general case. In the journal article referenced by the handbook¹, the methodology to estimate the Nusselt number for an arbitrarily varying flux distribution is described. Basically, the authors describe an analytical derivation where they solve the energy equation by breaking the arbitrary flux distribution into the average flux around the tube plus the variation from the average. The authors claim the theoretical results are within 10% of experimental data for $0.7 \le Pr \le 75$. The model accounts for variations in the radial and circumferential thermal eddy diffusivities for turbulent flow ($\epsilon_{H\rho}$ and $\epsilon_{H\theta}$) which are based on experimental data. The local Nusselt number, $Nu(\theta)$, can be calculated if the flux variation can be expressed in terms of a Fourier series.

In the case of a receiver tube, the flux distribution varies approximately with cosine of the angle from the tube crown assuming the flux is specular (parallel rays). See Figure C-1a). Normalizing the flux distribution by the average flux, $q''_0 = q''_{net}/\pi$, the distribution can be represented as $q''(\theta)/q''_0 = 1 + F(\theta)$ where:

 $F(\theta) = \begin{cases} \pi \cos(\theta) & 0^{\circ} \le \theta \le 90^{\circ} \\ 0 & 90^{\circ} \le \theta \le 270^{\circ} \\ \pi \cos(\theta) & 270^{\circ} \le \theta \le 360^{\circ}. \end{cases}$

 $F(\theta)$ is represented by the Fourier series:

 $F(\theta) = \sum_{n=1}^{\infty} F_n(\theta) = \sum_{n=1}^{\infty} a_n \cos(n\theta)$

where

$$a_{1} = \pi/2$$

$$a_{n} = \frac{\sin((1-n)\pi/2)}{1-n} + \frac{\sin((1+n)\pi/2)}{1+n}$$

Figure C-1b) shows the comparison of the flux distribution to Fourier series representation (n=0 to 6). Once the Fourier series representation is known, the fully developed, local Nusselt number is calculated from:

$$Nu_{\omega}(\theta) = \frac{2(q^{"}(\theta) / q^{"}_{o})}{G_{o} + \sum_{n=1}^{\infty} G_{n}F_{n}(\theta)} = h(\theta)D/k$$

¹"Turbulent Heat Transfer in a Circular Tube with Circumferentially varying Thermal Boundary Conditions," J. Heat. Mass. Transfer, Vol. 17, pp 1003-1018, (1974).



Figure C-1. a) Flux distribution around an asymmetrically heated tube with insulation on the unilluminated side, and b) comparison of flux distribution to Fourier series representation (six terms).

where G_o and G_n are found from solutions to the energy equation and are functions of the Prandtl, Pr, and Reynolds, Re, numbers. They are tabulated in the referenced article.

Figure C-2 shows a comparison of the Nusselt number computed by the above method to that computed by the Dittus Boelter equation - a commonly used correlation for uniformly heat tubes $(Nu=0.023Re^{0.8}Pr^{0.4})$. As can be seen, the analytical estimate of the heat transfer coefficient is greater in value. The authors also state for Pr=8, the dependence of the Nusselt number upon Reynolds number exceeds the power of 0.8 and thus the Dittus-Boelter equation tends to gives more conservative results the higher the Reynolds number. This has been cited by other researchers. According to the referenced article, the deviations between the derivation and experimental data do not exceed 10% and are generally much less. Note, the Pr and Re number for nitrate salts vary from approximately 3.2 and 100,000, respectively, at 1050°F to 10.2 and 30,000, respectively, at 550°F.

This method will give an accurate estimate of localized heat transfer coefficients for a nonuniformly heated tube.





Figure C-2. Comparison of analytical calculation of Nusselt number which accounts for variations in flux to that determined by the Dittus-Boelter equation for Pr=10 and Re=30,000. Nu(θ) drops to zero between 90° to 180°.

Appendix D. Strain Equations for a Receiver Tube Under High Flux

Assuming a flux profile on the tube that follows a cosine function (Eq. D-1), a relation can be found between the tube strain and flux, tube material properties, and heat transfer coefficient. The plane strain in the tube is the sum of the strain in the tube wall due to the temperature difference across the wall and the strain due to the tube front-to-back temperature difference (Eq. D-2). The flux profile, strain equation, ε , and the tube inside and outside crown temperatures are defined below (assuming thin walled tubes):

$$q''(\theta) = q''_{net}\cos(\theta)$$
(D-1)

$$\varepsilon = \alpha \left[\left(\frac{T_{o,c} - T_{i,c}}{2(1-\upsilon)} \right) + \left(\frac{T_{o,c} + T_{i,c}}{2} - T_{avg} \right) \right]$$
(D-2)

$$T_{o,c} = \frac{q''_{nct} t_{wall}}{k} + T_{i,c}$$
(D-3)

$$T_{i,c} = T_s + \frac{q_{net}^{"}}{h_c}$$
 (D-4)

The average tube temperature can be approximated by:

$$T_{avg} = \frac{q_{net}^{n}}{\pi h_c} + \frac{q_{net}^{n} t_{wall}}{2\pi k} + T_s$$
(D-5)

Substituting these into the strain equation yields:

$$\varepsilon = \frac{\alpha q''_{net}}{\pi} \left[\frac{t_{wall}}{2k} \left(\frac{\pi (2 - \upsilon) - (1 - \upsilon)}{(1 - \upsilon)} \right) + \frac{(\pi + 1)}{h_c} \right]$$
(D-6)

Eq. D-6 shows how the flux, tube thickness, material properties and heat transfer coefficient at the crown affect the strain. Also note that the heat transfer coefficient is a function of the salt velocity and temperature. Assuming the control system has anticipatory capabilities, the flow rate and thus the heat transfer coefficient will be tied to the incident flux. At nominal operating conditions, a deviation in the heat transfer coefficient of 10% will only result in a 5% change in strain.

Appendix E. Molten and Solid Nitrate Salt Properties

The following properties are for molten and solid nitrate salt. Table E-1 shows the density, heat capacity, thermal conductivity, absolute and kinematic viscosities, Prandtl number, and thermal diffusivity as a function of temperature for molten salt. These data were compiled from various sources. Many properties were obtained for an equimolar ratio of sodium nitrate (46% by weight) and potassium nitrate (54% by weight). We have assumed the difference is not significant. For further details on salt properties please refer to *A Review of the Chemical and Physical Properties of Molten Alkali Nitrate Salts and Their Effect on Materials Used for Solar Central Receivers*, R.W. Bradshaw and R.W. Carling, SAND87-8005, printed April 1987.

Molten Nitrate Salt

Composition:

Sodium Nitrate	NaNO ₃	60% by weight
Potassium Nitrate	KNO ₃	40% by weight

Physical Properties (300-600°C, T is in °C):

Density (kg/m³): $\rho = 2090 - 0.636 \text{ T}$

Heat Capacity (J/kg•K): Cp = 1443 + 0.172 T

Thermal Conductivity (W/m•K): $k = 0.443 + 1.9 \times 10^{-4} \text{ T}$

Absolute Viscosity (mPa•s): $\mu = 22.714 - 0.120 \text{ T} + 2.281 \times 10^{-4} \text{ T}^2 - 1.474 \times 10^{-7} \text{ T}^3$

Other Molten Salt Properties:

Isotropic Compressibility (NaNO₃) at the melting point: $2x10^{-10}$ m²/N

 Speed of Sound:
 1763.3 m/s (5785.1 ft/s) at 336°C (637°F)

 KNO3:
 1740.1 m/s (5709 ft/s) at 352°C (666°F)

Change in Sound Speed with Temperature:NaNO3:0.74 m/s•KKNO3:1.1 m/s•K

Phase Change Nitrate Salt Properties

Freezing Point: Solidifies at 221°C (430°F) Start to crystallize at 238°C (460°F) Heat of Fusion - (based on molecular average of heat of fusion of each component): $h_{sl} = 161 \text{ kJ/kg}$

Change in Density Upon Melting: $\Delta V/V_{solid} = 4.6\% \implies V_{liquid} = 1.046 V_{solid}$

Solid Salt

Density, ρ: NaNO₃: 2260 kg/m³ at room temperature KNO₃: 2190 kg/m³ at room temperature Heat Capacitance, Cp: NaNO₃: 37.0 cal/K•mol = 1820 J/kg•K near melting point KNO₃: 28.0 cal/K•mol = 1160 J/kg•K near melting point Thermal Conductivity, k: KNO₃: 2.1 W/m•K
T		ρ		Ср		k		μ		v		Pr	α	
Tempero	ature	Den	sity	Heat Co	pacity	Thermal Co	onductivity	Absolute \	√is⊂osity	Kinematic	Viscosity	Prandtl	Thermal D	iffusivity
С	F	Kg/m^3	lbm/ft^3	J/kg/K	Btu/Ibm/F	W/m/K	Btu/h/ft/F	Pa s	lbm/ft/h	m^2/s	ft^2/h		m^2/s	ft^2/h
270	518	1918	119.8	1489	0.3558	0.493	0.2850	0.00404	9.78	2.11E-06	0.082	12.20	1.73E-07	0.00669
280	536	1912	119.4	1491	0.3562	0.495	0.2861	0.00376	9.10	1.97E-06	0.076	11.33	1.74E-07	0.00673
290	554	1906	119.0	1493	0.3566	0.497	0.2872	0.00350	8.47	1.84E-06	0.071	10.52	1.75E-07	0.00677
300	572	1899	118.6	1495	0.3570	0.499	0.2883	0.00326	7.89	1.72E-06	0.067	9.77	1.76E-07	0.00681
310	590	1893	118.2	1496	0.3574	0.501	0.2894	0.00304	7.36	1.61E-06	0.062	9.09	1.77E-07	0.00685
320	608	1886	117.8	1498	0.3578	0.503	0.2905	0.00284	6.87	1.51E-06	0.058	8.47	1.78E-07	0.00689
330	626	1880	117.4	1500	0.3582	0.505	0.2916	0.00266	6.43	1.41E-06	0.055	7.90	1.79E-07	0.00694
340	644	1874	117.0	1501	0.3586	0.507	0.2927	0.00249	6.02	1.33E-06	0.051	7.38	1.80E-07	0.00698
350	662	1867	116.6	1503	0.3591	0.509	0.2938	0.00234	5.65	1.25E-06	0.048	6.91	1.81E-07	0.00702
360	680	1861	116.2	1505	0.3595	0.510	0.2949	0.00220	5.32	1.18E-06	0.046	6.48	1.82E-07	0.00706
370	698	1855	115.8	1507	0.3599	0.512	0.2960	0.00207	5.02	1.12E-06	0.043	6.10	1.83E-07	0.00710
380	716	1848	115.4	1508	0.3603	0.514	0.2971	0.00196	4.75	1.06E-06	0.041	5.76	1.84E-07	0.00715
390	734	1842	115.0	1510	0.3607	0.516	0.2982	0.00186	4.51	1.01E-06	0.039	5.46	1.86E-07	0.00719
400	752	1836	114.6	1512	0.3611	0.518	0.2993	0.00178	4.30	9.68E-07	0.038	5.18	1.87E-07	0.00723
410	770	1829	114.2	1514	0.3615	0.520	0.3004	0.00170	4.11	9.29E-07	0.036	4.95	1.88E-07	0.00728
420	788	1823	113.8	1515	0.3619	0.522	0.3015	0.00163	3.94	8.94E-07	0.035	4.73	1.89E-07	0.00732
430	806	1817	113.4	1517	0.3623	0.524	0.3026	0.00157	3.80	8.64E-07	0.033	4.55	1.90E-07	0.00736
440	824	1810	113.0	1519	0.3628	0.526	0.3037	0.00152	3.67	8.39E-07	0.032	4.39	1.91E-07	0.00741
450	842	1804	112.6	1520	0.3632	0.528	0.3048	0.00147	3.56	8.16E-07	0.032	4.24	1.92E-07	0.00745
460	860	1797	112.2	1522	0.3636	0.529	0.3059	0.00143	3.47	7.97E-07	0.031	4.12	1.93E-07	0.00750
470	878	1791	111.8	1524	0.3640	0.531	0.3070	0.00140	3.38	7.80E-07	0.030	4.01	1.95E-07	0.00754
480	896	1785	111.4	1526	0.3644	0.533	0.3081	0.00137	3.31	7.66E-07	0.030	3.91	1.96E-07	0.00759
490	914	1778	111.0	1527	0.3648	0.535	0.3092	0.00134	3.24	7.53E-07	0.029	3.82	1.97E-07	0.00763
500	932	1772	110.6	1529	0.3652	0.537	0.3103	0.00131	3.18	7.42E-07	0.029	3.74	1.98E-07	0.00768
510	950	1766	110.2	1531	0.3656	0.539	0.3114	0.00129	3.12	7.31E-07	0.028	3.66	1.99E-07	0.00773
520	968	1759	109.8	1532	0.3660	0.541	0.3125	0.00127	3.06	7.20E-07	0.028	3.59	2.01E-07	0.00777
530	986	1753	109.4	1534	0.3664	0.543	0.3136	0.00124	3.01	7.09E-07	0.027	3.51	2.02E-07	0.00782
540	1004	1747	109.0	1536	0.3669	0.545	0.3147	0.00122	2.95	6.97E-07	0.027	3.43	2.03E-07	0.00787
550	1022	1740	108.6	1538	0.3673	0.547	0.3158	0.00119	2.88	6.84E-07	0.027	3.35	2.04E-07	0.00791
560	1040	1734	108.2	1539	0.3677	0.548	0.3169	0.00116	2.81	6.69E-07	0.026	3.26	2.05E-07	0.00796
570	1058	1727	107.8	1541	0.3681	0.550	0.3180	0.00113	2.72	6.52E-07	0.025	3.15	2.07E-07	0.00801
580	1076	1721	107.4	1543	0.3685	0.552	0.3191	0.00109	2.63	6.32E-07	0.024	3.04	2.08E-07	0.00806
590	1094	1715	107.0	1544	0.3689	0.554	0.3202	0.00104	2.52	6.08E-07	0.024	2.91	2.09E-07	0.00811
600	1112	1708	106.7	1546	0.3693	0.556	0.3213	0.00099	2.40	5.80E-07	0.022	2.76	2.10E-07	0.00816

Table E-1. Molten Nitrate Salt Properties: 60% NaNO₃, 40% KNO₃.

Appendix F. Selected Sets of Data and Other Information

Thermocouple Layout on Panels	101
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Panel Thermocouple Layout





SETUP INFORMATION FOR THE PANAMETRICS ULTRASONIC FLOWMETER

PROMPT	SETTING
System Units	METRIC
Volumetric Units	liters
Time Units	minutes
Decimal Digits	2
Totalizer Units	liters
Decimal Digits	2
Analog Out Units	Volumetric
Analog Out Zero	0.0 liters/min (4 mA)
Full Scale	500.0 liters/min (20 mA)
Error Handling	Force Low
Response Time	30 readings
Fluid Type	Other (for Molten Sodium Nitrate-60% and Potassium Nitrate-40%)
Fluid Sound Speed	1800.0 m/s (nitrate salt, 1812 m/s was measured when clamp on flowmeter was work)
Reynolds Correction	Active
Kin. Viscosity	1.863 E-6 m^2/s @ 288 C (550F) nitrate salt
Meter Factor K	1.000
Transducer #	91 for the wetted flow cell (Channel 1) 116 for the clamp on transducer (Channel 2)

The setup for each type of transducer is different and continues on the next page.

The Following Apply to the CLAMP ON TRANSDUCERS. (Note the clamp on transducer temperature should not exceed 288 C (550 F). It should be removed before operating at higher temperatures.)

Pipe Temperature	93 C (Wedge Temperature - measured half way up wedge)
Wall Thickness	3.91 mm (0.154 in for 2" dia SCH 40 SS piping)
Pipe I.D.	52.50 mm (2.067 in)
# Traverses	2
Pipe Material	Stainless Steel
Ріре Туре	Round
Zero Cutoff	0.3 m/s
Xducer Spacing S	58.00 mm (enter actual dimension)

This is the space needed for the clamp on transducers as computed from the parameters entered into the computer. If the actual spacing doesn't match this value, the value can be overwritten to match the actual physical spacing.

The Following Apply to the WETTED TRANSDUCERS. (Note the wetted transducer temperature should be monitored and the sensor itself - which is out of the fluid - should not exceed 288 C (550 F). It should be removed before operating at higher temperatures.)

Path Length P	256.4816 mm (10.0977 in from Panametrics)
Axial Dimension L	157.5054 mm (6.2010 in from Panametrics)
Pipe I.D.	52.50 mm (2.067 in)
Ріре Туре	Round '
Zero Cutoff	0.3 m/s
Type Parameter 909 to enter parameters for wetted tra	ansducer 91:
Transducer Number	91
Transducer type	Wetted
Tranducer Frequency	1.0 MHz
Transducer Tw (delay)	36 µsec (or 36.7 per Mike Pouglia of Panametrics)
Transducer THETA 1	N/A
Transducer Wedge Soundspeed	N/A m/scc (ft/sec)
Metal Clamp-on Flow transducers Numbers:	

CTS-1.0-HT	CTS-1.0-HT
1192256	CTS. 1.0 MHz
1.0 MHz	S/N 693286
XDCR#21	XDCR #21
on elbow: 2R0308	

Part Numbers on Components in Molten Salt Experiments

Tee and cap for Corrosi	on Experiments:
•	E-CON E0204-300 S-2063 316 ISZ
	E-CON E0204-300 S-2063 316 ISZ
2" Flange:	
Clamp.	GRAYLOC 2
o na na pr	182F304 GNS0218
	CANADA SN48302
Body (2 of thes	e):
	PN115405 GRAYLOC® 2GR20 BW
	2SCH40 SA182-F316L G1316 S07037700
Checkvalve:	REFLANGE V-CON 3-900
	316 216302
(Clamp side):	F04 S-3063
4" Flange (on checkvalv	ve):
(Clamp):	REFLANGE C-04
(Body):	R-CON F04-0304 S-3063 316 216302
4" Flange:	
(Clamp):	REFLANGE C-04
(Body, 2):	R-CON S4063 316 91461
6" Flange (8 bolt):	
(Body, 2):	E-CON E0604-300 S-6065 316 AJM
• • · ·	E-CON E0604-300 S-6065 316 LDI

Panametrics Flow Meter - Electronics

Model 6468-22-1000-0 Serial Number 791 Software Version 4.D Weight of Components

31 lbs: from elbow to blind flange for corrosion coupons to first half of 2" grayloc flange

14.5 lbs: 2" grayloc clamp

39 lbs: 2nd half of 2" grayloc flange + 2x3 reducer + 3" V-CON checkvalve + half of 3" inner 4" outer R-CON flange

27 lbs: 2nd half of 3" inner, 4" outer R-CON flange to 1st half of 4" R-CON flange

27 lbs: 1st R-CON 4" clamp

29lbs: 2nd R-CON 4" clamp

42 lbs: 2nd half of 4" R-CON flange + 4x6 reducer + 1st half of 6" E-CON flange.

42 lbs: 2nd half of 6" E-CON flange + 6"x2" reducer + elbow

Total weight: 251 lbs

Total length outer edge of elbow to outer edge of elbow: 100"



Added 2-1-94 4" ANSI Ring Type flange, 300#, oval grove, oval ring, stainless steel

Ring Type Flange added between 4" R-CON Flanges

43.1 lbs: 2nd half of 3" inner, 4" outer R-CON flange to 1st half of 4" Ring-type flange 36.5 lbs: 2nd half of 4" Ring-type flange to 1st half of 4" R-CON flange New Total Weight: 303.6 lbs

CRTF	Panel Co	d Fill Test, 1	2/01/93			
TEST	• • • • • • • • • • • • • • • • • • • •	1st pass	2nd pass	3rd pass	4th pass	Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.4494	475	48	48	46	<u>46</u>	80
9.4508	480	. 48	48	46	46	80_
9.4522	485	48	48	. 46	46	80
9.4536	490	48	48	46	46	80
9.455	495	48	48	46	46	80
9.4564	500	48	48	46	46	80
9.4581	505	: 48	48	46	46	80
9.4594	510	. 48	48	46	46	80
9.4608	515		_48	45	46	
9.4622	520	. 48	48	. 45	45	. 80
9.4636	525	48	48	45	45	80
9.465	530		48	45	45	80
9,4664	535	. 48	. 49		. 45	. 80
9.4678	540	. 48		. 45	45	. 80
9.4692	545	. 48	. 49	. 45	45	. 80
9.4706	. 550	. 48	. 49	. 45	45	80
9.4717	555	48	49	45	45	. 80
9.4731			49	45	45	80
9.4744	565	. 48	. 49	. 45	45	
9.4758	570	. 48	49	. 45	45	80
9.4//2	5/5		49	45		. 80
9.4/80	580	283	49	45	45	
9.48	585	. 432	49	45	45	
9.4814	· 590	. 542	104	. 45	45	
9.4828		500	231	40	40	09
9.4642			300	40	40	
9.4850	005	. 589	408	. 69	45	
9.4809	01U		498	. 108	45	120
9.4003	010		492	200	49	140
0.4011			501	200	130	100
0.4025	. 630	578	510	201	180	210
0 /030	635	577	520	270	203	210
0 /053	640		520	304	200	225
0 1067	640	575	516	314	242	201
0 /083	650	574	517	325	200	310
0 /007	655	573	520	330	308	340
0 5011	000	572	525	342	- 323	354
0 5025	665	. 572	520	. 353	33/	381
9.5020		571	531	370	354	
0.5053	. 675		532	385	364	
0 5067	070 A80		533		381	<u>4</u> 43
0 5081			538	<u></u> <u></u>	305	455
9.5004				 	485	476
9.5108	695	570	541	494	507	488

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CRTF	Panel Col	d Fill Test,	12/01/93			
TEST		1st pass	2nd pass	3rd pass	4th pass	Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.5122	700	570	541	504	518	500
9.5136	705	570	543	505	519	505
9.5147	710	570	543	512	527	514
9.5161	715	570	543	518	532	523
9.5175	720	570	544	521	534	529
9.5189	725	570	544	523	537	534
9.5203	730	570	544	525	539	538
9.5217	735	570	545	526	540	543
9.5231	740	570	545	528	542	545
9.5244	745	570	545	530	543	548
9.5258	750	570	546	532	. 544	551
9.5272	755	570	546	533	545	553
9.5286	760	570	546	535	546	555
9.5303	765	570	547	536	547	557
9.5317	770	570	547	537	549	558
9.5331	775	569	547	538	550	559
9.5344	780	569	547	538	550	559
9.5358	785	569	548	539	551	561
9.5372	790	569	548	540	551	562
9.5386	795	569	548	540	551	562
9.54	800	569	548	542	552	563
9.5414	805	569	548	542	552	563
9.5425	810	569	550	543	553	564
9.5439	815	569	550	543	553	564
9.5453	820	569	550	543	553	564
9.5467	825	569	550	544	553	564
9.5481	830	569	550	544	555	564
9.5494	835	569	550	544	555	566
9.5508	840	569	550	545	555	566
9.5522	845	569	550	545	555	566
9.5536	850	569	550	545	555	566
9.555	855	569	550	545	555	566
9.5564	860	569	550	545	556	566
9.5581	865	569	550	546	556	566
9.5594	870	568	550	546	556	566
9.5608	875	568	550	546	556	566
9.5622	880	568	550	546	556	566
9.5636	885	568	550	546	556	566
9.565	890	568	550	546	556	566
9.5664	895	567	550	548	556	567
9.5678	900	567	550	548	557	567
9.5689	905	567	550	548	557	567
9.5703	910	567	550	548	557	567
9.5717	915	567	550	548	557	567
9.5731	920	567	550	548	557	567

	RTF	Panel Col	d Fill Test,	12/01/93			
TES	st -		1st pass	2nd pass	3rd pass	4th pass	Upper he
Tin	ne	• •	TEW4	TEW17	TEE12	TEE9	TEWUH19
hc	bur	Time	DEG F	DEG F	DEG F	DEG F	DEG F
ſ	9.5744	925	567	550	548	557	567
	9.5758	930	567	550	548	557	567
ł	9.5772	935	567	550	548	556	567
	9.5786	940	. 567	550	. 548	554	567
-	 9.58	945	567	550	548	552	567
ľ	9.5814	950	567	550	548	549	567
	9.5831	955	. 567	550	548	548	567
-	9.5844	960	567	550	548	547	567
	9.5858	965	567	550	. 548	546	567
1	9.5872	970	. 567	550	. 548	. 546	567
	9.5886	975	567	550	. 548	. 545	567
	9.59	980	566	550	548	545	567
	9.5914	985	566	550	548	545	567
	9.5928	990	566	550	550	545	567
	9.5942	995	565	550	. 550	. 543	567
ľ	9.5953	1000	565	550	550	. 543	567
	9.5967	1005	565	550	550	. 548	567
	9.5981	1010	565	550		555	567
	9.5994	1015	564	550	550	557	567
	9.6008	1020	564	550	550	. 557	566
	9.6022	1025	564	550	550	. 557	566
-	9.6036	1030	564	550		557	566
1	9.605	1035	564	550	550	557	566
	9.6064	1040	564	550	550	557	566
ļ.	9.6078	1045	564	550	550	557	566
	9.6092	1050	564	550	549	557	566
	9.6106	1055	564	550	549	557	566
[9.6122	1060	564	550	549	557	566
	9.6136	1065	564	550	549	557	566
	9.615	1070	564	550	549	557	566
{	9.6164	1075	_ 564	550	549	557	566
[9.6178	1080	564	550	549	557	565
	9.6192	1085	564	550	549	557	565
L	9.6206	1090	564	550	549	557	565
	9.6219	1095	564	550	549	557	565
_	9.6233	1100	564	550	549	557	565
	9.6244	1105	564	550	. 549	557	565
L	9.6258	_1110	564	550	550	557	565
	9.6272	1115	564	549	550	557	565
	9.6286	1120	564	549	550	557	565
	9.63	1125	564	549	550	557	565
	9.6314	1130	564	549	550	557	565
<u> </u>	9.6328	_1135	564	549	550	558	565
Ľ.	9.6342	1140	564	549	550	558	566
	9.6356	1145	564	550	550	558	566

CRTF	Panel Col	d Fill Test,	12/01/93			
TEST		1st pass	2nd pass	3rd pass	4th pass	Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.6369	1150	564	550	550	558	566
9.6383	1155	564	550	551	558	566
9.64	1160	564	550	551	558	566
9.6414	1165	564	550	551	558	566
9.6428	1170	564	550	551	558	566
9.6442	1175	564	550	551	558	566
9.6456	1180	564	550	551	558	566
9.6469	1185	564	550	551	558	566
9.6483	1190	564	550	551	558	566
9.6497	1195	564	550	551	559	566
9.6511	1200	564	550	551	559	566
9.6522	1205	564	550	551	559	566
9.6536	1210	564	550	551	559	566
9.6553	1215	564	550	551	559	566
9.6567	1220	568	550	551	559	566
9.6578	1225	571	551		559	566
9.6592	1230	574	555	551	559	566
9.6606	1235	576	557	551	559	566
9.6619	1240	577	559	551	560	567
9.6633	1245	578	561	554	561	568
9.6647	1250	579	562	555	562	570
9.6661	1255	579	562		. 563	571
9.6675	1260	580	563	558	566	572
9.6689	1265	580	563	559	566	573
9.6703	1270	580		560	567	574
9.6717	1275	580	565	560	568	574
9.6731	1280	580	565	561	568	575
9.6744	1285	580	565	561	_ 570	576
9.6761	1290	580	565	563	570	578
9.6775	1295	580	565	563	571	578
9.6789	1300	580	566			578
9.6803	1305	580	566	564	. 571	579
9.6817	1310	577	566	564	571	579
9.6831	1315	574	565	564		579
9.6844	1320	570	562	564	571	579
9.6858	1325	568	560	564	571	579
9.6872	1330	566	557	564	571	579
9.6886	1335	565	554	563		578
9.69	1340	565	553	560	570	577
9.6911	1345	564	552	559	567	576
9.6925	1350	564	552	556	565	575
9.6939	<u>135</u> 5'	564	550	555	563	573
9.6953	1360	564	550		562	572
9.6967	1365	564	550	554	561	571
9.6981	1370	564	550	553	560	571

CRTF	Panel Co	old Fill Test,	12/01/93			
TEST		1st pass	2nd pass	3rd pass	4th pass	Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.6994	137	5 564	550	553	560	570
9.7008	138	0 564	550	553	560	569
9.7022	138	5 564	550	552	559	569
9.7036	139	0 564	550	552	559	568
9.705	139	5 564	550	552	559	568
9.7064	140	0 564	550	552	559	568

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Cold Fill Test of 2 inch Pipe

Cold Pipe	Test	i	Sched	dule 4	0, 2in (pipe	
Sept. 24, 19	993		Salt Te	empe	rature.	, 524 F	
	Outsic	de Pip	e Terr	perat	ure, d	eg F	
Channel	439	440	441	442	443	444	445
Hrs:Min:Sec			i				
9:16:55	367	262	103	99	96	126	613
9:17:00	363	263	104	99	96	126	613
9:17:05	362	263	103	99	96	125	613
9:17:10	362	_263	103	99	96	126	613
9:17:15	362	263	103	98	96'	_126	_613
9:17:20		_263	104	99	96	125	613
9:17:25	363	263	102	. 99	96	125	613
9:17:30	363	_262	103		96	126	613
9:17:35	<u> 3</u> 61:	262	_103	. 99	96	125	613
9:17:40	<u>383</u>	_268	111	_100	. 95	125	613
9:17:45	<u>415</u>	_281	144	122	.100	125	613
9:17:50	444	302	194	157	124	141	607
9:17:55	462	320	240	191	152	164	592
9:18:00	475	341	292	230	186	194	572
9:18:05	485	358	344	275	222	227	555
9:18:10	493	377	393	334	277	280	540
9:18:15	496	_ 391	_421	377		331	532
9:18:20	_496_	_ 405_	_ 445_	416	395	384	528
9:18:25	499	415	458	440	_ 431	420	527
9:18:30	500	425	4/0	460	460	451	527
9:18:35	502.	434	480	4/3	4/8	_ 469_	529
9:18:40	504	441	_ 487_	483	. 490	482	529
9:18:50	507	455	498	498	503	499	531
9:18:55		400	.501	_ 501	500	503	532
9:19:00	508	405	.505	500	509	507	532
9:19:05	509	408	500	508	510	508	532
9:19:10	508	4/2	508	510	513	510	532
9:19:15		4/5	510	51Z	514	512	532
9:19:20	509	4/8	511	513	515	512	532
9:19:25			511	513	515	512	532
9:19:30	511	483	514	515	517	514	532
9:19:35	511	485	514	517	518	515	532
9:19:40	511	487	515	517	519	516	532
9:19:45	510	400	510	519	519	515	532
9:19:50		490	- 517	519	519	517	532
9:17:55	512	491	51/	ວ ເອ 	520	510	532
9.20:00	513	493	_ບເ/ 	- 019 - 500	520	519 510	520
9.20.00	515	490		_02U 	52U 601	_019 _610	522
9.20.10	510	490	510	500	5021	- 519 - 520	520
0.20.10	14 517	<u>47</u> /. <u>107</u>	500	501	500	520	522
0.20.20	- <u>914</u> - 514	. 47/ 	- 020 - 510	. 021 	522	520 520	522
0.20.20	514	100	521	522	522	520	522
9.20.00	515	47 <u>7</u> /00	510	521	521	520	522
9:20:35	515	499	_519	_ 521_	521	520	532

Cold Fill Test of 2 inch Pipe

Cold Pipe	Test		Schee	dule 4	0, 2in	pipe	
Sept. 24, 19	793 :		Salt Te	empei	rature	, 524 F	
i	Outsic	de Pip	e Terr	perat	ure, d	leg F _l	
Channel	439	440	441	442	443	444	445
Hrs:Min:Sec			I				
9:20:40	516	501	520	522	523	521	532
9:20:45	517	502	520	523	523	522	532
9:20:50	516	503	521	524	523	521	533
9:20:55	516	503	520	524	524	522	533
9:21:00	517	503	521	524	524	523	533
9:21:05	516	504	521	524	524	523	533
9:21:10	519	504	522	525	524	523	533
9:21:15	518	505	522	524	524	522	533
9:21:20	516	505	522	525	524	523	533
9:21:25	517	505	522	525	525	523	533
9:21:30	517	507	523	526	525	523	533
9:21:35	517	507	523	526	525	524	533
9:21:40	518	507	523	525	525	524	533
9:21:45	517	507	523	525	526	524	534
9:21:50	516	507	523	526	525	524	533
9:21:55	518	508	523	526	525	525	533
9:22:00	517	508	523	526	525	524	533
9:22:05	519	508	523	526	526	525	533
9:22:10	518	509	523	527	526	525	533
9:22:15	519	507	523	526	525	523	532
9:22:20	519	509	524	526	527	525	533
9:22:25	518	510	524	527	527	525	533
9:22:30	518	509	523	526	525	524	533

Flow meter calibration data summary.

	Total Bias	and Rando	m Uncertai	nty Percent	s and Urss	Uncertaint	ies	·	: : - · ··	
Flow	FT-720 Vo	rtex Flow	PF-001 We	etted Ultra	PF-002 Cla	ampon Ultr	FT-730 Vc	ortex	FT-800 Vo	ortex
L/min	Bias	Random	Bias	Random	Bias	Random	Bias	Random	Bias	Random
Average	B 	1955/N^.5	Ві	1955/N^.5	Ві	1955/N^.5	BI	1955/N^.5	BI	1955/N^.5
Flow, It/mi	%	%	%	%	%	%	%	%	%	%
102.58	9.76	0.63	3.84	0.55	8.47	0.50	9.90	0.47	5.29	0.44
155.40	11.58	0.29	4.14	0.51	12.78	0.55	11.55	0.39	7.29	0.27
197.41	12.56	0.18	4.56	0.44	12.97	0.42	12.50	0.22	8.48	0.21
244.65	15.09	0.21	6.35	0.31	13.27	0.30	15.62	0.35		
Flow	Urss		Urss	······································	Urss		Urss	+	Urss	· · · ·
102.5759	9.77976	:	3.878089		8.485958	• •	9.91473	i ·	5.310453	
155.3991	11.58529		4.168351	· · · · · ·	12.79488		11.55541		7.295545	
197.4063	12.55799		4.581304		12.97705		12.49935		8.48723	
244.6471	15.08722		6.358041		13.27571	I — - ·	15.62751			

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Flow meter calibration data summary.

	Bias and F	landom Un	certainty Pe	rcents Rela	ative to Bub	bler Refere	ence			
					•	T 	• :	•		1
Flow	FT-720 Vo	rtex Flow	PF-001 We	etted Ultra	PF-002 Cla	ampon Ultr	FT-730 Vo	rtex	ⁱ FT-800 Vo	rtex
L/min	Bias	Random	Bias	Random	Bias	Random	Bias	Random	Bias	Random
	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5
Lt/min	%	%	%	%	%	%	%	%	%	%
245.07	15.52159	0.475089	6.862377	0.662462	-11.1397	0.488859	15.82366	0.481864	· _	
245.07	13.99688	0.239153	4.261886	0.230269	-12.9097	0.200013	14.08849	0.290354		
196.22	12.42478	0.232202	3.896936	1.145752	-10.4407	0.944796	12.56068	0.435271	7.226531	0.348303
191.20	13.99572	0.071855	4.027049	0.149455	-10.8986	0.125255	13.66786	0.060468	9.22606	0.171739
155.47	12.56275	0.753997	4.490394	1.213737	-8.18096	1.074611	12.56275	0.674396	7.159739	0.480827
155.19	10.07565	0.12859	1.012406	0.081947	-12.3653	0.25961	10.29978	0.201509	5.663095	0.24198
102.99	8.110337	1.133905	0.300727	0.940323	-6.15803	0.721195	8.490264	0.658884	3.086858	0.699224
102.16	9.834467	0.130553	-0.22997	0.152059	-8.94488	0.272782	9.767941	0.282077	4.198763	0.17449
154.91	10.90267	0.179409	-0.45872	0.614047	-14.4883	0.671667	10.51535	0.412473	5.932066	0.129107
156.03	10.16607	0.099755	1.122052	0.125268	-13.7377	0.177755	10.1898	0.27912	6.035729	0.236388
200.13	11.02	0.299602	1.208081	0.386784	-13.964	0.498647	10.88372	0.25495	7.597939	0.187905
202.08	10.38117	0.10355	0.711803	0.070636	-14.2525	0.116727	10.46034	0.114129	6.214532	0.137835
246.46	13.39638	0.089405	3.323362	0.277316	-14.7587	0.349742	14.27843	0.499605		
242.00	15.44113	0.048174	5.7871	0.059108	-12.0118	0.152921	16.38737	0.134167	·	

T1		1'	1	•	1.4.4	
FIOW	meier	can	nrai	ion	data.	summary
	meter	· · · · ·	orac		ouu	Summary.

Flow mete	r calibrati	on data su	mmary.							
	Bias and F	Random Un	certainty Le	vels Relati	ve to Bubbl	er Referenc	e		· · · · · · · · · · · · · · · · · · ·	
Flow	FT-720 Vo	rtex Flow	PF-001 W	etted Ultra	PF-002 CI	i ampon <u>Ult</u> r	FT-730 Vo	 ortex	FT-800 Vo	l
L/min	Bias	Random	Bias	Random	Bias	Random	Bias	Random	Bias	Random
	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5
Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min
245.07	38.04	1.164281	16.82	1.623467	-27.30	1.198025	38.78	1.180883		;
245.07	34.30	0.586083	10.44	0.564311	-31.64	0.490163	34.53	0.711559		· · · · ·
196.22	24.38	0.455627	7.65	2.248196	-20.49	1.853879	24.65	0.85409	14.18	0.6834
191.20	26.76	0.137384	7.70	0.285752	-20.84	0.239483	26.13	0.115611	17.64	0.32835
155.47	19.53	1.172231	6.98	1.886982	-12.72	1.670686	19.53	1.048475	11.13	0.74753
155.19	15.64	0.199558	1.57	0.127173	-19.19	0.402888	15.98	0.312721	8.79	0.37552
102.99	8.35	1.167861	0.31	0.968482	-6.34	0.742792	8.74	0.678615	3.18	0.72016
102.16	10.05	0.133369	-0.23	0.15534	-9.14	0.278667	9.98	0.288162	4.29	0.17825
154.91	16.89	0.277923	-0.71	0.951224	-22.44	1.040483	16.29	0.638965	9.19	0.3
156.03	15.86	0.155645	1.75	0.195453	-21.43	0.277347	15.90	0.435503	9.42	0.3688
200.13	22.05	0.599587	2.42	0.774063	-27.95	0.997932	21.78	0.510226	15.21	0.37605
202.08	20.98	0.209255	1.44	0.142743	-28.80	0.235883	21.14	0.230634	12.56	0.278538
246.46	33.02	0.220348	8.19	0.683476	-36.37	0.86198	35.19	1.231332		·
242.00	37.37	0.11658	14.00	0.14304	-29.07	0.370062	39.66	0.324677	i	r

Flow meter calibration data summary.

Percent	FT-72	0 Vor	tex Flow	PF-001 W	etted Ultra	PF-002 Cl	ampon Ultr	FT-730 Vc	ortex	FT-800 Vo	rtex	East Cal	West Cal	Total Cal	Num of pts	195
Flow	Ave		Std	Ave	Std	Ave	Std	Ave	Std	Ave	Std		Ĩ	:	Ν	
	L/min	ļ	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	; I	
· _		1		<u> </u>				!	L				1	L	i	· · ·
10	0 28	3.10	5.11	261.88	7.12	217.77	5.26	283.84	5.18			103.55	141.51	245.07	77.00	. 2
10	0 27	9.37	2.57	255.51	2.48	213.43	2.15	279.59	3.12			103.55	141.51	245.07	77.00	2
	0 22	0. <u>60</u>	0.83	203.87	4.09	175.73	3.37	220.87	1.55	210.40	1.24	<u>1: 89.88</u>	106.34	196.22	15.00	2.131
s	0 21	7.96	0.56	198.90	1.17	170.36	0.98 _	217.33	0.47	208.84	1.34	1 91.55	99.65	191.20	67.00	2
- E	0 17	5.00 _.	<u>2.51</u>	162.45	4.05	142.75	j 3.58	175.00	2.25	166.60	1.60	0 [!] 84.0 <u>1</u>	71.45	155.47	20.00	2.086
e	0 17	0.83	0.68	156.76	0.43	136.00	1.37	171.17	1.06	163.98	1.2	<u>7 </u>	71.18	155.19	46.00	2
4	0 11	1.35	2.71	103.30	2.24	96.65	1.72	111.74	1.57	<u>106.17</u>	1.67	77.87	25.12	<u>102.99</u>	23.00	2.069
4	0 11	2.20	0.68	101.92	0.79	93.02	. 1.41	112.14	1.46	106.45	0.90) _: 77.87	24.28	102.16	103.00	2
6	0 17	1.80	0.76	154.20	2.61	132.47	2.85	171.20	1.75	164.10	0.55	5 84.29	70.62	154.91	30.00	2
6	0 17	1.89	0.57	157.78	_0.72	134.59	1.02	171.93	1.60	165.44	1.36	6 84.29	71.73	156.03	54.00	2
8	0 22	2.18	1.72	202.55	2.22	172.18	2.87	221.91	1.47	215.33	1.08	3 90.71	109.41	200.13	33.00	2
8	0 22	3.06	0.74	203.52	0.50	173.28	0.83	223.22	0.82	214.64	0.98	<u>91.27</u>	<u>110.81</u>	202.08	50.00	2
10	0 27	9.48	0.51	254.65	1.58	210.09	2 <u>.0</u> 0	281.65	2.85		<u> </u>	104.95	141.51	246.46	23.00	2.069
10	0 27	9.36	0.48	256.00	0.59	212.93	1.54	281.65	1.35			100.48	141.51	242.00	69.00	2
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<u> </u>	CRTF	NET-90	-·	99 POIN	T D/	ATA	FILE;		42.0					•			
Time	Time	DATE: Time	Time	May) PF	- <u>001</u>	PE-002	FT730	iFT80	00 P	T720	CALE FI	CCALW.F	L(FCV80		o ii	LT899
MST	hour	min	sec	Lt/mir	í <u>L</u> t	/min	Lt/min	Lt/min	Lt/mi	in P	SIG			Lt/min	Inch	j	inch
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11.53417	<u>11</u>		32	3	288	265	219	2	288	57	56	: 1	0	0	55	22	0
11.53556			32	8	288	265	219	<u> </u>	288	60	56		0	0	55	22'	- · · · · · · · · · · · · · · · · · · ·
11.53694	11	}	2	- 13	288	265	219		288	57	56		0	0	55 61	22	0
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11.54111	11		32	28	283	265	219	- 2	82	62	57		0	0	61	22	0
11.5425	11		32	33	283	265	219	2	282	62	57		0	0	61	22	0
11.54389	11		32	38	283	260	219	2	282	62	57	• • •	0	0	61	. 22	0
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11,54667	. 11	>	22	40 53	283	260	219		202	63	57		0.	0	62	21	. 3
11.54944	11	3	32	58	283	260	219		282	60	57	- 7	0	0	62	21	. 6
11.55083	11		33	3	283	260	216	ં ટ	282	63	57		ด่	0	62	20	8
11.55222	11	. 3	33	8	283	260	216	. 2	282	59	57		0	0	62	20	11
11.55361	. <u>11</u>	}	33	13	283	260	216	- 2	282	61	57		0:	0	62	20	13
11.555	11	· ·· ·- }	3 <u>3</u> 33		280	260	216		282	57 62	57	•	0	0	55 62	19	18
11.55778	11	· <u>-</u>	33	28	280	260	216	- 2	281	59	57	•	0	ō	62	19	19
11.55917	11		33	33	280	260	216	. 2	281	57	57		0	0	62	18	21
11.56056	11		33	38	280	258	216	2	281	62	57		0	0	62	18	24
11.56194	11		33	43	280	258	216	. 2	281	65	57		0	0	62	18	. 27
11.56333	11	;	53 12	48	280	258	216		281	61 60	57	-	0	0.	62	18 18	27 28
11.56611	11	· ···- <u>*</u>	33	58	280	258	210	2	281	59	57		0	0	56	18	29
11.5675		<u>}</u>	34	3	280	258	213		281	63	- 57		0	ō	63	18.	30
11.56889	11		34	8	280	258	213	2	281	60	57		0	0	57	18	30
11.57028	<u>11</u>		34	13	280	258	213	. 2	281	62	57		0	0	62	18	31
11.57194			34	19	281	258	213		281	53	57	• •	0	0	53	18	
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11.5775	11		34	39	281	257	213		282	61	57	• •	0	0	57	20	15
11.57889	11		34	44	281	257	213	<u> </u>	282	61	57		0	0	63	20	11
11.58028	11		34	49	281	257	213	. 4	282	61	57		0	0	.57	20	7
11.58167	11		34	54	281	257	- 213		282	60 60	57		<u>0</u>	0	.5/ 	- 21	
11 58444	11		35	4	281	257	215	-	282	63	57		0	ö	63	21	- · · · · č
11.58583	11		35	9	281	257	215		282	60	57		0	0	63	21	ō
11.58722	11		35	_14	280	257	215	. 4	282	61	57		o	0	63	21	0
11.58861	11		35	19	300 ₁	257	220		243	61	56		0	0.	63	22	0
11.59	11	·	35	24	335	264	233		129	52	43		0	0	57 57	- 22-	0
11.59278	11	· · }	35	34	349	281	242	··- · .	157	57	34	•	o O	0	57	22	0
11.59417	11		35	39	349	287	247		163	57	32		o	0	50	23	Ē
11.59556	11		35	44	355	287	240	i ·	163	47	30		0	0	50	23_	0
11.59694	11		35	49	355	301	228		169	. 47	31		0	0	24	23	0
11.59833	11		35	54 50	342	308	216		126	2	41		0. 0.	0	5	23	c c
11.60111	<u> </u>		36	4	315	301	200		99	2	. 40		0	o	5	23	· c
11.6025	11		36	9	303	301	200	1	82	2	64		0	0	5	23	C
11.60389	11		36	14	289	301	206	_	59	2	71		0	0	5	23	0
11.60528	11	•	36	- 19	277	294	206		46	2	75		0	.0	5	. 23	0
11.60667					2/1	283	206		21. 11	2	80 80		0	0	5	23	. U
11.60944	<u>-</u> !! 11		36	34	265	257	206		5	2	85		ō	ō	5	23	· · · · · · · · · · · · · · · · · · ·
11.61083	11		36	39	258	252	206		16	2	86		o j	0	5	24	C
11.61222	11		36	44	268	246	206	È.	32	26	66		0	0	44	24	0
11.61361			36	49	323	251	_ 212		116	63	50		0	0	63	24	0
11.615	$\frac{11}{11}$		36	54	338	269	225		139	58	41		0	0	5/ 51	23	
11.61778	1 11		37	4	305	277	230		300	61	48		0	0	57	23	· · č
11.61917		·	37	9	299	277	230		293	57	50		0	0	57	23	c
11.62056	្រា		37	14	293	277	230	<u> </u>	288	62	53		0	0	65	23	1
11.62194	11		37	19	288	277	230	4	288	63	54		0	0	58	22	4
11.62333	· 11		5/ 37	24	288	270	225		288 288	63 50	55		0 0	0	63 63	22	. 4
11.62611	. 11	• • •	37 -	34	288	270	225		282	66	56		0	0	63	22	f
11.6275	i 11		37	39	288	264	220		282	62	57		0	0	63	22	
11.62889	11	;	37	44	288	264	220	<u>.</u> 2	282	62	57	- 	0	0	63	22	9
11.63028	<u>11</u>		37	49	282	264	220		282	62	57		0	0	<u>63</u>	22_	10
11.63167	!!	•—·	37	54	282	264	220		282	65	57		U O	0	63	22	12
11.63306	11		3/ 38	. 59 	282	204	220		202	59 63	57		0	<u>.</u>	63	22	10
11.63583	$\frac{1}{11} \frac{1}{11}$		38	9	282	259	220		282	63	57	, ·	0	o	63	22	15

11.63722	1	11	3	8	14	282	259	220	28	2	59		57		0;		0.	63	l	22	16
11.63861		11	3	8	19	303	259	220	23	5	67		56		0		2	68	· _ ·-	22	17
11.64;	· · · · · ·	11	3	8	24	342	277	220	103	3	581		40 j		0	!	<u>)</u>	60		22	17[
11.64139		11:	3	8	29	350	288	237	12	1	54		35		0	_ '	<u>.</u>	53		22	18
11.64278		11	3	8		356	295	243	13	5	. 53		31		0	'	2	_ 53		22	18
11.64417		11!		8	39!	356	306	243	14*	1	53		29		0		<u>.</u>	53	• ·	22	19
11.64556		11		8	44	356		234	140	5	49		27		<u>0</u>	'	<u>,</u>	47		22	- 19
11.04094	· • .			0		362	323	214		Di Di	40.		20). 	-4/		22	20
11 64072	··	<u></u> :	·	8		362	323	201	15/	<u></u>	- 40		24	·	0	· }		47		22	20
11 65111		i T	3	ia.		362	329	196		<u>,</u>	34	- · · ·	23	· ·	0		·	35		23	21
11 6525		<u></u> ;		0		368	317	188	158	А	50		22		<u>0</u>	2		47		23	- 20
11 65389		11	3	۰. ۱۹	14	368	312	188	164	4	45		22:	-	0 0	- 6	<u>,</u> –	47		23	- 19
11.65528		11	3	9	19	368	312	188	164	4	41	· ·-	21		õ	- (Ď!	40		23	17
11.65667		TT:	3	9	24	368	312	178	164	4	44		20		0	(5; -	40		23	15
11.65806		11,	3	9ï	29	368	331	172	16	4	47		20		0) .	46	· -·	23	. 14
11.65944	;	11	3	19	34	368	331	172	169	9	48	:	20 [`]		0	()	46		24	11
11.66083		11	3	9	39	368	336	178	169	9	66		20	-	ō.	. ()	63		24	10
11.66222		11	3	9	44	368	329	178	162	2	5		23		0	. ()	4		24	. 8
11.66361		11;	3	9	49	362:	329	178	148	8	. 1		28		0	() _.	. 4	-	24	4
11.665		11 <u>i</u>	3	9	54	362	319 ¦	178	13	5	1		32		0 _.	()	_4		24	. 0
11.66639		11	3	<u>19</u>	59	349	319	178	_ 120	0	. 1.		38		<u>0</u> :	. (2	4		24	0
11.66778		11	4	0	4	343	319	178	106	5	- 11	1	42.		0		2	4	· <u> </u>	24	0
11.66917		11	4	0	9	338	319	183		4 5	- 1	-	4/ c1		0i A ⁱ			4		24	2
11.67104			4		<u> 14</u>	- 330 -	312	183	82	≤ 61	¦-		51:	• •	<u>0</u> .) N	4	-	24	
11 67333		11.	4	0	19, .	325	303	212	50	4	ן הב		50 50		0 <u>.</u>	}	·	20		24	
11 67472	·	÷	4'			348	298	213	113	. .	 	-	38		<u></u>		Ś	42	-	24	- 0
11.67611	··· - •	11	4	0	34	355	298	230	13	 1	47		34		ō.	Č	·	48		24	ő
11.6775		11	4	0	39	328	300	235	29	1	51		32		0	· - `) · ·	48		24	o
11.67889	· •	11	4	0.	44	322	294	235	313	3	54	- :	36		0 [.]	(54		23	0
11.68028	•••••	11	4	0	49	314	288	235	313	3	51		41		o	() [`]	54		23	0
11.68167		11	4	0	54	308	288	235	307	7	54		43		oj	. ()	54		23	0
11.68306		11	4	0.	59		_288	235	307	7	54		46		oj	. ()	54		23	0
11.68444	'	11_	4	1	. 4	301	288	230	30	1	54		49		0	().	55		23	0
11.68583	'	11	4	1	9	295	282	230	_ 295	5.	57	:	50 _.		0 _.	()	55		23	. 0
11.68722		11_	4	1	14	295	275	230	295	5	57	1	52		0	()	56		23	0
11.68861	!	11.		1		290		230	_ 289	9	57	:	53		0	0).	56	-	23	0
11.69	· -	11				- 290	2/5	225	285		. 60		54		0			50		23	
11 60279		1 <u> </u>	4		29	290	209	225	203	<u>.</u>	60	-	54 55	• •	0		· -	52 62		23	
11 69417		11			- 39	283	269	- 225	203	<u>.</u> .	60		55		o	- 2	Ś	62		22	ő
11.69556	·	11	4	1	44	283	263	225	283	3		}	56		o O	•	Ś	62		22	- 0
11.69694	· - · · · ·	11	4	1	49	283	263	225	283	3	- 60		56		o.	: č	j	62	-	22	ŏ
11.69833		11	4	1	54	283	263	219	283	3	62		56		o.	C) [`]	62	•	22	
11.69972	1	11	4	1	59	283	263	219	283	3	65	:	56		0	() 	62		22	0
11.70111		1 <u>1</u>	4	2	4	283	263	219	283	3	63	;	56		0	()[62		22	0
11.7025	1	11	. 4	2'	9	283	263	219	283	3.	63	_ !	56		0	().	62		22_	0
11.70389	1	11	4	2	14	283	_263	219	283	3.	. 59	:	57 _.		0.	()	62		22	0
11.70528		11	4	2		_ 283	263	219	283	3.	66		57		0	. ()	62		22	0
11.70667	.]	1	4	2	24	283	263	219	283	3	. 62		57		0	. ().	62		22	
		1	- 4	2	29	283	263	219	283	.	59		57		U.	(59		22	0
11.70944	}	1	4	21	34	283	263	219	283	5.	66		57		0	()	. 6/		22	0
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11.715	1	11	4	2	54	281	260	217	282	2	61		58		0	2	·	58	-	22	ő
11.71639	- 1	i1		2	59	281	260	217	282	2	56		58		o [`]	Ċ) [.]	58		22	ō
11.71778	1	11	4	3	4	281	260	217	282	2	63	:	58		0	Ċ) j	58	•-	22 [`]	· · · o
11.71917	1	11	4	3	9	281	260	217	282	2	63	:	58		0	Ċ)	65		22	0
11.72056	1	1	4	3	14	281	260	217	282	2.	66	9	58 _.		0 _.	C)	65		22	0
11.72194	1	1	4	3	19	281	260	217	282	2	64	9	58		0	().	65		22	_ 0
11.72333		1	4	3	24	281	260	217	282	2	64	!	58		o.	(<u>.</u>	65		22	ō
11.72472	1		4	3	29	281	260	217	_ 282	<u>.</u>	64		58 _.		U.	0	ł	65		22	
11.72583	1	11. 	4:	3	33	281	260	217	282		61		58 50		U A		,	65		22	S S
11 72961	_ !	4-	- 43	3	38	201	200	21/	282	<u>د</u> .	64 60	:	50 50		0. 0.		,	60 03		22	0
11 73	·	1	4	3	43 <u>A</u> R	202	257	217	202	<u>.</u>	00	;	58		o	- 7	, . 1	59		22	
11.73139	1		4	3	53	282	257	217	202	5	57	:	58		o.	· - 6)	- 59	· · -	22	ŏ
11.73278	1	ii -	_ · - 4	3	58	282	257	217	282	2	61		58		ō.)	65	•	22	·· ol
11.73417	- 1	11	- 4	4	3	282	257	217	282	2.	60		58		Ö	Ċ)	59	• •	21	4
11.73556	1	ĥ.	4	4	8	282	257	217	282	2	64	· .	58		o	C)	59		21	6
11.73694	<u>i</u>	1	4	4	13	282	257	217	282	2	57	:	58		0	()	59		20	8
11.73833	!	1	4	4	18	282	257	217	282	2	59		58	-	0	Ċ) _.	59	-	20	<u>10</u>
11.73972	1	11	4	4	23	282	_257	217	. 282	2	62	!	58		0	C)	66		20	13
11.74111	1	1	4	4	28	282	257	217	282	2	58	;	58	· _ ·	0).	59		19	15
11.7425	1	11	4	4	33	282	257	217	282	<u>. </u>	60	}	58		U	- 2		59		.19	19
11.74389]			4	38	282	257	217	282	<u>.</u>	67		50 50		0	- ?	,	00		19_1	20
1 11.74020			44	-+1	43	200	201.	21/	∠04	•	02		<i>.</i> 0		U			00		10	~~

11.74667	11	44	48	280	257	217	284	64	57	0	0 60	18 24
11 74806	11	44	53	280	263	213	284	61	57	0,	0. 601	18. 27
11 74000		441		280	263	213	284	57	- 57		60	18 27
11.74944		- 22 -		200	203		-204			^!	0 - 00	
11.75083		45		280	263	213	284		<u> </u>		0.00	2/
11.75222	<u>11</u>	45	8	280	263	213	284	<u>66</u>	57	<u>0</u> ,	0 <u>66</u>	19: 25
11.75361	11	45	13	280	263	213	284	66	57	0	0 66	19! 21
11.755.	11,	45	18	280	258	213	284	62	57	0	0 60	19 18
11 75639	<u> </u>	45	23	280	258	213	284	62	57	0	0 60	20 13
11.75770		45	20.	- <u>200</u>	250	- 212			E7	···· 0		201 10
11./5//8		45	20	280	230;	213	204	02			00	
11.75917	<u>1</u> 1]	45	33	280	258	213	284	58	_ 57		0 60	
11.76056	11	45	38	280	258	213	284	59	57	0	0. 60	21 3
11.76194	11	45	43.	281	258	213	280	59	57	0	0 60	21 1
11.76333	11.	45	48	281	258	213	280	59	58	0;	0 60	21 0
11 76472	11	45	53	281	258	213	280		58 -	0	0.00	22 0
11.704/2					230				50			
11.70011	!!	45		201	250			02			0 00	
<u>11.7675</u>	11!	46	3!		258	213	280	<u>59</u>	58		0 60	22 0
11.76889	11	46	8	281	258	213	280j	59	58	0	0; 60 ¹	22 0
11.77028	11	46	13	281	258	213	280	60	58	0	0 60	22 0
11.77167	11	46.	18	281	258	213	280	55	58	0	0 58	22 0
11 77306	11	46	- 23	281	258	213	280	59	58		0 58	22 0
11.77444	<u> </u>	46		201	. 250		200	62;		··· õ- ··	0	
11.77 444	i		20	201	236	213	_ 2001				0 00	22
11.77583	!!!	46	33	281	258	213	280	60	58	. 0'	0 58	22!0
11.77722	11	46	38	281	258	213	280	60	58	0,	0 58	22 0
11.77861	11	46	43	282	258	213	282	60	58	0	0 58	22; 0
11 78	11	46	48	282	258	213	282	65	58		0 65	22 0
11 78130	<u> </u>	46	53	282	258	216	282	60	58	<u> </u>	n <u>50</u>	
11.70139	<u> </u>		50	- 202	- 200		202				<u>0</u>	· · · <u><</u>
11./82/8		40	58	282	258	216	282	· - 5/	- 58		<u>v. 59</u>	22 0
<u>11.78417</u>	<u>11</u>	47		282	258	216	282	_62	58	0	0 59	.22 0
11.78556	11.	47	8	282	258.	216	282	58	58	0	0 59	22 0
11.78694	11	47	13	282	258	216	282	62	58	0	0 65	22 0
11 78833	11	47	18	282	258	216	282	61	58	0	0 - 65	22 0
11 79072				202	200	216	202		50	-	0	
11.70972				202	230	210	- 202				<u> </u>	
11.79111	11	4/:	28		258	216	282	62	58.	0	0 58	220
11.79278	<u>11.</u>	47	34	282	258!	216	282	63	58	0	0 58	22 0
11.79417	11,	47	39	281	258,	216	282	60	58	0	0 58	22 0
11.79556	11	47	44	281	258	216	282	59	58	0	0 58	21 2
11 79694	11	47 -	49	281	258	216	282	56	58	0	0 58	21 5
11.70034				- 201	- 250	210	202		50		<u> </u>	21
11.79633	· · · · ·	4/		201	258	215	_ 202	63			0	21
11.79972	. 11	_ 47	59	281 ₁	258	_215	282	57	. 58	0 _.	0 57	20 9
11.80111	11	48	4	281	258	215	282	57	58	0	0 57	20 12
11.8025	11	48	9	281	258	215	282	60	58	0.	0. 57	19 14
11.80389	11	48	14	281	258	215	282	59.	58	0;	0 62	19 16
11.80528	11	48	19	281	256	215	282	57			62	10 19
11.00520		40					- 202 -		50		0 02	· · · · · · · · · · · · · · · · · · ·
11.60067		401		_ 201	250	215	.282	60	. 58		0 62	1820
11.80806	11!	_ 48	29	281	256	_215	282	63	58	0	0 62	18 23
11.80944	11	48	34	281	256	215	282	59	58	0	0 62	18 25
11.81083	11	48	39	280	256	215	282	64	58.	0	0. 62	18 27
11.81222	11	48	44	280	256	215	281	64	58	0	0 62	18 28
11 81361	11	48		280	256	215	291	64		<u>.</u>	0 60	19 - 26
11.015		40	<u></u>		230	. 213	- 201			· · · · · · · · · · · · · · · · · · ·	<u>0</u> . <u>02</u> . <u>0</u> .	10 20
11.815	111	48	54	2801	256	214	281	. 59	_ 57.		0 62	18 27
11.81639	!!!	48	59	280	256	214	281	63	57		<u>u 61</u>	
11.81778	<u>11</u>	49	4	280	256	214	281	60	57	0	0 59;	19 21
11.81917	11	49	9	280	256	214	281	57	57	0	0 59	19 17
11.82056	11	49	14	280	256	214	281	60	57	·	0 60	20 14
11 82104	11	401	10	280	256	214	281		57	0-	0 60	20 - 1
11 00000		40		- 200.	200	214			::		<u> </u>	
11.02333		49	<u> </u>	200	200	214	201	30			<u>v </u>	5
11.82472	11	49	29	280	256	214	281	123	57	. 0	0 123	212
11.82611	11	_ 49	34	280	256 <u>-</u>	214	281	127	57	0 _.	0 127	21 0
11.8275	11	49	39	281	256	214	281	125	58	0	0 121	21 0
11.82889	11	49	44	281	256 ⁱ	214	280	120	58	0 .	0 121	22 0
11.83028	11	49	49	281	256	214	280	211	58		0 188	22
11 83167	11	40	54	281	255	212	280	226	- 50		· <u>·</u> ·····	
11.00107		40	. 24	201	200	.212	200	220	. 59	······································	~	<u><u><u></u></u></u>
11.83306			29	201	256	212	280	236	59	U.	0 231	0
11.83444	11	50	4	281	256	212	280	236	_ 59	0	0 236	_220
11.83583		50	9	281	256	212	280	239	59	0	0 236	22 0
11.83722	11	50	14,	281	256	212	280	237	59	0	0 242	22 0
11.83861	11	50	19.	281	255	212	280	260	60	· o ·	0 254	22 0
11 84	11	50	24	275	255	212	280	270		<u> </u>	0 270	22
11 94120		- 20			255		- 200			·	<u>v. </u>	
11.04139			29	2/5	255	212	2/4	270	61.	<u> </u>	<u>v</u> 270	0
11.84278		50'	34	275	255	212	274	272	62	0	0 270	220
11.84417	11	50	39	275,	255	212	274	272	62	0	0 270	22 0
11.84556	11	50	44	275	255	212	274	272	62	0	0 270	22 0
11.84694	11	50	49	275	250	212	274	- 272	62	0	0 270	22 ^
11 84833	<u> </u>	50	54	275	250	200	274	272	62	···		
11 94070	<u> </u>										<u>~</u>	22, 0
11.049/2			28	215	200	209	214	- 212	02		2/0	0
11.85111	11:	51	4	275	250	209	274	268	63	0	0 268	22 0
11.8525	11.	51	9	275	250	209	274	257	63	0	0 257	22 0
11.85389	11	51.	14	275	250	209	274	257	63	0	0 257	22 0

11.85667	11	51	24	268	250	209	268;	244	66	0	0	244	22 0
11.85806	11	51	29	268	250	209	268	244	67	0.	0	244	22 0
11.85944	11	51	34	263	244,	209	268	244	68.	0;	0,	245	22 0
11.86083	11	51	39	263	244	204	262,	239	70	0 [:]	ō	238	22 0
11.86222	11	51	44	263	244	204'	262	239	71	0	0	238	22 0
11.86361	11	51	49	256	244	204	256	239	72	o	0	238	. 22 0
11.865	11	51	54	256	239	204	256	239	73	0	- o	238	22 0
11.86639	11	51	59	256	239	204	256	242	73	0,		238	22 0
11.86778	11	52	4	256	239	199	256	239	74	0	0	236	22 0
11.86917	11	52	9	251	239	199	250	228	76	0	Ō	228	22 0
11.87056	11	521	14	251	233	199	250	228	78	0		228	22 0
11.87194	11	52	19	244	233	194	243	228.	791	ō		228	22 0
11.87333	11	52'	24	244	233	194	243	228	80	- 5!		228	22 0
11 87472	11	52		244	227	194	243	228	80	···	0	228	~ 22 0
11 87611	11	- 52	34	244	227	194	243	228	81	ň	ŏ	223	22
11.8775		52	39.	238	227	180	243	218		ō		216	
11 87889	11	- 52	44	232	222	189	238	216	85.	ň	- 0	216	22 0
11 88028	11	52		232	222	189	231	213	87	<u>0</u> .	0	200	. 22 0
11 88167	· · · · · · · ·	52	54	226	216	184	225	208		<u>0</u>	0	200	
11.88306	11.	52	- 50	226	216	194	225	200		Å	_0;	203	
11.88444	- · · · · · · · ·	- 52		220	210	104	225	200		Å	<u>.</u>		· <u></u>
11 00502			- 4	221	-211	179	225	208	901	0:.		209	
11 89722	11		14	221	211	170	221	208		<u> </u>		209	· _ · · · · <u>22</u> _ · · · · ·
11.00722		. 55	- 14	221	_ 200		221	200	91	0.	<u>.</u>	209	
11 00	· · · · · · · · · · · · · · · · · · ·	53	19	221	200	170	221	211	91	<u>.</u>	0	209	······································
11 00 120	<u></u>	- 33	24	221	200	- 170 -	- 221	211	- 91	<u> </u>	Š.	209	0
11.03139	11	. 53		221	200	170	221	211		ÿ		209	. 22
11.092/0	<u></u>	- 53		221	200	170	221	211	91	-0		- 212	22 0
11.09417	<u> </u>		. 39	221	- 206	<u> </u>		211	91	Ö	<u>0</u> .	212	
11.895501		- 53	44	221	200	1/3		211	_91	U	Ŷ.	212	22 0
11.89694		53	49.	221	200		221	211	- 91	<u> </u>	<u>0</u> .	- 212	22 0
11.89833	<u></u>	53	54	. 221	200	1/3	. 221	211		0	0	212	22: 0
11.89972				221	200	1/3	221	211	92			_ 212	
11.90111			4	219	200	173	221	211		_0	. 0	. 212	22 0
11.9025		54		219	200	173	218	211	92	0	<u>0</u>	212	22 0
11.90361	11	. 54	13	219	200	173	218	211	92	0	0	212	220
		_ 54	18	219	200	173	218	211	92	0	0	212	220
11.90639	11	54	23j	219	_200	173	218	211	92	0	0	212	22 0
11.90778		54	28	219	200	<u>173</u>	218:	211	92'	. O :	0.	212	22 0
11.90917	11;	54	33	219	200	1 <u>7</u> 3¦	218	211 ₁	92	0 <u>.</u>	<u> </u>	210	0
11.91056	<u>11</u>	54	38	219	200	<u> 171' </u>	218	211	92	0	0	210	. 22 0
11.91194	11	54	43	_219_	200	_171	218	211	92	0	0	210	220
11.91333	11	54	48	219	200	171	218	211	92	0	0	210	220
11.91472	<u>11</u>	54	53		200	171	2 <u>18</u>	211	92	0	0	210	22 0
11.91611	11	54'	58	219	200	<u> 171 </u>	218	211	92	0	0	210	21 2
11.9175	11	<u> </u>	<u> </u>	218	200	171	218	211	92	0	0	<u>210</u>	21. 4
11.91889		55		218	200	171	218	210	92	0	0'	210	217
11.92028	11!	<u> 55 </u>	13	_ 218 _:	200	171	218	210	92	0	0	210	20 8
11.92167	11	55	18	218	200	171	218	210	92;	0	0,	210	20 11
11.92306	. 11	55	23	218 [,]	200	_171	218	210	92	0	0'	210	20: 12
11.92444	11	55	28	218	200	171	218	210	92	0.	0	210	20 15
11.92583	. 11	55	33	218	200	171	218	210	92	0	0	209	19 16
11.92722	11	55	38	218	200	171	218	210	92	0	0	209	19 18
11.92861	11	55	43	218	200	171	218	210	92	0	0	209	19 20
11.93	11	55	48	218	199	171	218	210	92	0	0	209	19 23
11.93139	11	55	53	218	199	171	218	210	92	0	0	209	18 25
11.93278	11	5	58	218	199	171	218	210	92	0	0	209	18 27
11.93417	<u>11</u>	56	3,	217	199	171	218	207	92	0	0	209	18 27
11.93556		56	8	217	199	171	217	207	92	0	0	209	18 26
11.93694	11	56	13	217	<u>199i</u>	_ 171	217	210	92	0	0	209	19 21
11.93833	11	56	18,	217	199	171	217	210	92	0	0	209	19 17
11.93972	11	56	23	217	199	171	217	207	_ 92	0	0	209	20 13
11.94111	11	56	28	217	199	171	217	207	92	0	0,	209	20 8
11.9425	11	56	33	217	199	171	217	207	92	0	. ol	207	21 5
11.94389	11	56	38	217	199	170	217	207	92	0	0	207	21: 1
11.94528	11	56	43	217	199	170	217	207	92	0	0	207	21 1
11.94667	11	56	48	217	200	170	217	210	92	0.	0	207	22 1
11.94806	11	56	53	217	200	170	217	210	92	o í	0	207	22 1
11.94944	11	56	58	217	200	170	217	208	92 [.]	0	0	207	22 1
11.95083	11'	57	3	218	200	170	217	208	92.	0	0	207	22 1
11.95222	11;	57	8	218	200	170	217	208	92	0	0	207	22 1
11.95361	11	57	13	218	200	170	217	208	92	0	0.	207	22 1
11.955	11	57	18	218	200	170	217	208	92	0	0	207	22 1
11.95639	11	57	23	218	200	170	217	208	921	0	0,	207	22 1
11.95778	11	57	28	218	200	170	217	208	92	0	0	207	22 1
11.95917	11	57	33	218	200	170	217	208	92	0		209	22 1
11.96056	11 -	57	38	218	200	170	217	208	92	<u> </u>		209	22 0
11.96194	11	57	43	218	200	170	217	208	92		0:	209	22 0
11.96333	11	57	48.	218	198	170	217	208	92	Ō.		209	22 0
11.96472	11	57	53	218	198	170	217	211	93	0.	0	209	22 0

	11.96611	11	57	58	218	198	170	217	208	93.	0) (0	209	22 0
	44.0075			· · · · · · · ·	010	100	+70			- '00'	• •		··	200	
		· <u>-</u>						<'''.	200	- 93		'. '	0	209	
	11.96889	11	58'	8	218	198	170	217	208	93	() (0	209	22 0
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	11.97028	11	58	13	218	198	170	217	208	93	() (0	209	22 0
	11 07167	11	59	18	219	109	170	217	208		'n	i i	n	200	22 0
	11.57107			- 10 -	210			<u>~</u> '.	200	33.	_ `	' '	•	205	
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	44.07444					100						· .	<u>.</u>	000	an'
	11.97444		58	28	218	198	170	217	208	93		'. '	0	209	22 0
	11 97583	11	58	33	218	198	170	217	208	93	í í) (0	209	21 2
		·						<u> </u>			· · ·]	• •			
	11.97722	11	58	38	218	198	169	217	208	93	() 1	0	209	21 3
	11 07961	11		42	210	100	160		200		~		<u></u>	200	21 6
	11.97001		50	.43_	210	190	109	21/	200	93		· · · ·	U.	209	21. 0
	11.98	11	58	48	218	197	169	217	208	93	() (0	209	20 8
		·			2.00		100	- <u></u>				· -			
	11.98139	11	58	53	218	197	169	217	208	92	() '	0	209	20 10
	11 09270	11	E 0	E0	210	107	160	217	200	02	· r	· · ·	n'	200	20 12
	11.902/0	· - ' <u>-</u>			_ 210	197	109	· · · ·	200.	52.	, i	. '	·	203	
	11.98417	11	59	3	218	197	169	217	208	92	() i	0	209	20 14
- 1							4.00		000	00		· .	· ·	000 ¹	··· · · · ·
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	11.30034	!' 					103	£1/.	200			' . '	•	203	13, 10
	11.98833	11	59	18	218	197	169	217	208	92	() 1	0	209	19 20
	44 00070								- 000				· ·		40.00
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I	11.9925	11	59	33	218	197	169	217	208	92	() 1	0	209	18 27
I	11.00200			20	010	+07	170		200	00.	•	· .	<u>^</u> .	200°	10 07
1	11.99309		59				. 170.	217.	200	32	, c	· · · '	•.	209	10 27
- 1	11 99528	11	59	43	218	197	170	217	208	92	() (0	209	18 27
													<u>,</u>	000	10 05
	11.99667	11	59	48	218	198	170	217	208	92)	0	208	19 25
- [11 99806	11	59	53	211	198	170	210	187	96	0	<u>, </u>	n	187	19 19
	11.00000												~ .	101	15 15
I	11.99944	11	59·	58 [,]	206	198	170	204	187	98	() i	0.	187	20 15
	12 00002	10			100	· - 100	170	204	- 107			с · ·	<u>^</u>	107	20 10
I	12.00083		Y	3	199	192	170	204	18/	- 39	V	· · · · '	v	10%.	10
	12.00222	12	0	8	199	192	164	198	187	100	() (0	187	21 6
											-	· ·	· - · ·		
	12.00361	12	U	13	199	187	164	198	187	101	() 1	0	187	21 2
	12 005	12	0	18	100	197	164	109	180	101	()	∩	187	21 0
- 1	12.005	· · · · · · · · · · · · · · · · · · ·	- ··				104	130	. 103	101		· . ·	· _	107.	<u> </u>
	12.00639	12	0	23·	199	187	160	198	189	101	() 1	0	187	22 0
- 1	10.00770		·· ^·				100	100	100	100		Č.	<u>^</u> .	170	
- 1	12.00778			20	199	10/	160	190	. 180	102	, i	'	0	170	
I	12.00917	12	0	33	186	182	160	192	174	105	() (0	176	22 0
í	10.000	· -:	·									• • •			
	12.01056	12	0	38	186	182	154	186	176	105	0) (0	176	22 0
	12 01104	12		42	196	176	154	- 196	176	105		, , , , , , , , , , , , , , , , , , ,	<u>^</u>	176	່ ວວ່ ດ
-	12.011.34	<u> </u>	· · · · ·				1.34	100	_ 1/2_	102.		·. ·	·	112.	<u> </u>
	12.01333	12	. 0	48	186	176	154	186	174	106	() (0	176	22 0
1	10 01 170											· -	<u> </u>		
1	12.01472		_ U	53	186	1/1	149	181	1/4	106			0	176	22 0
í	12 01611	12	- 0.	58	180	171	149	181	171	107	, in the second s	· ·	ດ່	168	22 0
	12.0.011		_ •			· · - · · ·			'.			· · · ·	•.	100	
	12.0175	12	1	3	180	171	149	181	167	108	() 1	0	168	22 0
	12 01990		·· • ··			100	140	170	107	100		, -· .	A	100	
	12.01009	12		e ⁰ _		100	149	175	. 107	100	, c	, '	U	100	22 0
	12.02028	12	1	13	175	166	144	175	167	108	() (0	168	22 0
ł			- <u> </u>	···											
ļ	12.02167	. 12	1	18	175	166	144	175	167	109	L L) '	0	168	22 0
- 1	12 02306	12	1.		176	166	144	175	167	100	0	· · ·	۸İ	168	່ ວວ່ ດ
-	12.02300	· · · · · · · · · · · · · · · · · · ·	'	20	175		144	. 175	107	109.		'. '	•.	100	. 22 _ 0
	12.02444	12	1	28	175	166	144	175	167	109	0) 4	0	168	22 0
ł	10 00500	10	1.11		175	100		475	107	100	-	÷.	<u> </u>	100	
	12.02565				. 1/5	100:	144	1/5	'0'.	109			0	100	
	12 02722	12	1	38	175	160	144	175	167	109	· · · ·)	0	168	22 0
- 1							- 122					· · ·			
	12.02861	12'	1	43	175	160.	144.	175	167	109	0) (0	168	22 0
	12.03	12	1	49	175	160	144	175	164	100		, i	o	160	
- 1	12.00			···· *••		_ 100.	_ 144		104	103	· ·	' '	<u>.</u>	100	22. 0
1	12.03139	12	1	53	175	160	144	175	167	109	0) (0	168	22 0
i i	10.00070	10								400		•			
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	12 03417	12		3	175	160	130	175	167	100	Ċ	.	ດີ	166	22 0
- 1										103.		·. ·	·	100	
	12.03556	12	2	8	175	160	139	173	167	109) (0	166	22 0
1	12 03604	12	· .	12	170	160	1201	172	167	100	· .	, i	o	166	·
	12.00004		٤				1391	/3.		. 109		'. <u>.</u> '	•:	100	<u> </u>
- 1	12.03833.	12	2	18	172	160	139	173	167	109	0) (0	166	21 3
									111-		-	•	<u> </u>		
	12.03972	12	2	23	1721	160	139	173	164.	109	C	, (U .	166	21 5
1	12 04111	10		29	172	160	- 120		104	. 100	~	, i	A	166	21 7
{	2.04111	<u> </u>			_ '' ~	100	139	173	104.	10.9	L L	· · · ·	·	100	41 /
- 1	12.0425	12	2	33	172	157	139	173	164	109	0) (0	166	21 9
í	12 04200			20	170	457	100		-		-		o [.]	100	
	12.04389	12	Z	38	1/2	15/	_139	1/3	164	109	_ C		v.	166	20 11
I	12.04528	12	2	43	172	157	130	172	16/	100	~	,	0 [`]	166	20 12
ļ.	10.01020		<u> </u>					1/3	. 104	103	L L	'	.		
	12.04667	12	2	48	172	157	139	173	164	109	0) (0	166	20 15
ſ	12 04922			E.A.	170	157	120	170	104	- 100	_		· · · ·	160	
	12.04000		<u> </u>		_ 14		139	173.	104.	109	U	<u>.</u>	<u> </u>	100	
	12.04972	12	21	59!	172	157	136.	173	164	109	C		0	162	19 19
ŀ	10.05111	— ·;;;·· —		— ř. i - –							·	··`	· — –		
I	12.05111	12	3	4'	1/2	157	136	173	164	109	C		V	162	19 21
1	12 0525	12	3	9	172	157	136	171	16/	100	· · ·	· - · · -	0 ^{, .}	162	10 22
1			·				100				·	· '	.		
	12.05389	12;	3	14	170	157	136	171	164	109	C). (0	162:	19 25
ŀ	12 05529	10			170	1.57	100	+	100	100	7	·	<u>م</u>	160	
ļ.	12.00020		J			!?/	130		104	. 109	. · ·	· '	~.	102	19 27
	12.05667	12	3	24	170	157	136	171	165	109	C) (0	162	18 29
ł	12 05900							220			2	·	<u>.</u>	100	
	12.05806	12:	3	291	170	157	136	171	165	109	c	n – I	v	162	18 29
1	12.05944	12	3	34	170	157	136	171	165	100	r) '	0	162	19 27
	10.000 44					· · · · · · · · · · · · · · · · · · ·		'_'-		103	L.		<u> </u>		
- 1	12.06083	12	3,	39	170	157	136	171	165	109	c		υ	162	20 21
l l	12 06202	10	2		170	167	120	171	100	100		i .	n'	160	20 10
l.					_1/U_L_	!>/!	130		105	109			v	102	
	12.06361	12	3	49	170	157	136	171	165	109	ſ) (0	162	20 10
ŀ	10 005		<u> </u>							100	-	· ·	<u>,</u>	100	
I	12.005		<u> </u>	54	. 170	15/	130	1/1	165	109		(v	102	4
- (12.06639	12.	3	59	170	157	135	171	165	100	···· .		0	165	21 1
· •	10.000		<u> </u>					!!!-			· · ·· ·				
I	12.06778	12	4	4 i	170	157.	135	171	165'	109	C		υ	165	22 0
	12 06917	12	_ ·	a	170	157	135	170	160	100	• • •		n	165	
ļ.	12.00317			<u> </u>				1/2		109	U	· · · · · · ·	·	105	0
	12.07056	12	4	14	171	157	135	172	165	109	C) (0 -	165	22 0
ł	10 07101		··										·		
Į	12.0/194	12	4	19	171	15/	135	172	165	109	_ C	. (v	165	22 0
ľ	12.07333	12	4	24	171	157	135	172	165	100			0	165	22 0
1	10.07.000]								· · _ · · ·	'	<u>.</u>		
	12117472	12	4.	20-	171	157	125.	172	165	100	C			166	<u>۸</u> רני

12.07611	12	4	34	171	157	135	172:	165	109	0	0	165	2	2 0
12 0775	12		39	171	157	135	172	165	109		<u> </u>	165		2 0
12 07890	12			171	157	125	- 172	105	100		<u>~</u> .	105		<u> </u>
12.07003					157	135	172	105	109			105		2
12.00020		. 4.	49		157	135	172	163	109		_0!	165	2	2 0
12.08167	- 12		54			135	172	163	109	0	<u> </u>	165	2	1 2
12.08306	<u>12</u>	4.	59	_171	157	137	172	163	109	<u> </u>		161.	2	<u>1 </u>
12.08444	12	5	4	171	157	137	172	163	109	0	0:	161	2	16
12.08583	12	5	9	171	157	137	170	166	109	0	0	161	2	1 7
12.08722	12	5	14	171	157	137	170	163	109	0,	0	161	2	1 9
12.08861	12	5	19	171	157	137	170	163	109	0	0	161	20	0 11
12.09	12	5	24	171	157	137	170	163	109	<u> </u>	<u> </u>	161		13
12 09139	12			171	157	127	170	- 162 -	100		Å.	161		
12.03133	12	_ <u>_</u>	24	171		107	170	-103	109		<u> </u>			
12.09276	_ 12	5.	34	<u>1/1</u> .	156	13/	1/0	166	109.	0	<u>0</u>	161	21	2
12.09417	12	<u>5</u>	39	171	156	137	170	163	109	0	_0	161	19	<u>9 19</u>
12.09556	12	_5	44;	171:	156	137	170	163	109	0	0	161	19	9 _ 21
12.09694	12	5	49	171	156	137	170	163	109	0	0	161	19	9 22
12.09833	12	5	54	171	156	137	170	163	109	— <u>-</u>	0	161	19	25
12.09972	12	5	59	171	156	134	170	163	109	0 -	0	165	19	26
12,10083	12	6		171	156	134	170	163	109		0	165	1/	28
12 10222	12		я. Я	171	156	134	170	163	100		<u>.</u>	165	19	
12 10261				170	150		170	160	- 103		~ ···	105		<u></u>
12.10301	12		13	170	150	134	170	103	109		<u>v</u>	105		29
12.105		0.	18		- 150	134	- 170	100	109		0			<u> </u>
12.10639	12	<u> </u>	23	170	156	134	170	159	109	0	0		- 19	<u></u> . 20
12.10778	12	6	28	145	156	134	150	124	117	0	0	120	20	2 14
12.10917	12	6	33	127	145	128	127	118	118	0	0	120	21	1. 10
12.11056	12	6	38	127	137	117	127	118	118	0	0	120	21	1 3
12.11194	12	6	43	127	130	117	127	118	118	0	o	120	22	2 0
12.11333	12	6	48	121	125	112	122	111	119	0	0	108	22	2 <u>.</u> .
12,11472	12	6	53	115	119	106	116	108	120	0	0	108	- 22	n
12 11611	12	- <u>-</u>	58	115	113	106	110	108	120	ů.	0	108		<u>,</u> ,
12 1175	12	- 7		116	112	101	110	100	120		õ.	100	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	<u>,</u> ,
10 11000	- 12	<u></u>		115		101	110	105	120		<u>.</u>	100		
12.11889	12	<u>′</u> .	. 8	115	107	101	110	105	120	0	0	105	. 22	<u> </u>
12.12028	12		13	115	. 107	101	110	107	120	0 _.	0 _.	105		2 _ 0
12.12167		7.	18	115	107	101	110	107	120	<u>0</u>	0	105	22	2
12.12306	12	7	23	115	107	96 i	110	107	120	_ 0:	0	105	22	2 0
12.12444	12	7	28	115	107	96	110'	107	120	0	0	105	22	2 0
12.12583	12	7	33	115	107	96	110	104	120	o	0 [`]	105	22	2 0
12.12722	12		38	115	102	96	110	104	120	0	o .	105	22	2
12 12861	12	7	43	109	102	96	110	104	120	<u> </u>	0	105	22	5 ñl
12 13	12		48	100	102	06	110	104	120	õ.	õ	105		
12 12120	12	···,	60	100	102		110	104	120	0.	· ·	105		
12.13133		<u>-</u>		109	102	90		104	120	0.	<u>.</u>	105	22	୍ ଧ
12.13278				-109	. 102	96		108	120		0	105	4	<u>- 4</u>
12.13417	12	8!	. 3!	109	102	. 96	113	108	120	Oļ j	0 <u>'</u>	105		2 0
12.13556	12	8		109	102	96	113	108 ₎	120	0	0	106	22	20
12.13694	12	8	13	109	102	96	113	105	_120	0	0	106	22	20
12.13833	12	8	18	109	102	96	113	105	120	0	0	106	22	2 0
12.13972	12	8	23	109	102	96	113	105	120	0	0	106	22	2 0
12.14111	12	8	28	109	102	96	["] 113 ["]	105	120	0	0	106	22	2 0
12.1425	12	8	33 -	109	102	96	113	105	120	0	0	106	22	s: <u>-</u>
12.14389	12	8	38	109	102	96	113	108	120		۰ ۱	106	. 22	
12 14528	12	- <u>-</u>	13 -	112	102	06	112	100	120		<u>.</u>	106		; ·· · ·· ··
12 14667	·· <u>· -</u>			110	102	50		100	120		<u>~</u>	100		는 쉬
12.1400/		<u>°</u> .	····*	112	102	90		100	120		<u> </u>	100		
12.14806	12	ð.	53.	112	102	96		108	_ 119	_ <u>0</u> :	<u>v</u>	106	- 22	·4
12.14944	12	<u>8</u> .	_ 58,	112	102	. 96		108	119	_ U_	<u>о</u>	106	21	6
12.15083	12	- 9	3	112	102	96	114	108	119	0	0	106	21	. 8
12.15222	12	9	8	112	102	. 96	114_	108	119	_0	0	<u>108</u>	21	10
12.15361	12	9.	13	112	102	96	114	108	119	0 ₁	0	108	21	11
12.155	12	9	_ 18 _	112	102	96	114	108	119.	0	0	108	21	14
12.15639	12	9	23	112	102	95	114	108	119	0	0	108	21	15
12.15778	12	9	28	112	102	95	114	108	119	° O'	0	108	21	17
12.15917	12'	9.	33	112	102	95	114	108	119	- oi	0	108	20	18
12.16056	12	9	38	112	102	95	114	106	119	0	0	108		
12.16778	12	10	<u> </u>	112	102	95	112	106	119		0.1	108		
12 16917	12	10		112	102	05	112	106	110	ŏ.	0	100	10	
12 17054	12	10		110	102	90 05	112	100	_ 110		0	100	- 19	<u> </u>
12.17050	- 12	10		112	102	92	-112	106	119	U O	V	108	- 19	
12.17194	-14	10	19	112	102	95	112	106	119	U:	U.	108	19	. <u>32</u>
12.1/333	12:	10	24	112	102	94	112	106	119	0 _.	0	108	19	32
12.17444	12	10	28	112	102	94	112	106	_119_	0	0	108	19	32
12.17583.	12	10	33	112	102	94	112	106	119	0	0	108	19	. 32
12.17722	12	10	38	112	102	94	112	107	119	0	0	108	19	32
12.17861	12	10	43	112	102	94	112	107	119	0	0	108	19	32
12.18	12	10	48	112	102	94	112	107	119	o – –	0	108	19	32
12,18139	12	10	53	112	102	94	112	107	120	0	0	108	- 19	32
12 18278	12	10	- 58 -	112	102	94	111	107	120		0	108		
12 19417	10	11		112	102	04		107	120	<u>ŏ</u>	<u>~</u>	100	19	
12.10417			. 3	112			!!!	107	- 120.	<u> </u>	<u> </u>	100	19	
12.10550		븠	<u>8</u>	- 112	102			107	120	v	v	107	. 19	
12.18694	12		13	112	102	94		107	120	0	0	107		32
12.18833	12	11	18	112	. 102	94	111	107	120	0	0	107	19	32
12.18972	12	11	23.	112	102	93	111	107	120	0	0	107	10	a 32

12.19111	12	11	28	112	102	93	111	107	120	0.	0	107	19	32
12.1925	12	11	33	112	102	93	111	107	120	0	0	107	19	32
12.19389	12	11	38	112	103	93	111	105	_120	0	0	107	19	32
12.19528	12	11	43	112	103	93	111	109	119	. <u>0</u> ,		107	<u> 19 </u>	32
12.19667	12		48	112	103	93:	111	109	119	0	0	107	19	32
12.19806	12		53		103	93	111	109	119		0	107	19	- 32
12.19944	- 12	12	20	112	103	93	113	106	119		0	107	19	32
12.20222	12	12	8	112	103	93	113	106	119		0	108	i 19	
12.20361	12	12	13	112	103	93	113	106	119	0	0	108	19	32
12.205	12	12	18	112	103	93	113	106		0	0	108	19	31
12.20639	12	12	23	112	103	92	113	106	119		0	108	19	29
12.20778	12	12	28	112	103	92	113	106	119	0	0	108	19	25
12.20917	12	12	_33	112	103		113	106	119		0	108	20	18
12.21056	12	12	38		103	92	<u>113</u>	106	. 119	0-	0	108	$\frac{21}{21}$	
12.21194	12	12	431	113	103	92	113	106	120	·	^	108	21	····
12 21 472	12	12	<u>48</u> 52	112	103	- 32	113	- 106	120	- 0		105	22	- <u></u>
12,21611	12	- 12	58	113	103	92	112	106	120	· · · · · · · · · · · · · · · · · · ·	· o	108	3 22	····· 0
12,2175	12	13.	3	113	103	92	112	106	120	- <u> </u>		108	22	0
12.21889	12	13	8	113	103	92	112	106	120	0	0	107	22	0
12.22028	12	13	13	113	103	92	112	106	120	0	0	107	22	
12.22167	12	13	18	113	103	92'	112	106	120	0	0	107	22	Ō
12.22306	12	13	23	113	_ 103	92	112	106	120	<u>0</u>	0	107	22	
12.22444	12	13	28		103	92	112	106	120	<u>0</u>	0	107		
12.22583	12		33	113	103	92.	112	106	120	U Oİ	0	107	22	. 0
12 22861	12	13	38	113	102		112	106	120	- 0'		107		· – 0
12 23	12	13	48	112	102	92	112	106	120	ö. –	···	107	22	··· 0
12.23139	12	13	53'	112	102	92	112	106	120	0. ·	0	107	22:	· · ĭ
12.23278	12	13	58	112	102	92	114	107	120	0 -	0	107	22	2
12.23417	12	14	3	112	102	92	114;	107	120	0	0	107	22	4
12.23556	12	14	8	112	102	92	114	107	120	0	0	108	321	6
12.23694	12	14	13	112	102	92	. 114	107			0	108	321	
12.23833	12 -	14	18	112	102'	92'	- 114	107	120	· · · · 0'.	·	108	21	
12.23972	12.	14	23	112	102	95	114	107	120			108	21	11
12.24111	12	14:	20	112	102	<u>95</u>	114	107	120	- 0	<u>0</u>	108	21 ··· · <u>41:</u> 21	
12 24389	12		38	112	101	95	114	107	120	0 0	0	108	21	16
12.24528	12	14	43	113	101	95	114	107	120	0_	0	108	3 21	18
12.24667	12	14	48	113	101	95	114	107	120	0	0	108	20	20
12.24806	12	14	53	113	101	95	109	107	120	0	0	108	3 20	22
12.24944	12	14	58	113	101	95	109	106	120	0	0	108	3 20	23
12.25083	12	15	3	113	101	95	109	106	120	- 0	- 0	108	<u>3i 20</u>	25
12.25222	12	15,	8j	113	101	95	109	_106	120	0	<u> </u>	104	20	
12.20301	12	15	- 13	- 113	101	95	109	106	120	0		104	· · · · · · · · · · · · · · · · · · ·	29
12 25639	12	15	23	113	101	92	109		120	0		104	· <u>20</u> 1. 19	
12.25778	12	15	28	113	101	- 92	109	106	120	0	· ··õ	104	19	32
12.25917	12	15	33	113	101	92	109	106	120	0	0	104	<u>19</u>	32
12.26056	12	15	38	113	101	92	109	106	120	0	i	104	19	32
12.26194	12	15	43	111	101	92	109	106	120	0	0	104	19	32
12.263331	12	15	48	111	101	92	109	106	120	0	0		19	32
12.26472		15	53	111	101		112	106	120	0:	0		19	. 32
12.26611	12	15	58	111	- 1011	92	112:	107	120	ů.	0	-104	19	32
12 26880	<u>12</u>	⁰¹	. <u>3</u>	$-\frac{111}{111} -$	101	- <u>92</u>	112	107	120	U n	-0	104	19 19	32
12.27028	12	16	13 -	111	101	92	112	107	120	ō	- 0	106	<u>. </u>	32
12.27167	12	16.	18	111	101	92	112	107	120	ů.	ŏ	106	5 19	32
12.27306	12	16	23	111	101	92	112	107	120	0	0	106	519	32
12.27444	12	16	28	111	101	92	112	107	120	0		100	6 19	32
12.27611	12	16	34	111	101	92	112	107	120	0	. <u>. 0</u>	100	5 19	32
12.2775	12'	16		113	102	92	112	107	120	<u> </u>	0	106	5 19	
12.27889	<u>12</u>	16	44	113	102	- 92	112	107	120	0	0	106	<u>. 19</u>	32
12.28028	12	16	49	113	102	92	112	107	120	0		· 106	<u>-</u> 19	
12 28306	12	16	- 54	113	102	92	112	107	120	0	^	100	, 19 , 10	
12.28444	- 12	17'	4	113	102	92	113	105	120		. 0	106	19	32
12.28583	12	17		113	102	92	113	105	120	· 0	· 0	106	5 19	32
12.28722	12	17	14	113	102	92.	113	105	120	0	0	106	5 19	32
12.28861	12	17	19	113	102	92	113	105	120	0	Ō	106	<u>19</u>	32
12.29	121	17	24	113	102	91	113	105	120	0	0	10€	6 19	32
12.29139	121	17	29	113	102	91	113	105	120		0	106	i 19	32
12.29278	12	··· <u>17</u>	34.	113	102	91	113	105	_ 120	<u>_0</u>	0	106	5 19	32
12.29417	12	17	39		100	91	113	105	120	0		106) <u>19</u>	31
12.29556	12	17	44			91	112	105	120	<u>.</u>		106	5. <u>.</u>	20
12 29833	12	<u> </u>		111	100	01	112	105	120	v	· · _ 0	10/	20	22
12.29972	12	17	59	117	- 100		118	143	118	 0		129	21	<u>10</u>
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12.30111	12	18	_ 4!	160	105	99	160	160	111	0	0 159	21 4
12.3025		18			$-\frac{123}{121}$	106	160	160		. 0	0:	22 1
12.30528	12	18	19	166	136	117	166	160	· <u> </u>	· · · · · ·	0 159	22 1
12.30667	12	18	24	166	136	122	166	160	111		0 160	22 1
12.30806	12	18	29	166	142	122	166	164	109	0	0 166	
12.30944	12	18	34	171	148	127	166	164	109	01	0 1 <u>66</u>	1
12.31083	. 12	. <u>18</u>		171	148	127	<u>- 166</u> -	164	109	0 ₁	0 166	
12.31222	12	18	44	171	148	127	172	164	109		0 166	-22
12.315	12	18		171	153	127	172	164	109	0 ·	0 166	22 1
12.31639	12	18	59	171	153	132	172	164	109	0	0 166	22 1
12.31778	12	19	4.	171	153	132	172	164	109	0	0 166	22 1
12.31917	12	. 19	9	171	153	132	172	164	109	0	0 166	22 0
12.32050	- 12	19	14	171	153	132	172	164	109	- 0	0 166	22
12.32333	12	19	24	171	153	132	172	164	109	0	0: 166	22 0
12.32472	12	19	29	171	153	132	172	164	109	0	0 164	22 0
12.32611	12	19	34	172	153	132	172	164	109	0	0 164	22 0
12.3275	12	19	<u>39</u> i _	- 172 -	153	132	$\frac{172}{172}$	164	_109	0	0 164	
12.32889	12	19	44	172	156	132	172	- 164	109	0	0 164	22 0
12.33167	12	19	54.	172	156	132	172	164	109	0	0 164	22 0
12.33306	12	19 ¹	59	172	156	135	172	164	109	0	01 <u>64</u>	22 0
12.33444	12	20	4	172	156	135	172	164	109¦	0	0 164	0
12.33583	12	. 20	9,.	172	156	135	172	164	109	0	0 164	22 0
12.33722	12	20 <u>1.</u> 20	14	_ <u>1/2</u> _	156	135	172	164	1091 -	0	0 <u>164</u>	22 0
12.34	12	20	24	172	156	135	172	164	109		0 164	21 4
12.34139	12	20	29	172	156	135	172	164	109	0	0 164	21 6
12.34278	12	20	34	173	156	135	172	164	109	0	0 164	21 8
12.34417	. 12.	. 20		173	156	135		164	_ 109.	0	0 <u>164</u>	$-\frac{21}{10}$
12.34556	12	. 20	44	173	155	135	169	164	109	<u>0</u>	0 164	$\frac{20}{20}$ $\frac{12}{14}$
12.34833	12	20	49 54	173	157	135	169	167	109	·	0 164	20 15
12.34972	12	20	59	173	157	135	169	164	108	0	0 164	20 18
12.35111	12	21	4	173	157	135	169	164	108	0	0 164	19 19
12.3525	_ 12	21	. 9.	173	157	135	169	164	108	0	0 164	19 22
12.35389	12	. 21	<u>14;</u>	173	157	135	169	164	108		$\frac{0!}{164!}$	
12.35528	12	21	- 19:	173	157	135	169	164	108		0 164	19 25
12.35806	12	21	29	173	157	135	169	164	108	0	0 164	18 29
12.35944	12	21	34	172	157	135	169	164	108	0	0 164	18 29
12.36083	12	21	39	172	157	135;	169	164	108	0	0 164	18
12.36222	12	21	44.	172	157	135		164	108		0 164	
12.365	12	21	- 49.	172	157	135	171	164	108	. 0	0 164	20 15
12.36639	12	21	59	172	157	134	171	165	109	0	0 164	21 9
12.36778	12	22	4	172	157	134	171	165	109	0	0 164	21 6
12.36917	12	22	9	172	157	134	171	165	109	0	0 164	22 1
12.37056	12	22.	- 14	172	157	134	171	165	109		0 164	1
12.37194	12	22	24	172	157	134	171	165	109	0 .	0 164	$\frac{22}{22}$ $\frac{1}{1}$
12.37472	12	22	29	172	157	134	171:	165	109	- oj	0 165	22 1
12.37583	12	22	33	171		134	171	165	109	0	0 165	1
12.37722		221	38	171	157	134	171	165	109	0	0 165	22 1
12.37861	12	22	43	1/1	157	134	173	165	109		U: 165	22 1
12.38167	12	22		171 -	158	134	173	165	109	0	0 165	22
12.38306	12	22	59	171	158	134	173	167	109	0	0165	1
12.38444	12	23	4	171	158	134	173	167	109	0	0 165	22 1
12.38556	12	23	8	171	158	134	173	167	109		0: 165	
12.38694	12	23	13	171	158	134	173	167	109		U 165	22 0
12.38972	- 12	23		171	158	134	173	167	109		0 165	22 0
12.39111	12	23	28	171	158	134	173	167	109	0	0 165	22 0
12.3925	12	23	33	172	158	134	173	167	109		0 165	22 0
12.39389		23		172	158	_ 134	173	167	109	0	0. 165	22 0
12.39528	- 12	23	43!	172	158	134	172	164	109	<u>vi</u>	0 165	- 22 0
12.39806	12	23	53	172	158	134	172	164	109		0 165	22 0
12.39944	12	23	58	172	158	134	172	164	109	0	0 165	22 - 0
12.40083	12	24	3	172	158	134	172	164	109		0 165	220
12.40222	12	24	8	172	158	134	172	164	109	0;	0 165	22 0
12.40361	12	24	13	172	158	134	172	164	109	0	0 165	
12.405	12	24	23	172	158	134	172	164	109		0: 165	
12.40778	12	24	28	172	158	134	172	167	109	0	0 166	22 0
12,40917	12	24	33	172	158	134	172	167	109	0	0 166	22, 0

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12 41056	12	24.	38	172	158	134	172	167	109	0	0	166	22	0
12 41194	12	24	43	172	158	134	174	167	109	·		166	22	·
12 41333	12			172	150	134	174	167	100	··· õ. ·	· · č	166	21	
12.41333	12		40	. 1/2	- 159	134	1/4			· <u>v</u> .	, v	100	- 21	
12.41472	12	24	53	1/2	159	134	. 174	167	109	<u>.</u> 0	U.	100	21	5
12.41611	12	24	58	172	<u>159</u> !	137	174	167	108	.0	_0_	166	21	6
12.4175	12	25'	3!	172	159	137 ₁	174	167	108	0.	0	166	21	9
12.41889	12	25	8	172	159	137	174.	167	108	0	0	166	20	 10
12 42028	12	25	13	172	159	137	174	167	108	0	0	166	20	
12 42167	12	25	18	172	150	137	174	167	109	··· õ.		166	20	14
12.42107		-25-		- 172	1.53			107	100	<u>.</u>		100	20	
12.42306	12		23!		159		1/4	16/	. 108		0	166	20	16
12.42444	12	25	281	172	159	137	174	167	108	0	0	166	20	18
12.42583	12	25	33	174	159:	137	174	167	108	0	0	166	19	20
12.42722	12	25	38	174.	159	137	174	167	108	. o	o	166	19	22
12 42861	12	25	43	174	159	137	173	167	108		0	166	19	24
10 42					150		170	107	100			100	10	
12.43		25	40	174	- 159	137	1/3	10/	_ 108					20
12.43139	12		53	174'	159	137	173	167	108	<u> </u>		166	. 18	. 28
12.43278	12	25	58	174	159	137	173	167	108	0	. 0	166	18	29
12.43417	12	26 ¹	3	174	159	138	173	167	108	0	0	166	18	30
12.43556	12	26	8	174	159	138	173	167	108	o	o	166	18	31
12 43694	12	26	13	174	159	138	173	167	108	· •		166	18	31
12 43933	12	-26		174	150	120	172		100			166	10	30
12.40000	10					100	175	- 107	. 100.	· · ·	· ·	100	10	52
12.43972			23		129	_ 138		16/	108	0.		100	_18	30
12.44111	12	26	28	_ 174	159	138	173	164	108	_ 0 <u>.</u> .	0		19	25
12.4425	12	26	33!	174	159	138	173	164	108	0	0	164	19	19
12.44389	12	26	38	173	159;	138	173	167	108,	o	0	164	20	15
12.44528	12	26	43	173	159.	138	172	167	108	0	0	164	21	8
12 44667	12	26	48	173	158	138	172	167	108	- 0		164	21	4
12 44906		26	52	- 1731 -	150	120	170	- 162 -	100		·	164	21	· 7
12.44800					_ 150	1.30			108		· ·	104	22.	!!
12.44944	12	26	58	173	158	138	172	163	109	_0	0 _.	164	22	1
12.45083	12		3	173	158	134	172	163	109	0	0	164	. 22	1
12.45222	12	27	8	173 ⁱ	158	134	172	166	109	0.	0.	164	22	1
12.45361	12	27	13	173	158	134	172	166	109	0.	o	164	22	- 1
12.45528	12	27	19	173.	158	134	172	166	109		0	164	22	1
12 45667	12	27		172	159	124	172	166	100	ů.	Ň.	160	·	
12.45007				- :/	150				105			103		
12.45806	12	2/	29	181	158	134	187	199	103	0	<u> </u>	199	22	1
12.45944	12	27	34	195 ₁	164	140	195	. 199	100	.0	_ 0 _	199	22	1
12.46083i	12'	27	39	195	170	140	195.	199	99	0	0	199	22	1
12.46222	12	27	44	202	170	146	202	199	98.	0	0	199	22	1
12.46361	12,	27	49	202.	176.	151.	202	199	98	0	0	199	22	1
12 465	12	27	54	202	176	151	202	199	98	·	· · .	198	22	·· .
12 46620		27	50	- 202	101				- 50					
12.40033	12			202		151				·	·	. 209		
12.46778	12		4	_209!	181	157	208_	211	94	0	. 0	209	22	0
12.46917	12 _!	28	9:	209	188	<u>157</u>	208	211	93	.0	_ 0.	209	22	0
12.47056	12	28	14	215	188	157	215	211	931	0.	0	209	22	0
12.47194	12	28	19	215	193	162	215	211	93	0	0	209	22	Ó
12.47333	12	28	24	215	193	162	215	211	93	0	<u> </u>	209	22	· · · · · · · · · · · · · · · · · · ·
12 47472	12.	28	29	215	193	162	215	208	93	. <u>.</u>		210		
10 47611					100	- 102		200					22	0
12.47011				_215	193		215	210	91		<u>v</u> .	216	22	- 0
12.4775		28		_ 220	_ 198	162'	220	216	. 91	0	0	216	22	. 0
12.47889	12	28	44	220	198	168	220	216	90	0!	0	216	22	0
12.48028	12	28	49	220	198	168	220.	216	90	0	0	216	22	ō
12.48167	12	28	54	220.	198	168	220	216	90	0	. 0	216	22	
12 48306	12 -	28	59:	220	198	168	220	216	90	0		216	22	· · · ol
12 48444	12	201		220	109	1691	- 220	216	00	<u></u>	· · · ·	216	22	
10.40500			··			00		410		Š.		210	22	· · · ·
12.40583	12	<u>- 29</u> ;	· · · <u>A</u> i ·	220	203	108	220	216	90	U.	U.	216	22	. 0
12.48/22	12	-29	14	220	203	173	220	216	90	0	0	216	22	0
12.48861	12'	<u>29</u> !	19!	220	203	173	220 ₁	216	90	0	0	216	22	0
12.49	12	29	24	220	203,	173	220	213	90	0	0	216	22	Ö
12.49139	12'	29	29	220	203	173	220	213	90	0	0	216	22	0
12.49278	12	29	34	220	203	173	220	213	90	- <u>.</u> .	0	215		· · ·
12 49417	12	20	30	223	203	172	202	213		·~!		215	- 20	
12 40556	12	20		222	202	172					~ ~		5	- 2
12.45550		-23		_223	200		223	213	- 50	<u>v</u>	<u>,</u>			
12.49094	12	291	491	223	203	1/3	223	216	90	υ	·0.	215	22	0
12.49833	12	29	54	223	203	173	223	216	90	0.	0	215	22	0
12.49972	12	_29	59	223	203	173	223	216	89	_ 0	0	215	22	0
12.50111	121	30	4	223	203	173;	223	216	89	_ o.		215	22	o
12.5025	12	30	91	223	204	173.	223	216	89	0	0	215	22	-··· ^.
12,50389	12	30	14	223	204	174	223	216	80	0	····	215	22	
12 50528	12	30	10	222		174		216		,	· X	215		
10 50007	14				204		223	210			<u>}</u>	_215	22	v
12.50667	12	30		223	204	174	_223	216	89	0	0'	215	_ 22	0
12.50806	12	30'	29	223	204	174	223	216	89	0	0	215	22	0
12.50944	12	30	341	223	204	174	223	216	89	0	0	214	22	0
12.51083	12	30	39	224	204	174	223	216	89	0		214	22	· n
12.51222	12	30	44	224	204	174	- 222	216	- 80		ñ	214	22	
12 51261	10	- 20				 174 -				· · ·		214		
12.51301	12	30			204	<u>!/4</u>			69		- · <u>-</u> · <u>·</u>	214	22	
12.515	12	30	54	224	204	174	223;	215	89!	0	0 _i	214	22 _:	0
12.51639	12	30	<u> </u>	224	204	174	223	215		0	0'	214	22	0
12.51778	12	31	4	224	204	174	223	215	89	0	0	214	22	0
12.51917	12	31	9	224.	204	174	223	215	89	0	o	214	22	- · · ō

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12.52056	12	31	14	224	204	174,	223	215	89,	0	0	214	22	0
12.52194	12	31	19	224	204	174	223	215	89	0	0	214	22	0
12.52333	12	31	24	224	204	174	223	215	89	0	0	214	22	0
12.52472	12	31	29	224	204	174	223	215	. 89	0,	<u>. 0</u> :	214	22	
12.52611	12	31	34	224	204	174	223	215	89	0		214:	22	<u></u>
12.52/5	12		39	224	204	1/4	223	215	89			214	22	
12 53028	12	31	44	224	204	174		215	801			214	22	
12.53167	12	31	54	224	204	174	223	215	89		- 0	214	21	5
12.53306	12	31	59	224	204	174	223	215	89	<u> </u>		214	21	7
12.53444	12	32	4;	224	204	174	223	215	89	0	0;	214	20,	9
12.53583	12	321	9	224	203	174	223	215	89	0	0	214	20	11
12.53694	12	32	13	224	203	173:	223	215	_ 89	0	0	214	20	13
12.53833		321	18	224	203	173	223	_215	89	0	<u> </u>	214	19	15
12.53972	12:	32	23	224	203	173	223	215	<u> </u>	0		214		17
12.54111	12.	32	28	224	203	$-\frac{173}{170}$	223	215	89		- 0	214	19	- 19
12 54380	12	- 32		224	203	- 173	223	215	89	<u> </u>		215	19	- 22
12 54528	12	32	43	222	203	173	222	215	89:		<u> - - </u>	215	18	26
12.54667	12	32	48	222	203	173	222	215	89			215	18	27
12.54806	12	32	53	222	203	173	222	215	89	0		215	18	26
12.54944	12	32	58	222,	203	173	222	212	89	0	0	215	19	23
12.55083	12	33	3,	222	203	173	222	212	89	0	0	215	19	19
12.55222	12		8	222	204	173	222	212	89	0	0	215 ₁	20	14
12.55361	12	33	13	222	204	174	222	212	89	0	0	215		11
12.555	12	- 33	18	222	204	174:	222	215	. 89	0	0	215	20!	6
12.55639	12	33	23	222	- 204	174	222	215			0'	215	- 21	2
12.55017	12	33	28	222	204	1/4	222	215				215	21:	-귀
12.56056	12	33	38	223	204	174:		215	89		- ~	214		¦
12.56194	12	33	43	223	204	174	224	215	89		_ <u>₀</u>	214		- · 1
12.56333	12	33	48	223	204	174	224	215	89	0	0	214	22	1
12.56472	12	33	53	223	204	174	224	215	89		0	214	22	1
12.56611	12	33	58	223	204	174	224	215	89	0	0	214	22	1
12.5675	12	34	3	223	204	174	224	215	89	O	<u> </u>	214	22	1
12.56889	12	34		223	203	174	224	215	89	0¦		214	22	- !
12.57028	12	34		223	203	172		212	- 89			214	22!	
12.57306	12	34	23	223	203	172	224	215	801		- 10	214	21	
12.57444	12	34	28	223	203	172	224	215	89		01	214	21	- 5
12.57583	12	34	33	223	203	172	224	215	89	0	· ·	215	21	
12.57722	12	34	38	223	203	172	224	215	89	0,	0	215	20'	9
12.57861	12	34	43	223	203	172	224	215	89	0	0	215	20	11
12.58	12	34	48	223	203	172	224	215	89 j	0		215	20	14
12.58139	12	. 34	53	223	203	<u>172</u>	_ 224	215	_ 89	0'		215		15
12.58278	12			223	203	172	224	215	89		0;	215	191	18
12 58556	12	35 -		223	- 203	- 172	224	215			<u> </u>	215		20
12.58694	12	35		223	- 204	174	224	- 215	89	0:	- 0	215	18	~ 24
12.58833	12	35	18	223	204	174	224	213	89		ŏ	215	18	26
12.58972	12	35	23	223	204	174	224	213	89	0 [°]	0	215.	18	26
12.59111	12	35	28	223	204	174	224	216	87	0	0	189	19	25
12.5925	12	35	33	250	204	174	252	71	72	0	0	74	19	22
12.59389	12		38	261	211	179	258	71	67	0,	0	74	19	19
12.59528	12		43	267	225	187'	265	62	64	0 ₁	0	67	20;	15
12.59806	12	35	40	273	236	192	2/2	. 64	61	···· 0'	- <u>U</u>	<u>60</u>	- 20	- 12
12.59944	121	35.	58	273	236	198	277	61	61	. 01	0	60	21	
12.60083	12	36	3	273	243	198	277	60	60	· <u>0</u> ,	·· ŏ	60	21	3
12.60222	12:	36	_8	273	243	204	277	60	60	0	0	60	21	1
12.60361	12	36	13	273	249	204	277	63	60	0	0	60	21	1
12.605	12'	36	18	273	249	204	277	60	60	0	0	60	21	1
12.60639	12	36	23	279	249	204	277	58	59:	0		60	22	1
12.60806	- 12	36	29		254			. 57	_ 59:	0'	0	54		!
12.60944	12		- 34	279	254	209	2//	63	59	;	- 0	57	<u>22</u>	—¦[
12 61222	12	36	44	279	254	209	277	66	59	···· 0	0	64	22	- 1
12.61361	12	36	49	279	254	209	277	63	59	0	· ·· · <mark>o</mark> · · <u> </u> ·	64	22	;
12.615	12	36	54	279	254	209	283	63	59	0	0	64	22	1
12.61639	12	36	59	279	254	209	283	58	59	0	0	58	22	_ 1]
12.61778	12	37	4	279	254	209	283	62	59	0.	0	58	22	1
12.61917	12	37	9	279	254	209	283	62	59	0	00	58	22	0
12.62056	12:	37	14	279	254	209	283	63	59	0:		65	22	
12.62194	12	37	19	2/9	254	209	283				U	- 59	22	
12.02333	12	3/	24	280	254	209	283	. 59	<u>59</u>	<u> </u>	,	59	22	%
12.62611	12	37	34	280	256	212	203	56	58	0		59	22	尚
12.6275	12	37'	39	280	256	212	283	62	58	ŏ		59	22	ŏ
12.62889	12	37	44	280	256	212	283	65	58	o i	0	63	22	0

12 63028	12	37	49	280	256	212	283	62	58	0	0 5	8 22	0
12 63167	12			200	256		2941	63	59		<u> </u>		0
12.03107	- 12				250					<u> </u>		<u></u>	· - · õ
12.63306	12		59	280	_ 250	212	284	29		<u> </u>	<u> </u>	<u> </u>	
12.63444	12	38	4.	280	256	212	284	59	58	0:	0 5	6	0
12.63583	12	38	9	280	256	212	284	63	58	0	0 6	3 22	0
12 63722	12	38	14	280	256	212	284	59	58	0	0 6	3 22	
12.00722			- 10		- 250	010		64			<u> </u>	2 22	
12.03801	12		19	280	200	212	284	- 04		<u> </u>	<u> </u>	22	
12.64	12	38	24	279	256	212	284	64	58	_0	0 6	<u>3'21'</u>	3
12.64139	12	38	29 ¹	279	256	212	284.	58 ¹	58	0	0 5	7 21.	5
12 64278	12	38	34	279	256	212	284.	59	58	01	0 5	7 21	7
12 64417	10		20	270	256	212	204	50			<u> </u>	7 20	
12.04417				279	230	. 212	204				<u> </u>	20	
12.64556	12:	38	44	279!	256	212	284	59	58		<u> </u>	<u>/20</u>	_12
12.64694	12	38	49	279	256	212'	284	63	58	0	01 6	3 20	14
12.64833	12	38	54	279	256	212	282	58;	58	0	0 5	7 19	17
12 64972	12	38.	591	279	256	212	282	58	58	0	0 6	2 19	19
10 651111	10	20	4	270	200					- <u>0</u> -	<u> </u>	2	22
12.03111	12			2/9	230		202				<u> </u>		
12.6525	12		9	279	256	212	282		58	0	0 <u>'</u> <u>5</u>	<u>/ 18</u>	24
12.65389	12	39	14	279	256	212	282	58	58	0	05	7 18	26
12.65528	12	39	19	279	256	212	282	60	58	0.	0 5	7 18	26
12 65667	12	30	24	280	256		282	60	58		<u>0</u> 5	7 18	26
12.00007	12				250	- 212				<u> </u>	<u> </u>	,	
12.058001		39	29	280	250		282				<u>v</u>	/	. 25
12.65944	. 12	39	34	280	255		282	60		0:	0 5	7 <u>: 19</u> :	22
12.66083	12	39	39	280	255	211	282	56	57	0	0! 5	3 <u> </u> 19	19
12.66222	12	39	44	280	255	211	282	59'	57	0	0 5	9; 20;	15
12 66333	12	30	49	280	255	211	282	62	57	······	0	9 20	12
10.00470			<u> </u>		200		- 202	67			·	7	· <u>'</u> ÷
12.004/2	12		53	280	205	. 211	281	0/			<u>v </u>	<u>/ 21</u>	ð
12.66611	12	39	58	280	255	211	281	64	57'	_0;	<u>0 6</u>	7 21	. 5
12.6675	12	40	3	280	255	211	281	56	57	0.	0, 6	0 21	1
12.66889	12	401	8	280	255	211	281	56	57	0	0 5	6. 21	1
12 67028	12	40	12	200	255	211	201				<u></u>	2 22	
12.07020	12		13	200	255						<u>. </u>	<u> </u>	·
12.6/16/	12	40	18	280	255	<u>211</u>	281	65	57	0 <u> </u>	0 6	222	
12.67306	12	40	23	280	255	211	281	61		0	06	2 22	1
12.67444	12	40	28'	280	255	212	281	62	57'	0	0 6	2 22	1
12 67611	12	40	34	280	256	212	281	61	58		0 6	2 22	1
12 6775	- 13	40		- 200	255			61		<u> </u>	<u> </u>	<u>-</u> · <u></u> · · · ·	
12.0775		- 49			250	212		<u> </u>			<u> </u>	<u> </u>	
12.67889	12	40	44	280	256	212		64	58		06	2 . 22	!
12.68028	12·	40	49	280	256	212	281	60	58	0	0 6	2 22	1
12.68167	121	40	54	280	256	212	281	63	58		0.6	2 22	· - 1
12 68306	12	40	59	280	256	212	281	60		0	<u>0 </u>	2 22	1
12 69444		41		200	256	212		- 67			<u> </u>		
12.00444	.12	41		280	250	212				0	<u> </u>	<u> </u>	
12.68583	12!	41	9	280	256	212	281	63	581	_0:	0	3 22	0
12.68722	12	41	14	280	256	212	281	58	58	0	0 6	3 22	0
12.68861	12	41.	19	280	256	212	281	61	58	0	0 6	3 22	0
12 69	12	41	24	279	256	212	281	58	58	0	0 6	3 22	0
10 60120	10				250	014				· · · ·	<u> </u>	2	
12.09139	12		29	2/9	250	214!	- 201	. 03.			· · _ · ·	J. <u>22</u>	
12.69278	12	41!	34		257	214		63	58	0	0	3 22	. Ū
12.69417	12	41	39	279	257	_ 214	281	64	58	<u> </u>	<u>0 </u>	3 21	0
12.69556	12	41	44	279.	257	214	281	61	58	0:	06	3 21	2
12.69694	12	41	49	279	257	214	281	61	58	o	0 6	3 21	6
12 609331	12	41	54	270	257	214		65		<u></u> ;		3 20	
10.00044			- 59		257	- 214	200			<u> </u>	<u> </u>	20	
12.09944	12	41	58	2/9	257	214	283		_ 58!	_0	<u> </u>	3, 20	. 10
12.70083	12	42	<u>3j</u>	279	257	214	283	60	. 58	_0	<u>v </u>	320	11
12.70222	12	42	8	279	257	214	283	60	58	0	06	319	15
12,70361	12	42	13	279	257	214	283	60	58	0'	о <u> </u>	1 19	17
12 705	12	42	18	270	257	214			58	0	و. ء 0	1 10	- 10
12 70620	12			- 270	257	214					<u> </u>	1 10	
12.70039		42' ···	2	219	237	214	283	50			<u></u>	<u> 10</u>	
12.70778	12	42	28,	279	257	214;	283	58'	58'	_0	<u> </u>	1 18'	24
12.70917	12	42	331	279	256	214	283	54	57	0.	0 5	5' 18	. 27
12.71056	12'	42	38	279	256	214	283	61	57	0	0' 6	1 18	28
12,71194	12.	42	43	279	256	214	283	63	57	0,	0 6	1 18	26
12 71333	12			270	256	214	283	50	57	0	0 6	1 10	
10 71 470		40			2.50						<u> </u>		
12./14/2	12	42	53	- 2/9	250	214	280	_ 58	5/!		<u>v 6</u>	18	29
12.71611	12:	42	58	279	256	214	280	58	57	0	0 _ 6	1 <u>18</u>	30
12.7175	12 ⁱ	43	3	279	256	214	280	61	57	0	0 6	1 18	30
12.71889	12	43	8.	279	256	214	280	 59 [`]	57.	0	а 1	1 18	31
12 72028	12	431	13	279	256	214	280	63	57	- 0	<u>ة</u>	1 18	- 32
10 70167	10			270	256		200		 	ő · · ·	<u> </u>		202
12.72107	12'	40		2/9	200	214				<u> </u>	<u> </u>	18	32
12.72306	12	43	23	279	256	214	280	62	57		υ <u>. 6</u>	1, 18	32
12.72444	12	43	28	279	256	216	280	59	57	0	0 5	5 18	32
12.72583	12	43	33	279	256	216	280	59	57	0	0 5	5 18	32
12 72722	12	43	38	279	256	216	280	57	57	0	<u> </u>	5 18	32
10 70001	12	40			250	040	<u> </u>			õ	<u> </u>	<u>10</u>	
12.72861	12	43	43	2/9	250	216	280	50	5/	<u>v</u> .	u <u>6</u>	4 18	32
12.73	12	43	48	279	256	216	280	61	. 57	0	v <u>.</u> 6	u <u>. 18</u>	<u>. 32</u>
12.73139	12	43	53	279	256	216	278	60	57	0	0 6	0 18	32
12.73278	12	43	58	279	256	216	284	65	57	0	0 6	5 18	28
12,73417	12	44	31	279	256	216	284	61	57	0	0 5	7 19	24
10 72556				<u></u>		216		···· č			<u> </u>		20
	12	0.01	<u>u</u> .		2 m - ·	~			F /			/ 113	~
12.70000	12	44	<u> </u>	279	250	- 210			5/		U	<u> 19</u>	
12.73694	12	44	8 13	279	256	216	284	62	57 57	0	0 6	7 <u>19</u> 3 <u>20</u>	17

12.73972	12	44	23	280	256	216	284	57	57	0	0	57	20 ₁ 10
12.74111	12	44	28	280	256	215	284	57	57	.0	0	57	21 6
12.7425	12	. 44	33	280	258	215	284	60	57'	0.	0	57	$\frac{21}{21}$ $-\frac{3}{21}$
12.74389	12	44	43	280	258	215	278	. 60	57		0	<u>57</u>	21. 1
12.74667		- 44	48	280	258	215	278		57		0	63.	22 1
12.74806	12	44	53	280	258	215	278	62	57	· · • •	0 -	61	22 1
12.74944	12	44	58	280	258	215	284	62	57	0	0	61	22 1
12.75083	12	45	3	280	258	215	284	56	57	0	0	54	22 1
12.75222	12	<u>45</u>	8	280	258	215	284	56	57	0	0	54	. 22 1
12.75361	12	45	- 13	280	258		284	63	57	0	0	63	$\frac{22}{20}$ - 1
12.755	_ 12	- 45		280	258	215	284	62	57	- 0	0	63	$\frac{22}{22} - \frac{1}{1}$
12 75806	- 12	45	29	280	257	215	284	59	58	_ 0	0	57	22 1
12.75944	12	45	34	280	257	215	284	62	58	 0	0	57 57	22 1
12.76083	12	45	39	280	257	215	284	59	58	0	0	57	22 1
12.76222	12	45	44	280	257	215	284	59	58	O	0	57	22 1
12.76361	12	45	49	280	257	215	284	67	58.	0	0	66	1
12.765	12	45		280	257	215	284	64	58		0	66	1
12.76639	12	45	59!	280	257	215		60	- 58'		0	58	$\frac{22}{22}$ $-\frac{1}{1}$
12 76917	12	40	4.	280	257	215	203	50			<u>. </u>	58	22 1
12.77056	12	- 46	<u></u>		257	215	283	59	58		0	58.	22 1
12.77194	12	46	19	280	257	215	283	66	58	· · _ ·	0	66	22 1
12.77333	12	46	24	281	257	215	283	66	58	0	0	66	22 1
12.77472	12	46	29	281	257	215	283	70	58		0	66	22 1
12.77611	12'	46	34	281	257	215	283	66	58	0	<u> </u>	66	. 221
12.7775	12	46		281'	257	215	283	62	<u>58</u>	- 0	0	60	1
12 78028	12	40	⁴⁴	281	25/	215	283	61	58		<u>vi</u>	60	$\frac{22}{22} \frac{1}{4}$
12,78167	12	46	- 49.	281	257	215	283	64		. 0		60 60	22 1
12.78306	12	46		281	257	215	280	- 64		·· 0 · ·	. <u>o</u>	60	22 1
12.78444	12	47	4	281	257	215	280	60	58	0	0	60	22 1
12.78583	12	47	9	281	257	215	280	65	58	0	0	60	22 1
12.78722	. 12	. 47.	14:	281	257	215	280	62	58	0,	0:	60	,22 1
12.78861		47	19	. 281	257	215	280	58 _	58	. 0	0	60	$\frac{22}{22}$ $\frac{1}{1}$
12.79	- 12.	-47	24	283	257	215	280	63	58	-0	0	67	$\frac{22}{22}$ $-\frac{1}{1}$
12 79278	12	. 47.	34	283	257	216	280	62	58	0.	0	61	22
12.79417	12	47		283	257	216	280	62	58:	0.	0	61	22 1
12.79556	12	47	44	283	257	216	280	58	58		0	61	22 1
12.79694	12	47	49	283	257	216	280	62	58	0	0	61	22 1
12.79833	12	47	54	283	_257	216	280	58	58	0	0	61	22 1
12.79972	12	47	59	283	257	216	280	58	581	0	0	61	22 1
12.80111	12	48		283	- ²⁵⁷	216	280	61	58		0	61	$\frac{22}{22} 1$
12 80389	12	40.	<u>_</u>	283	257	216	280	63			···	601 601	-22
12.80528	12	48	19	283	257	216	280	59	58	<u>0</u> .	0	60	22
12.80667	12	48	24	281	257	216	280	62	58	0	0;	60	22 1
12.80806	12	48	29	281	257	215	280	61	58		0	60	22 1
12.80917	12	48	33	281	257	215	280	59	58	0	0	59	22 1
12.81056	12	48		281	_257	. 35	280	63	58		0	59	1
12.81194	12	48		281	25/	- 3 -	280	60 ₁	58		<u>.</u>	59.	22 1
12.81472	12	40		281	257	3	280	57	58		ö	59. 59.	22 1
12.81611	12	48	58.	281	257	40	281	64	58	- ŏ: —	-0	- <u>-</u> : 59	22 - 1
12.8175	12	49	3	281	257	17	281	60	58	<u> </u>	0	65	22 1
12.81889	12	49	8	281	257	214	281	64	<u>58</u>	_0	0	65	1
12.82028	<u>12</u>		13	281	257	_214	281		58	_ 0	0	6 <u>5</u>	22 1
12.82167		49		281,	257	214	281	61	58		0	59! 50	- 22
12 82444	12	49	23	280	257	214	- 281	61	58	0:	0	59.	$\frac{22}{22} \frac{1}{1}$
12.82583	12		33	280	259	214	281	61	58	0	õ	59	22 1
12.82722	12	49	38	280	259	214	281	61	58	0	0	59	22, 1
12.82861	12	49	43	280	259	214	281	61	58	0	0	57	22 1
12.83	12	49	48	280	259	214	281	60	58	0	0	60	221
12.83139	12	49	53	280	259	214	_281	55	58	0	0	54.	221 1
12.83278	12 -	49	- 58	280	259	214	280	58	58	0	0	60 C 1	22 1
12.83417		<u>-50</u>		280	259	214	280	61	58		<u>.</u> - –	61 61	$-\frac{22}{22}$ 1
12.83694	12	50.	0	280	259	- 213	280	- 65		<u>0</u>	0	66	
12.83833	12	50!	18	280	259	213	280	62	58:	<u>0</u>	ō	58	22 1
12.83972	12	50	23	280	259	213	280,	58	58	0	0	58	22 1
12.84111	12	50	28	280	259	213	280	69 ⁱ	58	0	0	63	221
12.8425	12	50	33	260	257	213	261	111	73	0	0 1	15!	_221
12.84389	12	50	38	234	234	196	233!	119	88	0	0 1	22	22 1

CRTF NET-90 99 POINT	DATA FILE							··-·				}				- !	1	1			1	
Time Time Tim	e FT720	IPF-001	PF-002 FT	730 FT8	00 TE	EE16 TE	Ē15 1	EE14 TEE1	3 TEE 12	TËËŪ	TEE10	TEE9	TEE8	TEE7	TEE6	TEE5	TEE4	TEE3	TEE2	TEE1	TEEUH17	TEELH18 TEELH19
hour min sec	GPM	LVmin	LVmin GF	M GPN		EGF	GFD	EG F DEG	F DEG F	DEG	DEG F		DEGF	DEGF	DEGF	DEG F	DEG F	DEGF	DEGF	DEGF	DEGF	DEG F DEG F
- 12 0	19 37	4 412	289	- <u>/2</u> 85.	156	- 590	592	· · · 592	591 5	<u>88</u>	508 5	90 <u>59</u> 921 59	<u>91</u> . <u>5</u> 92 5	597 5	931 - 5	91 5	84	1 59	10 58	0 59	31	589 583
12 0	34 36	412	297	265	158	594	593	593	593 6	00	508 5	921 59	3 5	598 5	94 5	92 5	35 59	1 50	1 59	0 59	4 593	591 585
12 0	49 33	341	262	321	196	594	593	596	5931 6	00	508	92 59	97 5	598 5	94 5	91 5	59	11 59	11	0 59	3 594	592 585
$-\frac{12}{12}$ $-\frac{1}{11}$	19 38	336	279	81	- 183	594	596	597	<u>590</u> 5 590 5	<u>97</u>	508 5	89 60	<u>15 5</u> 02 5	595 <u>5</u>	92 5	90 5	82 <u>58</u> 9 82 589	9 59	0 58	8 <u>59</u> 8 59	2 594	
12 1	33 38	0 ¹ 411	299	117	144	592	591	594	591 6	00 1	612 5	90 59	97 5	597 5	931 5	91 5	84 590	0 59	0 58	9 59	3 594	592 584
	49 38	346	285	141	144	592	593	594	593 6	01	622 5	91 59	3 5	598 5	93 5	91 5	B4 59	1 59	59	0 59	4 594	592 585
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	2 min	Sec -	GPM vii r	Lt/min		IGPM 0		UEG F	UEG F	UEG F 546	IDEG F	10EG F 537	UEG F 543	<u>UEG</u> F [] 547	<u>JEG</u> ⊢ [538	<u>534</u>	<u>DEG</u> F [DE0 536	548.	⇒ ⊧ ∣D <u>E</u> 503	539	535	533 54	9 567	562	556
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hour	min	Sec	GPM	LVmin	Lt/min	GPM	GPM	DEG F DE	3 F DEG F	DEG F D	EG F DEG	F DEG F	DEG F	DEGE	DEG F DEG	SF DEG F	DEG P	DEGF	DEGF			EG F DEG F					
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hour	min	SOC	DEG F	DEGF	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEGF	DEG F	DEG F	DEGF	DEGF	DEG F	DEGF	DEG F	DEG F	DEG F	DEG F	DEG F
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hour	i, m	in	Sec	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEGF	DEG F	DEG F	DEG F	DEG F DEG F	DEGF	DEG F	DEG F	DEGF	DEG F i	DEG F	DEG F	DEG F	DEGF	DEG F
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	3 18	48	287	265	- 323	316	348	314	185	344	316	30	318	291	- 316	251	314	4 3	06 27	3 332	541	493	517	430	592
1	3 19	3	287	264	320	315	347	314	185	343	315	300	317	290	315	250	31:	3 3	05 27	2 331	541	493	517	429	592
L1	3 19	18	286	5 264	319	314	346	313	184	342	314	300	316	290	314	249	312	2 3	04 27	3 331	541	493	<u>517</u>	429	591
1	3 19	33	283	263	318	314	345	312	. 182	<u>341</u>	313	299	315	289	313	248	31	$\frac{1}{3}$	03 27	2 330	541	493	517	429	
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i	3 20	34	282	261	315	310	340	309	179	337	308	296	311	285	310	245	30	6 3	00 27	1 329	542	493	517	429	591
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- 1	3 21	4	280	259	312	309	338	307	- 179	335	306	294	1 309	. 284	308	243	3 30	5 2	<u>99</u> - <u>27</u>	0 329	543	493	517	429	
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	3 22	,	2/3	254	303	303	- 330	299	174	328	295	28	7 301	277	302	230	7 29	7 2	93 26	8 327	545	5 494	518	429	594
	3 23	33	27:	253	303	301	328	299	174	327	297	28	7 300	276	300	236	5 29	6 2	92 26	8 327	540	494	518	429	594
	3 23	48	273	252	303	300	327	298	174	326	296	28	5 299	275		230	5 29	5 2	91 26	8 327	7 546	5 494	518	429	593
	3 24		27	252	302	300	326	297	173	325	295	28	5 299	275	299	23	5 29	4 2	90 26	8 326	546	6 494	518	428	593
	3 24	16	27	250	301	299	325	296	172	324	294	28	5 297	274	298	234	4 29	3	90 26	326	5. 540	5 494 7 406	518	428	593
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	3 25		26	247	297	296	321	293	170	321	291	28	2 294	271	295	23	1 29	0 2	87 26	326	54	7 495	518	429	594
1	3 25	3	264	3 247	296	295	320	292	169	320	290	28	294	270	294	23	1 29	0 2	87 26	32	54	B 495	518	429	594
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	20		200	240	299	293	317	290	167	- 317	20/	2/	8 290	200	292	223	9 <u>20</u> 9 28	5 2	84 26	7 - 32	55	496	519	429	597
-·	13 26	49	26	5 244	292	291	316	288	166	i <u>316</u>	285	27	7 289	266	290	22	7 28	5 2	84, 26	325	5 55	0 ¹ 496	519	429	596
-	3 27	172	26	244	291	291	315	287	165	315	285	27	6 288	266	290	22	7 28	4 2	83 26	325	555	0 496	519	429	589
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1- 1	3 2	<u>34</u>	26	4 242	289	289	313	- 286	164	314	283	27	5 <u>286</u>		288	220	5. <u>28</u>	<u>2</u> . 2	26	324	1 <u>55</u>	0 496	519	430	5/8
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	13 28	3 48	3 26	239	285	286	309	282	161	310	279	27	282	261	284	22	2 27	8 2	26	5 32	3 _ 55	497	519	431	565
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Time	'Tır	ne Time	TEW18	TEW17	TEW16	TEW15	TEW14	TEW13	TEW12	TEW11	TEW10	TEW9 TE	W8 T	EW7 T	EW6 T	TEW5	TEW4	TEW3	TEW2	TEW1	TEWUHIS	TEWLH20	TEWLH21	E970 T	E990
hour	mi	n isec	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	IDEG F	DEG F	DEGF	EGF İÐ	EG F D	EGF C	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEGF	DEGF	DEGF jD	EG F
	13; -	29	33 2	8 23	6 283	283	307	280	160	i 307	276	270	279	259	282	221	275	276	26	5 322	552	499	519	433	563
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	13	30	- 3 2	5 23	5 281	282	j 305	278	159	306	275	268	278	257	281	219	274	275	26	5 322	552	499	518	433	563
1	13	30	18 2	5 23	5 279	281	304	278	156	305	274	267	277	256	280	218	273	274	26	5 322	1 553	499	518	434	563
	13	30.	34 2	4 23	4 279	280	303	277	158	304	273	267	276	256	279	218	272	· 273	26	6 321	553	500	518	434	564
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	13	31	4 2	4 23	3 277	279	301	275	157	[.] 303	271	265	275	254	278	217	271	· 272	26	5 321	554	500	519	434	564
· · ·	13	31	19 2	3 23	3 276	278	300	274	156	302	270	265	274	253	277	217	270	272	26	5 321	555	500	519	434	564
	13i -	31	34 2	3 23	2 276	278	300	273	150	301	269	264	273	253	276	216	269	271	26	5 320	555	500	519	434	563
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1	13	32	4 2	52 23	2 275	5 276	298	272	155	300	268	263	271	251	275	215	268	269	26	5 319	555	500	519	434	562
·	13	32	19 2	2 23	0 274	276	297	272	153	299	267	262	270	251	274	214	267	269	¹ 26	3 319	555	500	519	434	562
	13	32	34 2	23	0 273	275	296	271	153	298	266	261	270	250	273	213	266	268	j 26	31 31 8	555	500	519	434	561
	13	32	49 2	22	9 271	274	296	270	153	298	265	260	269	249	272	212	264	267	26	318	556	500	519	434	560
	13	33	4 2	22	9 271	273	295	270	152	297	264	260.	268	249	272	212	264	266	26	310	5 556	501	519	434	560
	13	33	19 24	9 22	8 270	273	294	269	153	ui 296	264	259	267	248	271	211	263	266	26	316	556	501	520	434	559
	13	33	33 2	19 22	8, 269	272	293	268	152	295	263	259	266	247	270	211	262	266	26	316	556	501	520	434	559
	13	33	48 2	18 22	7 269	272	293	267	152	295	262	258	265	247	270	210	262	265	26	51 316	557	501	520	434	560
	13	34	3 2	16 22	71 268	271	292	267	151	294	261	257	265	246	269	210	261	264	26	315	557	502	520	434	560
-	13	34	18 2	6 22	6 266	5 270	291	266	151	293	261	256	264	245	268	209	260	264	26	315	557	502	521	434	560
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	13	34	48 2	16 22	5 265	269	290	264	151	292	259	256	263	244	267	208	259	263	26	319	558	503	_521	435	562
	13	35	3 2	15 22	5 264	268	289	264	151	291	258	255	262	243	266	208	259	263	25	59 314	558	503	521	_ 435	562
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	13	35	33 2	14 22	3 263	267	287	262	150	290	257	254	261	242	265	206	257	262	25	8 313	559	505	522	435	564
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	13	36	3 2	14 22	3 262	266	286	261	149	289	256	253	259	241	264	205	256	260) 25	57 313	559	505	523	435	564
	<u>13</u>	36	18 <u>2</u>	13 22	3' 262	? <u> _265</u>	285	260) 149	<u>288</u>	255	252	258	240	263	<u>205</u>	255	260	25	6 <u>313</u>	3 <u>. 560</u>	505	523	434	- 564
-	13	36	34'2	13 22	1 26	264	284	260	$\frac{149}{149}$	287	255	252	259	241	264	. 206	255	260	25	6 <u>31</u> 2	560	506	523	434	- 564
	13	36	49 2	13 22	1 259	264	284	259	149	287	254	252	259	242	264	. 208	256	262	25	31:	560	506	523	434	- 563
	13	37	4 2	12 22	0 259	263	283	259	149	286	254	251	260	244	265	210	258	264		8	560	506	523	434	563
1_	13	37	19 2	10 21	9 25	3 263	283	258	149	286	254	252	2611	246	266	213	259	260	<u>25</u>	91 310	560	507	523	434	563
	13	37	34 2	10 21	9 25	262	282	25	149	285	254	252	- 262	249	267	216	261	260	25	31	560	507	523	434	
	13	371	49 2	39 21	9 25	261	281	25	14	284	254	252	264	252	5 <u>P</u> A	. 221	- 263	- 270	26	310 - 310	30	508	524	434	
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<u> </u> _	13	38i	34 2	30 [°] <u>2</u> 1	25	259	279	25	140	283	254	252	200	202	2/5	-232	269	2/2	- 26	32	5 302	509	525	434	
<u> </u>	13		49 - 2	<u>se 21</u>	6 25 C 00	259	2/8	254	148	282	254	253	270	264		235	2/1	280	20	26 32	502	510	525	434	504
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TEST	DAT	E: Wed De	oc 15 19	93 7:39:18	3 am	·	. <u> </u>			
Time		Time	Time	FT720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour		min	sec	Lt/min	Lt/min	Lt/min	Lt/min	PSIG	PSIG	PSIG
	7	40	3	0	56	4	0	-2	-2	
	7	40	18		68	4	0			
		40	33		61	3		-2	-2	
		40	40	- 0	59	5			2	
⊢		40		0	59	5	· 0			
<u> </u>		40	10	0	59	5	Ň	.2		
	7	40	13	0		5	0	.2	2	<u>├</u>
}	7	40	16				0	-2		
	7	46	- 19	0	58	5	0	-2		-1
	7	46	22	0	60	5		-2		-1
	7	46	25	0		5	0		-2	1
· ·	7	46	28	0	69	5	Ö	-2	-2	1
	7	46	31	0	62	5	0	-2	-2	-1
	7	46	34	0	56	5	0	· -2	-2	•1
	7	46	38	0	56	5	0	-2	-2	· · · · · · · · · · · · · · · · · · ·
	7	46	41	0	61	5	0	-2	-2	-1
	7	46	44	0	61	5	0	-2	-2	-1
<u> </u>	7	46	47	0	61	5	0	-2	-2	-1
··	7	46	50	_0	61	5	0	-2	-2	1
	7	46	53	0	61	1	0	-2	-2	· _ · 1
	7	46	56	0	68	1	0	-2	-2	-1
	7	46	59	0	59	1	0	2	2	1
	7	47	2	0	59	1	0	-2	-2	-1
	7	47	6	0	66	7	0	·•2	-2	
ļ	7	47	9	0	66	1	0	<u>-2</u>	<u></u>	4 . <u>-1</u>
	7	47	12	0	66	1	0		-2	<u>.</u>
ļ	7	47	15	0	66	1	0	· •2	-2	-1
	7	47	18	0	55	8	0	-2	-2	1
	7	47	21	0	69	2	0	-2		
	7	47	34	0	76	6	0	-2	-2	
L		47	49	0	64	· 5	<u> </u>	-2	-2	_]
		48	4	0	68	5	0			
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		48	34	0	/1	5		-2		
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		49	4	0	53	· 4				
		49	- 19	0	50	<u> </u> ,				· · · ·
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<u>⊢</u>	·· <u></u> 7	51	18	0	50		n	····	-2	-1
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	7	51	48		45	,,		2		
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·•• ··	7	52	18	0	51	2	0	-2	-2	-1
	7	52	33	0	56	7	0	-2	-2	-1
· · ·	7	52	48	0	56	7	0		-2	-1
	7	53	3	0	56	5	0	-2	-2	•1
	7	53	19	0	51	5	0	2	-2	-1
	7	53	34	0	55	5	0	-2	-2	· •1
	7	53	49	0	52	5	0	2	-2	-1
	7	54	4	0	52	1	0	-2	-2	-1
	7	54	19	-1	52	5	0	·2		-1
<u> </u>	7	54	34	-1	52	5	0	-2		-1
L	7	54	49	-1	50	5	0	-2	2	<u>-1</u>
		55	4	-1	50	5	0	-2	<u> </u>	-1
<u> </u>	7	55	19	0	55	1	<u> </u>			-1
		55	33	214	322	2		106	83	-1
I		55	49	320	309	2	0	111	103	-1
		56	3	320	303	2		110	103	· -1
<u>⊢</u> - ·-		56	18	392	367	225	<u> </u>	46	33	<u>. </u>
- ·		56	33	403	385	192		02	49	<u> </u>
	- 7	56	48	397	3/9	186	·0	64	5U	,
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Time	Time		Time	FT720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour	min		Sec	Lt/min	Lt/min	Lt/min	Lt/min	PSIG	PSIG	PSIG
	7	57	18	386	361	162	0	68	53	10
	7	57	33	386	373	148	0	71	57	14
	7	57	48	387	302	5	0	68	55	15
	7	58	3	387	289	5	0	68	55	15
	7	58	18	387	336	5	0	68	55	15
	7	58	34	387	352	5	0	68	55	15
	7	58	49	74	335			-3	16	13
<u> </u>	7	59	4	4	-4	4	0	-6	31	10
	7	59	19	4	-4	4	0	-6	31	9
·	<u>7</u>	_59	34	4	-4	4	0	-6	30	9
}	<u></u>	-59	49	4				- - 0	30	8
	8	0	4	0			<u>0</u>	-0	30	0
			19	0	-5		0	-0-	30	7
·	0	0	48		-5	6	0	<u>. </u>	30	7
	8	1	40	0	-5	1	0	-6		6
	8	1	18	0	-5	2	0	-6	30	6
	8	- 1	33	0		7	0		30	6
	8	1	48	0		7	0	-6	30	5
	8	- 2	3	0	-5		0	-6	30	5
	8	2	18	0	j -5	0		-6	30	5
	8		33	i 0	-5	0	0	-6	30	4
r	8	2	48	0	-5	1	0	-6	29	4
	8	3	3	0	-5	1 1	0	-6	29	4
	81	3	18	0	-5	1	0	-6	29	4
	8	3	34	0	-5	0	00	-6	29	3
	8	3	49	0	-5	6	0	-6	28	3
	8	4	4	0	-5	7	0	-6	28	3
	8	4	19	0	-5	1	0	-6	28	3
	8	4	34	0	-5	7	0	-6	28	2
l	8	4	49	0	-5	7	0	-6	28	2
	8	5	4	0	-5	<u>1</u>		-6	28	2
	8	5	19	0	-5	1	0	-6	28	2
	8	5	33	0	-5	0	0		28	2
	8'	5	48	i <u> </u>	-5	0	0	-6	27	
	8	6	3	3	· <u>5</u>	6	0	-6	. 5	0
	<u>. 8</u>	<u> </u>	18	399	-5	221	0	50	49	
	<u> </u>	0	33	399	380	100	0	64	51	<u></u>
ŀ	<u> </u>		40		359	171		66	5 <u>1</u>	<u>-</u>
	<u></u>		19	393	367	150		00 00	55	12
	8		33	380	358	30		67	55	16
	8		48	387	361	4		68	55	15
	8	8		387	382	μ			55	15
•	8	8	19	387	382	4		68	55	15
	8'	8	34	387	347	4		68	55	15
	8	- 8	49	387	320	6	0	68	55	15
	8	9	4	387	359	5	·0	68	55	15
	8	9	19	387	371	5	0	68	55	15
	8	9	34	387	309	5	0	68		15
	8	9	49	386	361	5	0	68	55	15
	8	10	4	386	352	6	0	68	55	15
	8	10	19	386	370	6	0	68	55	15
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	8	10	49	386	361	1 1	0	68	55	15
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	8	12	 	300	267		:0	89	55	
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	8	13	18	387	300	<u> </u>	i	68	55	15
	8	13	33	387	360	; <u> </u>	i 0	68	55	15
i	8	13	48	386	401	0		68	55	15
	8	14	4	386	359	0	i — č	68	55	15
	8	14	19	386	355	i 2	i 0	68	55	15
	8	14	34	386	385	1	C	68	55	15
I	8	14	49	386	383	2	0	68	55	15

Time	Time		Time	FT720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour	min		sec	Lt/min	Lt/min	Lt/min	Lt/min	PSIG	PSIG	PSIG
	8	15	4	386	362	6	0	68	55	15
	8	15	19	386	390	2	0	68	55	15
	8	15	34	387	378	2	0	68	55	15
	8	15	49	387	383	5,	0	68	55	15
	8	16	4	387	370	0	0	68	55	15
	8	16	19	387	398	1	0	68	55	15
	8.	16	33	387	349	<u> </u>	0	68	55	15
·	8	16	48	388	351	1		68	55	15
	8	17	3	388	353	1		68	55	15
	8	17	18	388	364	1		68	55	15
	8	17	33	388	364	i:				15
	8	17	48	387	360			60	55	15
	8	18		387		<u> </u>		68		
	0	10	10		350			60		15
I		10	10			· · · · · · · · · · · · · · · · ·		60	55	15
	0	- 10						60	55	15
	0	10	40		300			60	55	
<u> </u>	<u> </u>	- 19				· _		60		15
	8				342			0		15
	8	- 19		388	340	/		68		
	8	19	49	388	342	7		68	55	15
<u> </u>	8	_20	4.	388		6	0	68	55	15
L	8	_20	19	388	314	7.	0	68	55	<u> </u>
<u> </u>	8	_20	34	388	322		0	68		15
	8	_20	49	388	385	2	0	68	54	15
	8	21	4	388	364	2	0	68	54	15
	8	_21	19	388	356	2	0	68	54	15
	8	21	34	388	386	1	0	68	55	15
-	8	21	48	387	372	7.	0	68	55	15
	8	22	3	387	359	1!	0	68	55	15
	8	22	18	387	398	2,	0	68	55	15
	8	22	33	387	354	1	0	68	55	15
·	8	22	48	386	357	6	0	68	55	15
	8	23	3	386	378	1	0	68	55	15
·	8	23	18	386	359	1		68	55	15
	8	23	33	386	335	2		68	55	15
	8	231	48	388	366	2	0	68	55	15
	8 -	24	3	388	382			68	55	15
• • •	8	24	18	388	337	2	·	88	55	15
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		25	10		350	······		60		10
	<u>o</u> i	20				2		0	55	13
	0	- 25			325		0	0		15
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·	<u>8</u>	26	19		403		0		55	15
·	8	26		386	362	<u>1</u> ·	0	68	55	15
L	8	26	49	386	376	1	0	68	55	15
<u> </u>	8	27	4	386	402	2	0	68	. 55	15
L	8	27	19	386	354	1	0	68	55	15
]	8	27	33	386	367	2	0	68	55	15
	8	27	48	387	366	5	0	68	55	15
	8	28	3	387	379	5	0	68	55	15
	8	28	18	387	335	5	0	68	55	15
	8	28	33	387	375	5	0	68	54	15
	8	28	48	387	337	8	0	68	54	15
	8	29	3	387	361	2	0	68	54	15
	8	29	18	387	303	2	0	68	54	15
	8	29	33	387	371	2	- 0	68	55	15
	8	29	48	388	338	0	0	68	55	15
	8;	30	4	388	375	7	0	68	55	15
	8	30	- 19	388	401	1		68	53	15
	8	30	34	380	357	7	0	88	53	15
	8	30	49	389	363	2				15
i	8	31	A	380	370			60	<u></u>	15
	8	31	10			A		<u>. 00</u>		17
	8	21	24			<u> </u>		0-	20	
	8 -	- 31	34	!		<u> </u>		·	30	10
}	<u>0</u>	20		<u>.</u>		<u> </u>				
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├ ──·	0	- 32	18			<u>0</u>	<u> </u>	-0	30	

Time	Time	Time	FT720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour	min	sec	Lt/min	Lt/min	Lt/min	<u>Lt/min</u>	PSIG	PSIG	PSIG
· •-	8 32	48		-5	2	<u>. </u>	·····	-36	11
	8 33		0	-5	<u> </u>	0	-0	35	10
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	8 33	48	<u> </u>	5	7	- 0	· · · · <u>-</u> 6	35	- j
h	8 34	3	0		1	0	-6	35	9
	8 34	18	6		1	0	-6	35	
	8 34	34	6	-5	2	0	-6	35	8
	8 34	49	1	-5		<u>'</u> 0	-6	35	7
	8 35	44	1	-5	1	0	6	<u>. 33</u>	?
<u> </u>	835	19	6	-5	2	0	-6	33	
	8 35	34	└── <u></u>		2	<u> 0</u>	· •6	33	. 6
	8 35	49		· ··		: _ <u>0</u>	-0		د . ء .
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	8 37	18	0	-5	· · · · · · · · · · · · · · · · · · ·	0	-6	30	4
	8:37	33	0	-5	1	0	6	29	3
.	8 37	48	0	-5	0	Ō	-6	29	3
L	8 38	3	0	-5	1	0	-6	29	3
	_838	18	0	-5	2	0	-6	29	3
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	8 39	18	0		2	. 0	-b	27	- 2
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	8 40	19	400	358	195	0	62	52	2
	8 40		394	380	184	· · 0	65	52	5
	8 40	49	394	348	172	···- ē	67	52	
	8j 41	4	388	355	160	ō	69	55	- 12
	8 41	19	382	351	45	0	68	55	16
	8 41	34	382	365	7	0	68	55	16
	8 41	49	382	365	1	0	68	55	15
	8 42	4	388	367	1	0	68	55	15
	8: 42	<u> </u>	388	354	2	0	68	55	15
 	8 42	- 34	<u> </u>	364	2	·	<u>68</u>	55	15
	8 42	48	388	380					15
	8: 43 P 43			350	2	·0	60	55	15
	<u> </u>	1 33	388	3/3		0	68	55	15
	8 43	48	388	352		0	68		
	8 44		386	355		·· · · · · · ·	68	55	15
	8 44	18	386	399			68	55	15
	8 44	33	386	307		i õ	68	55	15
<u> </u>	8 44	48	386	356	7	0	68	55	15
	8 45	3	387	379	7	0	68	55	15
	8 45	19	387	376	7	0	68	55	15
	8 45	34	387	386	1	0	68	55	15
·	8 45	49	387	354	2	0	68	55	15
	8 46	4	386	335	2	0	68	55	15
	8 46	19	386	393	^2	0	68	55	15
	46	34	386	333		0	08		
	8 40	49	300	333		. U	80	55	15
	8 47	10	387	397		0	68	55	13 15
	8 47	33	387	340		<u> </u>	68	55	15
	8 47	48	387	366	1	0	68	55	15
1	8 48	3	385	374	0		68	55	15
·	81 48	18	385	336	2	0	68	55	15
	8 48	33	385	353	1	Ó	68	55	15
	8 48	48	385	394	2	0	68	55	15
	8 49	3	389	381	4	0	68	55	15
	8 49	18	389	343	4	0	68	55	15
	8 49	33	389	361	4	0	68	55	15
	8 49	48	389	376	4	0	68	. 55	15
	<u>8</u> 50	3	38/	355	2	· 0	80	55	15
,	a. 50	18		.1.18.	2		08		

Time	Time	Tin	ne F	720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour	min	sec	:Lt	/ <u>m</u> in	Lt/min	Lt/min	Lt/min	PSIG	PSIG	PSIG
	8	50	. 34	387	301	2		0	68 5	5 15
	8	50	49	387	386	2		0!	68 5	5 <u>1</u> 5
<u> </u>	8	51	4	386	347	2		0	68' 5	5 15
	8	51	19	386	366	1	1	0	68 5	5 15
	8	51	34	386	303	2		0:	68 5	5 15
}··	8'	51	49	386	359	2	· · · · ·	0	68 5	5 15
	<u>ei</u>	52	4	388	341	7		0	68 5	5 15
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	8	52	48 <u>.</u>	388		<u> </u>	· ·	:	68 5	5 15
	8	53	<u> </u>	<u>387</u>	369	<u> </u>	, ·	0	68 5	5 15
	81	53	18	387	.337	6		0	68 5	5 15
	8	53i	33	387	365	2		0	.68 5	5 <u>1</u> 5
	8	53	48	387	378	5		0	68 ₁ 5	5 15
	8	54·	3'	389	368	0		0	68 5	5 15
	B	54	18	389	353	2		0,	68 5	5 _: 15
	8' <u></u>	54	33	389	343	7		0	68 5	5 15
	8	54	48	389	337	1 1		0	68 5	5 15
	8	55:	4	386	356	1	i	0	68 5	5 15
	8	55:	19.	386	372	··	i	o O	68 5	5 15
	e e	551	- 34	200	1	· · - ·-';	; ·· —	<u> </u>	68 5	5 15
	o	55			337		· ·	- di	69 5	5 13 5 16
	<u> </u>			- 300	405	<u>`</u>	! - —	<u> </u>	69:	5 10
} <u>−</u>	<u>.</u>	201	4	387	368	0		<u>v</u> .	00 5	ບ 15 ຮໍ່ເ
<u>↓</u>	<u>8</u> .	56	19	<u>387</u>	362	4	!	·	08 5	o <u>.</u> 15
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	8;	56	48	387	377	4		0	68 5	5 ₁ 15
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	8!	57	18	386	349	0		0	68 5	5 15
	8	57	33	386	376	0		0	68 5	5 15
	8	57	48	386	355	i – 1	• •	0	68 5	5 15
	8.	58	3	389	358	2		0	68 5	5 15
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<u> </u>	8	59	18	388	355	<u> 2</u>	l		08 5	15
	8	59	33	389	<u> </u>	7	!	0	<u>_68</u> 5	o 15
L	81	59	49	389	331	6	:	0	68 _ 5	<u>5</u> 15
	9:	0	4	389	379	2		0	.68 _ 5	5 15
	9	0	19	389	395	<u> </u> 1	:	.0'	68 5	5 15
l	9	0,	341	385	354	6		0	68 5	5 15
r	9	0.	49:	385	370	6	1	0	68 5	5 15
	9'	1	4	385	356	7	:	o	68 5	5 15
	91		19	385	367	. 4		0	68 5	5 15
<u>├</u>	9	1	33	388	373	<u> </u>	1	0	68	5 15
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	9	3	33	388	373	2	· · · · · ·	0	68 5	5 15
	9	3	48	388	313	2	1	0	68 5	15 15
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r · ·	9	4:	34	386	386	- <u>-</u>	1	0.	68 5	5 15
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	9	51	49	1		5		0	. 6	14
L	9	6	4	1	3	5		0	63	15 13
	9	_6	19	0	-5	0		0	-6 3	16 ₁ 12
[9 _i	6	33	0	5	2	<u> </u>	0	-6 3	1 <u>6,</u> 12
	9	6	48	0	-5	6	1	0	-6 3	11 1 1
F	9	7	31	6	-5	. C	, - ·	0	-6 3	15 11
	9:	7	18			1		0:	6	15 10
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	9	7	48				<u>i</u>	0	-6	5
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Time	Time	Time	FT720		PF-001	T730	FT800	PT710	PP-00	1	PT720
hour		sec	Lt/min		Lt/min L	_t/min	Lt/min	PSIG	PSIG		PSIG
	9	8'	-18	- 9	-5	·	···		-0	35	
	9	8	48'	4	-51	·(, 	0.	-6	35	—— .
· —	9	9	4	4		() 	0	-6	33	
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	9	9	34	_4	-5		2	0	-6	33	
	91	<u> </u>	49	<u> </u>		1	<u> </u>	0	-6	32	L
	9	$\frac{10}{10}$ -		. 0	-5		<u> </u>	0.	-6	32	
· ·= =	9	10	34		-5		· · -	0	-6	30	
	9	10	49	ō		2	2	0	-6	30	
	9	11	4	0	-5			0	-6	30	
	9	11	18	0	-5	7	7	0	-6	29	
	9	11	34	2	-5	2	2	0	-6	29	
- ·	9			2	-5	·€	<u>.</u>	<u>0'</u>	-6	29	
	9	12	3	- 2			,	0.	-6	29	
	9	12	33	- 6	-5	'		0	-0 <u>1</u> -6:	27	
	9	12:	48.	ō	<u></u>	' 1	'	ŏ. — ·	-6	27	
		13	3	0	-5	4	,	0.	-6	27	·
	9	13	18	0	-5	4	<u> </u>	0	-6	26	
<u> </u>	9	13	33	0	-5		<u>.</u>	0	-6	26	<u>.</u> .
	9	13	48	5	-5	1 <u>(</u>)	0	-6	12	
	9!		33	396	118		<u>. </u>	_0	62	52	
	9.	14	18	201	367	189	; —	<u> </u>	63	52	
	<u>9</u>	14	<u></u>	201	366	165		0	68	52	
	9	15		385	360	153	2 B:	0 -	70	57	14
[9	15	19 3	887	355	- 4	i . I	0	68	55	16
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	_ <u>9</u>	16	34 3	885			김 —	0	68	55	1
	- 9	17	_49 	895	355	4	<u>!</u>]	-0:	68	55	1
	9	17.	18 3	386	326		i i	0	68	55	1
	9,	17	33 3	886	365			oi	68	55	1
	9	17	48 3	886	353	2	2	0	68	55	1
	9!	18	33	86	381	2	<u>!</u>	0 <u>'</u> .	68	55	1
	9'	18	_18;3	386		2	2	0	68	55	. 1!
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		19 -	18' 0	198	394	'	; - —		68.	55	
	9	19	33 3	886	387	' 7	, <u></u>	_0	68	55	
	9	19	48 3	86	345	1	· —	0	68	55	15
	9	20	3 3	86	340	1		oi	68	55	1:
	9	20	19 3	87	407	1		0	68	55	1
	9'	20:	343	87	386	Q		0	68	55	
	9	20	49: 3	87	368		}: ; ·	<u>_0'</u>	68 <u> </u>	55	
	.9	21		187	363	6	· ···	.0.	60 60	55	- 10
	9	21	34 3	87	411	- 6	<u></u>	0	68	55	19
	9;	21	49 3	87	393	ŭ	;; · —	0'	68	55	15
	91	22	4 3	87	348	1	·	0	68	55	- 15
	9	22	19 3	87	361	0)	0	68	55	15
-		. 22	343	87	361	1	•	0	68	55	15
	-9 .	22	48 3	87	359		<u>! </u>	0	68	55	15
·	<u>9</u> ; 0'	23	 	1981	3/2	Q	/: 	····	68	55	
		23	33 3	000 A88	365	b	<u>. </u>	_0.	68	55	!: 14
·	9.	23	48	86			:: <u></u> !i	0	67	55	<u>1</u>
	9	24	3 3	86	380	6	i	0	68	55	
	9	24.	18 3	87	308	6	5	0	68	55	15
	9'	24	33 3	87	366	1		0	68	55	1.
	9	24	48 3	87	328	1	;	.0	68	55	15
	9	25	3	87		8	¦	0	68	55	
	9	25	-18	80	302	2	i	U. 0.	68	22	
	-9	25	49 3	88	349	<u>_</u>	i		67	55	!! 1!

Time	Time	_	Time	FT720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour	min		sec	Lt/min	Lt/min	Lt/min	Lt/min	PSIG	PSIG	PSIG
	9	26	4	388	336	4	0	68	55	15
	9	26	19	387	372	4	0	68	55	15
	9	26	34	387	362	4	0	68	55	15
	9	26	49	387	392	4	0	68	55	15
	9	27	3	387	371	8	0	68	55	15
	9	27	18	384	296	1	0	68	55	15
ŀ	<u>a</u>	27		384	320	6	0	68		15
	<u>a</u> '	27	48	384	260			68	55	15
· ·	<u></u>	20	2	294	370			68	55	15
-		20	10	297	370	<u> </u>	0	68	55	15
	9	20	22	297	352		0	00	155	
	9	20		307	333			60	55	
	3	20		207	342	····	0	60		15
	9	29		307	354		°	60		15
	9	29		300						15
·	9	29		388	360	<u> </u>				
	9	-29	40	300	3/4		0		55	15
	9.	30		388	330	0	0		55	15
·	9	30	19	387	345	2	<u> </u>		55	10
	9	30	34	387	380		0		55	
	9	30	49	387	349	<u> </u>	0	68	55	15
	9	31	4	387	371	1	0	68	55	. 15
	9	31	19	388	385		0	68	55	15
	9	31	34	388	352	7	0	68	55	15
	9	31	49	388	351	<u> </u>	0		55	15
	9	32	4	388	325	1	0	68		15
	9	32	19	387	359	7	0	68	55	15
	9	32	34	387	365	2	0	68	55	15
	9	32	48	387	354	2	0	68	55	15
	91	33	3	387	343	7	0	68	55	15
	9	33	18	385	316	2	. 0	68	55	15
	9	33	33	385	344	1	0	68	55	15
	9	33	48	385	287	1	0	68	55	15
	9	34	3	385	334	1	0	68	55	15
	9	34	18	385	352	1	0	67	55	15
	9	34	33	385	351	6	0	68	55	15
	9	34	48	385	345	7	0	68	55	15
	9	35	4	385	334	7	0	68	55	15
	9	35	19	386	401	2	0	68	55	15
	9	35	34	386	346	6	i o		55	15
· · ·	9	35	49	391	361		0	68	55	. 15
	9	36	4	385	381	1	0	68	55	15
	9	36	19	385	309	···· 1	i o	68	55	15
	9	36	34	385	392	1	0	68	55	15
	9	36	49	385	336	·i	o		55	15
	9	37	4	388	331	·	0	67	55	15
	9	37	19	388	368	1	i Õ	68	55	15
	9	37	33	388	314	<u>'</u>	ñ	89 1	55	15
I	9	37	 	388	343	. . 9 я	0 0	89		15
	0	20	07	200		0				10
		20	10	200	301			60		15
- · -·		- 20	10	200		····· - ·· - ·· - ·· - ·· - ·· - ··	· · - · — · ^	00		10
	0	20	35	300		·		60	ວວ 	10
·	<u> </u>	- 30		300	3/2	· · · · · ·		70		
	3	39	3		315	- <u>-</u>	. 0	/8	09	; ip
	9	- 39	18	3	<u> </u>		· · - · · · ·	<u></u>	30	15
	9	- 39	33	3	-4	3	⊢°	-6		· 14
	9	39	48	3	-4	3	<u> </u>	·ŏ	30	·
	9	40	3	3	-4	<u> 3</u>	ļ <u>0</u>		- <u>- 36</u>	
	9	40	19	0	-5	4		-6	35	12
	9	40	34		-5	4	0	·	35	· · ·- <u>!</u> !
	9;	40	49	0	-5	4	0	-6	35	
	9!	41	4	0	-5	4	0	-6	35	10
<u> </u>	9	41	19	0	-5	2	0	-6	35	10
	9	41	34	0	-5	2	i0	-6	35	9
L	9	41	49	0	-5	0	0	-6	. 35	i 9

CRTF	NET-90 99	POINT D	ATA FIL	E	Check	4'	6"
TEST	DATE: Tue	May 3	1994 8	3:52:37	valve	flange	flange
Time	Time	Time	FT	720	TEPL-5	TEPL-8	TEPL-12
hour	min	sec	Lt/i	min	DEG F	DEG F	DEG F
	8	53	3	0	72	69	92
	8	53	18	0	72	69	92
	8	53	33	0	72	69	92
	8	53	48	0	72	70	92
	8	54	3	0	72	70	92
ľ	8	54	19	ō	72	70	92
	8	54	34	0	72	70	92
	8	54	49	0	71	68	91
	8	55	4	0	71	68	91
	8	55	19	0	71	68	91
	8	55	34	0	71	68	91
	8	55	49	0	72	70	92
	8	56	4	0	72	70	92
	8	56	18	0	72	70	92
	8	56	33	0	72	70	92
• •	8	56	48	0	72	69	92
	8	57	3	0	72	69	92
	8	57	18	323	72	69	92
	8	57	33	355	134	69	92
	8	57	48	361	223	80	98
	8	58	3	361	279	105	122
	8	58	18	361	329	154	145
	8	58	33	361	367	191	168
	8	58	48	360	391	241	193
	8	59	3	360	415	283	228
	8	59	18	360	438	320	265
ľ	8	59	33	360	451	344	288
	8	59	49	360	461	367	311
	9	0	4	360	472	390	336
-	9	0	19	360	484	402	347
ľ	9	0	34	360	496	414	372
	9	0	49	361	507	425	384
	_ 9	1	4	361	507	425	384
	9	1	19	361	518	437	395
	9	1	34	361	518	448	407
	9	1	49	359	530	448	407
	9	2	3	359	530	448	418
	9	2	18	359	541	461	418
	.9	2	33	359	541	461	429
	9	2	48	359	541	461	429
	9	3	3	359	552	. 472	441
1	9	3	18	359	552	. 472	441
	9	3	33	359	552	472	441
1	9	3	48	357	552	472	441
-	9	. 4	3	357	561	482	452
	9	4	18	357	561	482	452
	9	<u> 4 </u>	33	357	561	482	452
1	9	4	49	361	561	482	461

Thermal Shock Data for Components

Time	Time	Time	F	-T720	TEPL-5	TEPL-8	TEPL-12
hour	min	sec	Ĺ	_t/min	DEG F	DEG F	DEG F
	9	5	4	361	568	492	461
	9	5	19	361	568	492	461
	9	5	34	361	568	492	461
	9	5	49	359	568	492	472
· ·	9	6	4	359	572	500	472
	9	6	19	359	572	500	472
	9	6	34	359	572	500	472
}	9	6	48	358	572	500	479
)	9	7	3	358	575	505	479
1	9	7	18	358	575	505	479
	9	7	33	358	575	505	479
	9	7	48	358	575	505	488
	9	8	3	358	575	512	488
	9	8	18	358	578	512	488
	9	8	33	358	578	512	488
4	9	8	48	359	578	512	495
	9	9	3	359	578	516	495
	9	9	19	359	579	516	495
	9	9	34	359	579	516	495
	9	9	49	360	579	516	502
	9	10	4	360	579	523	502
	9	10	19	360	581	523	502
·	9	10	34	360	581	523	502
	9	10	49	359	581	523	507
	9	11	3	359	581	526	507
	9	11	18	359	581	526	507
	9	11	33	359	581	526	507
	9	11	48	358	581	526	507
ļ	9	12	3	358	581	530	512
ļ	9	12	18	358	583	530	512
	9	12	33	358	583	530	512
	9	12	48	358	583	530	512
	9	13	3	358	583	535	518
	9	13	19	358	584	535	518
	9	13	34	358	584	535	518
	9	13	49	358	584	535	518
	9	14	4	358	584	537	522
	9	14	19	358	584	537	522
	9	14	34	358	584	537	522
	9	14	49	358	584	537	522
	9	15	4	358	584	542	526
	9	15	18	358	586	542	526
}	9	15	33	358	586	542	526
	9	15	48	357	586	542	526
1 .	9	16	3	357	586	544	530
}	9	16	18	357	585	544	530
}	9	16	33	357	585	544	530
1	9	16	48	357	585	544	530
1	9	17	3	357	585	548	533
	9	17	18	357	586	548	533

Thermal Shock Data for Components

Time	T	ime	Time	F	T720	TEPL-5	TEPL-8	TEPL-12
hour	n	nin	sec	Ĺ	/min	DEG F	DEG F	DEG F
F	9		17	33	357	586	548	533
1	9		17	49	358	586	548	533
Ĩ	9		18	4	358	586	551	537
}	9		18	19	358	587	551	537
	9		18	34	358	587	551	537
	9		18	49	358	587	551	537
	9		19	4	358	587	552	540
ļ	9		19	18	358	587	552	540
[9		19	33	358	587	552	540
	9		19	48	358	587	552	540
	9		20	3	358	587	556	543
ľ	9		20	18	358	588	556	543
1	9_		20	33	358	588	556	543
	9		20	48	359	588	. 556	543
	9		21	4	359	588	557	545
	9		21	19	359	588	557	545
	9		21	34	359	588	557	545
	9		21	49	360	588	557	545
	9		22	4	360	588	557	548
	9		22	19	360	590	561	548
	9		22	34	360	590	561	548
	9		22	49	357	590	561	548
	9		23	4	357	590	561	550
	9		23	19	357	590	562	550
	9		23	34	357	590	562	550
	9		23	49	357	590	562	550
	9		24	3	357	590	562	552
	9		24	18	357	591	564	552
	9		24	33	357	. 591	564	552
	9		24	48	357	591	564	552
	9		25	3	357	591	564	555
	9		25	18	357	591	567	555
	9		25	33	357	591	567	555
	9		25	48	357	591	567	555
	9		26	3	357	591	567	556
	9		26	19	357	591	567	556
	9		26	34	357	591	567	556
	9		26	49	357	591	567	556
	9		27	4	357	591	567	558
	9		27	19	357	591	570	558
	9		27	34	357	593	570	558
ſ	9		27	48	356	593	570	558
ľ	9		28	3	356	593	570	560
[9		28	18	356	593	570	560
	9		28	33	356	592	570	560
	9		28	48	358	592	570	560

Data for Slow Cool Down of Components with Fan Simulating Nightly Cool Down.

		Check 4"fla	6"fla	
	Time Z 521	Z 522 Z 523	Z 524 Z	525
OCT20 1993 12:28:20 12 28 2	20 12.5 583	585 585	582	575 DEG F
OCT20 1993 12:43:20 12 43 2	0 12.7 586	588 588	586	581 DEG F
OCT20 1993 12:58:20 12 58 2	0 13.0 592	594 594	591	586 DEG F
OCT20 1993 13:13:20 13:13 2	20 13.2 574	582 579	581	575 DEG F
OCT20 1993 13:28:20 13 28 2	20 13.5 572	566 559	561	560 DEG F
OCT20 1993 13:43:20 13:43 2	20 13 7 584	550 539	543	546 DEG E
OCT20 1993 13:58:20 13 58 2	20 14 0 586	533 519	526	532 DEG E
OCT20 1993 14:13:20 14 13 2	0 14.2 579	518 501	506	524 DEG E
OCT20 1993 14:18:20 14 18 2	0 14.5 589	502 482		505 DEG E
OCT20,1993,14:43:20, 14, 43, 2	20 14.7 570	486 462	466	485 DEG E
OCT20 1993 14:58:20 14 58 2	0 15.0 591	460 402	400	474 DEG E
OCT20,1930 14:00:20 14 00 2	0 15.2 567	454 424	432	456 DEG E
OCT20,1993 15:28:20 15 28 2	0 15.5 585		415	438 DEG E
OCT20,1993 15:20:20 15 20 2	0 15.7 569	407 400	300	429 DEG E
OCT20,1993 15:59:20 15 59 2	0 16 0 575	423 330	384	412 DEG E
OCT20,1993 15:58:20 15 58 2	10 160 575	400 374	370	306 DEG E
OCT20,1993 10.13.20 10 13 2	0 16 5 572	270 242	259	390 DEG E
OCT20,1993 10.28.20 10 28 2	0 10.5 504	370 343	300	350 DEG F
OCT20,1993 16.43.20 16 43 2	0 10.7 575	250 217		360 DEG E
OCT20, 1993 10:58:20 10 58 2		30 317	202	300 DEG F
OCT20,1993 17:13:20 17 13 2	0 17.2 573	- 339 304	211	333 DEG F
00120,1993 17:28:20 17 28 2	<u>0 17.5 554</u>	321 292	201	339 DEG F
OCT20, 1993 17:43:20 17 43 2	0 17.7 575	315 202		334 DEG F
OCT20,1993 17:58:20 17 58 2		304 272	291	323 DEG F
OCT20, 1993 18:13:20 18 13 2	0 10.2 572	294 201	202	310 DEG F
OCT20, 1993 18:28:20 18 28 2	0 10.0 501	203 232	. 213	
00120,1993 18:43:20 18 43 2	0 18.7 571	273 243	200	290 DEG F
00120,1993 18:58:20 18 58 2		204 200	200	
OCT20, 1993 19:13:20 19 13 2	10. 10.5 5/0	255 227		264 DEG F
OCT20, 1993 19.28.20 19 28 2	0 19.5 547	24/ 210	241	271 DEG F
OCT20,1993 19.43.20 19 43 2		239 212	204	209 DEG F
OCT20, 1993 19:58:20 19 58 2	20.0 547	232 205	221	261 DEG F
OCT20,1993 20:13:20 20 13 2	20.2 500	224 198	221	250 DEG F
		210 192	215	
00120,1993,20:43:20,20,43,2	20 20.7 567	211 186	209	242 DEG F
00120,1993 20:58:20 20 58 2	20 21.0 545	205 181	204	234 DEG F
OC120,1993 21:13:20 21 13 2	20 21.2 565	199 176	199	234 DEG F
OCT20,1993 21:28:20 21 28 2	20 21.5 542	194 1/1	194	224 DEG F
OCT20,1993 21:43:20 21 43 2	20 21.7 563	188 166	189	223 DEG F
OCT20,1993 21:58:20 21 58 2	20 22.0 547	183 162	185	217 DEG F
00120,199322:13:20 22 13 2	20 22.2 562	179 157	. 181	208 DEG F
UCT20,1993 22:28:20 22 28 2	20 22.5 544	174 153	177	211 DEG F
OCT20,1993 22:43:20 22 43 2	20 22.7 567	170 149	172	203 DEG F
OCT20,1993 22:58:20 22 58 2	20 23.0 541	165 144	168	198 DEG F
OCT20,1993 23:13:20 23 13 2	20 23.2 564	162 142	166	199 DEG F
OCT20,1993 23:28:20 23 28 2	20 23.5 538	159 139	162	190 DEG F
OCT20,1993 23:43:20 23 43 2	20_23.7_563	155 135	159	192 DEG F
OCT20,1993 23:58:20 23 58 2	20 24.0 539	151 132	156	187 DEG F

Data for Slow Heat Up of Components with Two Heat Trace Circuits.

Heatup With Two Circuits						
	CheckV	4"Flange	6"flange			
Time,hr	TEPL-4	TEPL-8	TEPL-10			
0	104.8205	104.8205	104.8205			
0.4135	137.351	169.8815	148.1945			
0.827	202.412	281.931	238.557			
1.2405	245.786	354.221	289.16			
1.654	285.5455	401.2095	354.221			
2.0675	325.305	433.74	397.595			
2.481	383.137	484.343	444.5835			
2.8945	379.5225	469.885	448.198			
3.308	404.824	502.4155	495.1865			
3.7215	415.6675	502.4155	495.1865			
4.135	422.8965	506.03	502.4155			
4.5485	433.74	516.8735	516.8735			
4.962	448.198	527.717	527.717			
5.3755	459.0415	538.5605	538.5605			
5.789	451.8125	520.488	520.488			

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