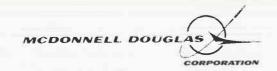


MOLTEN SALT ELECTRIC EXPERIMENT (MSEE)

System Operation



MCDONNELL DOUGLAS CORPORATION

Molten Salt Electric Experiment
(MSEE) System Operation

MOLTEN SALT ELECTRIC EXPERIMENT (MSEE)

SYSTEM OPERATION

31 AUGUST 1984



FORWARD

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MSEE Evaluation Plan

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Phase II Test Plan

Plan for tests during Phase II which will provide data needed for evaluation.

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Section 1 INTRODUCTION

1.1 BACKGROUND

Solar thermal central receiver systems have been under development since the early seventies. The first central receiver system in the United States (Solar One) uses water/steam as a heat transfer fluid in the receiver. Subsequent studies and test programs investigated molten salt, liquid sodium, and hot air as heat transfer fluids. They all possess certain advantages over water/steam, but many feel that molten nitrate salt is the most promising heat transfer fluid, particularly for utility-scale electric power plants with thermal storage.

A complete molten salt system experiment has been built at the Department of Energy (DOE) Central Receiver Test Facility (CRTF) located at Kirtland Air Force Base, Albuquerque, New Mexico. The CRTF heliostat field concentrates reflected solar energy onto a molten salt cooled solar receiver located on top of the 200-foot-tall CRTF test tower. Molten salt is pumped from a "warm" salt storage tank at ground level up the tower to the solar receiver where it is heated by absorbing solar energy and then returns to a "hot" salt storage tank at ground level. A hot salt pump delivers salt from the hot tank to a molten salt steam generator which produces steam to power a turbine/generator which feeds electricity into the local power grid.

This experiment is being conducted in two phases. The Phase I design, construction, installation, checkout, and verification effort has been completed. In Phase II, system characterization tests are being performed and the system will be operated and evaluated by utility and industry personnel. This document provides the data to be utilized by the utility and industry participants in their training and operation. The system may be run for an additional period in a potential third phase.

A consortium consisting of utilities, industries and the Electric Power Research Institute (EPRI), has helped construct and support operation of the experiment. The consortium is supplying half of the project's funding through either cash contributions or donations of in-kind engineering services. The other half is supplied by the DOE, through Sandia.

1.2 OBJECTIVES

The MSEE is designed as a first full-system experiment of future large-scale, central station power plants. The test and evaluation program is designed to provide data to be used in the design and operation of these commercial plants. This will be accomplished by a thorough characterization of the MSEE itself and by identifying features that should be changed in a commercial plant or its prototype. Operation of the MSEE by utility and industry personnel can make a significant contribution to this evaluation as well as provide familiarization with the operation of this type of solar power plant. Accordingly, the specific objectives of this operational phase are:

- Demonstrate operation of a molten salt cooled central receiver solar power plant to participating utility and industry personnel. This also demonstrates power plant control by a distributed digital central system.
- 2. Obtain an evaluation by the participants of the MSEE design and operation and of the training methods employed in this program.

Section 2 TRAINING AND OPERATING SESSIONS APS TEAM (SEPTEMBER 24 - OCTOBER 12, 1984)

Monday, September 24 -- Orientation and Master Control Subsystem

8:00	Introduction Conference Room
9:00	CRTF Projects Review and Safety Briefing Conference Room
9:30	Break
9:45	MSEE System Overview Conference Room
10:00	Tour of MSEE Field and Control Room
11:30	Discussion and Questions Conference Room
12:00	Master Control Subsystem Conference Room (Sections 3.2 and 4)
1:00	Console Operation Control Room (Sections 4 and 5.1.1)
4:00	Complete

Tuesday, September 25 -- Receiver and Thermal Storage Subsystems (Sections 3.3 and 3.4)

8:00	Subsystem Description Conference Room
9:00	Tour of Receiver and Thermal Storage Subsystems Tower and
	Field
10:00	Control Loops and Instrumentation Conference Room
11:00	Operation, Alarms and Trips Conference Room
12:00	Training - Receiver Loop Operation Conference Room
	(Section 7 and P&ID)
	Check Lists
	Procedures
	Console Instruction (individually in Control Room)
	(Sections 5.1.2, 5.1.3, and 5.1.4)
4:00	Complete

Wednesday, September 26 -- Receiver Operations

```
8:00
                  Training - Receiver Loop Operation -- Conference Room
                  Receiver Start-up Using Simulation -- Control Room (rotate
                  groups)
       11:00
                  Test on Receiver Loop Start-up and Operation -- Conference
                  Room
       12:00
                  Receiver Cold Flow -- Control Room (Section 5.2.1).
        4:00
                  Complete
Thursday, September 27 -- Receiver Operation
        8:00
                  Receiver Steady State Operation (Section 5.2.2).
        4:00
                  Complete
Friday, September 28 -- Receiver Loop Operation
        8:00
                  Receiver Cold Flow (Section 5.2.1) -- Control Room
       10:00
                  Receiver Operation with Simulated Clouds (Section 5.2.3) --
                  Control Room
        4:00
                  Complete
Monday, October 1 -- Steam Generation Subsystem (Sections 3.5 and 3.7)
        8:00
                  Subsystem Description -- Conference Room
        9:00
                  Tour of Steam Generator and HRFS Subsystems -- Field
       10:00
                  Control Loops and Instrumentation -- Conference Room
       11:00
                  Operations, Alarms and Trips -- Conference Room
       12:00
                  Training - Steam Generator Operation -- Conference Room
                  (Section 7 and P&ID)
                    Check Lists
                    Procedures
                    Console Instruction (individually in Control Room
                      (Section 5.1.5)
```

4:00

Complete

Tuesday, October 2 -- Steam Generator Operation

The second of th

8:00	Training Steam Generator Operation Conference Room
11:00	Test on Steam Generator Start-up and Operation Conference
	Room
12:00	Steam Generation Operation (Section 5.2.5) Control Room
4:00	Complete

Wednesday, October 3 -- Charge Thermal Storage with Propane Heater, Operate Steam Generator

8:00	Thermal Storage Charging with Propane Heater (Section 5.2.4)
	Control Room
12:00	Steam Generator Operation (Section 5.2.5) Control Room
4:00	Complete

Thursday, October 4 -- Electric Power Generation Subsystem (Sections 3.6 and 3.7)

8:00	Subsystem Description Conference Room
9:00	Tour of EPGS and HRFS Field
10:00	Control Loops and Instrumentation Conference Room
11:00	Operations, Alarms and Trips Conference Room
12:00	Training - EPGS Operation - Conference Room
	(Section 7 and P&ID)
4:00	Complete

```
Friday, October 5 -- Operation of EPGS
```

8:00 Operation of Full Electric Loop (Section 5.2.6) -- Control

Room and field

Teams will rotate between Control Room and Turbine Room in

A.M. and P.M.

4:00 Complete

Monday, October 8 -- System Operation

8:00 Discussion of System Operation -- Conference Room

10:00 System Steady State Operation (Section 5.2.7) -- Control

Room and field

Rotate groups between locations

4:00 Complete

Tuesday, October 9 -- System Operation

8:00 System Steady State Operation

(Section 5.2.7)

EPGS Steady State Performance

(Section 5.2.8)

Rotate groups between Control Room and field

4:00 Complete

Wednesday, October 10 -- System Operation

8:00 System Steady State Operation

(Section 5.2.7)

EPGS Steady State Performance

(Section 5.2.8)

Rotate groups between Control Room and field

4:00 Complete

Thursday, October 11-- System Operation and Debriefing

8:00	System Steady State Operation (Section 5.2.7) Control
	Room and field
12:00	Debriefing Conference Room
2:00	Briefing on Solar One
4:00	Complete

Friday, October 12 -- Tour of Solar One
System Operation
Controls

Section 2 TRAINING AND OPERATING SESSIONS PNM TEAM (SEPTEMBER 4 - 21, 1984)

Tuesday, September 4 -- Orientation and Master Control Subsystem

8:00	Introduction Conference Room
9:00	Safety Briefing Conference Room
9:30	Break
9:45	MSEE System Overview Conference Room
10:00	Tour of MSEE Field and Control Room
11:30	Discussion and Questions Conference Room
12:00	<pre>Master Control Subsystem Conference Room (Sections 3.2 and 4)</pre>
1:00	Console Operation Control Room (Sections 4 and 5.1.1)
4:00	Complete

Wednesday, September 5 -- Receiver and Thermal Storage Subsystems (Sections 3.3 and 3.4)

8:00	Subsystem Description Conference Room
9:00	Tour of Receiver and Thermal Storage Subsystems Tower and
	Field
10:00	Control Loops and Instrumentation Conference Room
11:00	Operation, Alarms and Trips Conference Room
	(Section 7 and P&ID)
	Check Lists
	Procedures
	Console Instruction (individually in Control Room)
	(Sections 5.1.2, 5.1.3, and 5.1.4)

4:00 Complete

Thursday, September 6 -- Receiver Operations

```
8:00 Training - Receiver Loop Operation -- Conference Room
Receiver Start-up Using Simulation -- Control Room (rotate
groups of two)

11:00 Test on Receiver Loop Start-up and Operation -- Conference
Room

12:00 Receiver Cold Flow -- Control Room and Field (Section 5.2.1).
Rotate groups of two in Control Room and two in field.
```

4:00 Complete

Friday, September 7 -- Receiver Operation

8:00	Receiver Steady State Operation (Section 5.2.2).
	Rotate groups of two in Control Room and two in field.
4:00	Complete

Monday, September 10 -- Steam Generation Subsystem (Sections 3.5 and 3.7)

8:00	Subsystem Description Conference Room
9:00	Tour of Steam Generator and HRFS Subsystems Field
10:00	Control Loops and Instrumentation Conference Room
11:00	Operations, Alarms and Trips Conference Room
12:00	Training - Steam Generator Operation Conference Room
	(Section 7 and P&ID)
	Check Lists
	Procedures
	Console Instruction (individually in Control Room)
	(Section 5.1.5)

4:00 Complete

Tuesday, September 11 -- Steam Generator Operation

8:00 Training -- Steam Generator Operation -- Conference Room

11:00 Test on Steam Generator Start-up and Operation -- Conference Room

12:00 Steam Generation Operation (Section 5.2.5) -- Control Room and Field

One group of two in Control Room; other group of two in field

4:00 Complete

Wednesday, September 12 -- Charge Thermal Storage with Propane Heater, Operate Steam Generator

8:00 Thermal Storage Charging with Propane Heater (Section 5.2.4)

-- Control Room and Field

12:00 Steam Generator Operation (Section 5.2.5) -- Control Room and field. Rotate groups from Tuesday P.M. assignments

Thursday, September 13 -- Receiver Loop Operation

8:00 Receiver Cold Flow (Section 5.2.1) -- Control Room and field
12:00 Receiver Operation with Simulated Clouds (Section 5.2.3) -Control Room and field
4:00 Complete

Friday, September 14 -- Electric Power Generation Subsystem (Sections 3.6 and 3.7)

8:00 Subsystem Description -- Conference Room
9:00 Tour of EPGS and HRFS -- Field
10:00 Control Loops and Instrumentation -- Conference Room
11:00 Operations, Alarms and Trips -- Conference Room
12:00 Training - EPGS Operation - Conference Room
(Section 7 and P&ID)
4:00 Complete

Monday, September 17 -- Operation of EPGS

8:00 Operation of Full Electric Loop (Section 5.2.6) -- Control Room and field

Team of two will rotate between Control Room and Turbine Room in A.M. and P.M.

4:00 Complete

Tuesday, September 18 -- System Operation

8:00	viscussion or System uperation Conference Room
10:00	System Steady State Operation (Section 5.2.7) Control
	Room and field
	Rotate groups of two between locations
4:00	Complete

Wednesday, September 19 -- System Operation

8:00 System Steady State Operation
(Section 5.2.7)
EPGS Steady State Performance
(Section 5.2.8)
Rotate groups of two between Control Room and field

4:00 Complete

Thursday, September 20 -- System Operation and Debriefing

8:00	System Steady State Operation (Section 5.2.7) Control
	Room and field
12:00	Debriefing Conference Room
4:00	Complete

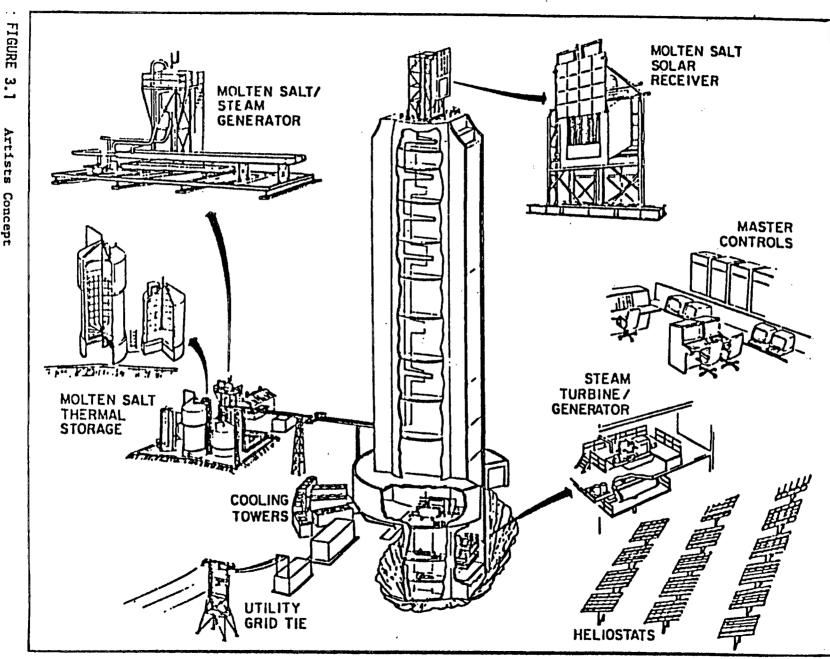
Friday, September 21 -- Tour of Solar One System Operation Controls

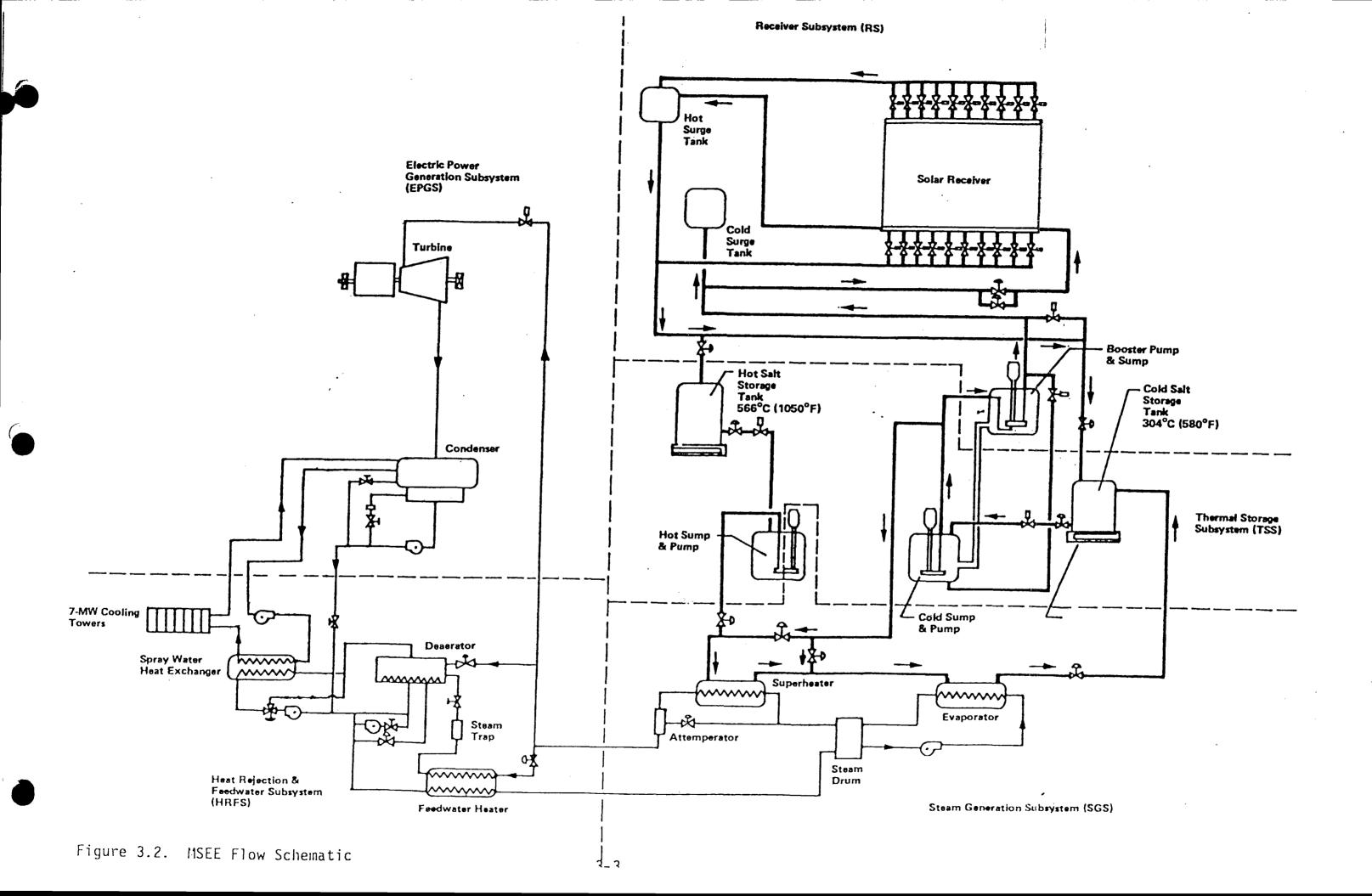
Section 3 MSEE SYSTEM DESCRIPTION

The MSEE system is shown as an artist's concept in Figure 3.1. It is designed to demonstrate the conversion of solar energy to electricity using molten salt and water/steam as the working fluids. The molten salt is the energy transfer medium from the receiver through thermal storage to the steam generation subsystem and water/steam is the energy transfer medium from the steam generation subsystem to the electric power generation subsystem. The system schematic is shown in Figure 3.2. The receiver, located at the top of the CRTF tower, receives concentrated solar energy from the collector field. Molten salt from the cold storage tank, located at ground level, is pumped up the tower piping and through the receiver. In the experiment, cold salt is nominally defined to have a temperature of 306°C (580°F). The salt is heated to 1000° in the receiver, flows through a downcomer, and is throttled into the hot salt storage tank. Hot salt is defined to have a nominal temperature of 1000°. Hot salt from storage is pumped through the steam generator superheater and evaporator, and is returned to the cold storage tank. An additional flow of cold salt is injected in the salt line between the superheater and evaporator to reduce the salt temperature entering the evaporator; this is to allow the use of low alloy steel in the evaporator. Main steam from the steam generator is used to drive a conventional steam turbine-generator. There are two principal advantages of this molten salt receiver system over a water/steam receiver system: the steam generator and turbine are decoupled from the receiver by the thermal storage subsystem: and. molten salt from the receiver is used directly as the thermal storage fluid. thus providing an inexpensive source of thermal storage and a constant temperature heat source for the steam generator.

The system is divided into the following subsystems:

- a) Collector (CS)
- b) Master Control (MCS)
- c) Receiver (RS)
- d) Thermal Storage (TSS)
- e) Steam Generation (SGS)
- f) Heat Rejection and Feedwater (HRFS)
- g) Electric Power Generation (EPGS)





A tabulation of data describing the MSEE system is given on Table 3.1. A more detailed description of the MSEE subsystems is contained in the following subsections.

3.1 COLLECTOR SUBSYSTEM

The collector subsystem redirects, concentrates, and focuses solar radiation onto the tower-mounted receiver. The subsystem, which is already in place at the CRTF, consists of 221 two-axis tracking heliostats located north of the receiver tower, and its control system. Under optimum insolation and heliostat conditions, the heliostat field can concentrate approximately 5 MW, onto the receiver.

Each heliostat has 25 individual mirror facets totaling 37.2 m^2 (400 ft^2) of reflective surface. The facets are mounted on a structure and individually adjusted to provide a concentration ratio of 25 to 1 on the receiver. The structure has motor-driven azimuth and elevation gimbals, which allow it to track the sun during the day.

The heliostats are operated from the control room by the CRTF collector control system. (The CRTF collector control system is separate from the experiment master control subsystem.) The CRTF collector control system analyzes heliostat operating commands from a number of programmed test sequences or from the facility heliostat operator. Control signals are distributed to the heliostats through four heliostat array controllers and four heliostat interface modules. Each heliostat receives azimuth and elevation pointing information once every second and responds with its own status. Commands and data transmitted to the individual heliostats are received and executed by the heliostat control electronics. The electronics keep the drive motor power at the proper level until the gimbal axis encoders indicate that the desired position has been reached.

Location -- CRTF; on Kirtland Air Force Base, Albuquerque, NM
Heliostat Field -- Existing field of 221 heliostats each with 400 ft² of
mirror surface.

Tower -- Existing concrete tower, 200 ft. high with internal lifting module Master control -- EMCON D-2 distributed digital control system with central consoles; separate equipment protection system.

Receiver -- Refurbished from previous Subsystem Research Experiment.

- o Rating: 5 MW_{th}
- o Salt temperatures: in 590°F; out 1000°F (1050°F with propane heater)
- o Configuration: cavity with door
- o Absorber: single panel of 3/4 in Incoloy 800 tubes (18 passes, 16 tubes per pass)
- o Peak flux: 630 kW/m² (200,000 Btu/hr ft^2)

Thermal Storage -- Existing from previous Subsystem Research Experiment

- o Rating: 5.8 MW_{th} Hr when operating between 590°F and 1000°F
- o Type: 2-tank
 - Hot tank, internal insulation
 - Cold tank, external insulation

Steam Generator -- Supplied by Babcock and Wilcox

- o Type: Forced recirculation
- o 2 units: evaporator and superheater (both U-tube, U-shell) with steam drum separator
- o Rating: 11,000 lb/hr of steam at 940° F and 1100 psi (3.13 MW_{th})
- o Prototypical of commercial design

Turbine Generator -- GE rebuilt unit

- o Marine turbine
- o 750 kW $_{\rm e}$ rating (500 kW $_{\rm e}$ under nominal operating conditions)

Heat Rejection and Feedwater System -- existing at CRTF

- o Feedwater treatment only
- o 20,000 gallon demineralized water storage
- o Dry cooling, 7 MW_{th} capacity
- o Spray water heat exchanger to reject heat when turbine not in use or tripped off line

3.2 MASTER CONTROL SUBSYSTEM

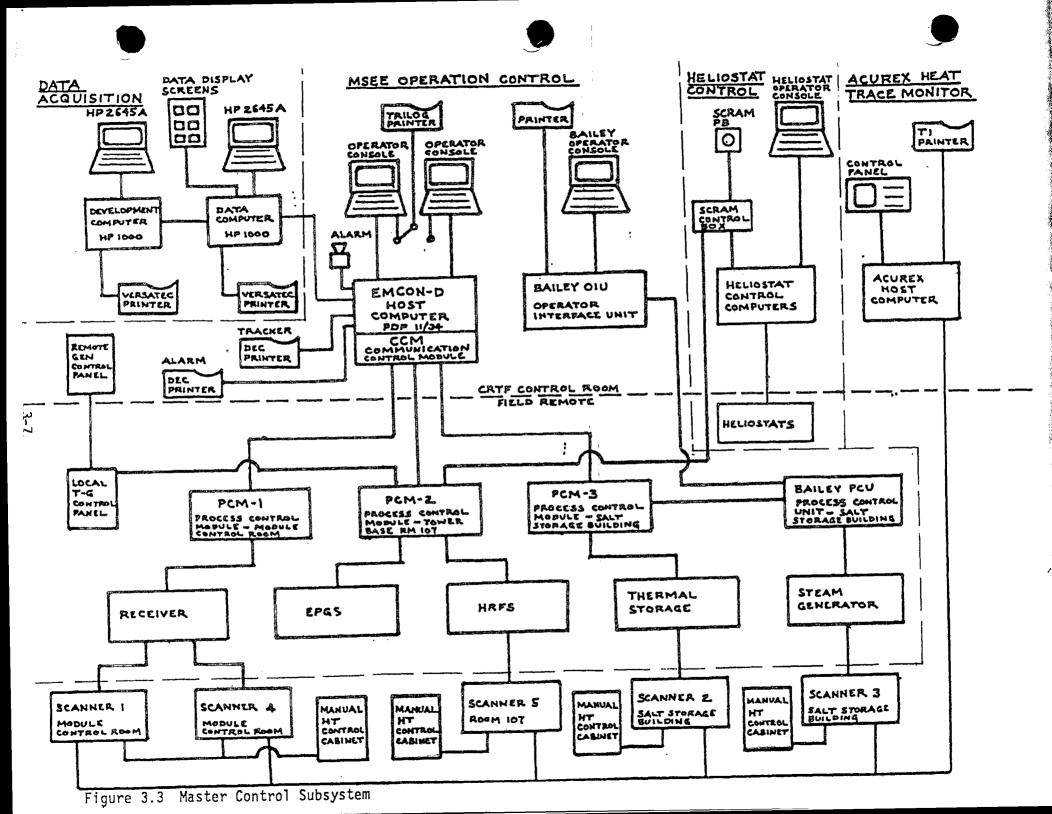
The master control subsystem (Figure 3.3) consists of an EMCON-D2 for system control and a equipment protection system. A Bailey network 90-system is used to directly control the SGS. Commands and set points are provided by the EMCON master control subsystem to the Network 90 for SGS operation and control. The equipment protection system is an independent hardwired relay shutdown system. These relay trip devices will shut down the receiver or the power generation ends of the MSEE when critical parameters reach preset limit values. These relay units are independent of the EMCON and network 90 control systems. Additionally, an Accurex Data Logger is used to collect and display all the temperature measurements relating to the heat tracing and data instrumentation.

3.2.1 EMCON System

The EMCON-D2 is a distributed digital control system consisting of two operator consoles, a host computer with its peripheral hardware, a communication control module, and three process control modules distributed among the subsystems. Two EMCON-D2 operator consoles are located in the CRTF main control room. The host computer is an existing DEC PDP 11/34 unit located in the control room. This computer links the operator with the process control modules, and analyzes data from the control modules for presentation on the operator consoles. The peripheral equipment includes two disk drives, an alarm system, and a data analysis system.

A communication control module links the host computer with the three field-located, process control modules. Each process control module is a small digital computer capable of monitoring a number of instrumentation points, and responding with a number of process control signals. Communications between the control modules and host computer are primarily limited to direct operator commands from the console and critical operating information from the subsystems for console display. This distributed control system reduces the number of instrumentation and control links between the subsystems and control room.

The process control module consists of a digital computer control unit, a multiplexer, an analog-to-digital converter, and a digital-to-analog converter. Analog signals from the process instrumentation are converted to



digital signals, selected in rotation by the multiplexer, and analyzed by the control unit. The module responds with an appropriate digital control signal which is passed through the multiplexer and sent to the appropriate controller. Each process control module is capable of monitoring 30 analog signals per second, monitoring 95 thermocouples, generating 20 analog control signals, and controlling over 100 on-off switches.

One process control module (PCM 1), located below the receiver in the tower elevator, is dedicated to the control of the receiver. A second module, (PCM 2) located at the base of the tower, controls the heat rejection and electric power generation subsystem. The third module, (PCM 3), located in the control building adjacent to the salt storage tanks, is used to control the thermal storage subsystem and to command the Network 90 controlled steam generation subsystem.

The receiver subsystem PCM will modulate the salt flow rate to the receiver to maintain, as closely as possible, a constant outlet temperature of 1000°F. Individual thermocouples are located on the receiver to measure intermediate salt temperatures. From this information, the control module estimates the flux on the receiver, and feed-forward a signal to the salt control valves at the receiver inlet. The control module also controls the receiver start-up and shutdown purge and drain valves.

Control of the thermal storage subsystem involves the operation of the two salt downcomer flow control valves, cold salt pumps, salt storage tanks and piping heat tracing, and the propane-fired salt heater. The downcomer throttling valves are controlled by the receiver control system to maintain a constant level in the receiver hot surge tank. Salt equipment heat trace temperatures are monitored continuously by the Acurex Data Logger. The propane-fired salt heater is operated intermittently, under manual control, during subsystem checkouts.

Automatic control of the heat rejection and electric power generation subsystem involves the control of the steam and condensate flows to the deaerator, steam flow to the feedwater heater, and the operation of the cooling water, spray water condensate, and feedwater pumps. The EPGS condenser

temperature, level and pressure are monitored by the master control subsystem. The deaerator temperature is maintained by controlling the steam flow from the main steam header. The final feedwater temperature is maintained by controlling the main steam flow to the feedwater heater.

Automatic control of the steam generation subsystem primarily involves the control of steam pressure, steam temperature, drum water level, and the evaporator salt inlet temperature through the network 90 control system. The water level in the drum is controlled by modulating the control valve downstream of the feedwater pump. Control of the main steam pressure is accomplished by modulating the salt flow control valve downstream of the evaporator. Steam temperature is controlled using an attemperator to mix steam from the steam drum with the output of the superheater. The evaporator salt inlet temperature is controlled by monitoring the inlet salt temperature, and modulating the cold salt control valve at the mixing tee between the superheater and evaporator.

3.2.2 Network 90 System

The Bailey Network 90 Control System consists of two units, one process control unit (PCU) and one operation interface unit (OIU).

The PCU architecture is based on two key modules, the Controller Module (COM) and the Logic Master. Together, these modules provide a mix of both modulating and sequential control functions including: base, cascade, or ratio PID control, high/low and rate limiters, engineering units conversion, general function generator, square root, summation, multiplication, lead/lag, and transfer select, or, and, not, time delay, and several others. The controller module can service up to four analog and three digital inputs and two analog and four digital outputs. The COM also provides A/D and D/A conversion, alarm limit checking (absolute and deviation) and notification, point quality checking and interlocking.

The Operator Interface Unit (OIU) provides the high level operator interface for the Network 90 system. The OIU consists of a color CRT-based table-top console, with functional keyboard, mass storage device, and console driver electronics.

In operation, the unit performs the system information display and control requirements. The OIU console includes a CRT keyboard and pushbutton hardware for process overview, alarm indicating, loop control, trending, tuning and configuration functions.

The OIU uses microprocessor, memory and I/O modules to support system functions. It furnishes monitoring, supervisory, recording and display capability at centralized or distributed locations, along with engineering functions.

3.2.3 Data Acquisition

The DAS utilizes both the EMCON-D2 and an HP-1000. EMCON collects the data and HP-1000 stores and displays data. Data collected by the EMCON system is transmitted to the HP-1000 system on a terminal-to-terminal data link. The tag list for the data to be collected is in a file of 180 tags, which are divided into 6 groups of 30 tags. One group of 30 is transmitted every 10 seconds, giving a total update rate of once a minute. The data are then time tagged with day of the year, hour, minute, second, millisecond. Then the data are stored in a data file and/or displayed on one of six CRTs in a graphical form. Also, the data are transmitted in integer format, not floating point, but they are in engineering units. The data files are divided into eight-hour blocks, so if a test runs longer than eight hours, another eight-hour block is assigned to that test's file. Normally an 8-hour data block is stored in 19 tracks out of a maximum usable 1000 tracks.

The live data can be displayed on the 6 CRTs with 3 tags per screen, a time scale of 3 hours 20 minutes, and a Y-scale displayed of the first tag's display range. The other two tags are displayed using their respective ranges, but the scales are not shown on the plot. When the plot is full the plot scrolls left dropping the oldest 1/4 of the time scale data. This leaves 1/4 of the plot blank for new data. These plots can have hard copies made, but not automatically. The print is done by manual switch selection of each screen and a copy page switch.

Recovery of stored data can be done whenever live data files are not being made. These plots have a slightly different format, three being a maximum of five tags per plot, and the Y scale shown is that of the last tags range. These plots are not displayed on a CRT, but directly generated on the printer/plotter.

3.3 RECEIVER SUBSYSTEM

The receiver subsystem (Figure 3.4) captures the insolation redirected from the heliostat field and converts it to thermal energy in the molten salt. The subsystem consists of the receiver absorber panel, cavity enclosure with one vertical aperture door, insulation, heat tracing, cold surge tank, booster pump, hot surge tank, overflow tank, instrumentation, and control valves. The receiver is located at the top of the CRTF tower.

The receiver was tested in a previous subsystem research experiment. Since the initial experiment, the receiver has been refurbished. This refurbishment included instrumentation and control system modifications, minor structural and piping changes, and the replacement of the two original horizontal cavity doors with one vertical aperture door.

The receiver absorber is a single panel with 18 vertical passes having 16 tubes per pass. The tubes are Incoloy 800 with 19 mm (0.75 in.) outside diameter. Purge and drain valves are provided for each pair of passes.

The receiver surge tanks are designed to dampen changes in the salt flow rate and to maintain salt flow through the receiver in the event of a cold salt pump outage. The cold surge tank is pressurized with facility-supplied instrument air to supply the necessary head to force the salt through the receiver in the event of a pump outage, and to provide a surge volume within the tank. The hot surge tank operates at atmospheric pressure, and is vented to an adjacent overflow tank in the event of a control problem in the salt downcomer throttle valve.

The cold salt booster pump takes its suction from the discharge of the cold salt pump and provides the necessary head for the salt as it travels up the tower and through the receiver.

The cold salt line to the receiver starts at the booster pump, rises to the top of the hot storage tank, traverses the distance from the storage tanks to the receiver tower on an elevated pipe bridge, enters the tower, and runs up the east side of the tower in an existing pipe chase to the receiver. The hot salt line leaves the hot surge tank and traverses to the pipe chase. The hot salt downcomer carries the salt to the level of the pipe bridge. The hot salt line traverses the bridge, ending in a control valve which throttles the flow

to the hot storage tank. The salt piping is inclined between the storage tanks and the tower to ensure that the piping system will completely drain. The salt piping is electrically heat traced and insulated with calcium silicate and aluminum sheathing.

The receiver components are listed on Table 3.2; valves are described on Table 3.3; instrumentation is listed on Table 3.4; and control loops are described on Table 3.5.

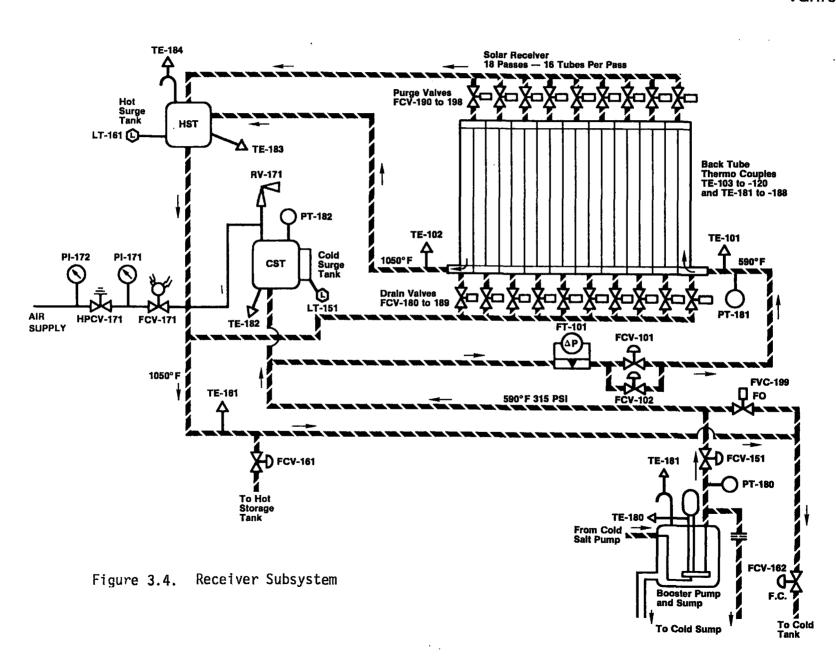


Table 3.2
Receiver Subsystem Components

Component	Description	Function	Nominal Operating Condition
Receiver	 - 18 ft wide x 13 ft high panel - 18 serpentine passes Incoloy 800 tubes 	- Heat molten salt with solar energy from heliostat field	- 590°F inlet salt - 1050°F outlet salt - 96,867 lb/hr
	- 16 tubes per pass - 3/4 in. dia. tubes		- 5 MW rating
Cold salt booster sump	- Carbon steel cylindrical tank	- Reservoir for cold salt pump	- 590°F salt - Atmospheric pressure
Cold salt booster pump	- Vertical cantilever type	- Supply additional head to outlet of cold salt pump to provide salt circulation through receiver	- 590°F salt - 96,867 lb/hr
Cold surge tank	Carbon steel cylindrical tank3 ft. dia.7 ft. high	 Dampen changes in salt flow rate Provide emergency salt flow through receiver until solar flux can be removed in the event of pump outage 	- Pressurized to 125 psi
Hot surge tank	Stainless steel cylindrical tank2 ft. dia.7 ft. high	- Dampen changes in salt flow rate	- Atmospheric pressure



RECEIVER SUBSYSTEM REMOTE OPERATED VALVES

VALVE	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-101 FCV-102	Valtek	2"	CA	FO	Receiver Flow Control	Near Receiver Lower West Corner
FCV-151	Valtek	2"	CA	FC	Receiver Fill Control Cold Surge Level Control	Above Hot Tank
FCV-161	Valtek	2"	CA	F0	Hot Surge Tank Level Control	Above Hot Tank
FCV-162	Valtek	2"	CA	FC	Hot Surge Tank Level Control (Receiver)	Above Hot Tank
FCV-180 thru FCV-189	Kieley-Mueller	1 1/2"	SV	FC	Receiver Fill and Drain	Below Receiver
FCV-190 thru FCV-198	Kieley-Mueller	1 1/2"	SV	FC	Receiver Purge	Above Receiver
FCV-199	Kieley-Mueller	2"	sv 1	FC	Allow Downcomer Backflow During Receiver Fill and	Above Hot Tank
	· ·	*	Calso	valve called to a liver	Permit Drainage to Cold Storage Tank During Shutdown	

Table 3.4
Receiver Subsystem Instrumentation

		Combine	D. C.	Alarm I	Levels		
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Boost Pump						
PT-180	Discharge pressure - gods to	РСМ 3	0-400	350	275	PSI	2
TE-180	Bearing temp	PCM 3	0-500	190		°F	10
TE-181	Sump vent temp Hot surge tank For the second temp to the second temp temp to the second temp temp temp temp temp temp temp temp	PCM 3	0-1200	350		°F	10
LT-161	1 1	PCM 3	0-100	70	15	inch	2
TE-183	Salt temp	PCM 1	0-1200	1070	500	°F	10
TE-184	Vent temp	PCM 1	0-1200	400		°F	10
LT-151	Leve1	PCM 1	0-100	90	10	inch	10
TE-182	Level normation so we dering normal Salt temp	PCM 1	0-1200	750	500	°F	10
PT-182	Pressure	PCM 1	0-200	180	10	PSI	10
TE-161	Downcomer outlet temp	PCM 3	0-1200	1070	500	°F	2
Sun	Solar insolation - not in a	PCM 3	0-1000			W/M ²	5
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Table 3.4
Receiver Subsystem Instrumentation

		Control	Display	Alarm	Levels		
Identifier	Description	Module	Range	High	Low	Dimension	Sampling Period (sec)
	Receiver						
PT-181	Inlet pressure -directly related	PCM 1	0-200	125	10	PSI	10
FT-101	Salt flow rate	PCM 1	0-100	100		KLB/hr	
TE-101	Salt inlet temp	PCM 1	0-1200	650	500	°F	2
TE-102	Salt outlet temp	PCM 1	0-1200	1060	500	°F	2
TE-103	Back tube-pass #1 outlet	PCM 1	0-1200	640	500	°F	2
TE-104	Back tube-pass #2 outlet	PCM 1	0-1200	665	500	°F	2
TE-105	Back tube-pass #3 outlet	PCM 1	0-1200	690	500	°F	2
TE-106	Back tube-pass #4 outlet	PCM 1	0-1200	720	500	°F	2
TE-107	Back tube-pass #5 outlet	PCM 1	0-1200	750	500	°F	2
TE-108	Back tube-pass #6 outlet	PCM 1	0-1200	780	500	°F	2
TE-109	Back tube-pass #7 outlet	PCM 1	0-1200	810	500	°F	2
TE-110	Back tube-pass #8 outlet	PCM 1	0-1200	835	500	°F	2
TE-111	Back tube-pass #9 outlet	PCM 1	0-1200	865	500	°F	2
TE-112	Back tube-pass #10 outlet	PCM 1	0-1200	890	500	°F	2
TE-113	Back tube-pass #11 outlet	PCM 1	0-1200	920	500	°F	2
		•					•
l							

Table 3.4
Receiver Subsystem Instrumentation

		Control	Display	Alarm	Levels		
Identifier	Description	Module	Range	High	Low	Dimension	Sampling Period (sec)
	Receiver (cont.)						
TE-114	Back tube-pass #11 outlet	PCM 1	0-1200	950	500	°F	2
TE-115	Back tube-pass #12 outlet	PCM 1	0-1200	975	500	°F	2
TE-116	Back tube-pass #13 outlet	PCM 1	0-1200	990	500	°F	2
TE-117	Back tube-pass #14 outlet	PCM 1	0-1200	1010	500	°F	2
TE-118	Back tube-pass #15 outlet	PCM 1	0-1200	1030	500	°F	2
<u>~</u> TE-119	Back tube-pass #16 outlet	PCM 1	0-1200	1050	500	°F	2
TE-120	Back tube-pass #17 outlet	PCM 1	0-1200	1070	500	°F	2
TE-131	Back tube-pass #1 upper	PCM 1	0-1200	645	500	°.F	10
TE-132	Back tube-pass #5 upper	PCM 1	0-1200	745	500	°F	10
TE-133	Back tube-pass #8 upper	PCM 1	0-1200	815	500	°F	10
TE-134	Back tube-pass #11 upper	PCM 1	0-1200	915	500	°F	10
TE-135	Back tube-pass #14 upper	PCM 1	0-1200	980	500	°F	10
TE-136	Back tube-pass #17 upper	PCM 1	0-1200	1045	500	°F	10
TE-137	Back tube-pass #2 middle	PCM 1	0-1200	680	500	°F	10
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		·					
			,				

Table 3.4
Receiver Subsystem Instrumentation

		Combus	Dia 7	Alarm I	Levels		
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Receiver (cont.)						
TE-138	Back tube-pass #6 middle	PCM 1	0-1200	735	500	°F	10
TE-139	Back tube-pass #8 middle	PCM 1	0-1200	825	500	°F	10
TE-140	Back tube-pass #11 middle	PCM 1	0-1200	905	500	°F	10
TE-141	Back tube-pass #14 middle	PCM 1	0-1200	990	500	°F	10
TE-142	Back tube-pass #17 middle	PCM 1	0-1200	1045	500	°F	10
TE-143	Back tube-pass #1 bottom	PCM 1	0-1200	660	500	°F	10
TE-144	Back tube-pass #5 bottom	PCM 1	0-1200	725	500	°F	10
TE-145	Back tube-pass #8 bottom	PCM 1	0-1200	830	500	°F	10
TE-146	Back tube-pass #11 bottom	PCM 1	0-1200	895	500	°F	10
TE-147	Back tube-pass #14 bottom	PCM 1	0-1200	985	500	°F	10
TE-148	Back tube-pass #17 bottom	PCM 1	0-1200	1035	500	°F	10
TE-185	Header-pass #2 outlet	PCM 1	0-1200	665	500	°F	10
TE-186	Header-pass #3 outlet	PCM 1	0-1200	690	500	°F	10

Table 3.4
Receiver Subsystem Instrumentation

		Continal	Dia Zana	Alarm L	.evels		
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Receiver (cont.)						
TE-187	Header-pass #4 outlet	PCM 1	0-1200	720	500	°F	10
TE-188	Header-pass #5 outlet	PCM 1	0-1200	750	500	°F	10
TE-189	Header-pass #6 outlet	PCM 1	0-1200	780	500	°F	10
TE-190	Header-pass #7 outlet	PCM 1	0-1200	810	500	°F	10
TE-191	Header-pass #8 outlet	PCM 1	0-1200	835	500	°F	10
의 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전	Header-pass #9 outlet	PCM 1	0-1200	865	500	. °F	10
TE-193	Header-pass #12 outlet	PCM 1	0-1200	950	500	°F	10
TE-194	Header-pass #13 outlet	PCM 1	0-1200	975	500	°F	10
TE-195	Header-pass #14 outlet	PCM 1	0-1200	990	500	°F	10
TE-196	Header-pass #15 outlet	PCM 1	0-1200	1010	500	°F	10
TE-197	Header-pass #16 outlet	PCM 1	0-1200	1030	500	°F	10
TE-198	Header-pass #17 outlet	PCM 1	0-1200	1050	500 .	°F	10

Table 3.5
Receiver Subsystem Control Loops

(ontrolled Variable	Mode	Set Point	Controller Inputs	Controller Output
	Receiver salt flow	Constant flow (start-up & shutdown with receiver con- trol algorithm off scan Constant Outlet Temperature (Receiver con- trol algorithm	30 KLB/hr FD-101 1000°F SP. SALT	Flow set point (FD-101) Measured flow (FT-101) Temperature set point (SP. SALT) Outlet temperature (TE-102) Inlet temperature (TE-101) Salt flow (FT-101) Receiver back tube temperatures (TE-103 thru TE-120)	FCV-101/102 position FCV-101/102 position
3-21	Hot surge tank level	Operation	20 in FCV-161 FCV-162	Surge tank level (LT-161) Level set point	FCV-161 or FCV-162 position (selection based on salt temperature)
	Receiving storage tank selection	Operation	750°F	Downcomer salt temperature (TE-161)	TE-161 < 750°F Cold storage tank selected TE-161 > 750°F Hot storage tank selected
	Cold surge tank level	Operation	~85" LT-151	Cold surge tank level (LT-151) Level set point	FCV-151 position

when teles miches 750°F control goes from FeVIGI & FeVIGE to only FeVIGI (FeVIGE closes beckers you want the soult to go into hot storage tank)

PEUISI is in engrade with LTIST

3.4 THERMAL STORAGE SUBSYSTEM

The thermal storage subsystem provides a cold salt source for the receiver for daytime operation, and a hot salt source for the steam generator for day and early evening operation. The TSS can also furnish a source of thermal energy for overnight freeze protection of the receiver, steam generator, and salt piping and for early morning plant start-up. The subsystem includes the hot and cold salt storage tanks, propane-fired salt heater, cold salt pump and cold salt sump. The subsystem schematic is shown on Figure 3.15. Major components are described on Table 3.6; valves are listed on Table 3.7; instrumentation is described on Table 3.8; and control loops are given on Table 3.9.

The salt pump is of a vertical cantilever design. The impeller and casing are suspended below the liquid level in a sump; the bearings are located above the liquid level and do not contact the salt.

The hot salt tank employs a unique design. To allow the use of carbon steel in the structural portions of the tank, an internal refractory insulation is used to limit the temperature of the walls, roof, and floor. A waffled Incoloy liner separates the salt and the internal insulation, and the tank foundation is cooled with circulating water to limit the floor temperature. The outside of the tank is insulated in the conventional manner with calcium silicate and aluminum sheathing. The cold salt tank is similar in design to the hot tank except that it does not require the internal insulation and liner due to its lower operating temperature.

Figure 3-5. Thermal Storage Subsystem Schematic

3-23

Component	Description	Function	Nominal Operating Condition
Cold salt storage tank	- Carbon steel cylindrical tank - 12.3 ft. dia.	- Cold salt storage	- 590°F salt
	- 12.3 ft. high - 15 in fibrous external insulation		
Hot salt storage tank	Carbon steel cylindrical shell12.3 ft. dia. stainless steel	- Hot salt storage	- 1050°F salt
	- 12.3 ft. dia. stainless steel liner - 23.6 ft. high - 13-1/2 in. insulating firebrick		- Approx. 7 MW _t hr storage capacity
Cold salt sump	 between shell and liner 2 in. fibrous external insulation Carbon steel cylindrical tank 	Dumm us a sure in	
San Samp	- 59 in. dia 66 in. deep	- Pump reservoir	- 590°F salt - Atmospheric pressure
Cold salt pump	- Vertical cantilever type - 60 H.P. driver	 Pump salt from cold storage tank to cold salt booster pump, SGS, or propane heater 	- 590°F salt - 96,867 lb/hr
		; · .	

Table 3.6
Thermal Storage Subsystem Components - 2

Component	Description	Function	Nominal Operating Condition
Hot salt sump	- Stainless steel cylindrical tank - 48 in. dia 49 in. deep	- Reservoir for hot salt pump	- 1050°F salt - Atmospheric pressure
ot salt pump	- Vertical cantilever type - 7-1/2 HP driver	- Provide hot salt circulation through STS	- 1050°F salt - 64,680 lb/hr
ropane heater	- 3 MW propane fired heater - 9 ft. dia. shell - 24 ft. high - One stainless steel heating coil, 2.12 in. dia., 1640 ft. long	- Provide auxiliary salt heating capability	- 59,900 lb/hr salt - 590°F inlet - 1050°F outlet

Table 3.7 .
THERMAL STORAGE SUBSYSTEM REMOTE OPERATED VALVES

VALVE	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-201	Valtek	3"	CV	FC	Cold Sump Level Control	Cold Storage Tank Base South Side
FCV-211	Kieley-Mueller	3"	SV	FC	Cold Sump Isolation	Pump House North Side West End
FCV-221	Valtek	3"	CV	FC	Hot Sump Level Control	Hot Storage Tank Southwest Side
FCV-231	Kieley-Mueller	3"	SV	FC	Hot Sump Isolation	Outside Pumphouse Northeast Corner
FCV-241	Valtek	2"	CV	FC	Propane Heater Flow Control	Line to Propane Heater East of FCV-231
FCV-242	Valtek	1 1/2"	SV	FC	Propane Heater Isolation	Top of Hot Tank

		Control	Dia i	Alarm L	_evels		
Identifier	Description	Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Cold Storage Tank						
LT-281	Level	РСМ З	0-150	134	15	inch	10
TE-281	Lower temp	PCM 3	0-1200	700	500	°F	10
TE-282	Middle temp	PCM 3	0-1200	700	500	°F	10
TE-283	Upper temp	PCM 3	0-1200	700	500	°F	10
	Hot storage tank						
LT- 291	Level	PCM 3	0-200	190	10	inch	10
TE-291	Lower temp	PCM 3	0-1200	1070	500	°F	10
TE-292	Middle temp	PCM 3	0-1200	1070	500	°F	10
TE-293	Upper temp	PCM 3	0-1200	1070	500	°F	10
	Cold salt pump						
LT-201	Sump level	PCM 3	0-60	60	15	inch	2
TE-286	Bearing temp	PCM 3	0-500	190		°F	10
TE-211	Vent temp	PCM 3	0-1200	400		°F	2
	Hot Salt Pump						
LT-221	Sump level	PCM 3	0-48	41	15	inch	2
TE-231	Vent temp	PCM 3	0-1200	400		°F	2
							_

Table 3.9
Thermal Storage Subsytem Control Loops

Controlled Variable	Mode	Set Point	Controller Inputs	Controller Output
Cold sump level	Operation	23 in FCV-201 (45 in fill)	Sump level (LT-201) Level set point	FCV-201 position - Flow from cold storage tank
Hot sump level	Operation	20 in FCV-221	Sump level (LT-221) Level set point	FCV-221 position - Flow from hot storage tank
			,	

3.5 STEAM GENERATION SUBSYSTEM

The steam generation subsystem transfers sensible heat from the molten salt to produce superheated steam for the turbine-generator. The subsystem schematic is shown on Figure 3.6. The subsystem includes an evaporator, steam drum, boiler recirculation pump, superheater, and attemperator.

The evaporator and superheater are U-tubes, U-shell heat exchangers, with low pressure salt on the shell side and high-pressure water and steam on the tube side. This shell and tube configuration has been selected to minimize thermal stresses, due to differential expansion, in the tubes and tubesheets.

A conventional steam drum, located above the evaporator, separates water droplets from the saturated steam before the latter enters the superheater, and receives feedwater from the feedwater heater. A forced recirculation design was selected, since it is preferred for power plants requiring daily start-up and shutdown.

The superheater outlet steam can be attemperated by mixing with a small amount of saturated steam from the drum. The salt flow from the superheater to the evaporator is also attemperated to 850°F, when necessary, by mixing with salt flow from the cold tank. This allows chrome-moly piping and fittings, rather than stainless steel, to be used in the evaporator.

Warmup of the steam generation subsystem is accomplished by isolating the subsystem and preheating with the subsystem's electrical heater.

Major subsystem components, valves, instrumentation, and control loops are described on Tables 3.10 through 3.13.

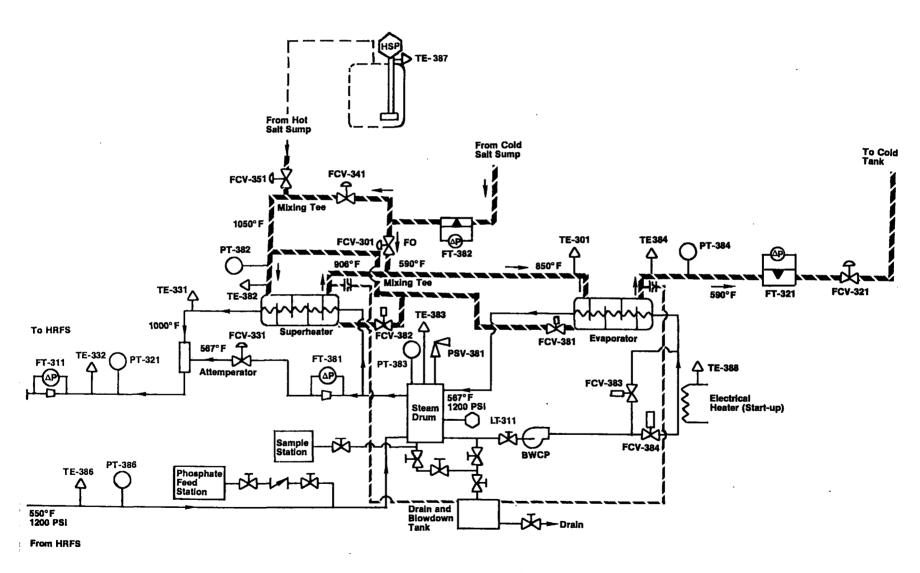


Figure 3.6 . Steam Generation Subsystem Schematic

Component	Description	Function	Nominal Operating Condition
Evaporator	 U-tube/U-shell counterflow heat exchanger 8 in. dia. chrome - moly shell (salt) 27 chrome-moly tubes 0.875 in. dia. 68 ft avg. length (water) 	- Evaporate subcooled water to produce saturated steam/water mixture	 - 850°F salt inlet - 590°F salt outlet - 78,550 lb/hr salt flow rate - Subcooled water inlet - 567°F, 1200 psi saturated steam/water outlet - 2.15 MW rating
Superheater	 U-tube/U-shell counterflow heat exchanger 6 in. dia. stainless steel shell (salt) 23 stainless steel tubes 0.500 in. dia. 33 ft. avg. length (steam) 	- Heat saturated steam to superheat condition	- 1050°F salt inlet - 906°F salt outlet - 64,680 lb/hr salt flow rate - 567°F 1175 psi saturated steam inlet - 1000°F. 1100 psi superheated vapor outlet - 10,530 lb/hr steam flow rate - 0.98 MW rating
Steam Drum	 Cylindrical pressure vessel with elliptical heads 24 in ID 6 ft 10 in overall height 2 in thick carbon steel Contains primary cyclone steam separator and primary & secondary steam scrubbers 	 Separate steam/water mixture exiting evaporator Supply saturated steam to superheater Provide feedwater surge volume 	- 567°F - 1200 psi

Component	Description	Function	Nominal Operating Condition
Boiler water circulation pump	- Canned centrifugal type - 5 HP driver	- Provide circulation of subcooled water from the steam drum to evaporator. Maintain high recirculation rate over full range of operating conditions.	- 560°F - 119 GPM - 111 ft. head
Start-up heater	- Chamber type electric heater - 3 40-kW heating elements - 2 15-kW heating elements	 Raise temperature and pressure of water during cold start-up to avoid salt freeze-up in evaporator Heat boiler water to maintain temperature and pressure of water/steam system during diurnal hold 	- Cycled during diurnal hold - Bypassed during normal operation
Steam attemperator	- Mixing tee	- Mix saturated steam from steam drum with super-heated steam from super-heater to control steam delivery temperature to turbine	 1053 lb/hr dry saturated steam at 567°F 10,529 lb/hr superheated steam at 1000°F 1100 psi 11,582 lb/hr delivery steam at 950°F 1100 psi
Salt attemperator (evaporator inlet)	- Mixing tee	- Mix cold salt with superheater outlet salt to limit evaporator inlet salt temperature to 850°F because of Cr-Mo construction	 - 64,680 lb/hr at 906°F - 13,870 lb/hr at 590°F - 78,550 lb/hr at 850°F supplied to evaporator

Table 3.10. Steam Generation Subsystem Components - 3

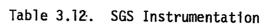
Component	Description (2)	Function	Nominal Operating Condition
Salt start-up attemperator (superheater inlet)	- Mixing tee	- Mix cold salt with hot salt from hot tank to provide a controlled temperature increase of salt entering superheater during start-up	- Full flow of cold salt at start-up - No cold salt flow during operation
Heat tracing	- Electrical heating element - Inconel sheath	- Maintain heat exchangers and salt piping above the freezing point of salt	- Temperature monitored by thermocouples - Cycle as required
		- Provide freeze protec- tion of feedwater piping and instrumentation during shutdown	
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Table 3. 11 SGS REMOTE OPERATED VALVES

VALVE	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-301	Valtek	1"	CV	F0	Evaporator Salt Temperature Control and Cold Salt Fill	SGS Skid West Side South End
FCV-321	Valtek	2"	CA	F0	Main Salt Flow Control	SGS Skid South End
FCV-331	Fisher	1"	CV	F0	Steam Attemperator Temperature Control	SGS Skid North Side Steam Drum
FCV-341	Valtek	1"	CV	FC	Main Salt Fill	SGS Skid West Side Middle
FCV-351	Valtek	2"	CV	F0	Hot Salt Flow Control	Outside Pumphouse Northeast Corner
FCV-381	Kieley-Mueller	1"	SV	FC	Evaporator Salt Drain	SGS Skid West Side Middle
FCV-382	Kieley-Mueller	1"	SV	FC	Superheater Salt Drain	SGS Skid West Side Below Steam Drum
FCV-383	Dresser	4"	SV	F0	Evaporator Water Supply	SGS Skid Southeast Corner
FCV-384	Valtek	2"	SV	F0	Start-up Heater Supply	SGS Skid Below FCV-383

Table 3.12% SGS Instrumentation

		0	D.S J	Alarm L	evels		
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Feedwater						
PT-386	Pressure	PCM-3/ Bailey	0-1500	1500		PSI	5
TE-386	Temp	PCM-3/ Bailey	0-750	575	500	°F	10
	Steam Drum						
PT-383	Pressure	PCM-3/ Bailey	0-1500	1250	950	PSI	5
TE-383	Fluid temp	PCM-3/ Bailey	0-750	575	500	°F	10
LT-311	Fluid level	PCM-3/ Bailey	-17 to +23	. 4	-4	inch	2
	Evaporator						
TE-301	Salt inlet temp	PCM-3/ Bailey	0-1200	880	500	°F	2
TE-384	Salt outlet temp	PCM-3/ Bailey	0-1200	640	500	°F	2
PT-384	Salt outlet pressure	PCM-3/ Bailey	0-200			PSI	5
FT-321	Salt flow rate	PCM-3/ Bailey	0-100			KLB/hr	2
			•				



			5. -	Alarm L	.evels		
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Superheater						
PT-382	Salt inlet pressure	PCM-3/ Bailey	0-200	100		PSI	5
TE-382	Salt inlet temp	PCM-3/ Bailey	0-1200	1070	500	°F	5
TE-331	Steam outlet temp	PCM-3 Bailey	0-1200		910	°F	2
FT-381	Attemperator steam flow	PCM-3/ Bailey	0-2500			lb/hr	5
FT-382	SGS Cold Salt Supply	PCM-3/ Bailey	0-16	,		KLB/hr	5
	Steam Delivery						
PT-321	Pressure	PCM-3/ Bailey	0-1500	1150	950	PSI	2
TE-332	Temp	PCM-3/ Bailey	0-1200	990	910	°F	2
FT-311	Flow rate	PCM-3/ Bailey	0-100	12.6	3.2	KLB/hr	2
TE-387	Hot Salt Pump Bearing	PCM-3	0-500	190		°F	10
TE-388	Start-up Heater 5 Element Temp	PCM-3/ Bailey	0-1200	1100	500	°F	10
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Mode	Set Point	Controller Inputs	Controller Output
SGS start-up	1000 psig FCV-491	Delivery pressure (PT-321) pressure set point	FCV-491 position - SGS steam flow
Boiler following	1100 psig SP. SP	Delivery pressure (PT-321) Pressure set point (SP. SP) Steam flow (FT-311) Salt flow (FT-321)	FCV-321 position - SGS main salt flow
Operation	950°F SP. ST	Delivery temperature (TE-332) Temperature set point (SP. ST)	FCV-331 position - Steam attemperator flow
Operation	O in SP. DL	Drum level (LT-311) Level set point (SP. DL) Feedwater flow (FT-411) Steam flow (FT-311)	FCV-411 position - Feedwater flow
Operation	850°F SP. EST	Inlet temperature (TE-301) Temperature set point (SP. EST)	FCV-301 position - Cold salt flow
Diurnal Shutdown	~ 520°F	Circulation heater outlet temperature (TE-388)	Electric immersion heater elements on/off
	SGS start-up Boiler following Operation Operation Diurnal	SGS start-up Boiler 1100 psig FCV-491 Boiler 1100 psig SP. SP Operation 950°F SP. ST Operation 0 in SP. DL Operation 850°F SP. EST Diurnal ~520°F	SGS start-up 1000 psig FCV-491 Delivery pressure (PT-321) pressure set point

3.6 ELECTRIC POWER GENERATION SUBSYSTEM

The electric power generation subsystem converts the enthalpy in the main steam flow to electricity. The subsystem (Figure 3.7) includes the steam turbine, electric generator, electric power equipment, condenser, condensate pump and storage tank. The electrical one-line diagram is shown on Figure 3.8.

The turbine-generator set is a skid-mounted unit located at the north end of the receiver tower complex at the 80 ft. level (20 ft. below grade). This skid consists of a turbine, generator, and auxiliary equipment. The turbine is a seven-stage, single flow machine, operating at 17,400 rpm. Inlet steam conditions are rated at 940°F and 1050 psia. A single reduction gearbox reduces the turbine shaft speed to the generator speed of 1,200 rpm. The 750 kW generator operates at 450V, and is cooled by circulating water through air cooling coils located above the generator. The turbine-generator auxiliaries include a lubricating oil pump, lube oil cooler, air ejection vacuum pump and mechanical-hydraulic governor. The allowable rate of change in load is 10 percent per minute from 30 to 100 percent of rated capacity.

A shell and tube condenser, supported by a separate frame, is located directly below the turbine. Access to the condenser is on the floor 40 ft. below ground. Condensate from the hot well of the condenser will be transferred to the deaerator when the water level in the deaerator requires makeup. Otherwise, the condensate is pumped to a storage tank. Condensate from this tank is piped back to the condenser hot well when the hot well level requires water.

Major components of the EPGS, valves, instrumentation, and control loops are described on Tables 3.14 through 3.17.

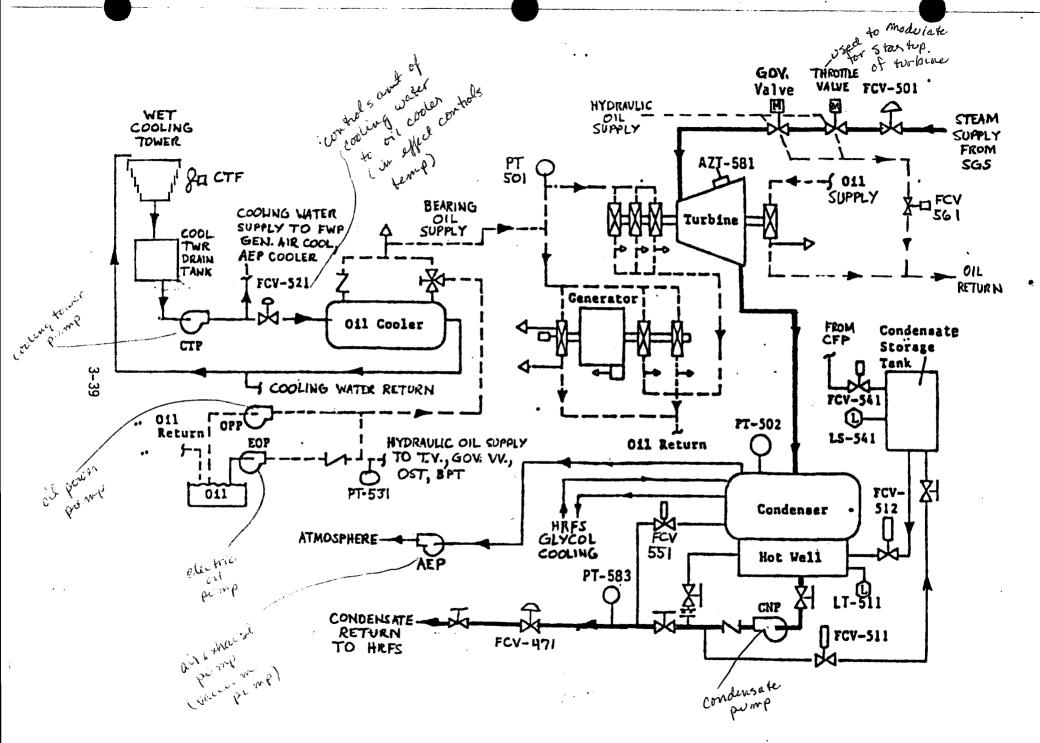


Figure 3.7. Electric Power Generation Subsystem Schematic

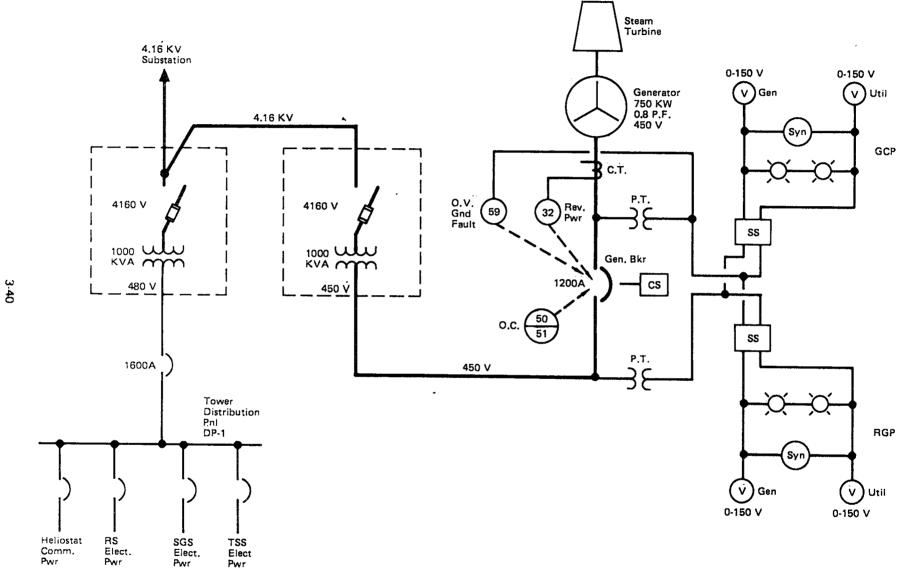


Figure 3.8. MSEE Electric Generator One-Line Diagram

Table 3.14
Electric Power Generation Subsystem Components

Component	Description of	Function	Nominal Operating Condition
Turbine	Axial flow condensing type7 stage	- Expand steam to drive electric generator	 940°F 1050 psig throttle steam 133°F 2.5 psia exhaust steam 7800 lb/hr steam flow 17,443 RPM 1000 HP
Electric generator	- AC generator - 450 volt, 3 phase - 1200 RPM - Solid state excitor	- Generate electric power	 750 kW_e (rating) 600 kW_e (maximum in MSEE) 0.8 power factor rating
Condenser	 Crossflow shell and tube heat exchanger Rectangular shell (condensate) 438 tubes, 5/8-in. dia. 7-1/2 ft long (glycol/water coolant) Cylindrical hot well 	- Condense turbine exhaust steam - Provide turbine exhaust vacuum	 2.5 psia saturated steam inlet 133°F condensate outlet 7800 lb/hr steam/water flow 1200 GPM glycol/water coolant flow
Condensate pump	- Turbine type - 2 stage - 20 HP driver	- Pump condensate from hot well to deaerator	- 133°F water - 260 psi head (mfg rating) - 18 GPM (mfg rating)

Table 3.14 Electric Power Generation Subsystem Components

Component	Description	Function	Nominal Operating Condition	
Air exhaust pump	- Nash vacuum pump - 5 HP driver	- Provide condenser vacuum	 5 in Hg condenser pressure (ABS) 75 CFM (mfg. rating) 	
Electric oil pump	- Viking gear pump	- Provide bearing oil pressure during turbine start-up and shutdown (turbine-driven pump provides oil pressure during operation)	- Off during operation	
Cooling tower pump	-Aurora centrifugal pump	- Provide coolant circulation through oil cooler	- 35 psi head (mfg. rating) - 120 GPM (mfg. rating)	
Wet cooling tower	-Fan forced wet cooler -1/2 HP fan motor	- Reject oil coolant heat	- 110°F coolant outlet temp	

Table 3.15
EPGS REMOTE OPERATED VALVES

VALVES	MANUFACTURER	SIZE	TYPE	FAIL POSITION	FUNCTION	LOCATION
FCV-501	Valtek	2"	SV	FC	Turbine Steam Isolation	TWR Level 80 North Turbine Northeast Corner
FCY-511	Asco	1/2"	SV	FC	Hotwell Overflow	TWR Level 60 North Condenser Platform Northwest
FCV-512	Asco	3/4"	SV	FC	Hotwell Make-up	TWR Level 80 Northeast Condensate Storage Tank
FCV-521	Masoneilan	2"	CV	F0	Oil Cooler Water . Flow Control	TWR Level 80 North Turbine/Generator Overhead
FCV-541	Asco	3/4"	SV	FC	Condenser Storage Tank Make-up	TWR Level 80 Northeast Condensate Storage Tank
FCV-551	Asco	1/2"	SV	FC	Condenser Recirculation	TWR Level 60 North Condenser Platform Northwest
TVM	GE w/auma Actuator	1 1/2"	CV	FC	Turbine Steam Supply Throttle	Turbine North Side
SNM	GE		CV		Turbine Sync Speed Control	Turbine Center
Fcv-:61	ASCO	1/2"	SV	F0	Close throttle valve in emergency trip (dumps hydraulic oil)	Turbine

TABLE 3.17. **EPGS INSTRUMENTATION** CONTROL DISPLAY ALARM LEVELS SAMPLING **IDENTIFIER** DESCRIPTION MODULE RANGE HIGH **DIMENSION** LOW PERIOD (sec) Turbine Steam Supply Pressure PT-581 PCM 2 0 - 1500800 PSI 5 PT-582 Steam Seal Pressure PCM 2 0 - 1500PSI 5 TE-581 PCM 2 Exhaust Temp 0 - 500۰F TT-583 Steam Supply Temp PCM 2 0 - 1200۰F 990 800 TT-501 Outboard Bearing Oil Temp PCM 2 0 - 500170 110 ٩F TT-502 Inboard Bearing Oil Temp PCM 2 0-500 170 110 ٥F TE-503 Gear Outboard Bearing PCM 2 0 - 500170 110 ٥F 011 Temp AZT-581 Vibration PCM 2 0-100 100 PCT (0-5 g)5 Generator JT-581 Power PCM 2 0-960 kw 5 ET-581 Voltage PCM 2 0-600 450 480 Volt IT-581 Current PCM 2 0-1200 Amp PFT-581 Power Factor PCM 2 0 - 1 - 01.0 0.85 PCT VT-581 VARS PCM 2 0 - 960KVA ST-582 Speed PCM 2 0 - 15001270 rpm ST-581 Frequency PCM 2 0-100 60 PCT (55-65 Hz) 40 TT-510 Stator Winding 1 Temp PCM 2 0-500 260 ٩F TT-511 Stator Winding 2 Temp PCM 2 0 - 500260 ٥F TT-512 Stator Winding 3 Temp PCM 2 0 - 500260 ٥F TT-513 Stator Winding 4 Temp PCM 2 0 - 500٥F 260 TT-514 Stator Winding 5 Temp PCM 2 0 - 500۰F 260 TT-515 Stator Winding 6 Temp PCM 2 0 - 500260 ٥F TE-508 Cooling Air Outlet Temp PCM 2 0 - 500100 ٥F TT-507 Outboard Bearing Oil PCM 2 0 - 500٥F 170 110 TE-505 Gear Outboard Bearing PCM 2 0 - 500170 110 ٩F 0il Temp TE-506 Gear Inboard Bearing PCM 2 0 - 500170 110 ٥F 5 011 Temp PT-502 Condenser Pressure PCM 2 15 0-30 In Hg 5 PT-583 Condensate Pump Discharge PCM 2 0 - 400300 240 PSI Pressure LT-511 Hot Well Level PCM 2 0-15 16 8 Inch 2 TE-582 Cooling Tower Pump PCM 2 0-500 100 40 ٥F 5 Discharge Temp PT-531 011 Pump Discharge PDM 2 0 - 200100 **PSI** 55 5 Pressure TT-521 Bearing Oil Supply Temp PCM 2 0-500 ٥F 140 100 2 PT-501 Bearing Oil Supply Press. PCM 2 0-50 40 10 PSI

Table 2 17

ontrolled Variable	Mode	Set Point	EPGS Control Loops		
oncrotted variable	Mode	Set Point	Controller Inputs	Controller Output	
Condenser hot well level			Hot well level (LT-511)	FCV-512 open/close - makeup FCV-511 open/close - dump	
Condensate storage tank level	Operation	12 in min 30 in max	Storage tank level (LS-541)	FCV-541 open/close - supply from cycle fill pump	
				FCV-542 open/close - CMUP Stand pipe air overpressure	
Turbine/generator oil temperature	Remote operation	125°F FCY-521	Oil temperature (TT-521)	FCV-521 position - cooling water flow	

3.7 HEAT REJECTION AND FEEDWATER SUBSYSTEM

The heat rejection and feedwater subsystem rejects waste heat to the atmosphere, pressurizes and heats the condensate to the final feedwater temperature. The subsystem (Figure 3.9) includes the cooling towers, circulating water pump, deaerator, spray water heat exchanger, spray water pump, feedwater pump, feedwater heater, demineralizers, chemical feeders, water analyzers, and condensate makeup pump.

The cooling towers consist of six forced-draft, finned-tube water-to-air heat exchangers. They originally were designed as Freon condensers for refrigeration systems.

The deaerator is used as a direct contact feedwater heater and deaerator and to reject steam generated by the SGS. It is a horizontal, cylindrical pressure vessel, designed to operate at 250 psia and 400°F. It includes a steam header with mixing spargers near the bottom of the tank, water spray nozzles across the top, and two immersion electric heaters. Feedwater, stored in the deaerator, is heated by steam from a branch off the SGS mainline to the turbine. The feedwater is circulated by a spray water pump at 400 gpm from the bottom of the deaerator to the spray nozzles in the vapor space at the top of the deaerator where the water condenses the steam and is thereby heated. Oondensate from the turbine condenser, blended into this spray water, is also heated to 400°F and deaerated.

The feedwater heater is a vertical, cylindrical pressure vessel with an internal steam condensing coil. Feedwater from the deaerator is heated on the tube side as steam from a branch of the SGS mainline condenses on the shell side. The saturated liquid from the coil is cascaded down to the deaerator through a steam trap. Main steam is used for feedwater heating in the feedwater heater and the deaerator because there are no external extraction points on the turbine.

Major components, valves, instrumentation, and control loops are described on Tables 3.18 through 3.21.

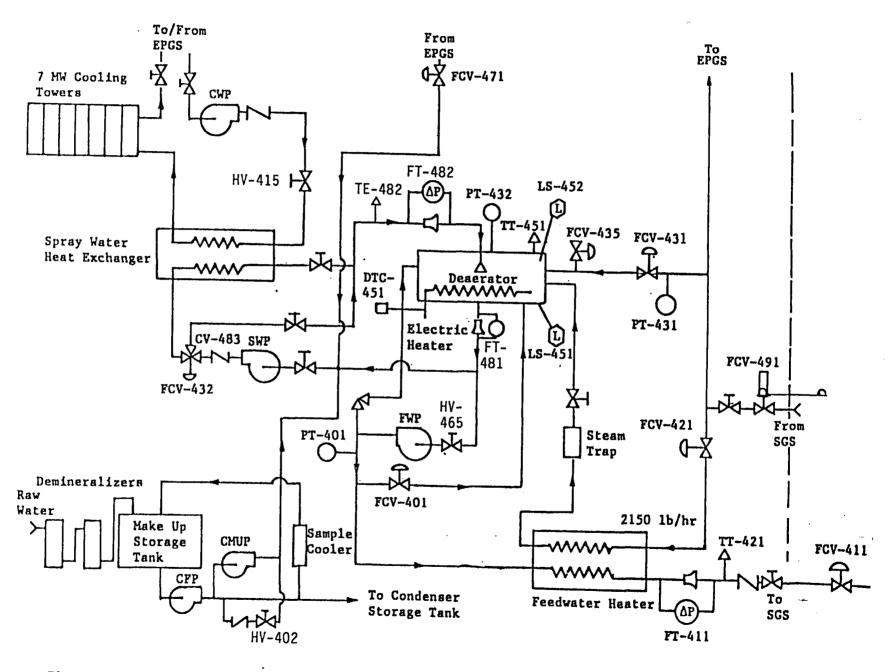


Figure 3.9. Heat Rejection and Feedwater Subsystem Schematic

Table 3.18
Heat Rejection and Feedwater Subsystem Components

Component	Description at	Function	Nominal Operating Condition
Feedwater heater	 Shell and coiled tube counterflow heat exchanger 35 in ID 2.5 in thick carbon steel shell (feedwater) 4 ft 8 in overall height 30 coiled tubes 0.500 in. dia. 43 ft long (steam) 	- Raise feedwater temperature to SGS inlet condition	 950°F superheated steam inlet 545°F saturated liquid outlet 2150 lb/hr steam flow rate 401°F feedwater inlet 550°F feedwater outlet 11,582 lb/hr feedwater flow rate 0.59 MW heat transfer
Deaerator	 Horizontal tank 5 ft ID 12 ft long Contains 15 submerged mixing nozzles, 1 overhead spray nozzle, 2 147-kW electric immersion heaters 	 Degasify condensate Heat condensate for delivery to feedwater heater Provide alternate steam dump when turbine is not operating 	401°F250 psi0.63 MW heat transfer
Spray water heat exchanger	- Shell and tube heat exchanger - 24 in. dia. shell	- Reject excess heat from deaerator when utilized as alternate steam dump	- No flow from deaerator during normal operation

Table 3.18
Heat Rejection and Feedwater Subsystem Components - 2

Component	Description of	Function	Nominal Operating Condition
Feedwater pump	High speed centrifugal type18,770 pump RPM150 HP driver	- Provide high pressure feedwater to the steam generator (through the feedwater heater)	 Inlet: 250 psi, 401°F water 1450 psi head (mfg rating) 60 GPM (mfg rating)
Spray water pump	- Vertical turbine type - 3 stage - 7-1/2 HP driver	- Provide circulation from deaerator to spray water heat exchanger and/or its bypass and return to deaerator overhead spray nozzle	- 401°F
Cooling water pump	- Centrifugal type - 40 HP driver	- Provide glycol/water circulation for spray water heat exchanger - cooling tower - con- denser circuit	- 132°F glycol/water - 40 psi head - 1200 GPM
cooling towers	- 6 units - Forced draft, finned-tube, glycol/water-to-air heat exchangers	- Reject waste heat to atmosphere	 94°F air 132°F glycol/water inlet 120°F glycol/water outlet 2.4 MW heat rejection

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VALVE	MANUFACTURER	SIZE	TYPE	FAIL POSITION	FUNCTION	LOCATION
FCV-401	Fisher	2"	CV	F0	Feedwater Pump Pressure Control	Southwest of Deaerator
FCV-411	Kieley-Mueller	2"	CV	FC	Feedwater Flow Control	SGS Skid Northeast
FCV-421	Kieley-Mueller	2"	CV	F0	Feedwater Heater Temperature Control	Above Feedwater Heater
FCV-431	Kieley-Mueller	2"	CV	FC	Main Steam Pressure Control	Southwest of Deaerator
FCV-432	Kieley-Mueller	3"-3 way	CV	To SWHX	Deaerator Pressure Control	Between Deaerator and Spray Water Heat Exchanger
FCY-4/1	Valtek	1"	CA	FC	Condensate Control to Deaerator	Above North Door to Spray Water Pump Room
FCV-483	Atkomatic	1"	SV		Deaerator Vent Block	Above Deaerator
FCV-484	Atkomatic	1/4"	SV		Deaerator Vent Bypass	Above Deaerator
FCV-485	ASÇ0	2"	SV		Demineralized Water Storage Tank Fill	Above Culligan Beds
FCV-491	Kieley-Mueller	2"	CV	FC	SGS Steam Delivery Control During Start- Up	North End of SGS Skid

TABLE 3.20. HRFS INSTRUMENTATION

IDENTIFIER	DESCRIPTION	CONTROL Module	DISPLAY RANGE	ALARM HIGH	LEVELS LOW	DIMENSION	SAMPLING PERIOD (sec)
	Main Steam						
PT-431	Pressure	PCM 2	0-1500	1200	900	PSI	2
TE-483	Temp	PCM 2	0-1200	990	850	Inch	10
	Deaerator						
PT-432	Pressure	PCM 2	0-400	250	200	PSI	2 2
TE-451	Fluid Temp	PCM 2	0-500	400	300	°F	2
TE-481	Steam Temp	PCM 2	0-500	400	300	°F	10
LT-471	Fluid Level	PCM 2	0-30	30	10	Inch	2
	Spray Water						
PT-482	Pressure	PCM 2	0-400	300	200	PSI	5
FT-482	Flow Rate	PCM 2	0-160			KLB/hr	5
TE-482	Temp	PCM 2	0-500	445		۰F	10
FT-481	Feed/Spray Water Flow	PCM 2	0-160			KLB/hr	5
	Rate						
	Feedwater						
PT-481	FWP Supply Pressure	PCM 2	0-400		170	PSI	5 2
PT-401	FWP Discharge Pressure	PCM 2	0-1500	1400	900	PSI	2
PT-484	FWP Coolant Pressure	PCM 2	0-100			PSI	5 5
PT-483	FWH Outlet Pressure	PCM 2	0-1500	1230	1180	PSI	5
FT-411	Flow Rate	PCM 2/	0-160 Bailey			KLB/hr	2
FT-421	FWH Outlet Temp	PCM 2	0-750	600	400	°F	2
	Cooling Water	,					
TE-484	SWHX Inlet Temp	PCM 2	0-500	130		°F	10
TE-486	Tower Outlet Temp	PCM 2/	0-500	110	32	°F	10

Controlled Variable	Mode	Set Point	Controller Inputs	Controller Output	
• • • • • • • • • • • • • • • • • • • •		5.20° 540°F FCV-421	Feedwater temperature (TE-421) Temperature set point	FCV-421 position - Feedwater heater Steam supply flow	
Feedwater pressure	Operation	1250 psig FCV-401	Feedwater pressure (PT-401) Pressure set point	FCV-401 position - FWP recirculation flow	
Steam delivery pressure	Manual salt flow GSTAT off	1080 psig PT-431	Delivery pressure (PT-431) Pressure set point	FCV-431 position - Deaerator steam dump	
Deaerator pressure	Operation - Desuperheating GSTAT off Boiler following GSTAT on	233 psig PT-432 233 psig PT-432	Deaerator pressure (PT-432) Pressure set point Deaerator pressure (PT-432) Pressure set point	FCV-432 position - Deaerator dump to SWMX FCV-431 position - Deaerator steam supply	
Deaerator temp.	DTC 451 DTC 452		Deaerator temperature (TE-451) Temperature set point	DTC-451/452 on/off - Electric heater control	
Deaerator level	Operation	15 in Garden FY-472 (14 in backup during turbine operation)	Deaerator level (LT-471) Level set point	FY-472 condensate - Makeup pump stroke position	
	Turbine Operation	15 in FCV-471	Deaerator level (LT-471) Level set point	FCV-471 position - Turbine condensate return from hot well	

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3.8 SYSTEM TRIPS

3.8.1 Equipment Protection Subsystem

The Equipment Protection Subsystem (EPS) is a hard-wired system using dedicated sensors and is designed to safe the MSEE in the event of any potentially unsafe condition. Subsequent to the EPS placing the system in a "safe" condition, operator action is required to shut the system down or to change into any other mode. The trip list for the EPS, including actions taken by the EPS and subsequently to be taken by the operator, are shown on Table 3.22, subdivided by subsystem.

3.8.2 <u>Turbine/Generator Trips</u>

Trips built into the turbine/generator are given on Table 3.2.3. Definitions and guidelines are given below.

A. Definitions

- 1. Turbine Trip Immediate turbine steam shutoff manual or auto.
- 2. Turbine Shutdown Gradual turbine steam shutoff manual.
- 3. Generator Trip Generator circuit breaker opened manual or auto.

B. Steam reactions to trips

- 1. Anticipated Steam control maintained manually or auto.
- 2. Upset Reliance on auto steam control SGS salt flow will stop and HRFS will attempt to desuperheat steam. Probable HRFS and SGS safety valve lifting if upset is uncontrolled.

C. Trip interlocks

- 1. A generator breaker trip always initiates a turbine SVC trip (auxiliary relay 32x closes FCV-501) and an EPST TR-586 (32x).
- 2. A generator breaker trip always initiates a turbine T.V. reset (auxiliary relay 32x resets T.V. closed) w/ZT-581 '0'% open.
- 3. A turbine T.V. reset and an EPS 2 & 3 reset will reopen FCV-501 unless manually closed (or tripped).
- D. All auto trips should be carefully reviewed determine the cause of the trip and correct the problem before resuming operations.
- E. Fail-safe follow-through guidelines

 These guidelines present items of concern to fail-safe the EPGS upon a
 major component failure, after a trip that did not function, or to back
 up an auto trip. Intimate familiarity with these guidelines is mandatory
 before EPGS operation to insure safe operation, both from a personnel and
 equipment standpoint.
 - Three items are of major concern to fail-safe the EPGS and MSEE operating systems:
 - a. Steam over-pressurization
 - b. Turbine trip
 - c. Generator trip
 - 2. Steam system reactions to turbine trips:
 - a. Over-pressurization
 - b. Possible HRFS/D-D & SGS/steam drum safety valve lifting
 - c. Desuperheating by HRFS/FCV-431 switchover to steam control to dump steam to D/D
 - d. FCV-432 D/D heat dump through SWHX and dry cooling tower

- 3. Turbine tripping is redundant-designed and may be fully utilized with these four trips:
 - a. Actuate ET emergency trip FCV-561 (oil trip)
 - b. Open generator breaker with breaker C.S. (electric trip)
 - c. Actuate EPS T-G trip button from control room (EPS backup)
 - d. Manually close throttle valve with hand wheel (manual)
- 4. Turbine-generator trip verification:
 - a. ST-582 speed decreasing
 - b. PT-532 hydraulic oil pressure decreasing (T.V. trip)
 - c. PT-581 steam pressure drops to zero (FCV-501 trip)
 - d. Generator breaker open green light on

NOTE

EOP operation is not mandatory upon a turbine trip since the shaft driven oil pump provides adequate oil flow for turbine coast down.

- 5. Generator trips are redundant-designed with turbine trips. Be aware that:
 - a. EPGS UPS provides emergency backup C/B trip power
 - b. Exciter voltage shutdown local disconnect switch shuts down all of the generator electrical power.

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM RECEIVER SUBSYSTEM TRIPS

TRIP	TRIP	INSTRUMENT	TRIP	
IDENTIFIER	CONDITION	IDENTIFIER	LEVEL	ACTION REQUIRED
	Operator Manual Trip		N/A	EPS - Defocus Heliostat
TR-181	Receiver Salt Outlet Temp High	TE-102A	1080°F	Operator - Control Receiver From The EMCON Console
TR-184	Receiver Tube Temp High	TE-140A and	925°F	
	During Hot Salt Production	TE-102A	>750°F	
TR-187	Loss of Receiver Door Open Signal	ZSH-DR	Contact Open	
TR-182	Boost Pump Pressure Low	PT-180A and	250 PSIG	EPS
	During Hot Salt	TE-102A	>750°F	 Defocus Heliostats Close FCV-151 After Time Delay
TR-183	Receiver Salt Inlet	PT-181A	8 PSIG	Operator
	Pressure Low During Hot Salt Production	and TE-102A	>750°F	 Shutdown Receiver from EMCON Console
TR-185	Hot Surge Tank Level High	LF-161A or	80 In	EPS - Defocus
neriostats		TE-184A	300°F	- Close FCV-101 and FCV-102 After Time Delay
				Operator - Shutdown Receiver From EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM RECEIVER SUBSYSTEM TRIPS (Continued)

		_	
TRIP	TRIP	INSTRUMENT TRIP	
IDENTIFIER	CONDITION	IDENTIFIER LEVEL	ACTION REQUIRED
TR-186	Boost Pump Sump Level High	TE-181A 400°F	EPS - Defocus Heliostats - Time Delay - Close FCV-151 - Turn Off Cold Salt Boost Pump - Turn Off Hot Salt Pump EMCON (Automatic) - Maintain Control of Receiver and HRFS Operator - Shut Down the Plant From the EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM THERMAL STORAGE SUBSYSTEM TRIPS (Continued)

TRIP	TRIP	INSTRUMENT		
<u>IDENTIFIER</u>	CONDITION	IDENTIFIER		ACTION REQUIRED
TR-281	Hot Salt Sump Level High	LT-221A or TE-231A	40 In 300°F	EPS - Close Sump Insolation Valve FCV-231
				Operator - Allow Time for Hot Salt Pump Operations To Bring Sump Level Down - Shut down SGS, HRFS, and EPGS From EMCON Console
TR-282	Cold Salt Sump Level High	LT-201A or TE-211A	55 In 350°F	EPS - Close Sump Insolation Valve FCV-211 - Defocus Heliostats Operator - Allow Time for Cold Salt Pump Operations To Bring Sump Level Down - Shut down the Plant From The EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM STEAM GENERATOR SUBSYSTEM TRIPS (Continued)

TOTO	THETRUMENT TOTAL	
		ACTION REQUIRED
Steam Drum Level Low	LT-311A -10 In	EPS - Close FCV-501 - Open Generator Circuit Breaker - Turn Off FWP (Drum Level High only)
Steam Drum Level High and Water Hot	LT-311A +17 In and TE-383A >250°F	EMCON (Automatic) - Dump Steam To Deaerator - Maintain Control of HRFS
·		Network 90 - Shut Off Salt Flow (Close FCV-301, 341, and 351) - Turn Off BWCP (Drum Level Low only)
		Operator - Shut Down SGS, HRFS, and EPGS From EMCON Console
Boiler Water Circulation Pump Failure	Motor Off Current Sensor	EPS - Close FCV-501 - Open Generator Circuit Breaker EMCON (automatic) - Dump Steam to Deaerator
	ŢĠ.:	- Maintain control of HRFS Network 90 - Shut Off Salt Flow (Close FCV=501, 341, and 351) Operator - Shut down SGS, HRFS, and EPGS
	Steam Drum Level High and Water Hot Boiler Water Circulation	Steam Drum Level Low LT-311A -10 In Steam Drum Level High LT-311A +17 In and and Water Hot TE-383A >250°F Boiler Water Motor Off Circulation Current Pump Failure Sensor

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM EPGS TRIPS (Continued)

TRIP IDENTIFIER	TRIP CONDITION	INSTRUMENT IDENTIFIER		ACTION REQUIRED
	Turbine Overspeed	OST	1320 RPM Generator	EPS - Close FCV-501 Open Generator Circuit Breaker
	Turbine Back Pressure High	ТВРТ	5 PSIG	
TR-58 4	Generator Bearing Temp High	TS-501A	180°F	EMCON (Automatic) - Dump Steam to Deaerator - Maintain Control of HRFS
TR-585	Generator Cooling Air Temp High	TS-502A	122°F	Operator - Control System From EMCON Console - Reduce Steam Flow
TR-586	Generator Circuit Breaker Trip		-Manual -Low/high Voltage -Low/high frequency	- Shut Down If Necessary
TR-587	Turbine Vibration High	AZT-581	5g	
TR-588	Steam Energy Low	TE-332 or PT-581A	750°F 770 PSI	
TR-583	Turbine Oil Pressure	PS-501A (LUBE) or	6 PSI	
		PS-531A (HYDR)	50 PSI	
TR-582	Manual T/G Emergency Trip	Control Room PB	Operator Initiate	

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM MASTER CONTROL SUBSYSTEM TRIPS (Continued)

TRIP CONDITION	ACTION REQUIRED
PCM 1 Microcomputer Failure - Loss of Receiver Displays - Loss of Salt Auto Flow Control	EPS - Defocus Heliostats
- Loss of Cold Surge Tank Auto Level Control	Operator - Control Receiver from PCM 1 - Drain Receiver If Necessary
PCM 2 Microcomputer Failure - Loss of HRFS and EPGS Displays - Loss of Feedback Control Loops	 Close FCV-301, FCV-341, and FCV-351 Turn Off FWP Close FCV-501 and FCV-491 After Steam Pressure Drops Open Generator Circuit Breaker Turn Off Condensate Pump
	Operator - Shut Down SGS From Console - Shut Down HRFS and EPGS From PCM 2
PCM 3 Microcomputer Failure - Loss of TSS Displays - Loss of Feedback Control Loops - Loss of SGS Displays	EPS - Defocus Heliostats - Time Delay - Close FCV-211 - Close FCV-231 - Turn Off Hot and Cold Salt Pumps - Turn Off Cold Salt Boost Pump - Close FCV-151 - Close FCV-501 - Open Generator Circuit Breaker
	EMCON (Automatic) - Dump Steam To Deaerator - Maintain Control of HRFS
	Network 90 (Automatic) - Interlocks Will Close FCV-301, FCV-341, and FCV-351
	Operator - Shut Down SGS From Network 90 Console - Shut Down Receiver, HRFS, and EPGS from EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM MASTER CONTROL SUBSYSTEM TRIPS (Continued)

TRIP CONDITION Simultaneous Failure of PCM 1, 2, and 3 Microcomputers - Loss of All Subsystem Control CCM Microcomputer Failure - Loss of PCM/Host Computer Communication Lin - Loss of Console Displays - Loss of Console Control Capability - Loss of Sequencing Operations Involving More Than One PCM	ACTION REQUIRED EPS Defocus Heliostats Time Delay Close FCV-211 Close FCV-231 Turn Off Hot and Cold Salt Pumps Turn Off Cold Salt Boost Pump Close FCV-151 Turn off FWP Close FCV-501 and FCV-491 After Steam Pressure Drops Open Generator Circuit Breaker Turn Off Condensate Pump
Operator Remote Manual Trip	Operator - Shut Down the Subsystems From PCM 1, 2, and 3 and Network 90
EMCON Host Computer Failure	PCMs and CCM Continue To Operate and Control The Plant
	Operator - Shut Down The Subsystems From PCM 1, 2, and 3

Table 3.23. TURBINE/GENERATOR TRIP LIST

MODE	DESCRIPTION	INITIATION
Manua 1	MGBT — Manual generator breaker trip	Breaker switch opened at local or remote generator control panel
Manual	ET - Emergency trip	ET "on" at EMCON console or local trip button actuated
Manual/auto	SVC - Stop valve closure	Close FCV-501
Manual/auto	OST - Overspeed trip	Local OST button
Manual	MTVC – Manual throttle valve closure	Close throttle valve (TVM)
Auto	GBT – Generator breaker trip	a. Reverse powerb. Ground faultc. Overcurrent

A tabulation of data describing the MSEE system is given on Table 3.1. A more detailed description of the MSEE subsystems is contained in the following subsections.

3.1 COLLECTOR SUBSYSTEM

The collector subsystem redirects, concentrates, and focuses solar radiation onto the tower-mounted receiver. The subsystem, which is already in place at the CRTF, consists of 221 two-axis tracking heliostats located north of the receiver tower, and its control system. Under optimum insolation and heliostat conditions, the heliostat field can concentrate approximately 5 MW+ onto the receiver.

Each heliostat has 25 individual mirror facets totaling 37.2 m^2 (400 ft^2) of reflective surface. The facets are mounted on a structure and individually adjusted to provide a concentration ratio of 25 to 1 on the receiver. The structure has motor-driven azimuth and elevation gimbals, which allow it to track the sun during the day.

The heliostats are operated from the control room by the CRTF collector control system. (The CRTF collector control system is separate from the experiment master control subsystem.) The CRTF collector control system analyzes heliostat operating commands from a number of programmed test sequences or from the facility heliostat operator. Control signals are distributed to the heliostats through four heliostat array controllers and four heliostat interface modules. Each heliostat receives azimuth and elevation pointing information once every second and responds with its own status. Commands and data transmitted to the individual heliostats are received and executed by the heliostat control electronics. The electronics keep the drive motor power at the proper level until the gimbal axis encoders indicate that the desired position has been reached.

Location -- CRTF; on Kirtland Air Force Base, Albuquerque, NM
Heliostat Field -- Existing field of 221 heliostats each with 400 ft² of
mirror surface.

Tower -- Existing concrete tower, 200 ft. high with internal lifting module Master control -- EMCON D-2 distributed digital control system with central consoles; separate equipment protection system.

Receiver -- Refurbished from previous Subsystem Research Experiment.

- o Rating: 5 MW_{th}
- o Salt temperatures: in 590°F; out 1000°F (1050°F with propane heater)
- o Configuration: cavity with door
- o Absorber: single panel of 3/4 in Incoloy 800 tubes (18 passes, 16 tubes per pass)
- o Peak flux: 630 kW/m² (200,000 Btu/hr ft^2)

Thermal Storage -- Existing from previous Subsystem Research Experiment

- o Rating: 5.8 MW_{th} Hr when operating between 590°F and 1000°F
- o Type: 2-tank
 - Hot tank, internal insulation
 - Cold tank, external insulation

Steam Generator -- Supplied by Babcock and Wilcox

- o Type: Forced recirculation
- o 2 units: evaporator and superheater (both U-tube, U-shell) with steam drum separator
- o Rating: 11,000 lb/hr of steam at 940° F and 1100 psi (3.13 MW_{th})
- o Prototypical of commercial design

Turbine Generator -- GE rebuilt unit

- o Marine turbine
- o 750 kW $_{
 m e}$ rating (500 kW $_{
 m e}$ under nominal operating conditions)

Heat Rejection and Feedwater System -- existing at CRTF

- o Feedwater treatment only
- o 20,000 gallon demineralized water storage
- o Dry cooling, 7 MW_{th} capacity
- o Spray water heat exchanger to reject heat when turbine not in use or tripped off line

3.2 MASTER CONTROL SUBSYSTEM

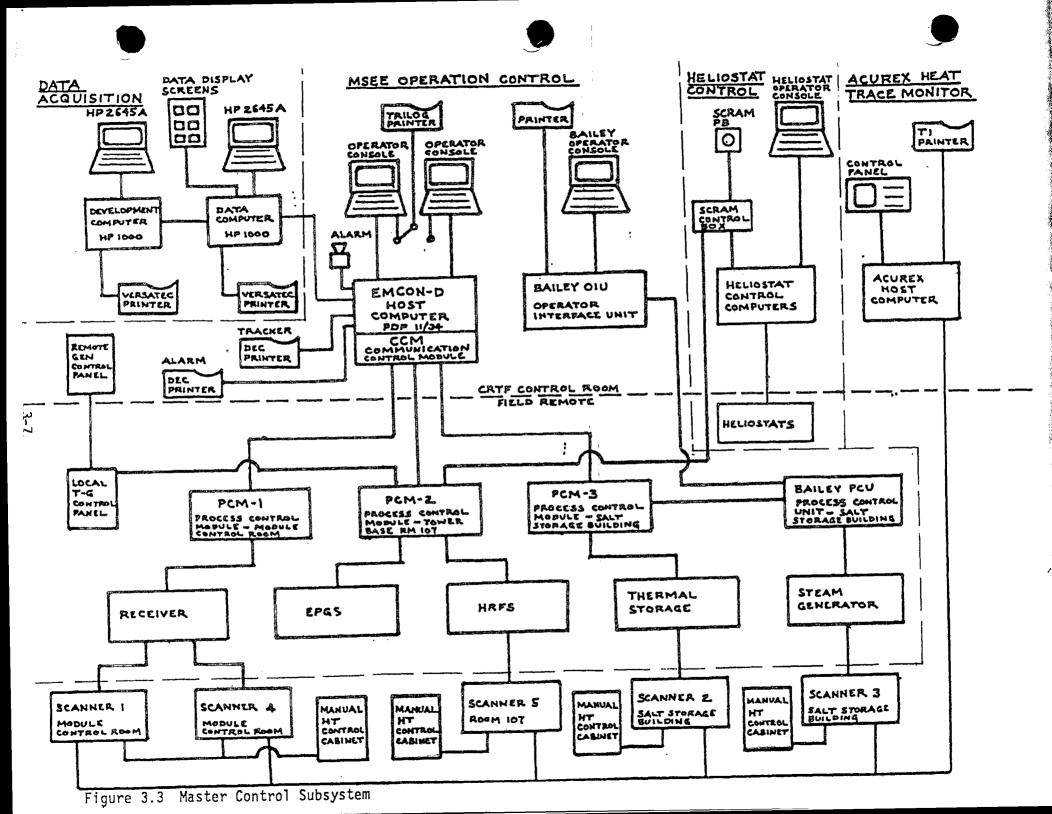
The master control subsystem (Figure 3.3) consists of an EMCON-D2 for system control and a equipment protection system. A Bailey network 90-system is used to directly control the SGS. Commands and set points are provided by the EMCON master control subsystem to the Network 90 for SGS operation and control. The equipment protection system is an independent hardwired relay shutdown system. These relay trip devices will shut down the receiver or the power generation ends of the MSEE when critical parameters reach preset limit values. These relay units are independent of the EMCON and network 90 control systems. Additionally, an Accurex Data Logger is used to collect and display all the temperature measurements relating to the heat tracing and data instrumentation.

3.2.1 EMCON System

The EMCON-D2 is a distributed digital control system consisting of two operator consoles, a host computer with its peripheral hardware, a communication control module, and three process control modules distributed among the subsystems. Two EMCON-D2 operator consoles are located in the CRTF main control room. The host computer is an existing DEC PDP 11/34 unit located in the control room. This computer links the operator with the process control modules, and analyzes data from the control modules for presentation on the operator consoles. The peripheral equipment includes two disk drives, an alarm system, and a data analysis system.

A communication control module links the host computer with the three field-located, process control modules. Each process control module is a small digital computer capable of monitoring a number of instrumentation points, and responding with a number of process control signals. Communications between the control modules and host computer are primarily limited to direct operator commands from the console and critical operating information from the subsystems for console display. This distributed control system reduces the number of instrumentation and control links between the subsystems and control room.

The process control module consists of a digital computer control unit, a multiplexer, an analog-to-digital converter, and a digital-to-analog converter. Analog signals from the process instrumentation are converted to



digital signals, selected in rotation by the multiplexer, and analyzed by the control unit. The module responds with an appropriate digital control signal which is passed through the multiplexer and sent to the appropriate controller. Each process control module is capable of monitoring 30 analog signals per second, monitoring 95 thermocouples, generating 20 analog control signals, and controlling over 100 on-off switches.

One process control module (PCM 1), located below the receiver in the tower elevator, is dedicated to the control of the receiver. A second module, (PCM 2) located at the base of the tower, controls the heat rejection and electric power generation subsystem. The third module, (PCM 3), located in the control building adjacent to the salt storage tanks, is used to control the thermal storage subsystem and to command the Network 90 controlled steam generation subsystem.

The receiver subsystem PCM will modulate the salt flow rate to the receiver to maintain, as closely as possible, a constant outlet temperature of 1000°F. Individual thermocouples are located on the receiver to measure intermediate salt temperatures. From this information, the control module estimates the flux on the receiver, and feed-forward a signal to the salt control valves at the receiver inlet. The control module also controls the receiver start-up and shutdown purge and drain valves.

Control of the thermal storage subsystem involves the operation of the two salt downcomer flow control valves, cold salt pumps, salt storage tanks and piping heat tracing, and the propane-fired salt heater. The downcomer throttling valves are controlled by the receiver control system to maintain a constant level in the receiver hot surge tank. Salt equipment heat trace temperatures are monitored continuously by the Acurex Data Logger. The propane-fired salt heater is operated intermittently, under manual control, during subsystem checkouts.

Automatic control of the heat rejection and electric power generation subsystem involves the control of the steam and condensate flows to the deaerator, steam flow to the feedwater heater, and the operation of the cooling water, spray water condensate, and feedwater pumps. The EPGS condenser

temperature, level and pressure are monitored by the master control subsystem. The deaerator temperature is maintained by controlling the steam flow from the main steam header. The final feedwater temperature is maintained by controlling the main steam flow to the feedwater heater.

Automatic control of the steam generation subsystem primarily involves the control of steam pressure, steam temperature, drum water level, and the evaporator salt inlet temperature through the network 90 control system. The water level in the drum is controlled by modulating the control valve downstream of the feedwater pump. Control of the main steam pressure is accomplished by modulating the salt flow control valve downstream of the evaporator. Steam temperature is controlled using an attemperator to mix steam from the steam drum with the output of the superheater. The evaporator salt inlet temperature is controlled by monitoring the inlet salt temperature, and modulating the cold salt control valve at the mixing tee between the superheater and evaporator.

3.2.2 Network 90 System

The Bailey Network 90 Control System consists of two units, one process control unit (PCU) and one operation interface unit (OIU).

The PCU architecture is based on two key modules, the Controller Module (COM) and the Logic Master. Together, these modules provide a mix of both modulating and sequential control functions including: base, cascade, or ratio PID control, high/low and rate limiters, engineering units conversion, general function generator, square root, summation, multiplication, lead/lag, and transfer select, or, and, not, time delay, and several others. The controller module can service up to four analog and three digital inputs and two analog and four digital outputs. The COM also provides A/D and D/A conversion, alarm limit checking (absolute and deviation) and notification, point quality checking and interlocking.

The Operator Interface Unit (OIU) provides the high level operator interface for the Network 90 system. The OIU consists of a color CRT-based table-top console, with functional keyboard, mass storage device, and console driver electronics.

In operation, the unit performs the system information display and control requirements. The OIU console includes a CRT keyboard and pushbutton hardware for process overview, alarm indicating, loop control, trending, tuning and configuration functions.

The OIU uses microprocessor, memory and I/O modules to support system functions. It furnishes monitoring, supervisory, recording and display capability at centralized or distributed locations, along with engineering functions.

3.2.3 Data Acquisition

The DAS utilizes both the EMCON-D2 and an HP-1000. EMCON collects the data and HP-1000 stores and displays data. Data collected by the EMCON system is transmitted to the HP-1000 system on a terminal-to-terminal data link. The tag list for the data to be collected is in a file of 180 tags, which are divided into 6 groups of 30 tags. One group of 30 is transmitted every 10 seconds, giving a total update rate of once a minute. The data are then time tagged with day of the year, hour, minute, second, millisecond. Then the data are stored in a data file and/or displayed on one of six CRTs in a graphical form. Also, the data are transmitted in integer format, not floating point, but they are in engineering units. The data files are divided into eight-hour blocks, so if a test runs longer than eight hours, another eight-hour block is assigned to that test's file. Normally an 8-hour data block is stored in 19 tracks out of a maximum usable 1000 tracks.

The live data can be displayed on the 6 CRTs with 3 tags per screen, a time scale of 3 hours 20 minutes, and a Y-scale displayed of the first tag's display range. The other two tags are displayed using their respective ranges, but the scales are not shown on the plot. When the plot is full the plot scrolls left dropping the oldest 1/4 of the time scale data. This leaves 1/4 of the plot blank for new data. These plots can have hard copies made, but not automatically. The print is done by manual switch selection of each screen and a copy page switch.

Recovery of stored data can be done whenever live data files are not being made. These plots have a slightly different format, three being a maximum of five tags per plot, and the Y scale shown is that of the last tags range. These plots are not displayed on a CRT, but directly generated on the printer/plotter.

3.3 RECEIVER SUBSYSTEM

The receiver subsystem (Figure 3.4) captures the insolation redirected from the heliostat field and converts it to thermal energy in the molten salt. The subsystem consists of the receiver absorber panel, cavity enclosure with one vertical aperture door, insulation, heat tracing, cold surge tank, booster pump, hot surge tank, overflow tank, instrumentation, and control valves. The receiver is located at the top of the CRTF tower.

The receiver was tested in a previous subsystem research experiment. Since the initial experiment, the receiver has been refurbished. This refurbishment included instrumentation and control system modifications, minor structural and piping changes, and the replacement of the two original horizontal cavity doors with one vertical aperture door.

The receiver absorber is a single panel with 18 vertical passes having 16 tubes per pass. The tubes are Incoloy 800 with 19 mm (0.75 in.) outside diameter. Purge and drain valves are provided for each pair of passes.

The receiver surge tanks are designed to dampen changes in the salt flow rate and to maintain salt flow through the receiver in the event of a cold salt pump outage. The cold surge tank is pressurized with facility-supplied instrument air to supply the necessary head to force the salt through the receiver in the event of a pump outage, and to provide a surge volume within the tank. The hot surge tank operates at atmospheric pressure, and is vented to an adjacent overflow tank in the event of a control problem in the salt downcomer throttle valve.

The cold salt booster pump takes its suction from the discharge of the cold salt pump and provides the necessary head for the salt as it travels up the tower and through the receiver.

The cold salt line to the receiver starts at the booster pump, rises to the top of the hot storage tank, traverses the distance from the storage tanks to the receiver tower on an elevated pipe bridge, enters the tower, and runs up the east side of the tower in an existing pipe chase to the receiver. The hot salt line leaves the hot surge tank and traverses to the pipe chase. The hot salt downcomer carries the salt to the level of the pipe bridge. The hot salt line traverses the bridge, ending in a control valve which throttles the flow

to the hot storage tank. The salt piping is inclined between the storage tanks and the tower to ensure that the piping system will completely drain. The salt piping is electrically heat traced and insulated with calcium silicate and aluminum sheathing.

The receiver components are listed on Table 3.2; valves are described on Table 3.3; instrumentation is listed on Table 3.4; and control loops are described on Table 3.5.

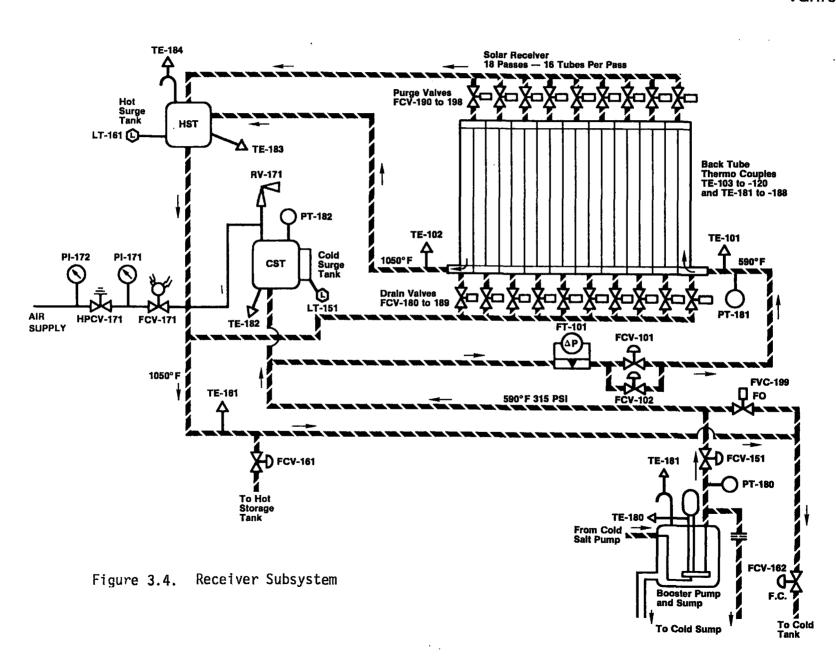


Table 3.2
Receiver Subsystem Components

Component	Description	Function	Nominal Operating Condition
Receiver	 - 18 ft wide x 13 ft high panel - 18 serpentine passes Incoloy 800 tubes 	- Heat molten salt with solar energy from heliostat field	- 590°F inlet salt - 1050°F outlet salt - 96,867 lb/hr
	- 16 tubes per pass - 3/4 in. dia. tubes		- 5 MW rating
Cold salt booster sump	- Carbon steel cylindrical tank	- Reservoir for cold salt pump	- 590°F salt - Atmospheric pressure
Cold salt booster pump	- Vertical cantilever type	- Supply additional head to outlet of cold salt pump to provide salt circulation through receiver	- 590°F salt - 96,867 lb/hr
Cold surge tank	Carbon steel cylindrical tank3 ft. dia.7 ft. high	 Dampen changes in salt flow rate Provide emergency salt flow through receiver until solar flux can be removed in the event of pump outage 	- Pressurized to 125 psi
Hot surge tank	Stainless steel cylindrical tank2 ft. dia.7 ft. high	- Dampen changes in salt flow rate	- Atmospheric pressure



RECEIVER SUBSYSTEM REMOTE OPERATED VALVES

VALVE	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-101 FCV-102	Valtek	2"	CA	F0	Receiver Flow Control	Near Receiver Lower West Corner
FCV-151	Valtek	2"	CA	FC	Receiver Fill Control Cold Surge Level Control	Above Hot Tank
FCV-161	Valtek	2"	CA	F0	Hot Surge Tank Level Control	Above Hot Tank
FCV-162	Valtek	2"	CA	FC	Hot Surge Tank Level Control (Receiver)	Above Hot Tank
FCV-180 thru FCV-189	Kieley-Mueller	1 1/2"	SV	FC	Receiver Fill and Drain	Below Receiver
FCV-190 thru FCV-198	Kieley-Mueller	1 1/2"	SV	FC	Receiver Purge	Above Receiver
FCV-199	Kieley-Mueller	2"	sv 1	FC	Allow Downcomer Backflow During Receiver Fill and	Above Hot Tank
	•	*	Calso Isolo	value catted tron alver	Permit Drainage to Cold Storage Tank During Shutdown	

Table 3.4
Receiver Subsystem Instrumentation

Identifier Description	Control Module	Display Range	Alarm Levels				
			High	Low	Dimension	Sampling Period (sec	
	Boost Pump						
PT-180	Discharge pressure - gots to	РСМ 3	0-400	350	275	PSI	2
TE-180	Bearing temp	РСМ З	0-500	190		°F	10
TE-181	Sump vent temp Hot surge tank For the second temp to the second temp temp to the second temp temp temp temp temp temp temp temp	PCM 3	0-1200	350		°F	10
LT-161	1 7	PCM 3	0-100	70	15	inch	2
TE-183	Salt temp	PCM 1	0-1200	1070	500	°F	10
TE-184	Vent temp	PCM 1	0-1200	400		°F	10
LT-151	Leve1	PCM 1	0-100	90	10	inch	10
TE-182	Level normation so we dering normal Salt temp	PCM 1	0-1200	750	500	°F	10
PT-182	Pressure	PCM 1	0-200	180	10	PSI	10
TE-161	Downcomer outlet temp	PCM 3	0-1200	1070	500	°F	2
Sun	Solar insolation - not in a	PCM 3	0-1000			W/M ²	5
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Table 3.4
Receiver Subsystem Instrumentation

		Control Module	Display Range	Alarm	Levels		
Identifier	Identifier Description			High	Low	Dimension	Sampling Period (sec
	Receiver						
PT-181	Inlet pressure -directly related	PCM 1	0-200	125	10	PSI	10
FT-101	Salt flow rate	PCM 1	0-100	100		KLB/hr	
TE-101	Salt inlet temp	PCM 1	0-1200	650	500	°F	2
TE-102	Salt outlet temp	PCM 1	0-1200	1060	500	°F	2
TE-103	Back tube-pass #1 outlet	PCM 1	0-1200	640	500	°F	2
TE-104	Back tube-pass #2 outlet	PCM 1	0-1200	665	500	°F	2
TE-105	Back tube-pass #3 outlet	PCM 1	0-1200	690	500	°F	2
TE-106	Back tube-pass #4 outlet	PCM 1	0-1200	720	500	°F	2
TE-107	Back tube-pass #5 outlet	PCM 1	0-1200	750	500	°F	2
TE-108	Back tube-pass #6 outlet	PCM 1	0-1200	780	500	°F	2
TE-109	Back tube-pass #7 outlet	PCM 1	0-1200	810	500	°F	2
TE-110	Back tube-pass #8 outlet	PCM 1	0-1200	835	500	°F	2
TE-111	Back tube-pass #9 outlet	PCM 1	0-1200	865	500	°F	2
TE-112	Back tube-pass #10 outlet	PCM 1	0-1200	890	500	°F	2
TE-113	Back tube-pass #11 outlet	PCM 1	0-1200	920	500	°F	2
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Table 3.4
Receiver Subsystem Instrumentation

		Control Module	Display Range	Alarm	Levels		
Identifier	Description			High	Low	Dimension	Sampling Period (sec
	Receiver (cont.)						
TE-114	Back tube-pass #11 outlet	PCM 1	0-1200	950	500	°F	2
TE-115	Back tube-pass #12 outlet	PCM 1	0-1200	975	500	°F	2
TE-116	Back tube-pass #13 outlet	PCM 1	0-1200	990	500	°F	2
TE-117	Back tube-pass #14 outlet	PCM 1	0-1200	1010	500	°F	2
TE-118	Back tube-pass #15 outlet	PCM 1	0-1200	1030	500	°F	2
<u>~</u> TE-119	Back tube-pass #16 outlet	PCM 1	0-1200	1050	500	°F	2
TE-120	Back tube-pass #17 outlet	PCM 1	0-1200	1070	500	°F	2
TE-131	Back tube-pass #1 upper	PCM 1	0-1200	645	500	°.F	10
TE-132	Back tube-pass #5 upper	PCM 1	0-1200	745	500	°F	10
TE-133	Back tube-pass #8 upper	PCM 1	0-1200	815	500	°F	10
TE-134	Back tube-pass #11 upper	PCM 1	0-1200	915	500	°F	10
TE-135	Back tube-pass #14 upper	PCM 1	0-1200	980	500	°F	10
TE-136	Back tube-pass #17 upper	PCM 1	0-1200	1045	500	°F	10
TE-137	Back tube-pass #2 middle	PCM 1	0-1200	680	500	°F	10
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Table 3.4
Receiver Subsystem Instrumentation

			D	Alarm L	_evels		
Identifier Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec	
	Desainer (seet.)		·				
	Receiver (cont.)				,		
TE-138	Back tube-pass #6 middle	PCM 1	0-1200	735	500	°F	10
TE-139	Back tube-pass #8 middle	PCM 1	0-1200	825	500	°F	10
TE-140	Back tube-pass #11 middle	PCM 1	0-1200	905	500	°F	10
TE-141	Back tube-pass #14 middle	PCM 1	0-1200	990	500	°F	10
ېن TE-142	Back tube-pass #17 middle	PCM 1	0-1200	1045	500	°F	10
19 TE-143	Back tube-pass #1 bottom	PCM 1	0-1200	660	500	°F	10
TE-144	Back tube-pass #5 bottom	PCM 1	0-1200	725	500	°F	10
TE-145	Back tube-pass #8 bottom	PCM 1	0-1200	830	500	°F	10
TE-146	Back tube-pass #11 bottom	PCM 1	0-1200	895	500	°F	10
TE-147	Back tube-pass #14 bottom	PCM 1	0-1200	985	500	°F	10
TE-148	Back tube-pass #17 bottom	PCM 1	0-1200	1035	500	°F	10
TE-185	Header-pass #2 outlet	PCM 1	0-1200	665	500	°F	10
TE-186	Header-pass #3 outlet	PCM 1	0-1200	690	500	°F	10
					1		

Table 3.4
Receiver Subsystem Instrumentation

		Contus	Diagram	Alarm L	.evels		_
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Receiver (cont.)						
TE-187	Header-pass #4 outlet	PCM 1	0-1200	720	500	٥F	10
TE-188	Header-pass #5 outlet	PCM 1	0-1200	750	500	°F	10
TE-189	Header-pass #6 outlet	PCM 1	0-1200	780	500	°F	10
TE-190	Header-pass #7 outlet	PCM 1	0-1200	810	500	°F	10
TE-191	Header-pass #8 outlet	PCM 1	0-1200	835	500	°F	10
မှ ည TE-192	Header-pass #9 outlet	PCM 1	0-1200	865	500	. °F	10
TE-193	Header-pass #12 outlet	PCM 1	0-1200	950	500	°F	10
TE-194	Header-pass #13 outlet	PCM 1	0-1200	975	500	°F	10
TE-195	Header-pass #14 outlet	PCM 1	0-1200	990	500	°F	10
TE-196	Header-pass #15 outlet	PCM 1	0-1200	1010	500	°F	10
TE-197	Header-pass #16 outlet	PCM 1	0-1200	1030	500	°F	10
TE-198	Header-pass #17 outlet	PCM 1	0-1200	1050	500 .	°F	10

Table 3.5
Receiver Subsystem Control Loops

(ontrolled Variable	Mode	Set Point	Controller Inputs	Controller Output
	Receiver salt flow	Constant flow (start-up & shutdown with receiver con- trol algorithm off scan Constant Outlet Temperature (Receiver con- trol algorithm	30 KLB/hr FD-101 1000°F SP. SALT	Flow set point (FD-101) Measured flow (FT-101) Temperature set point (SP. SALT) Outlet temperature (TE-102) Inlet temperature (TE-101) Salt flow (FT-101) Receiver back tube temperatures (TE-103 thru TE-120)	FCV-101/102 position FCV-101/102 position
3-21	Hot surge tank level	Operation	20 in FCV-161 FCV-162	Surge tank level (LT-161) Level set point	FCV-161 or FCV-162 position (selection based on salt temperature)
	Receiving storage tank selection	Operation	750°F	Downcomer salt temperature (TE-161)	TE-161 < 750°F Cold storage tank selected TE-161 > 750°F Hot storage tank selected
	Cold surge tank level	Operation	~85" LT-151	Cold surge tank level (LT-151) Level set point	FCV-151 position

when teles miches 750°F control goes from FeVIGI & FeVIGE to only FeVIGI (FeVIGE closes beckers you want the soult to go into hot storage tank)

PEUISI is in engrade with LTIST

3.4 THERMAL STORAGE SUBSYSTEM

The thermal storage subsystem provides a cold salt source for the receiver for daytime operation, and a hot salt source for the steam generator for day and early evening operation. The TSS can also furnish a source of thermal energy for overnight freeze protection of the receiver, steam generator, and salt piping and for early morning plant start-up. The subsystem includes the hot and cold salt storage tanks, propane-fired salt heater, cold salt pump and cold salt sump. The subsystem schematic is shown on Figure 3.15. Major components are described on Table 3.6; valves are listed on Table 3.7; instrumentation is described on Table 3.8; and control loops are given on Table 3.9.

The salt pump is of a vertical cantilever design. The impeller and casing are suspended below the liquid level in a sump; the bearings are located above the liquid level and do not contact the salt.

The hot salt tank employs a unique design. To allow the use of carbon steel in the structural portions of the tank, an internal refractory insulation is used to limit the temperature of the walls, roof, and floor. A waffled Incoloy liner separates the salt and the internal insulation, and the tank foundation is cooled with circulating water to limit the floor temperature. The outside of the tank is insulated in the conventional manner with calcium silicate and aluminum sheathing. The cold salt tank is similar in design to the hot tank except that it does not require the internal insulation and liner due to its lower operating temperature.

Figure 3-5. Thermal Storage Subsystem Schematic

3-23

Component	Description	Function	Nominal Operating Condition
Cold salt storage tank	 Carbon steel cylindrical tank 12.3 ft. dia. 12.3 ft. high 15 in fibrous external insulation 	- Cold salt storage	- 590°F salt
Hot salt storage tank	 Carbon steel cylindrical shell 12.3 ft. dia. stainless steel liner 23.6 ft. high 13-1/2 in. insulating firebrick between shell and liner 	- Hot salt storage	- 1050°F salt - Approx. 7 MW _t hr storage capacity
Cold salt sump	2 in. fibrous external insulationCarbon steel cylindrical tank59 in. dia.	- Pump reservoir	- 590°F salt
Cold salt pump	- 66 in. deep- Vertical cantilever type- 60 H.P. driver	- Pump salt from cold storage tank to cold salt booster pump, SGS, or propane heater	- Atmospheric pressure - 590°F salt - 96,867 lb/hr
		565, or propane heater	

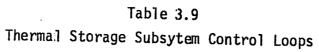
Table 3.6
Thermal Storage Subsystem Components - 2

Component	Description	Function	Nominal Operating Condition
Hot salt sump	Stainless steel cylindrical tank48 in. dia.49 in. deep	- Reservoir for hot salt pump	- 1050°F salt - Atmospheric pressure
dot salt pump	- Vertical cantilever type - 7-1/2 HP driver	- Provide hot salt circulation through STS	- 1050°F salt - 64,680 lb/hr
ropane heater	- 3 MW propane fired heater - 9 ft. dia. shell - 24 ft. high - One stainless steel heating coil, 2.12 in. dia., 1640 ft. long	- Provide auxiliary salt heating capability	- 59,900 lb/hr salt - 590°F inlet - 1050°F outlet

Table 3.7 .
THERMAL STORAGE SUBSYSTEM REMOTE OPERATED VALVES

VALVE	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-201	Valtek	3"	CV	FC	Cold Sump Level Control	Cold Storage Tank Base South Side
FCV-211	Kieley-Mueller	3"	SV	FC	Cold Sump Isolation	Pump House North Side West End
FCV-221	Valtek	3"	CV	FC	Hot Sump Level Control	Hot Storage Tank Southwest Side
FCV-231	Kieley-Mueller	3"	SV	FC	Hot Sump Isolation	Outside Pumphouse Northeast Corner
FCV-241	Valtek	2"	CV	FC	Propane Heater Flow Control	Line to Propane Heater East of FCV-231
FCV-242	Valtek	1 1/2"	SV	FC	Propane Heater Isolation	Top of Hot Tank

		Cautural	Dia i	Alarm L	_evels		
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Cold Storage Tank						
LT-281	Level	РСМ З	0-150	134	15	inch	10
TE-281	Lower temp	PCM 3	0-1200	700	500	°F	10
TE-282	Middle temp	PCM 3	0-1200	700	500	°F	10
TE-283	Upper temp	PCM 3	0-1200	700	500	°F	10
	Hot storage tank						
LT- 291	Level	PCM 3	0-200	190	10	inch	10
TE-291	Lower temp	PCM 3	0-1200	1070	500	°F	10
TE-292	Middle temp	PCM 3	0-1200	1070	500	°F	10
TE-293	Upper temp	PCM 3	0-1200	1070	500	°F	10
	Cold salt pump						
LT-201	Sump level	PCM 3	0-60	60	15	inch	2
TE-286	Bearing temp	PCM 3	0-500	190		°F	10
TE-211	Vent temp	PCM 3	0-1200	400		°F	2
	Hot Salt Pump						
LT-221	Sump level	PCM 3	0-48	41	15	inch	2
TE-231	Vent temp	PCM 3	0-1200	400		°F	2
							_



Mode	Set Point	Controller Inputs	Controller Output						
Operation	23 in FCV-201 (45 in fill)	Sump level (LT-201) Level set point	FCV-201 position - Flow from cold storage tank						
Operation	20 in FCV-221	Sump level (LT-221) Level set point	FCV-221 position - Flow from hot storage tank						
			·						
		·							
		,							
	Operation	Operation 23 in FCV-201 (45 in fill) Operation 20 in	Operation 23 in FCV-201 (45 in fill) Operation 20 in FCV-221 Sump level (LT-201) Level set point Sump level (LT-221) Level set point						

3.5 STEAM GENERATION SUBSYSTEM

The steam generation subsystem transfers sensible heat from the molten salt to produce superheated steam for the turbine-generator. The subsystem schematic is shown on Figure 3.6. The subsystem includes an evaporator, steam drum, boiler recirculation pump, superheater, and attemperator.

The evaporator and superheater are U-tubes, U-shell heat exchangers, with low pressure salt on the shell side and high-pressure water and steam on the tube side. This shell and tube configuration has been selected to minimize thermal stresses, due to differential expansion, in the tubes and tubesheets.

A conventional steam drum, located above the evaporator, separates water droplets from the saturated steam before the latter enters the superheater, and receives feedwater from the feedwater heater. A forced recirculation design was selected, since it is preferred for power plants requiring daily start-up and shutdown.

The superheater outlet steam can be attemperated by mixing with a small amount of saturated steam from the drum. The salt flow from the superheater to the evaporator is also attemperated to 850°F, when necessary, by mixing with salt flow from the cold tank. This allows chrome-moly piping and fittings, rather than stainless steel, to be used in the evaporator.

Warmup of the steam generation subsystem is accomplished by isolating the subsystem and preheating with the subsystem's electrical heater.

Major subsystem components, valves, instrumentation, and control loops are described on Tables 3.10 through 3.13.

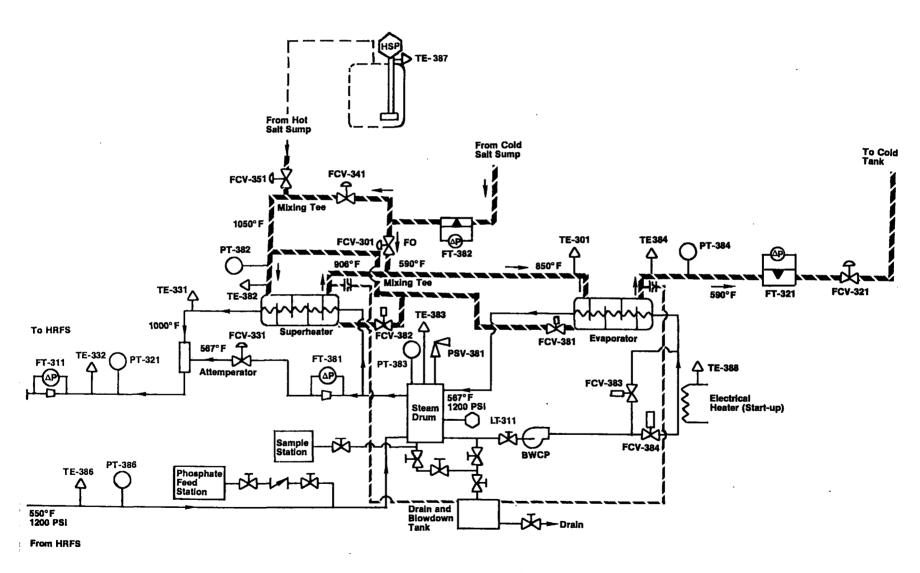


Figure 3.6 . Steam Generation Subsystem Schematic

Component	Description	Function	Nominal Operating Condition
Evaporator	 U-tube/U-shell counterflow heat exchanger 8 in. dia. chrome - moly shell (salt) 27 chrome-moly tubes 0.875 in. dia. 68 ft avg. length (water) 	- Evaporate subcooled water to produce saturated steam/water mixture	 - 850°F salt inlet - 590°F salt outlet - 78,550 lb/hr salt flow rate - Subcooled water inlet - 567°F, 1200 psi saturated steam/water outlet - 2.15 MW rating
Superheater	 U-tube/U-shell counterflow heat exchanger 6 in. dia. stainless steel shell (salt) 23 stainless steel tubes 0.500 in. dia. 33 ft. avg. length (steam) 	- Heat saturated steam to superheat condition	- 1050°F salt inlet - 906°F salt outlet - 64,680 lb/hr salt flow rate - 567°F 1175 psi saturated steam inlet - 1000°F. 1100 psi superheated vapor outlet - 10,530 lb/hr steam flow rate - 0.98 MW rating
Steam Drum	 Cylindrical pressure vessel with elliptical heads 24 in ID 6 ft 10 in overall height 2 in thick carbon steel Contains primary cyclone steam separator and primary & secondary steam scrubbers 	 Separate steam/water mixture exiting evaporator Supply saturated steam to superheater Provide feedwater surge volume 	- 567°F - 1200 psi

Component	Description	Function	Nominal Operating Condition
Boiler water circulation pump	- Canned centrifugal type - 5 HP driver	- Provide circulation of subcooled water from the steam drum to evaporator. Maintain high recirculation rate over full range of operating conditions.	- 560°F - 119 GPM - 111 ft. head
Start-up heater	 Chamber type electric heater 3 40-kW heating elements 2 15-kW heating elements 	 Raise temperature and pressure of water during cold start-up to avoid salt freeze-up in evaporator Heat boiler water to maintain temperature and pressure of water/steam system during diurnal hold 	- Cycled during diurnal hold - Bypassed during normal operation
Steam attemperator	- Mixing tee	- Mix saturated steam from steam drum with super-heated steam from super-heater to control steam delivery temperature to turbine	 1053 lb/hr dry saturated steam at 567°F 10,529 lb/hr superheated steam at 1000°F 1100 psi 11,582 lb/hr delivery steam at 950°F 1100 psi
Salt attemperator (evaporator inlet)	- Mixing tee	- Mix cold salt with superheater outlet salt to limit evaporator inlet salt temperature to 850°F because of Cr-Mo construction	- 64,680 lb/hr at 906°F - 13,870 lb/hr at 590°F - 78,550 lb/hr at 850°F supplied to evaporator

Table 3.10. Steam Generation Subsystem Components - 3

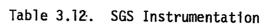
Component	Description (2)	Function	Nominal Operating Condition
Salt start-up attemperator (superheater inlet)	- Mixing tee	- Mix cold salt with hot salt from hot tank to provide a controlled temperature increase of salt entering superheater during start-up	- Full flow of cold salt at start-up - No cold salt flow during operation
Heat tracing	- Electrical heating element - Inconel sheath	- Maintain heat exchangers and salt piping above the freezing point of salt	- Temperature monitored by thermocouples - Cycle as required
		- Provide freeze protec- tion of feedwater piping and instrumentation during shutdown	
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Table 3. 11 SGS REMOTE OPERATED VALVES

VALVE	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-301	Valtek	1"	CV	F0	Evaporator Salt Temperature Control and Cold Salt Fill	SGS Skid West Side South End
FCV-321	Valtek	2"	CA	F0	Main Salt Flow Control	SGS Skid South End
FCV-331	Fisher	1"	CV	F0	Steam Attemperator Temperature Control	SGS Skid North Side Steam Drum
FCV-341	Valtek	1"	CV	FC	Main Salt Fill	SGS Skid West Side Middle
FCV-351	Valtek	2"	CV	F0	Hot Salt Flow Control	Outside Pumphouse Northeast Corner
FCV-381	Kieley-Mueller	1"	SV	FC	Evaporator Salt Drain	SGS Skid West Side Middle
FCV-382	Kieley-Mueller	1"	SV	FC	Superheater Salt Drain	SGS Skid West Side Below Steam Drum
FCV-383	Dresser	4"	SV	F0	Evaporator Water Supply	SGS Skid Southeast Corner
FCV-384	Valtek	2"	SV	F0	Start-up Heater Supply	SGS Skid Below FCV-383

Table 3.12% SGS Instrumentation

		Comtural	D4 7	Alarm L	evels		_
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec)
	Feedwater						
PT-386	Pressure	PCM-3/ Bailey	0-1500	1500		PSI	5
TE-386	Temp	PCM-3/ Bailey	0-750	575	500	°F	10
	Steam Drum						
PT-383	Pressure	PCM-3/ Bailey	0-1500	1250	950	PSI	5
TE-383	Fluid temp	PCM-3/ Bailey	0-750	575	500	°F	10
LT-311	Fluid level	PCM-3/ Bailey	-17 to +23	. 4	-4	inch	2
	Evaporator						
TE-301	Salt inlet temp	PCM-3/ Bailey	0-1200	880	500	°F	2
TE-384	Salt outlet temp	PCM-3/ Bailey	0-1200	640	500	°F	2
PT-384	Salt outlet pressure	PCM-3/ Bailey	0-200			PSI	5
FT-321	Salt flow rate	PCM-3/ Bailey	0-100			KLB/hr	2



			. .	Alarm Levels			
Identifier	Description	Control Module	Display Range	High	Low	Dimension	Sampling Period (sec
	Superheater						
PT-382	Salt inlet pressure	PCM-3/ Bailey	0-200	100		PSI	5
TE-382	Salt inlet temp	PCM-3/ Bailey	0-1200	1070	500	°F	5
TE-331	Steam outlet temp	PCM-3	0-1200		910	°F	2
FT-381	Attemperator steam flow	Bailey PCM-3/ Bailey	0-2500			lb/hr	5
FT-382	SGS Cold Salt Supply	PCM-3/ Bailey	0-16			KLB/hr	5
	Steam Delivery						
PT-321	Pressure	PCM-3/ Bailey	0-1500	1150	950	PSI	2
TE-332	Temp	PCM-3/ Bailey	0-1200	990	910	°F	2
FT-311	Flow rate	PCM-3/ Bailey	0-100	12.6	3.2	KLB/hr	2
TE-387	Hot Salt Pump Bearing	PCM-3	0-500	190		°F	10
TE-388	Start-up Heater 5 Element Temp	PCM-3/ Bailey	0-1200	1100	500	°F	10
			,				

Controlled Variable	Mode	Set Point	Controller Inputs	Controller Output
Steam delivery pressure	SGS start-up	1000 psig FCV-491	Delivery pressure (PT-321) pressure set point	FCV-491 position - SGS steam flow
	Boiler following	1100 psig SP. SP	Delivery pressure (PT-321) Pressure set point (SP. SP) Steam flow (FT-311) Salt flow (FT-321)	FCV-321 position - SGS main salt flow
Steam delivery temperature	Operation	950°F SP. ST	Delivery temperature (TE-332) Temperature set point (SP. ST)	FCV-331 position - Steam attemperator flow
Steam drum level	Operation	O in SP. DL	Drum level (LT-311) Level set point (SP. DL) Feedwater flow (FT-411) Steam flow (FT-311)	FCV-411 position - Feedwater flow
Evaporator salt inlet temperature	Operation	850°F SP. EST	Inlet temperature (TE-301) Temperature set point (SP. EST)	FCV-301 position - Cold salt flow
Boiler water temperature	Diurnal Shutdown	~ 520°F	Circulation heater outlet temperature (TE-388)	Electric immersion heater elements on/off

3.6 ELECTRIC POWER GENERATION SUBSYSTEM

The electric power generation subsystem converts the enthalpy in the main steam flow to electricity. The subsystem (Figure 3.7) includes the steam turbine, electric generator, electric power equipment, condenser, condensate pump and storage tank. The electrical one-line diagram is shown on Figure 3.8.

The turbine-generator set is a skid-mounted unit located at the north end of the receiver tower complex at the 80 ft. level (20 ft. below grade). This skid consists of a turbine, generator, and auxiliary equipment. The turbine is a seven-stage, single flow machine, operating at 17,400 rpm. Inlet steam conditions are rated at 940°F and 1050 psia. A single reduction gearbox reduces the turbine shaft speed to the generator speed of 1,200 rpm. The 750 kW generator operates at 450V, and is cooled by circulating water through air cooling coils located above the generator. The turbine-generator auxiliaries include a lubricating oil pump, lube oil cooler, air ejection vacuum pump and mechanical-hydraulic governor. The allowable rate of change in load is 10 percent per minute from 30 to 100 percent of rated capacity.

A shell and tube condenser, supported by a separate frame, is located directly below the turbine. Access to the condenser is on the floor 40 ft. below ground. Condensate from the hot well of the condenser will be transferred to the deaerator when the water level in the deaerator requires makeup. Otherwise, the condensate is pumped to a storage tank. Condensate from this tank is piped back to the condenser hot well when the hot well level requires water.

Major components of the EPGS, valves, instrumentation, and control loops are described on Tables 3.14 through 3.17.

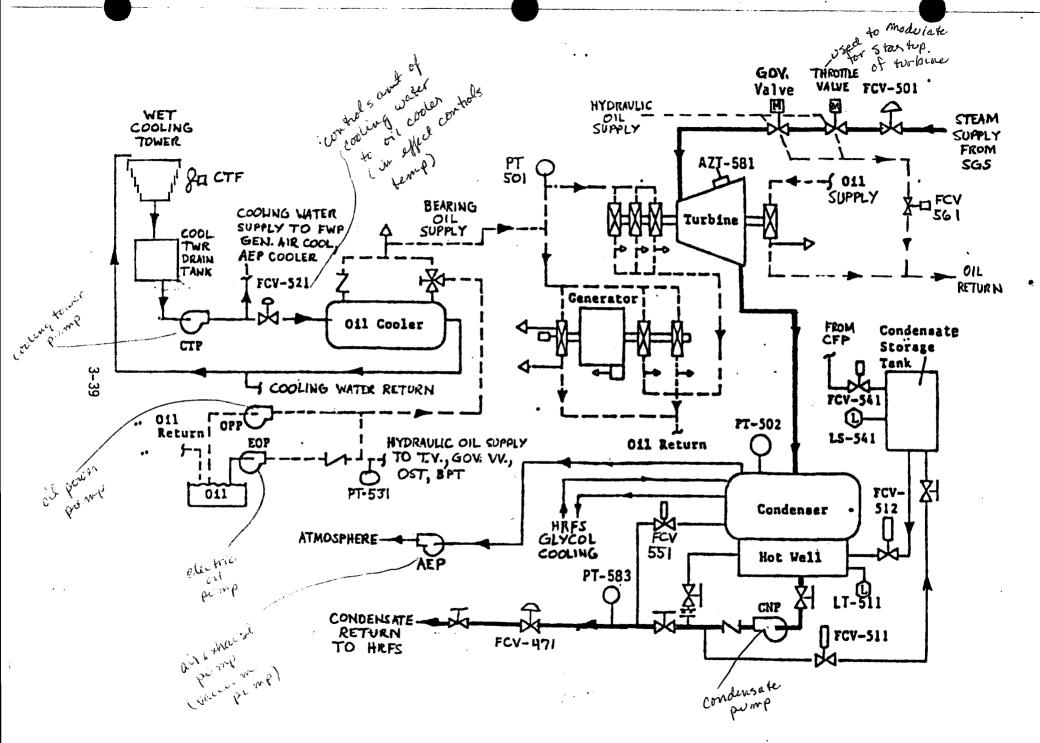


Figure 3.7. Electric Power Generation Subsystem Schematic

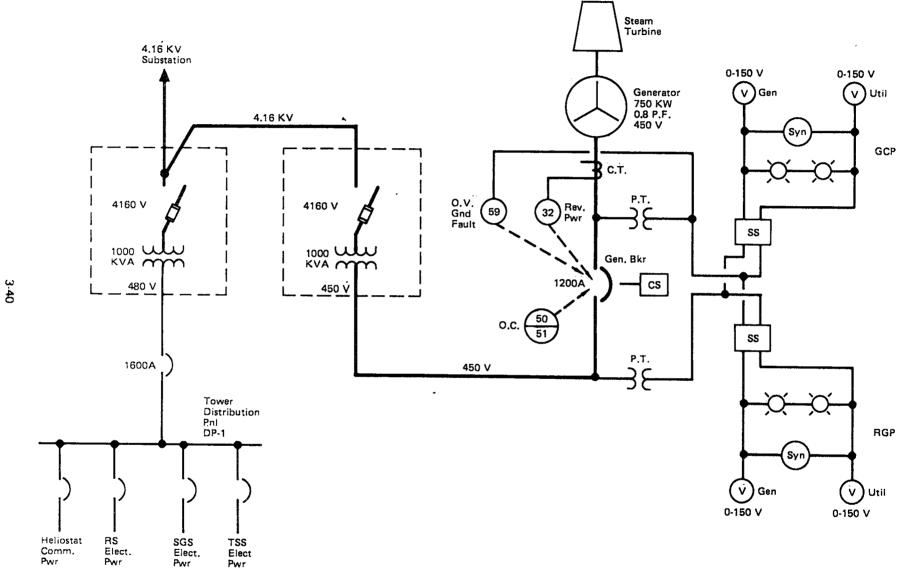


Figure 3.8. MSEE Electric Generator One-Line Diagram

Table 3.14
Electric Power Generation Subsystem Components

Component	Description of	Function	Nominal Operating Condition
Turbine	Axial flow condensing type7 stage	- Expand steam to drive electric generator	 940°F 1050 psig throttle steam 133°F 2.5 psia exhaust steam 7800 lb/hr steam flow 17,443 RPM 1000 HP
Electric generator	AC generator450 volt, 3 phase1200 RPMSolid state excitor	- Generate electric power	 750 kW_e (rating) 600 kW_e (maximum in MSEE) 0.8 power factor rating
Condenser	 Crossflow shell and tube heat exchanger Rectangular shell (condensate) 438 tubes, 5/8-in. dia. 7-1/2 ft long (glycol/water coolant) Cylindrical hot well 	- Condense turbine exhaust steam - Provide turbine exhaust vacuum	 2.5 psia saturated steam inlet 133°F condensate outlet 7800 lb/hr steam/water flow 1200 GPM glycol/water coolant flow
Condensate pump	- Turbine type - 2 stage - 20 HP driver	- Pump condensate from hot well to deaerator	- 133°F water - 260 psi head (mfg rating) - 18 GPM (mfg rating)

Table 3.14 Electric Power Generation Subsystem Components

Component	Description	Function	Nominal Operating Condition	
Air exhaust pump	- Nash vacuum pump - 5 HP driver	- Provide condenser vacuum	 5 in Hg condenser pressure (ABS) 75 CFM (mfg. rating) 	
Electric oil pump	- Viking gear pump	- Provide bearing oil pressure during turbine start-up and shutdown (turbine-driven pump provides oil pressure during operation)	- Off during operation	
Cooling tower pump	-Aurora centrifugal pump	- Provide coolant circulation through oil cooler	- 35 psi head (mfg. rating) - 120 GPM (mfg. rating)	
Wet cooling tower	-Fan forced wet cooler -1/2 HP fan motor	- Reject oil coolant heat	- 110°F coolant outlet temp	

Table 3.15
EPGS REMOTE OPERATED VALVES

VALVES	MANUFACTURER	SIZE	ТҮРЕ	FAIL POSITION	FUNCTION	LOCATION
FCV-501	Valtek	2"	SV	FC	Turbine Steam Isolation	TWR Level 80 North Turbine Northeast Corner
FCY-511	Asco	1/2"	SV	FC	Hotwell Overflow	TWR Level 60 North Condenser Platform Northwest
FCV-512	Asco	3/4"	SV	FC	Hotwell Make-up	TWR Level 80 Northeast Condensate Storage Tank
FCV-521	Masoneilan	2"	CV	F0	Oil Cooler Water . Flow Control	TWR Level 80 North Turbine/Generator Overhead
FCV-541	Asco	3/4"	SV	FC	Condenser Storage Tank Make-up	TWR Level 80 Northeast Condensate Storage Tank
FCV-551	Asco	1/2"	SV	FC	Condenser Recirculation	TWR Level 60 North Condenser Platform Northwest
TVM	GE w/auma Actuator	1 1/2"	CV	FC	Turbine Steam Supply Throttle	Turbine North Side
SNM	GE		CV		Turbine Sync Speed Control	Turbine Center
Fcv-:61	ASCO	1/2"	SV	F0	Close throttle valve in emergency trip (dumps hydraulic oil)	Turbine

TABLE 3.17. **EPGS INSTRUMENTATION** CONTROL DISPLAY ALARM LEVELS SAMPLING **IDENTIFIER** DESCRIPTION MODULE RANGE HIGH **DIMENSION** LOW PERIOD (sec) Turbine Steam Supply Pressure PT-581 PCM 2 0 - 1500800 PSI 5 PT-582 Steam Seal Pressure PCM 2 0 - 1500PSI 5 TE-581 PCM 2 Exhaust Temp 0 - 500۰F TT-583 Steam Supply Temp PCM 2 0 - 1200۰F 990 800 TT-501 Outboard Bearing Oil Temp PCM 2 0-500 170 110 ٩F TT-502 Inboard Bearing Oil Temp PCM 2 0-500 170 110 ٥F TE-503 Gear Outboard Bearing PCM 2 0 - 500170 110 ٥F 011 Temp AZT-581 Vibration PCM 2 0-100 100 PCT (0-5 g)5 Generator JT-581 Power PCM 2 0-960 kw 5 ET-581 Voltage PCM 2 0-600 450 480 Volt IT-581 Current PCM 2 0-1200 Amp PFT-581 Power Factor PCM 2 0 - 1 - 01.0 0.85 PCT VT-581 VARS PCM 2 0 - 960KVA ST-582 Speed PCM 2 0 - 15001270 rpm ST-581 Frequency PCM 2 0-100 60 PCT (55-65 Hz) 40 TT-510 Stator Winding 1 Temp PCM 2 0-500 260 ٩F TT-511 Stator Winding 2 Temp PCM 2 0 - 500260 ٥F TT-512 Stator Winding 3 Temp PCM 2 0 - 500260 ٥F TT-513 Stator Winding 4 Temp PCM 2 0 - 500٥F 260 TT-514 Stator Winding 5 Temp PCM 2 0 - 500۰F 260 TT-515 Stator Winding 6 Temp PCM 2 0 - 500260 ٥F TE-508 Cooling Air Outlet Temp PCM 2 0 - 500100 ٥F TT-507 Outboard Bearing Oil PCM 2 0 - 500٥F 170 110 TE-505 Gear Outboard Bearing PCM 2 0 - 500170 110 ٩F 0il Temp TE-506 Gear Inboard Bearing PCM 2 0 - 500170 110 ٥F 5 011 Temp PT-502 Condenser Pressure PCM 2 15 0-30 In Hg 5 PT-583 Condensate Pump Discharge PCM 2 0 - 400300 240 PSI Pressure LT-511 Hot Well Level PCM 2 0-15 16 8 Inch 2 TE-582 Cooling Tower Pump PCM 2 0-500 100 40 ٥F 5 Discharge Temp PT-531 011 Pump Discharge PDM 2 0 - 200100 **PSI** 55 5 Pressure TT-521 Bearing Oil Supply Temp PCM 2 0-500 ٥F 140 100 2 PT-501 Bearing Oil Supply Press. PCM 2 0-50 40 10 PSI

Table 2 17

ontrolled Variable	Mode	Set Point	EPGS Control Loops	
oncrotted variable	Mode	Set Point	Controller Inputs	Controller Output
Condenser hot well level	Remote operation (TCP. MS on) (EN.HLC on)	9 in min 14 in max	Hot well level (LT-511)	FCV-512 open/close - makeup FCV-511 open/close - dump
Condensate storage tank level	Operation	12 in min 30 in max	Storage tank level (LS-541)	FCV-541 open/close - supply from cycle fill pump
				FCV-542 open/close - CMUP Stand pipe air overpressure
Turbine/generator oil temperature	Remote operation	125°F FCY-521	Oil temperature (TT-521)	FCV-521 position - cooling water flow

3.7 HEAT REJECTION AND FEEDWATER SUBSYSTEM

The heat rejection and feedwater subsystem rejects waste heat to the atmosphere, pressurizes and heats the condensate to the final feedwater temperature. The subsystem (Figure 3.9) includes the cooling towers, circulating water pump, deaerator, spray water heat exchanger, spray water pump, feedwater pump, feedwater heater, demineralizers, chemical feeders, water analyzers, and condensate makeup pump.

The cooling towers consist of six forced-draft, finned-tube water-to-air heat exchangers. They originally were designed as Freon condensers for refrigeration systems.

The deaerator is used as a direct contact feedwater heater and deaerator and to reject steam generated by the SGS. It is a horizontal, cylindrical pressure vessel, designed to operate at 250 psia and 400°F. It includes a steam header with mixing spargers near the bottom of the tank, water spray nozzles across the top, and two immersion electric heaters. Feedwater, stored in the deaerator, is heated by steam from a branch off the SGS mainline to the turbine. The feedwater is circulated by a spray water pump at 400 gpm from the bottom of the deaerator to the spray nozzles in the vapor space at the top of the deaerator where the water condenses the steam and is thereby heated. Oondensate from the turbine condenser, blended into this spray water, is also heated to 400°F and deaerated.

The feedwater heater is a vertical, cylindrical pressure vessel with an internal steam condensing coil. Feedwater from the deaerator is heated on the tube side as steam from a branch of the SGS mainline condenses on the shell side. The saturated liquid from the coil is cascaded down to the deaerator through a steam trap. Main steam is used for feedwater heating in the feedwater heater and the deaerator because there are no external extraction points on the turbine.

Major components, valves, instrumentation, and control loops are described on Tables 3.18 through 3.21.

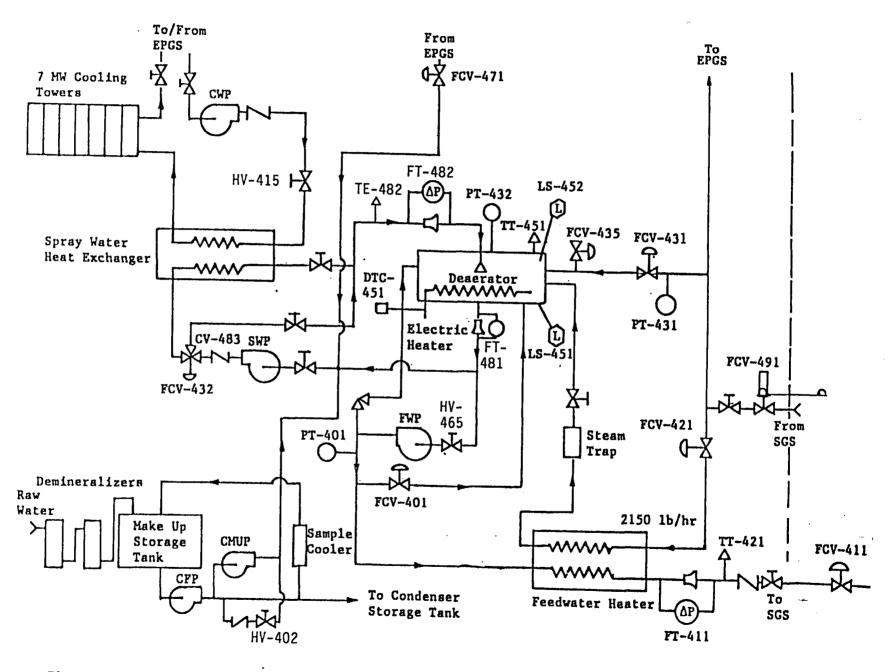


Figure 3.9. Heat Rejection and Feedwater Subsystem Schematic

Table 3.18
Heat Rejection and Feedwater Subsystem Components

Component	Description at	Function	Nominal Operating Condition
Feedwater heater	 Shell and coiled tube counterflow heat exchanger 35 in ID 2.5 in thick carbon steel shell (feedwater) 4 ft 8 in overall height 30 coiled tubes 0.500 in. dia. 43 ft long (steam) 	- Raise feedwater temperature to SGS inlet condition	 950°F superheated steam inlet 545°F saturated liquid outlet 2150 lb/hr steam flow rate 401°F feedwater inlet 550°F feedwater outlet 11,582 lb/hr feedwater flow rate 0.59 MW heat transfer
Deaerator	 Horizontal tank 5 ft ID 12 ft long Contains 15 submerged mixing nozzles, 1 overhead spray nozzle, 2 147-kW electric immersion heaters 	 Degasify condensate Heat condensate for delivery to feedwater heater Provide alternate steam dump when turbine is not operating 	401°F250 psi0.63 MW heat transfer
Spray water heat exchanger	- Shell and tube heat exchanger - 24 in. dia. shell	- Reject excess heat from deaerator when utilized as alternate steam dump	- No flow from deaerator during normal operation

Table 3.18
Heat Rejection and Feedwater Subsystem Components - 2

Component	Description of	Function	Nominal Operating Condition
Feedwater pump	High speed centrifugal type18,770 pump RPM150 HP driver	- Provide high pressure feedwater to the steam generator (through the feedwater heater)	 Inlet: 250 psi, 401°F water 1450 psi head (mfg rating) 60 GPM (mfg rating)
Spray water pump	Vertical turbine type3 stage7-1/2 HP driver	- Provide circulation from deaerator to spray water heat exchanger and/or its bypass and return to deaerator overhead spray nozzle	- 401°F
Cooling water pump	- Centrifugal type - 40 HP driver	- Provide glycol/water circulation for spray water heat exchanger - cooling tower - con- denser circuit	- 132°F glycol/water - 40 psi head - 1200 GPM
cooling towers	- 6 units - Forced draft, finned-tube, glycol/water-to-air heat exchangers	- Reject waste heat to atmosphere	 94°F air 132°F glycol/water inlet 120°F glycol/water outlet 2.4 MW heat rejection

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VALVE	MANUFACTURER	SIZE	TYPE	FAIL POSITION	FUNCTION	LOCATION
FCV-401	Fisher	2"	CV	F0	Feedwater Pump Pressure Control	Southwest of Deaerator
FCV-411	Kieley-Mueller	2"	CV	FC	Feedwater Flow Control	SGS Skid Northeast
FCV-421	Kieley-Mueller	2"	CV	F0	Feedwater Heater Temperature Control	Above Feedwater Heater
FCV-431	Kieley-Mueller	2"	CV	FC	Main Steam Pressure Control	Southwest of Deaerator
FCV-432	Kieley-Mueller	3"-3 way	CV	To SWHX	Deaerator Pressure Control	Between Deaerator and Spray Water Heat Exchanger
FCY-4/1	Valtek	1"	CA	FC	Condensate Control to Deaerator	Above North Door to Spray Water Pump Room
FCV-483	Atkomatic	1"	SV		Deaerator Vent Block	Above Deaerator
FCV-484	Atkomatic	1/4"	SV		Deaerator Vent Bypass	Above Deaerator
FCV-485	ASÇ0	2"	SV		Demineralized Water Storage Tank Fill	Above Culligan Beds
FCV-491	Kieley-Mueller	2"	CV	FC	SGS Steam Delivery Control During Start- Up	North End of SGS Skid

TABLE 3.20. HRFS INSTRUMENTATION

IDENTIFIER	DESCRIPTION	CONTROL Module	DISPLAY RANGE	ALARM HIGH	LEVELS LOW	DIMENSION	SAMPLING PERIOD (sec)
	Main Steam						
PT-431	Pressure	PCM 2	0-1500	1200	900	PSI	2
TE-483	Temp	PCM 2	0-1200	990	850	Inch	10
	Deaerator						
PT-432	Pressure	PCM 2	0-400	250	200	PSI	2
TE-451	Fluid Temp	PCM 2	0-500	400	300	°F	2
TE-481	Steam Temp	PCM 2	0-500	400	300	°F	10
LT-471	Fluid Level	PCM 2	0-30	30	10	Inch	2
	Spray Water						
PT-482	Pressure	PCM 2	0-400	300	200	PSI	5
FT-482	Flow Rate	PCM 2	0-160			KLB/hr	5
TE-482	Temp	PCM 2	0-500	445		°F	10
FT-481	Feed/Spray Water Flow	PCM 2	0-160			KLB/hr	5
	Rate						
07 407	Feedwater	DOM O	0.400		170	PSI	E
PT-481	FWP Supply Pressure	PCM 2	0-400	1400	170	PSI PSI	5
PT-401	FWP Discharge Pressure	PCM 2	0-1500	1400	900	PSI PSI	2 5
PT-484	FWP Coolant Pressure	PCM 2	0-100	1220	1100	PSI PSI	5
PT-483	FWH Outlet Pressure	PCM 2	0-1500 0-160	1230	1180	KLB/hr	ა 2
FT-411	Flow Rate	PCM 2/	U-16U Bailey			KLD/III	2
FT-421	FWH Outlet Temp	PCM 2	0-750	600	400	°F	2
	Cooling Water	,					
TE-484	SWHX Inlet Temp	PCM 2	0-500	130		°F	10
TE-486	Tower Outlet Temp	PCM 2/	0-500	110	32	°F	10

Controlled Variable	Mode	Set Point	Controller Inputs	Controller Output
Feedwater temp.	Operation	5.20° 540°F FCV-421	Feedwater temperature (TE-421) Temperature set point	FCV-421 position - Feedwater heater Steam supply flow
Feedwater pressure	Operation	1250 psig FCV-401	Feedwater pressure (PT-401) Pressure set point	FCV-401 position - FWP recirculation flow
Steam delivery pressure	Manual salt flow GSTAT off	1080 psig PT-431	Delivery pressure (PT-431) Pressure set point	FCV-431 position - Deaerator steam dump
Deaerator pressure	Operation - Desuperheating GSTAT off Boiler following GSTAT on	233 psig PT-432 233 psig PT-432	Deaerator pressure (PT-432) Pressure set point Deaerator pressure (PT-432) Pressure set point	FCV-432 position - Deaerator dump to SWMX FCV-431 position - Deaerator steam supply
Deaerator temp.	Start-up	390°F DTC 451 DTC 452	Deaerator temperature (TE-451) Temperature set point	DTC-451/452 on/off - Electric heater control
Deaerator level	Operation	15 in Garden FY-472 (14 in backup during turbine operation)	Deaerator level (LT-471) Level set point	FY-472 condensate - Makeup pump stroke position
	Turbine Operation	15 in FCV-471	Deaerator level (LT-471) Level set point	FCV-471 position - Turbine condensate return from hot well

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3.8 SYSTEM TRIPS

3.8.1 Equipment Protection Subsystem

The Equipment Protection Subsystem (EPS) is a hard-wired system using dedicated sensors and is designed to safe the MSEE in the event of any potentially unsafe condition. Subsequent to the EPS placing the system in a "safe" condition, operator action is required to shut the system down or to change into any other mode. The trip list for the EPS, including actions taken by the EPS and subsequently to be taken by the operator, are shown on Table 3.22, subdivided by subsystem.

3.8.2 <u>Turbine/Generator Trips</u>

Trips built into the turbine/generator are given on Table 3.2.3. Definitions and guidelines are given below.

A. Definitions

- 1. Turbine Trip Immediate turbine steam shutoff manual or auto.
- 2. Turbine Shutdown Gradual turbine steam shutoff manual.
- 3. Generator Trip Generator circuit breaker opened manual or auto.

B. Steam reactions to trips

- 1. Anticipated Steam control maintained manually or auto.
- 2. Upset Reliance on auto steam control SGS salt flow will stop and HRFS will attempt to desuperheat steam. Probable HRFS and SGS safety valve lifting if upset is uncontrolled.

C. Trip interlocks

- 1. A generator breaker trip always initiates a turbine SVC trip (auxiliary relay 32x closes FCV-501) and an EPST TR-586 (32x).
- 2. A generator breaker trip always initiates a turbine T.V. reset (auxiliary relay 32x resets T.V. closed) w/ZT-581 '0'% open.
- 3. A turbine T.V. reset and an EPS 2 & 3 reset will reopen FCV-501 unless manually closed (or tripped).
- D. All auto trips should be carefully reviewed determine the cause of the trip and correct the problem before resuming operations.
- E. Fail-safe follow-through guidelines

 These guidelines present items of concern to fail-safe the EPGS upon a
 major component failure, after a trip that did not function, or to back
 up an auto trip. Intimate familiarity with these guidelines is mandatory
 before EPGS operation to insure safe operation, both from a personnel and
 equipment standpoint.
 - Three items are of major concern to fail-safe the EPGS and MSEE operating systems:
 - a. Steam over-pressurization
 - b. Turbine trip
 - c. Generator trip
 - 2. Steam system reactions to turbine trips:
 - a. Over-pressurization
 - b. Possible HRFS/D-D & SGS/steam drum safety valve lifting
 - c. Desuperheating by HRFS/FCV-431 switchover to steam control to dump steam to D/D
 - d. FCV-432 D/D heat dump through SWHX and dry cooling tower

- 3. Turbine tripping is redundant-designed and may be fully utilized with these four trips:
 - a. Actuate ET emergency trip FCV-561 (oil trip)
 - b. Open generator breaker with breaker C.S. (electric trip)
 - c. Actuate EPS T-G trip button from control room (EPS backup)
 - d. Manually close throttle valve with hand wheel (manual)
- 4. Turbine-generator trip verification:
 - a. ST-582 speed decreasing
 - b. PT-532 hydraulic oil pressure decreasing (T.V. trip)
 - c. PT-581 steam pressure drops to zero (FCV-501 trip)
 - d. Generator breaker open green light on

NOTE

EOP operation is not mandatory upon a turbine trip since the shaft driven oil pump provides adequate oil flow for turbine coast down.

- 5. Generator trips are redundant-designed with turbine trips. Be aware that:
 - a. EPGS UPS provides emergency backup C/B trip power
 - b. Exciter voltage shutdown local disconnect switch shuts down all of the generator electrical power.

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM RECEIVER SUBSYSTEM TRIPS

TRIP	TRIP	INSTRUMENT	TRIP	
IDENTIFIER	CONDITION	IDENTIFIER	LEVEL	ACTION REQUIRED
	Operator Manual Trip		N/A	EPS - Defocus Heliostat
TR-181	Receiver Salt Outlet Temp High	TE-102A	1080°F	Operator - Control Receiver From The EMCON Console
TR-184	Receiver Tube Temp High	TE-140A and	925°F	
	During Hot Salt Production	TE-102A	>750°F	
TR-187	Loss of Receiver Door Open Signal	ZSH-DR	Contact Open	
TR-182	Boost Pump Pressure Low	PT-180A and	250 PSIG	EPS
	During Hot Salt	TE-102A	>750°F	 Defocus Heliostats Close FCV-151 After Time Delay
TR-183	Receiver Salt Inlet	PT-181A	8 PSIG	Operator
	Pressure Low During Hot Salt Production	and TE-102A	>750°F	 Shutdown Receiver from EMCON Console
TR-185	Hot Surge Tank Level High	LF-161A or	80 In	EPS - Defocus
neriostats		TE-184A	300°F	- Close FCV-101 and FCV-102 After Time Delay
				Operator - Shutdown Receiver From EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM RECEIVER SUBSYSTEM TRIPS (Continued)

		_	
TRIP	TRIP	INSTRUMENT TRIP	
IDENTIFIER	CONDITION	IDENTIFIER LEVEL	ACTION REQUIRED
TR-186	Boost Pump Sump Level High	TE-181A 400°F	EPS - Defocus Heliostats - Time Delay - Close FCV-151 - Turn Off Cold Salt Boost Pump - Turn Off Hot Salt Pump EMCON (Automatic) - Maintain Control of Receiver and HRFS Operator - Shut Down the Plant From the EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM THERMAL STORAGE SUBSYSTEM TRIPS (Continued)

TRIP	TRIP	INSTRUMENT		
<u>IDENTIFIER</u>	CONDITION	IDENTIFIER		ACTION REQUIRED
TR-281	Hot Salt Sump Level High	LT-221A or TE-231A	40 In 300°F	EPS - Close Sump Insolation Valve FCV-231
				Operator - Allow Time for Hot Salt Pump Operations To Bring Sump Level Down - Shut down SGS, HRFS, and EPGS From EMCON Console
TR-282	Cold Salt Sump Level High	LT-201A or TE-211A	55 In 350°F	EPS - Close Sump Insolation Valve FCV-211 - Defocus Heliostats Operator - Allow Time for Cold Salt Pump Operations To Bring Sump Level Down - Shut down the Plant From The EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM STEAM GENERATOR SUBSYSTEM TRIPS (Continued)

TOTO	THETRUMENT TOTAL	
		ACTION REQUIRED
Steam Drum Level Low	LT-311A -10 In	EPS - Close FCV-501 - Open Generator Circuit Breaker - Turn Off FWP (Drum Level High only)
Steam Drum Level High and Water Hot	LT-311A +17 In and TE-383A >250°F	EMCON (Automatic) - Dump Steam To Deaerator - Maintain Control of HRFS
·		Network 90 - Shut Off Salt Flow (Close FCV-301, 341, and 351) - Turn Off BWCP (Drum Level Low only)
		Operator - Shut Down SGS, HRFS, and EPGS From EMCON Console
Boiler Water Circulation Pump Failure	Motor Off Current Sensor	EPS - Close FCV-501 - Open Generator Circuit Breaker EMCON (automatic) - Dump Steam to Deaerator
	ŢĠ.:	- Maintain control of HRFS Network 90 - Shut Off Salt Flow (Close FCV=501, 341, and 351) Operator - Shut down SGS, HRFS, and EPGS
	Steam Drum Level High and Water Hot Boiler Water Circulation	Steam Drum Level Low LT-311A -10 In Steam Drum Level High LT-311A +17 In and and Water Hot TE-383A >250°F Boiler Water Motor Off Circulation Current Pump Failure Sensor

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM EPGS TRIPS (Continued)

TRIP IDENTIFIER	TRIP CONDITION	INSTRUMENT IDENTIFIER		ACTION REQUIRED
	Turbine Overspeed	OST	1320 RPM Generator	EPS - Close FCV-501 Open Generator Circuit Breaker
	Turbine Back Pressure High	ТВРТ	5 PSIG	
TR-58 4	Generator Bearing Temp High	TS-501A	180°F	EMCON (Automatic) - Dump Steam to Deaerator - Maintain Control of HRFS
TR-585	Generator Cooling Air Temp High	TS-502A	122°F	Operator - Control System From EMCON Console - Reduce Steam Flow
TR-586	Generator Circuit Breaker Trip		-Manual -Low/high Voltage -Low/high frequency	- Shut Down If Necessary
TR-587	Turbine Vibration High	AZT-581	5g	
TR-588	Steam Energy Low	TE-332 or PT-581A	750°F 770 PSI	
TR-583	Turbine Oil Pressure	PS-501A (LUBE) or	6 PSI	
		PS-531A (HYDR)	50 PSI	
TR-582	Manual T/G Emergency Trip	Control Room PB	Operator Initiate	

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM MASTER CONTROL SUBSYSTEM TRIPS (Continued)

TRIP CONDITION	ACTION REQUIRED
PCM 1 Microcomputer Failure - Loss of Receiver Displays - Loss of Salt Auto Flow Control	EPS - Defocus Heliostats
- Loss of Cold Surge Tank Auto Level Control	Operator - Control Receiver from PCM l - Drain Receiver If Necessary
PCM 2 Microcomputer Failure - Loss of HRFS and EPGS Displays - Loss of Feedback Control Loops	 Close FCV-301, FCV-341, and FCV-351 Turn Off FWP Close FCV-501 and FCV-491 After Steam Pressure Drops Open Generator Circuit Breaker Turn Off Condensate Pump
	Operator - Shut Down SGS From Console - Shut Down HRFS and EPGS From PCM 2
PCM 3 Microcomputer Failure - Loss of TSS Displays - Loss of Feedback Control Loops - Loss of SGS Displays	EPS - Defocus Heliostats - Time Delay - Close FCV-211 - Close FCV-231 - Turn Off Hot and Cold Salt Pumps - Turn Off Cold Salt Boost Pump - Close FCV-151 - Close FCV-501 - Open Generator Circuit Breaker
	EMCON (Automatic) - Dump Steam To Deaerator - Maintain Control of HRFS
	Network 90 (Automatic) - Interlocks Will Close FCV-301, FCV-341, and FCV-351
	Operator - Shut Down SGS From Network 90 Console - Shut Down Receiver, HRFS, and EPGS from EMCON Console

TABLE 3.22. EQUIPMENT PROTECTION SYSTEM MASTER CONTROL SUBSYSTEM TRIPS (Continued)

TRIP CONDITION Simultaneous Failure of PCM 1, 2, and 3 Microcomputers - Loss of All Subsystem Control CCM Microcomputer Failure - Loss of PCM/Host Computer Communication Lin - Loss of Console Displays - Loss of Console Control Capability - Loss of Sequencing Operations Involving More Than One PCM	ACTION REQUIRED EPS Defocus Heliostats Time Delay Close FCV-211 Close FCV-231 Turn Off Hot and Cold Salt Pumps Turn Off Cold Salt Boost Pump Close FCV-151 Turn off FWP Close FCV-501 and FCV-491 After Steam Pressure Drops Open Generator Circuit Breaker Turn Off Condensate Pump
Operator Remote Manual Trip	Operator - Shut Down the Subsystems From PCM 1, 2, and 3 and Network 90
EMCON Host Computer Failure	PCMs and CCM Continue To Operate and Control The Plant
	Operator - Shut Down The Subsystems From PCM 1, 2, and 3

Table 3.23. TURBINE/GENERATOR TRIP LIST

MODE	DESCRIPTION	INITIATION
Manual	MGBT — Manual generator breaker trip	Breaker switch opened at local or remote generator control panel
Manual	ET - Emergency trip	ET "on" at EMCON console or local trip button actuated
Manual/auto	SVC - Stop valve closure	Close FCV-501
Manual/auto	OST - Overspeed trip	Local OST button
Manual	MTVC – Manual throttle valve closure	Close throttle valve (TVM)
Auto	GBT – Generator breaker trip	a. Reverse powerb. Ground faultc. Overcurrent

Section 4 CONSOLE OPERATION

A detailed description of the MSEE control system and its operation is contained in this section. The subsystem architecture and functional description was given in Section 3.2.

4.1 EMCON CONSOLE DISPLAY SCREEN

The EMCON color console provides a variety of displays arranged in a hierarchy of system level, subsystem level, group level, and individual point level. For the operation of MSEE the console displays used most often include system and subsystem level color graphic diplays, 4 over 4 group displays, 22 line group displays and the single loop displays. An example of each of these types of displays is shown in Figures 4.1 through 4.5.

The graphic displays are used primarily to observe the status of the entire system or an individual subsystem, particularly to locate trouble areas in the operation. The group level 4 over 4 and 22 line displays are used to observe process variables and to operate controls in a particular area within the system. The single loop display is used to analyze the behavior of an individual process variable and to perform tuning of controls.

The lower left-hand corner of the screen is called the KEYBOARD ECHO AREA. It is here where the keys are displayed as they are hit. Keys are usually displayed in GREEN. Error messages are printed in the keyboard echo area in RED.

The lower right-hand corner of the screen is used to display the current time and date. When the Console KEYLOCK is UNLOCKED (Console Unprotected), the time and date are displayed in RED. When the Keylock is LOCKED, the time and date are displayed in YELLOW.

The remainder of the screen (46 lines high by 80 columns wide) is available for the various displays.

The status of each point (tag name) determines the color in which it is displayed:

1. WHITE - OFF-LINE

2. GREEN - NORMAL

3. BLUE - OFF SCAN, BAD SENSOR, or I/O ERROR

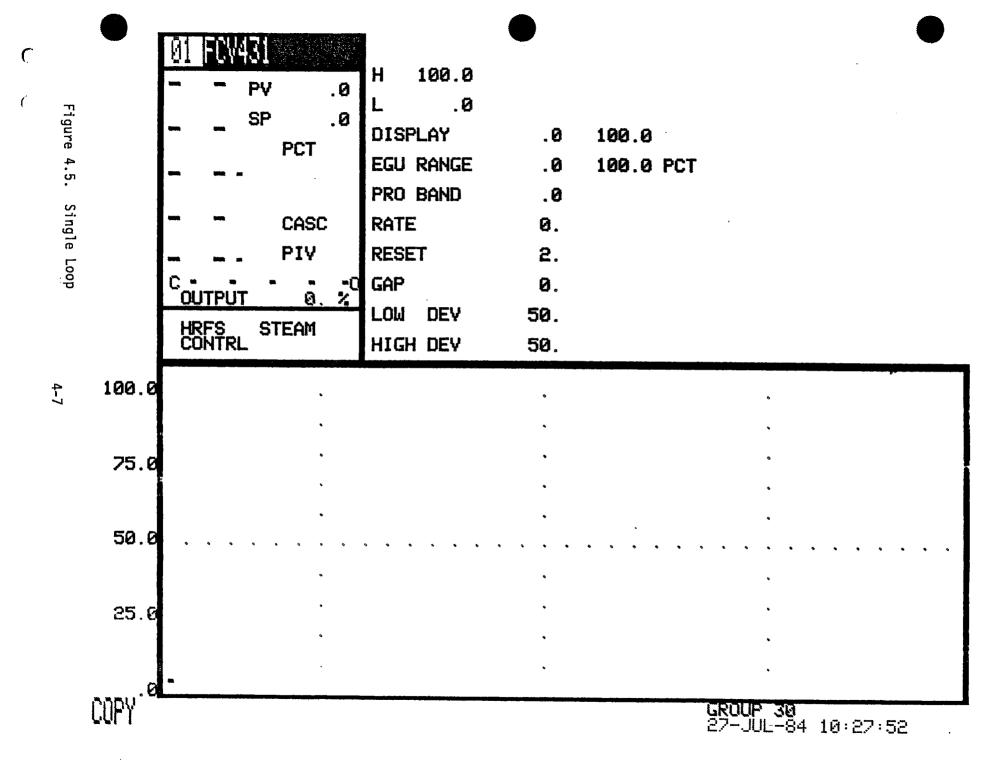
4. RED - LOW or HIGH ABSOLUTE ALARM, RATE-of-CHANGE ALARM

5. YELLOW - DEVIATION ALARM

Figure	FW199	02 FCVI01 XXX	03 FCV161 XXX	04 FCV151 XXX
re 4.3. 4 over 4 Group	- PV 1 ON MANL LOB	PV 98.8 SP 60.0 PCT MANL PIV	- PV .0 - SP 75.0 - IN - AUTO - PIV	PV 100.0 SP 100.0 PCT CASC PIV
	OUTPUT %	OUTPUT 100. %	OUTPUT 100. %	COUTPUT 100. %
4-5	RCYR DRAIN FILL ISOLAT	RCVR SALT FLOW CONTRL	RCYR DWNCMR HOT TANK	RCYR COLD SURGE TANK
	05 LT151 XXX	06 LT291 XXX	07 TE102 XXX	ÃÕ DD
	AT FITAT VVV	06 LT291 XXX	07 IE102 XXX	08 BP
	PV .0 SP 87.0 IN AUTO PID	PV 121.0 IN AIN	- PV 578 CL -99. F - CAL	PV 0. - PV 0. - OFF - MANL LOB
	- PV .0 - SP 87.0 IN - AUTO	PV 121.0	PV 578. _ CL -99. F	PV 0. OFF MANL

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01 FCV101 02 FCV102 04 FCV161 05 FCV162 07 FCV162 07 FCV162 09 FCV171 10 ZSH199 11 ZSL199 12 OPN.211 13 CLS.211	.2PCT XXX RCVR .1PCT XXX RCVR .0PCT XXX RCVR .8IN XXX RCVR .8IN XXX RCVR 29.8IN XXX RCVR 0.0FF RCVR 0.0FF RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR	SALT FLOW SALT FLOW SALT FLOW COLD SURGE DWNCMR COLD COLD SUMP DRAIN FILL CTANK AIR DRAIN FILL COLD SUMP COLD SUMP COLD SUMP COLD SUMP	CONTRL H CONTRL H TANK TANK H LEYEL ISOLAT ISOLAT ISOLAT ISOLAT ISOLAT	100.0 L 100.0 L 100.0 L 70.0 L 70.0 L 60.0 L	.0 PCM 1 .0 PCM 3 .0 PCM 3 .0 PCM 3 .15.0 PCM 3 PCM 3 PCM 3
14 ZSH211 14 ZSH211 15 ZSL211 16 DR.OPN 17 DR.CLS 18 ZSHDR 19 ZSLDR 20 LT281 21 LT291 22 PS281 COPY	0.0FF XXX TSS 0.0FF XXX TSS 1.0N XXX TSS 0.0FF RCVR 0.0FF XXX RCVR 1.0N XXX RCVR 1.0N XXX TSS 108.2IN XXX TSS 1.0N TSS	COLD SUMP COLD SUMP COLD SUMP CAVITY DOOR CAVITY DOOR CAVITY DOOR CAVITY DOOR CAVITY DOOR CAVITY DOOR COLD TANK HOT TANK SGS AIR	ISOLAT ISOLAT ISOLAT ISOLAT OPEN CLOSE OPEN CLOSED LEVEL LEVEL SUPPLY	134.0 L 190.0 L ROUP @2 7-JUL-84 15	PCM 3 PCM 3 PCM 1 PCM 1 PCM 1 PCM 1 15.0 PCM 3 10.0 PCM 3 PCM 3



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4.2 THE EMCON CONSOLE KEYBOARD

Figure 4.6 shows the keyboard layout.

Error Protection and Recovery

The Color Console keyboard is logically constructed to protect the operator from performing nonsense functions. For example, it will not allow the operator to change the setpoint of a contact input bit (because contacts have no setpoints!). If the operator tries to perform a nonsense operation, "WRONG KEY" will be displayed in the Keyboard Echo Area. However, the operator DOES NOT have to hit an "Error Clear" key when an error is encountered. He simply re-enters the correct keys. Likewise, if he makes a typing error, hitting <CLEAR ENTRY> will erase what he has typed and all he has to do is retype the line.

Functionally, the keyboard has several areas:

- 1. DATA ENTRY This area contains the NUMBER pad and ALPHABET for bringing points onto the display, entering numeric values, etc.
- 2. DISPLAY SELECTION This area contains keys that select the various display modes of the screen.
- 3. TUNING This part of the keyboard is used (usually by the process engineer) for tuning control loops. It is usually under keylock (password) protection.
- 4. OPERATION This part of the keyboard is used by the process operator for running the process. For example, it places loops in Auto or Manual status, changes Setpoints, etc.
- 5. SELECTION (optional). These keys select one of the eight controllers on the screen for tuning purposes.

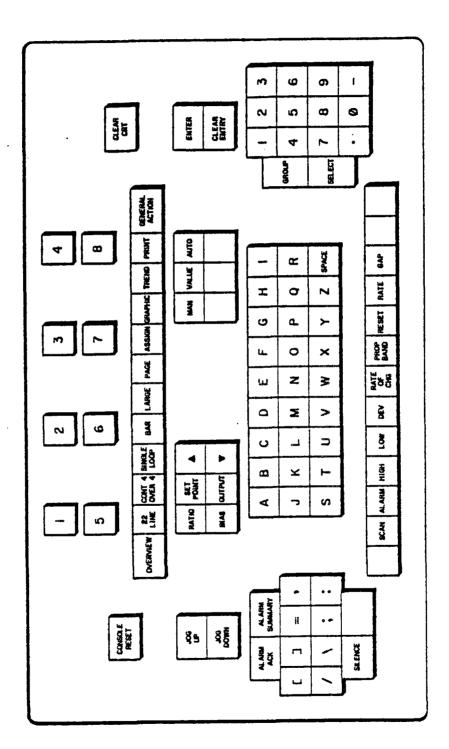


Figure 4.6. EMCON Console Keyboard Layout

There are two types of keys:

<u>Fixed Definition</u> - These are keys that are always legal to hit. They are limited to:

- 1. DISPLAY KEYS To change the display format of the screen.
- 2. CLEAR ENTRY To erase typing errors and clear previous keyboard entries.

<u>Variable Definition</u> - These keys may be legal or illegal or may perform different functions depending on the display mode of the screen and the type of point that is Selected. These keys are limited to:

- 1. DATA ENTRY KEYS For entering point names and data values.
- 2. POINT MODIFY KEYS For selecting the tuning parameter to be changed.
- 3. ALARM SILENCE/ACKNOWLEDGE KEYS To Silence and Acknowledge Alarms.
- 4. SELECT KEYS For Selelcting a line to change.

4.3 USE OF CONSOLE DISPLAYS

4.3.1 Bringing a Point onto the Display

NOTE: A single keystroke is designated by being enclosed in angle brackets < >. On the console itself, these brackets are NOT shown.

The Color Console allows the operator to bring a point or several points onto the display in three ways:

 GROUPS - by indicating which pre-defined group of points is to be displayed. Table 4.1 lists the pre-defined groups. To display one of these groups, press the <GROUP> key followed by the group number. For example,

<GROUP> <0> <2>

will bring group 2, receiver and thermal storage subsystem controls, onto the screen. Most of the pre-defined groups will initially be displayed in the 22 line format.

2. INDIVIDUALLY - by entering the tag name. When calling a point up at random, using the individual method, press the ENTER key after typing the tag name in order to bring the point onto the display. For example,

<F><T><1><0><1><ENTER>

will bring "FT-101" onto the screen.

3. JOGGING - using the "JOG UP" or "JOG DOWN" keys, the user may "step through" the data base either forward or backward.

Table 4.1. MSEE Group List

Group <u>Number</u>	<u>Group Name</u>
01 02 03	RS controls with drain and purge valves RS and TSS controls
03	RS and TSS instrumentation TSS pump house
05	TSS storage tanks for propane heater operations
06	RS back tube temp
07	RS header temp
08	RS drain micros
09	RS purge micros
10	RS pass temp
11	Critical instrument readings
12	RS fill and drain sequence
13	SGS operation
14	SGS operations
15	SGS instrumentation
16	SGS heater control
17	SGS valve micros
18	HRFS controls
19 20	HRFS pump controls
21	HRFS cooling fan controls Turbine operations
22	Turbine operations
23	Generator operations
26	EPS trips
27	EPS trips

4.3.2 Display of an Individually Entered Point

Once the point name is entered, the system will look up the name in the point name table. If it is NOT found, "NOT DEFINED" will be printed in RED in the Echo Area.

If the point name IS found, the point will be displayed:

- 1. At the TOP of the screen in Standard (22-line) mode.
- 2. In the TOP LEFT controller faceplate in a 4 over 4 mode.
- 3. As the single controller in Single Controller mode.

If more points are brought onto the screen than the screen can hold, the NEW points still are displayed as described above, and the OLD points are dropped off:

- 1. the BOTTOM in Standard (22-line) mode,
- 2. the BOTTOM RIGHT in 4 over 4 mode,
- 3. and replaces the single controller in Single Controller mode.

4.3.3 Selecting a Point

The SELECTED POINT is the single line or controller on the screen that is available for change. For example, the "SETPOINT" key will change the Setpoint of the SELECTED POINT.

The SELECTED POINT is always displayed in REVERSE VIDEO. That is, if the point's status were BAD SENSOR, it would usually be displayed in BLUE letters on a BLACK background. If it were the SELECTED POINT, it would be displayed in BLACK letters on a BLUE background.

In the 4 over 4 display, the point name and status of the SELECTEDP OINT are displayed in reverse video. A special display sequence will cause the selected controller to be refreshed (updated) at three times the rate of the other controllers. This provides a faster visual indication of the process, and is especially useful while tuning.

In the 22-line (standard) displays, the entire line of the SELECTED POINT is displayed in reverse video.

You may NOT select a point if graphics are displayed. The Console will remember the SELECTED POINT as you switch from one display mode to the next. For example, you may select controller #4 in 4 over 4 mode, switch to the 22-line mode, and switch back to the 4 over 4 display.

To select a point, simply hit the <SELECT> key, followed by the TWO digit controller or line number. For example,

<SELECT><0><3>

will select line #3 of a 22-line display or controller #3 of a 4 over 4 display.

If the line number is illegal for that particular display (for example, trying to select faceplate #9 on a 4 over 4 display) WRONG KEY will be printed in the Echo Area.

Another method available is the use of individual select keys numbered I through 8 on the upper panel. These allow the selection of one of eight faceplates or lines with a single keystroke. Simply press the key on the upper panel (not the Number Pad) to select the desired controller.

4.3.4 Clearing the Screen

In order to erase the screen completely, press <CLEAR CRT>. This also erases the display list and, therefore, you cannot flip back to the previous display.

4.3.5 4 Over 4 Display

To convert the current display to a 4 over 4 display, press <Cont 4-Over-4>. Eight controller faceplates will appear on the screen, and they will be filled in, left-to-right and top-to-bottom, with the first eight points at the top of the screen if the previous display was Standard 22 line.

If the Selected Point on the previous display was between lines one and eight, that point will remain selected. If the Selected Point was out of that range, Controller #1 (the top-left corner) will automatically be selected. The Selected Controller has the upper part of the faceplate, containing the point name and status in Reverse Video. Unacknowledged alarms will have a blinking status.

When in Controller Mode, the Console will refresh the Selected Point at three times the rate of the other points. This gives a faster visual response to operator and process changes.

Each controller faceplate is divided into three areas: upper, middle, and lower.

The upper box contains:

- Two yellow digits corresponding to the controller number (used for SELECT)
- 2. The Point name color-coded according to status,
- 3. The Point status characters, also color-coded. The Point status characters are as follows:

BLANK - Normal
H - High absolute alarm
L - Low absolute alarm
B - Bad sensor
O - Off scan
* - Off line
X - Off alarm

As explained earlier, the Point name and Status are displayed in reverse video if the controller is the Selected Controller.

The lower box contains:

1. The four words that comprise the Point Descriptors.

The middle box contains:

- A green vertical bar that graphically corresponds to the process measurement.
- 2. Two red vertical bars on either side of the measurement bar that graphically corresponds to the process setpoint.
- 3. A green horizontal bar that graphically corresponds to the controller output. If the controller is a velocity type and the feedback sensor is bad, a blue horizontal bar appears for the controller output. If a feedback sensor is not specified when the data base is generated, the controller output bar will not appear.
- 4. The numeric Engineering Units value of the process measurement, prefixed by the letters:

- 1. "SP" if the controller is a PID controller (with Setpoint)
- "CL" if the controller is a Calculation block, in which case the value corresponds to the calculation result, in percent, of EGU of PV.
- 3. The Engineering Units tag or label
- 4. The Controller type:
 - 1. AIN for Analog Inputs, scan-only
 - 2. CIB for Contact inputs
 - 3. LOB for Latching Contact Outputs
 - 4. PIV for Velocity-mode PID based on error
 - 5. PID for Positional-mode PID based on error
 - 6. CAL for Calculation.
 - 7. SSL for Signal Select/Limiter
 - 8. NLV for Non-Linear, Velocity PID based on error
- 5. The Controller Auto/Manual/Cascase/LOCL status.
- 6. The numeric value of the output being calculated by the control algorithm, displayed in percent. The direction of value movement is depicted by the "O" and "C" at each end of the output bar.

Some of the items mentioned above may not be displayed on a particular controller, based on the point type and controller type (if any exists).

If the point goes off line (the communications link fails), the bars will disappear and the point name will be displayed in white. When the point returns on line, the controller will be re-drawn.

4.3.6 Single Loop Display

The Single Loop display presents detailed information in a split-screen presentation. The single loop display always presents the SELECTED point.

After selecting a point on the screen (from the 22 line or 4 over 4 displays), press <SINGLE LOOP> to view the selected point in Single Loop format.

The upper half of the screen is presented in two quarters:

- 1. The left quarter contains a single controller faceplate display, containing information as described in the preceding section.
- 2. The right quarter contains the numeric values of the tuning parameters associated with the point on display. The tuning parameters that are displayed depend on the type of point and control block (if any) that is on the display. These may include:
 - 1. The high absolute alarm limit
 - 2. The low absolute alarm limit
 - 3. The engineering units range
 - 4. The display range (if scale expansion is used)
 - 5. Proportional band constant (PB)
 - Reset time (integral)
 - 7. Rate time (derivative)
 - 8. High and Low Deviation Limits

Some of these tuning parameters may be changed from the operator's console keyboard.

The bottom half of the screen is used for a real-time trend of the measurement of the point. The Y-axis is labeled in Engineering Units. The X-axis is the time base. The left margin is the time when the display is first called up, the right margin will be reached after approximately twelve minutes. The graph is plotted, much like a pen recorder, with a sample of the measurement being displayed every five seconds. When the right-hand margin is reached, the screen is erased and the display re-starts at the left margin.

A feature of this display is that the value is plotted in the color of the point status. For example, if the point is "Normal", the dots will be drawn in green. As the point enters its High Absolute Alarm area, the dots will change to red.

If no point is selected when the <SINGLE LOOP> key is hit (for example, when the screen is clear) "OFF LINE" will be displayed in the Keyboard Echo Area. If the point goes off line while on display, the faceplate will be blanked, as in the 4-Over-4 display, and the graph will turn white.

After the Single display mode is selected, other points may be called up at random by entering the Tag name. The screen will be erased and the new point will then be displayed.

You may return to the previous display from the Single display by simply pressing one of the display mode keys.

4.3.7 Standard 22-Line Display

To enter the Standard display mode, press <22-Line>. If a point display was already on the screen (for example, 4-Over-4, or Single) the display will be converted to the 22-line format. If the screen was clear, the Console will wait for points to be called up by entering the tag names.

The Standard display presents:

- 1. A yellow, two-digit line number
- 2. The Tag Name
- 3. The measurement, in Engineering Units
- 4. The engineering Units label
- 5. The Point status (blinking if unacknowledged)
- 6. The four Point Descriptor words
- 7. The High and Low, Alarm Limits (if applicable)
- 8. The PCM number where the point is located.

The Selected point is displayed in reverse video, and each line is color-coded according to its status. As points are added to the screen, by entering the tag name or Jogging Up or Down, these points are displayed at the TOP of the screen, and the other points move down and eventually off the bottom of the screen. The 22-line display shows the maximum number of points that may be contained on the screen. Therefore, you may notice for example, that when changing from a 4-Over-4 display to 22-Line, more than eight lines will be on the screen. This feature allows you to group points in such a way that the top eight points are control points, and the bottom fourteen may be used for other points.

4.3.8 Graphic Displays

The graphic displays are called up by pressing the <GRAPHICS> key followed by the number of the desired graphic and the <ENTER> key. For example, <GRAPHIC> <9><9><1><ENTER> will display the MSEE overall system graphic. The available graphic displays are:

990	Receiver Panel Warm Up Temperatures
991	MSEE Overall
992	Receiver Subsystem
993	Thermal Storage Subsystem
994	Steam Generator Subsystem
995	Heat Rejection and Feedwater Subsystem
996	Electric Power Generation Subsystem

The <CLEAR CRT> key must be pressed before the display can be changed. The graphics displays are for observing operations only and cannot be used for control.

4.4 CONTROL

4.4.1 Change Keys, Tuning Keys, Modify Keys

The operator's console supports a full set of keys that modify the characteristics of a loop on line. These keys perform immediate changes to the live point, but they do not effect any changes on the Host disk image of the control data base.

The MODIFY keys are divided into two categories: Process Operator functions and Process Engineer functions.

The Process Operator functions are those normally necessary for the daily operation of the plant. They may be performed by anyone at any time and can be likened to the functions available on the front panel of a typical analog controller. These keys include:

- 1. Switch to Automatic Control, <AUTO>
- 2. Switch to Manual Control, <MAN>
- 3. Change Set point, <SET POINT>
- 4. Change Output, <OUTPUT>
- Change Analog or Contact Value, <VALUE>

The Process Engineer functions are those used to change the characteristics of the control operation being performed. These changes must be done under keylock (Password) protection and therefore, are not immediately accessible to the operator.

These functions are parallel to those contained inside an analog controller, where the controller must be removed from its case in order to be changed. These keys include:

- 1. Change High Alarm LIMIT, <HIGH>
- 2. Change Low Alarm Limit, <LOW>
- 3. Change Rate-Of-Change Alarm Limit, <RATE of CHG>
- 4. Change Deviation Alarm Limits, <DEV>
- 5. Change Scan Status, <SCAN>
- 6. Change Host Alarm Status, <ALARM>
- 7. Change Rate (Derivative), <RATE>
- 8. Change Reset (Integral), <RESET>

- 9. Change Proportional Band, <PROP BAND>
- 10. Change Bias, <RATE>
- 11. Change Lag Time, <GAIN>
- 12. Change Ramp Time, <PROP BAND>
- 13. Change Gap, <GAP>

4.4.2 Success/Error Messages

If the Modify occurs successfully (is accepted by the remote computer)

DONE

will be printed (in green).

If the Modify function fails as a result of a communications link problem,

COMM LINK ERR

will be printed in red.

Other operator messages are discussed in their appropriate section.

4.4.3 Switch To Automatic Control, <AUTO>

In the case of a contact output, pressing <AUTO> will prevent the contact from being turned on or off with the <VALUE> key.

If the selected point is an analog input with a control block attached, pressing <AUTO> will put the output of that block in automatic or cascade mode.

In all other cases, the <AUTO> key is illegal and will print "WRONG KEY" if hit.

4.4.4 Switch To Manual Control, <MANL>

For a contact output, pressing <MANL> will allow the value of the contact to be changed using the <VALUE>.

For an analog input with a control block attached, pressing <MANL> will place the block in manual mode and allow the output of the control block to be changed using the <OUTPUT> key.

For all other blocks, <MANL> is illegal and will print "WRONG KEY" if hit.

4.4.5 Setpoints

The SETPOINT Key

The <SETPOINT> key, from its name, indicates that it will modify the setpoint of any block that has a setpoint.

When the key is pressed, it will print the name of the parameter that it is changing.

If the selected analog point does not have a changeable setpoint field, "NO TUNING" will be printed in red when the key is hit. Digital points will respond with "WRONG KEY".

Note also that the setpoint key is legal only for the 4-Over-4 and Single Controller display. If pressed for any other display, "WRONG KEY" will be printed.

Changing Setpoint -

If the selected point has a 3-term PID block (or one of its variations) attached, the <SETPOINT> key will modify the setpoint of the loop. It will print "SETPOINT" when the key is hit, followed by the current setpoint, in engineering units. For example,

SETPOINT 73.05

The operator may enter the new setpoint, in engineering units, followed by <ENTER>. If he does not wish to enter a new value, he may simply hit <ENTER> and no change will occur.

If the value was entered correctly, "*DONE*" will be printed.

If the value was typed incorrectly or if the value was outside the engineering units range, "CONVERT ERR" will be printed in red. The operator must try again, starting with pressing the <SETPOINT> key.

Cascaded Setpoints -

In some cases, the setpoint of the slave (or downstream) loop will be determined by the output of a master (or upstream) loop. For example, suppose the downstream loop is selected and the cascade is closed ("CASC" is displayed on the controller). When the <SETPOINT> key is hit, you will see:

WARNING: CASCADE CLOSED.

The operator may still enter a new value, but it will be replaced by the new upstream setpoint when the upstream block is scanned.

To change the downstream setpoint, the operator should put the upstream block in "MANUAL" to open the cascade. He may then:

- 1. Change the "OUTPUT" of the upstream block, thereby changing the downstream setpoint. This can be done only if the upstream block a PID-Type block.
- Change the "SETPOINT" of the downstream block, using the <SETPT> key. The warning message will not be shown.

Jogging Setpoints -

After pressing the <SETPOINT> key, the "INCREMENT /ON" DECREMENT/OFF" (up-arrow and down-arrow etchings, respectively) are defined to increase or decrease the setpoint by one percent of the full engineering units range each time they are hit. This is similar to holding a Bat-Handle to RAMP a setpoint.

For example:

<SETPOINT><INC-ON><INC-ON>

will increase the setpoint by two percent of full range. The change occurs each time the key is pressed; holding the <INC-ON> key down, for example, will not cause a continuing increase.

The setpoint value will not increase past 100 percent of full Engineering Units range nor decrease below zero percent.

4.4.6 Positional Output Commands

The OUTPUT Key

The <OUTPUT> key changes the output of a control block. When the <OUTPUT> key is pressed, one of the following prompts are given: "Positional Output" or "Incremental Output". Positional output requires the entry to be the absolute position between 0 and 100 percent. Incremental output requires the entry to be incremented or decremented from its current position. Entry range from -100 to 100%.

If the controller is in "AUTO" or "CASC" mode, then the output is being calculated by the controller's algorithm and is not changeable with the output key. An attempt to do so will cause

BLOCK IN AUTO

to be printed in RED.

Therefore, you must set the controller in manual mode using the <MAN> key.

The <OUTPUT> key is only valid for displays where controller output is shown (4-over-4 and single controller). If <OUTPUT> is struck on any other display, "WRONG KEY" will be printed.

If the selected block does not have a control block or if its control block does not have a changeable output, "NO OUTPUT" will be displayed when <0UTPUT> is hit.

Entering A New Output Value

After pressing the <OUTPUT> key, the operator may change the output by entering a new numeric value followed by <ENTER>. For positional output, the value is the absolute position between 0.0 and 100.0 percent of full output from 35 percent to 60 percent, the operator strikes:

<OUTPUT><6><O><ENTER>

For incremental output, the entry would be:

<OUTPUT><2><5><ENTER>

Jogging Outputs

Once the <OUTPUT> key is hit, the "INCREMENT/ON" (UPARROW) and "DECREMENT/OFF" (DOWNARROW) keys are defined to change the current output by one percent each time they are hit.

To decrease the output by 3 percent for example, the operator hits:

<OUTPUT><DEC-OFF><DEC-OFF>

The output will not decrease below zero, nor increase above 100 percent of output range.

4.4.7 <u>Digital Output Commands</u>

The <VALUE> key

The <VALUE> key is used for changing the value of a contact output (on/off or open/close commands).

If the selected point is a contact output, pressing the <VALUE> key will set the keyboard such that:

- Pressing <INCREMENT/ON> will turn the contact on (set its value to
 - Pressing <DECREMENT/OFF> will turn the contact off (set its value to 0).

For example, to turn a contact on, hit

<VALUE><INC-ON>

You can now immediately turn the contact off by striking <DEC-OFF> without having to strike the <VALUE> key, for example:

<VALUE><INC-ON><DEC-OFF>

The contact output must be in MANUAL mode to change its output using the <VALUE> key.

4.5 MISCELLANEOUS KEYS

4.5.1 Print Key

When the console has a standard 22 line display on the screen, the operator may press this key to have the display duplicated on the operator tracking typer. This is not an exact copy but a remake of the display by the tracking program. When all packets have been sent to the tracking program, the console will tell the operator that the task has been completed by displaying '*DONE*' in the keyboard echo area. The typing may continue depending on the speed of the typer.

For example:

<PRINT> *DONE*

4.5.2 COPY Key

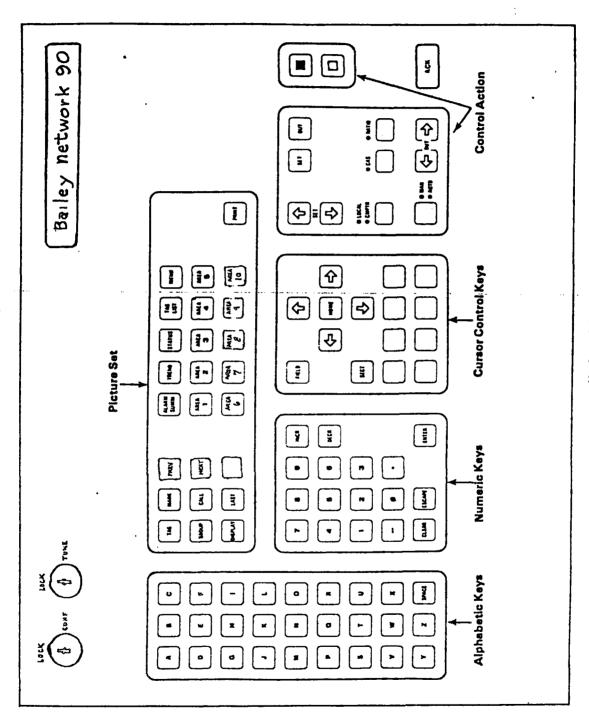
This key is for the copying of the CRT screen to the hard copy graphics printer. When this key is pressed, the console will echo 'COPY' at which time the screen will freeze until the copying process is finished. When the screen becomes unfrozen and the copying is done, the console will display in the echo area '*DONE*' indicating that the copying process is complete.

For example:

<COPY> *DONE*

4.6 BAILEY NETWORK 90 CONSOLE

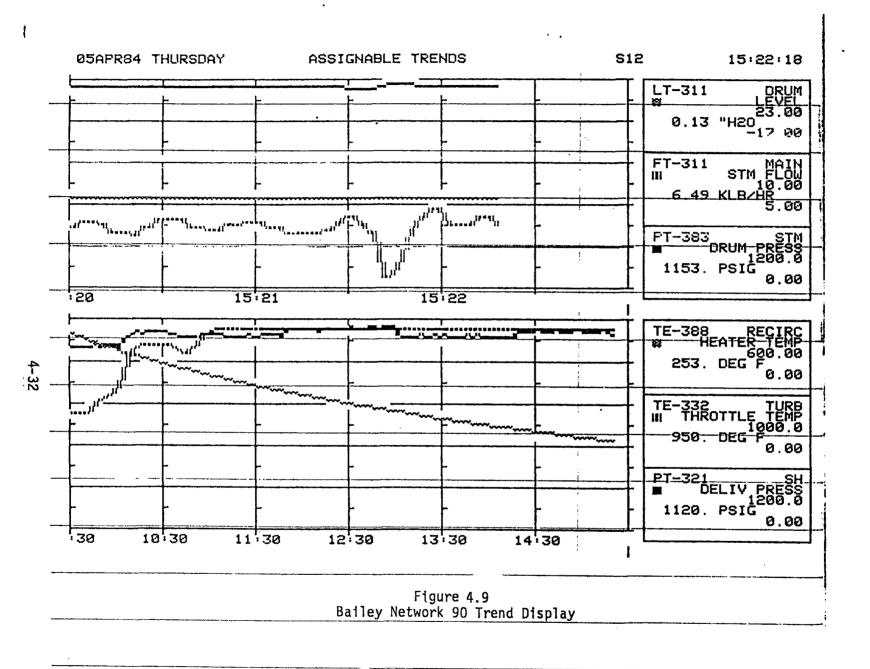
The Bailey Network 90 keyboard is shown in Figure 4.7. The Network 90 is used primarily as a display during SGS operation. Two displays are illustrated on Figures 4.8 & 4.9. Only one operational command is made from this system. Hence, full console operation will not be covered in this program.



Keyboard Layout

Figure 4.7

	•			
			•	
		i I		
	958-1 DRUM LEVEL-FLOI	d	S12 15:13:25	j
FCV-411 FEED WATER	ZT-411 POS	SP-411 MANUAL CONTROL	MAN-411 FEED WATER EMCON	
× — 10.0		CUNTRUL	WATER EMCON	
		-0.1 %	OFF	
	*	L		
-0.01 >< 0.01				
	LT-311 DRUM	TE-383 STM DRUM FLUID TEMP	PT-386 FEEDWATER PRESS	
- -7.0	-0.01 "H2O	563. DEG F	1184. PSIG	
CASC 82% LOCAL				
FT-311 MAIN	SP-DL: SET PNT FROM EMCON	TE-386 FEED	PT-797 CTM	
	PNI FRUM EMCON	WATER TEMP	PT-383 DRUM PRESS	
7.36 KLB/HR	0.004 "H2O	440. DEG F	1177. PSIG	
		L		•
FT-411 FEED WATER FLOW	SP-FWF FW FLOW SET POINT	EHAC AUTO DRUM PRES CONT	MAN-EHAC EMCON CONTROL	
7.29 KLB/HR	7.50 KLB/HR	ON M	1	~~~
	7.JU NLB/RK	OFF	ON	
	Figure			
	Bailey Network 90	Status Display		



Section 5 TRAINING MATERIAL

This section contains exercises to be conducted as part of the training and operating program.

5.1 PRE-OPERATIONAL CONTROL ROOM EXERCISES

5.1.1 EMCON Console Introduction

Part 1 - Display Familiarization

		KEY	<u>SECTION</u>	COMPLETED
1)	Choose and call up a group from the group list	GROUP	4.3.7	
2)	Place the group into a 4 over 4 display	cont 4 over 4	4.3.5	
3)	Select a point a) Using the select key	SELECT	4.3.3	
	b) Using the individual select keys	UPPER PANEL 1 – 8		

Part 1 - Display Familiarization (continued)

		KEY	<u>SECTION</u>	COMPLETED
4)	Place the selected point into a single loop display	SINGLE LOOP	4.3.6	
5)	Return to the 22 line display	22 LINE	4.3.7	
6)	Call up an individual point by entering the point name	ENTER	4.3.1	
7)	Call up each of the system and subsystem graphic displays. Press "CLEAR CRT" key when completed	GRAPHIC	4.3.8	
8)	Change a groups 4 over 4 display	PAGE		
	a) Call up group 14 (note position of FCV-431)			
	b) Place the group into a4 over 4 display			
	c) Press "PAGE" key twice (note display changes)			
	d) Return to 22 line display (note position of FCV-431)		
9)	Print a.22 line display	PRINT	4.5.1	
10)	Copy a 4 over 4 display	СОРУ	4.5.2	

		KEY	<u>SECTION</u>	COMPLETED
1)	Change a valve position	OUTPUT	4.4.6	
	a) Call up group 14 and include FCV-421 in a 4 over 4 display	·		
	b) Select FCV-421			
	c) Place in manual control	MAN	4.4.4	
	d) Change valve position to 40% open by entering the proper value	ENTER		
	e) Change the valve position by using the "UPARROW" and "DOWNARROW" keys	Δ ∇		
	f) Close the valve (0%)	,		
	g) Return valve to auto position			
2)	Change a setpoint	SET POINT	4.4.5	
	a) Call up group 14 and include FCV-432 in a 4 over 4 display			
	b) Select FCV-432			
	c) Change the set point to 200 PSI by entering the value			

<u>KEY</u> **SECTION** COMPLETED d) Change the set point using the "UPARROW" and "DOWNARROW" keys e) Change the set point to 233 PSI 3) Turn on a pump **VALUE** 4.4.7 a) Call up group 19 and select CFP.EN (cycle fill pump enable) b) Turn CFP.EN on c) Select CFP d) Turn CFP on e) Verify ZSHCFP "on"

f) Turn pump off

g) Verify ZSHCFP "off"

h) Turn CFP.EN off

		<u>KEY</u>	<u>SECTION</u>	COMPLETED
4)	Open receiver cavity door	VALUE	4.4.7	
	a) Call up group 02			
	b) Verify DR.CLS "off" (cavity door close)			
	c) Verify DR.OPN "off" (cavity door open)			
	d) Verify ZSHDR "off" (door open micro)			
	e) Turn DR.OPN "on" and observe door on video monitor			
	f) When ZSHDR indicates that door is fully open imme- diately turn DR.OPN "off"			
5)	Close receiver cavity door	VALUE	4.4.7	
	a) Verify DR.CLS "off"			
	b) Verify DR.OPN "off"			
	c) Verify ZSLDR "off"			
	d) Turn DR.CLS "on"			
	e) When ZSLDR indicates that door is fully closed, immediately turn DR.CLS "off"			

5.1.2 <u>Acurex Data System Familiarization</u>

- The Acurex data is displayed on page 02. If this page is not displayed on the display screen, ue the "PAGE FWD" or "PAGE BACK" key as required to change to this page.
- 2. Check the receiver purge and drain valve temperatures and verify that all are above 480°F.
 - a. Determine the channel numbers corresponding to the purge and drain valve thermocouples (see Rs heat trace instrumentation list).
 - b. Use the arrows on the keypad to move the cursor to the top channel number on the display screen.
 - c. Key in the first channel in the series of channels that you wish to display and press the "ENTER" key.
 - d. Repeat step c to check the remaining purge and drain valve temperatures.
- 3. Check FCV-101 and FCV-102 temperatures and verify that they are above $480^{\circ}F$.
- 4. Check channels 100-142. Note the thermocouple locations on the instrumentation list. Record any temperatures less than 480°F along with the corresponding channel.

5.1.3 Receiver Subsystem Instrumentation and Control

		<u>Completed</u>
1.	Review group 1 and locate the instrumentation and valve tag names on the P&ID.	-
2.	Repeat step 1 for group 2.	
3.	Repeat step 1 for group 3.	
4.	Repeat step 1 for group 12. Manual control of a cascaded valve from an	8ن_
	upstream control block.	
	a) On Acurex verify that FCV-151 temperature is above 480°F. Verified:	
	b) Place FCV-151 in cascade. (Group 2)	
	c) Place LT-151 in manual and output the valve that will position FCV-151 25% open.	
	d) Close FCV-151 and return LT-151 to auto.	
5.	Manual control of a cascaded valve from the downstream control block.	<u> (b</u>
	a) Place LT-151 in manual.	
	b) With FCV-151 in auto, change the set point to position the valve 25% open.	
	c) Return FCV-151 to closed position.	
	d) Return LT-151 to auto; note FCV-151 change	

C	om	o 1	et	ed
•				

6.	Manual valve control	CB
	a) Place FCV-151 in manual.	
	b) Output the proper value to position the valve 25% open.	
	c) Return FCV-151 to cascade.	-
7.	Change the salt outlet temperature set point	GB
	Note: The receiver control algorithm would have have to be "ON SCAN" to control the outlet temperature. However for this exercise, RCA will remain off.	
	a) Change SP.SALT to 1000°F.	
	b) Change SP.SALT to 750°F.	
8.	Constant receiver flow	
	a) On Acurex verify that FCV-101 and FCV-102 temperatures are above 480°F. Verified:	<u>CB</u>
	b) Place FCV-101 and FCV-102 in cascade.	
	c) Change FD-101 set point to 40 KLB/hr (F D=10 must be off scan).	
	d) Return FD-101 set point to 30 KLB/hr.	

e) Return FCV-101 and FCV-102 to manual control.

5.1.4 Thermal Storage Subsystem I	Instrumentation	and Control
-----------------------------------	-----------------	-------------

		Completed
1.	Review groupl 4 and locate the instrumentation and valve tag names on the P&ID.	
2.	Repeat step 1 for group 5.	
3.	Complete the following table.	

Day	Time
,	

Description	Tag Name	Value
Hot storage		
tank level		
Cold storage		
tank level		
Hot sump		
level		
Cold sump		
level		
Cold storage		
tank bottom		
temp		
Hot sump		
temp (Acurex)		
Cold sump		
temp (Acurex)		

4. How is the set point changed for the hot and cold sump levels?

5.	1	.5	SGS	Instr	umentati	on	and	Control

		Completed
1.	Review group 13 and locate the instrumentation and valve tag names on the P&ID.	
2.	Repeat step 1 for group 14.	
3.	Repeat step 1 for group 15.	
4.	Manual control of a Network 90 controlled valve.	
	a) On Acurex verify that FCV-321 temperature is above 480°F. Verified:	
	b) Turn/verify MAN.321 on. (Group 13)	
	c) Change SP.321 setpoint to position the valve 25% open.	
	d) Change SD 321 setnmint to close the valve	

el Change ston to English open valve lost of 1945

- a) Turn MAN. 321 off.
- b) FCV-321 will now control the main steam pressure to SP.SP setpoint. Change this setpoint to 1075 PSI.

5. Automatic control of a Network 90 controlled valve.

- c) Change SP.SP setpoint to 1100 PSI.
- d) Return MAN.321 to on.

6. Control of a Network 90 controlled isolation valve.

a) On Acurex verify that FCV-381 and FCV-382 temperatures are above 480°F. Verified:______

- b) FCV-381 and FCV-382 are controlled together. (Group 13)
- c) Turn FCV38182 on to open the valves.
- d) Check micros to verify valves open (Group 17).
- e) Turn FCV38182 off to close FCV-381 and FCV-382.
- f) Turn MAN.38182 off.
- 7. Change the position of FCV-331 using step, 4 as a guide. Return the valve position to 10% open when finished.

Receiver Steady State Operation

Operate receiver with heliostats on target to heat cold salt and 5.2.2 charge the hot salt storage tank. Description 0

Objectives

Introduce the oprator to hot salt production

- Calculate receiver power output 0
 - Determine collector/receiver efficiency

- RSS2- Hot and cold salt tanks warm and ready for operation with hot RS2- Receiver drained with trace heat on Initial System Conditions
 - tank level less than 20 inches.

 - SGS not applicable EPGS not applicable

procedure

7. Advise data system operator to load system 2. Advise data system operator to display the

following on the data display screens: Cold storage tank level

Hot storage tank level Receiver inlet salt temp Receiver outlet salt temp LT-287 LT-291 Hot storage tank temp TE-707 Receiver salt flow rate

3. Confirm receiver technician is completing receiver

4. Confirm thermal storage technician is completing

TSS pretest checklist (TOP #1).

5-14

<u>Completed</u>

5. Complete control room pretest checklist (COP #1) Sections I - VI.

6. Fill receiver and establish serpentine flow with receiver in solar charging configuration, SP.SALT at 750°F, and warm up heliostats on target (ROP #2).

- 7. Increase heliostat field in increments of 12-1/2% until salt flow rate exceeds 60 KLB/hr.
- 8. Increase SP.SALT to 850°F. Stabilize and confirm salt outlet temperature and flow switchover to hot tank.
- 9 Complete Table 5.1 after stabilizing at each of the noted operating conditions. Calculate the power and efficiency for each case as follows.
 - o Direct insolation power

$$P_D$$
 (watts) = A x N x (sun)

where: A = heliostat mirror surface area = $37.2m_2$

N = number of heliostats on target

Sun = solar insolation in W/M_2

o Receiver power output

$$P_R = C_p m\Delta T$$

$$P_{R}$$
 (watts) = 108 (FT-101)[(TE-102) - (TE-101)]

where: FT-101 = salt flow rate in KLB/hr

TE-102 = receiver outlet salt temp in °F

TE-101 = receiver inlet salt temp in °F

o CS/RS efficiency

$$\eta = \frac{P_R}{P_D}$$

Procedure

Completed

- 10. Scram heliostats and set receiver flow demand to 30 KLB/hr. Confirm flow switchback to cold tank at 700°F.
- 11. Shut down receiver (ROP #3).

Table 5.1. Receiver Steady State Operation

Operating	Condi	tions		Data					Calcu	late	
SP. SALT		iostat d (pct)	Number of Heliostats on Target	Time of Day	Solar Insolation (Sun)	Salt Inlet Temp (TE-101)	Salt Outlet Temp (TE-102)	Flow Rate (FT-101)	Direct Insolation Power	Receiver Power Output	CS/RS Efficiency
850	50%										
900	50%								• i		
850	75%										
900	75%				l						
950	75%									:	
900	100%				:						
950	100%										
1000	100%										

	<u>Begin</u>	<u>End</u>
Ambient Air Temp		
Relative Humidity		
Barometric Pressure		
Wind Speed		
Wind Direction		

5.2.3 Receiver Operation with Simulated Clouds

Description

O During receiver loop operation, simulate passing clouds by ramping heliostats on and off of the receiver.

Objectives

- o Demonstrate receiver operation through simulated cloud passage.
- o Familiarize operator with receiver control algorithm.

Initial System Conditions

- o RS2 Receiver drained with trace heat on
- o TSS2 Hot and cold salt tanks warm and ready for operation with hot tank level less than 20 inches
- o SGS not applicable
- o EPGS not applicable

Procedure	Completed

- Advise data system operator to load receiver data package.
- 2. Advise data system operator to display the following on the data display screens:

LT-281 Cold storage tank level

LT-291 Hot storage tank level

TE-102 Receiver outlet salt temp

FT-101 Receiver salt flow rate

- 3 Confirm receiver technician is completing receiver pretest checklist (ROP #1)
- 4 Confirm thermal storage technician is completing
 TSS pretest checklist (TOP #1)

- Complete control room pretest checklist

 (COP #1) Sections I VI.

 Fill receiver, establish serpentine flow with
 receiver in solar charging configuration SP.SALT
 at 900°F, and 25 percent of the heliostats on
 target.
- 7. Complete Table 5.2 for each of the noted transient cases. Allow receiver to stabilize before each case.
- 8. Shut down receiver (ROP #3).

Table 5.2. Receiver Operation with Simulated Clouds

D	Ini	tial	Hellos	Hellostat Translent					
Doc.	Conditions		1101103				Da	ta	
1843U	SP.SALT	Hellostat Field (Pct)	Final Hellostat Field (Pct)	Heliostat Increment (Pct)	Time Increment (Sec)	Time of First Heliostat Command	Salt Inlet Temp (TE-101)	Initial Salt Outlet Temp (TE-1012	Maximum Salt Outlet Temp (TE-102)
	900	25	75	12 1/2	60				
	900	25	75	25	60				
	900	25	75	25	30				
	900	25	75	50	-				
	950	50	100	12 1/2	60				
	950	50	100	25	60		ı		
5-20	950	50	ioo	50	-				
	1000	50	100	12 1/2	60				

	<u>Begin</u>	<u>End</u>
Ambient Air Temp		
Relative Humidity		
Barometric Pressure		
Wind Speed		
Wind Direction		

5.2.4 <u>Thermal Storage Charging with Propane Heater</u> Description

o Charge the hot salt tank using the propane heater.

<u>Objective</u>

o Familiarize operator with propane heater loop equipment and controls.

Initial System Conditions

- o RS not applicable
- TSS2 Hot and cold salt tanks warm and ready for operation with cold tank level greater than 80 inches.
- o SGS not applicable
- o EPGS not applicable

		<u>Completed</u>
Proced	<u>ure</u>	
	 Advise data system operator to load system data package. 	
	2. Advise data system operator to display the following on the data display screens:	

3. Confirm thermal storage technician is completing TSS pretest checklist (TOP #1)

LT-281 Cold storage tank level LT-291 Hot storage tank level TE-291 Hot storage tank temp Complete control room pretest checklist (COP #1)
 Sections I - IV and VI



- Start up propane heater (TOP #2)
- 6. Complete the following table for future reference:

		. , , , ,	K This
, ×	Salt Outlet Temp (Ch 142)	Stack Temp. (°F)	FCV-247 Position
CONTRA -	800		
	900 9 9 0 1000	11 ot	53 ° 2

8. Shut down propane heater (TOP #3)

5.2.5 Steam Generator Steady State Operation

<u>Description</u>

o Operate the steam generator using hot salt from storage, rejecting the steam through HRFS.

Objectives

- o Introduce the operator to SGS start-up and steady state and shutdown operations.
- o Familiarize the operator SGS equipment and controls.

Initial System Conditions

- o RS not applicable
- o TSS2 Hot and cold salt tanks warm and ready for operation with hot tank level greater than 80 inches and cold tank level greater than 30 inches.
- o SGS2- SGS warm and salt drained (diurnal shutdown).
- o EPGS not available

Procedure	Completed
 Advise data system operator to load system data package. 	
2. Advise data system operator to display the following on the data display screens:	

LT-281	Cold storage tank level
LT-291	Hot storage tank level
FT-321	SGS salt flow rate
FT-311	Steam flow rate
TE-382	Superheater salt inlet temp
TE-332	Main steam temp

- Confirm thermal storage technician is completing TSS pretest checklist (TOP #1).
- 4. Confirm steam generator technician is completing SGS pretest checklist (SOP #1).
- 5. Complete control room pretest checklist (COP #1)
 Sections I IV, VI, VII and Section VIII if not previously completed.
- 6. Start up SGS and establish approximately 3 KLB/hr steam flow in boiler following mode (SOP #2).
- 7. Increase the steam demand by manually ramping FCV-431 open to simulate turbine loading. Stabilize at each of the steam load conditions listed in the following table and complete the table for future reference.

Nominal Steam Load (KLB/hr)	Actual Steam Flow (FT-311)	FCV-431 Commanded Position (Pct)	Salt Flow (FT-321)	FCV-321 Position (Pct)	
-----------------------------------	-------------------------------------	---	--------------------------	------------------------------	--

Feedwater temp (TE-386)

Superheater salt inlet temp (TE-382)

8. Shut down SGS (SOP #3)

5.2.6 <u>Operation of Full Electric Loop</u> Description

o Generate steam using hot salt from storage and supply steam to EPGS to operate turbine and generate electricity.

Objectives '

- o Introduce the operator to EPGS operations.
- o Familiarize the operator with EPGS equipment and controls.

Initial System Conditions

- o RS not applicable
- o TSS2- Hot and cold salt tanks warm and ready for operation with hot tank level greater than 80 inches and temperature above 900°F.
- o SGS2- SGS warm and salt drained (diurnal shutdown).
- o EPGS2- EPGS pumps on (turbine standby).

<u>Procedure</u> <u>Completed</u>

1. Advise data system operator to load system data package.

2. Advise data system operator to display the following on the data display screen.

- LT-281 Cold storage tank level
- LT-291 Hot storage tank level
- FT-321 SGS salt flow rate
- FT-311 Steam flow rate
- JT-581 Generator power output
- ST-582 Generator RPM
- Confirm thermal storge technician is completing TSS pretest checklist (TOp #1).
- Confirm steam generator technician is completing SGS pretest checklist (SOP #1).
- 5. Confirm EPGS technician is completing EPGS pretest checklist (POP #1).
- Complete control room pretest checklist (COP #1)
 Sections I IV and VI IX except Section VIII
 if previously completed.
- 7. Start up SGS (SOP #2)/
- 8. Start up EPGS and locally synchronize generator to power grid.
- Transfer generator control to remote (control room) panel (POP #2).

10. Ramp up generator load to 500 kW. Stabilize and complete the following table.

Generator output (JT-581)	kW	
Date/time		
Turbine steam pressure (PT-581)	PSI	
Turbine steam temp (TT-583)	°F	
Main steamm flow rate (FT-311)	KLB/hr	
Superheater salt inlet temp (TE-382)	•F	
Salt flow rate (FT-321)	KLB/hr	

- 11. Shut down EPGS (POP #3).
- 12. Shut down SGS (SOP #3).

5.2.8 EPGS Steady State Performance

Description

Operate steam generator and turbine/generator at various steady state loads for performance evaluation.

Objectives

o Determine the following:

Turbine heat rate
EPGS/HRFS thermal efficiency
Turbine/generator efficiency

Initial System Conditions

- o SGS steady state operation
- o HRFS steady state operation
- o EPGS steady state operation

Procedure

- 1. Review the supplementary material provided at the end of this section.
- Record the water, steam, and generator operating data on the EPGS performance worksheet (Figure 5.3).
 Note: Space is provided for three steady state operating conditions.
- 3. Determine the water and steam enthalpy as follows and record on the worksheet.

- Main steam (h₀) and throttle steam (h₁) For the steam conditions locate the intersection of the constant pressure and constant temperature lines on the Mollier Chart (Figure 5.4). Read the enthalpy on the vertical scale.
- Constant entropy exhaust steam (h_x)

Locate the throttle steam conditions on the Mollier Chart and follow a vertical line (constant entropy) from this point downward to its intersection with the exhaust pressure (PT-502) line. Read the enthalpy at this intersection.

Saturated liquid at exhaust pressure (h_f)

$$h_f = \frac{BTU}{1b} = 83.0 + 8.1 [(PT-502) - 3.0]$$

PT-502 in inches of Hg

- Condensate (h2)

$$h_2 = \frac{BTU}{1b} = (TI-582) - 32$$

TJ-582 in °F

- Feedwater (h₃)

$$h_3 = \frac{BTU}{1b} = (TI-582) - 32$$

TE-386 in °F

- 4. Calculate the fraction of the main steam supplied to the turbine, X, and the steam flow, $\mathbf{W}_{\!_{1}}$, as shown on the worksheet.
- 5. Calculate the performance and efficiency as shown on the worksheet and compare to ratings.

Figure 5.3 EPGS Performance Worksheet

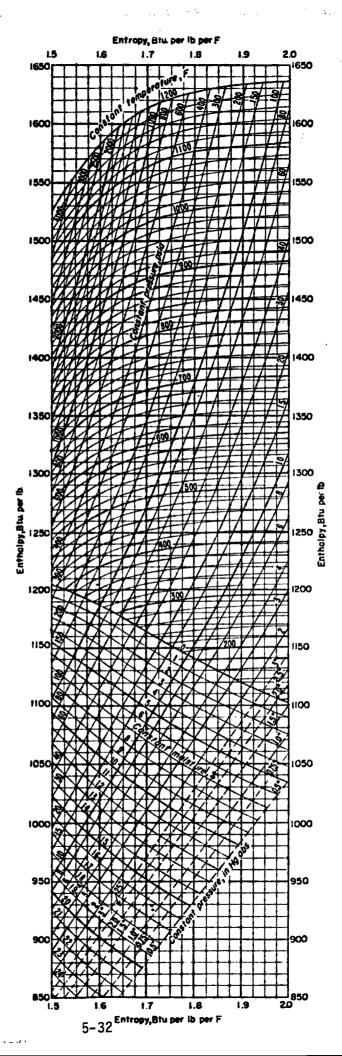


Figure 5.4 Mollier Chart

MEASURING STEAM

What are the vardsticks for steam? First if we have a fixed amount of steam in a closed space, we can measure weight or volume. Usually we measure steam flow in lb per hr. STEAM PROPERTIES. Certain other measurements identify the kind of steam as distinct from the amount, These are (1) temperature (2) pressure (3) quality - expressed as percent moisture or percent vapor of wet steam (4) degree of superheat - degrees F above saturation temperature (5) specific volume - cu ft per lb steam (6) enthalpy - Btu per lb (7) entropy and (8) internal energy. The two most commonly measured are temperature and pressure. With these two (plus an estimate of quality in the case of wet steam) the other properties can be read directly from steam tables. SATURATION PAIRS. When water is boiling, both the water and steam in contact with the water have the same temperature - called the saturation temperature. For each boiling pressure there is only one saturation temperature and vice versa. If you know one you can find the other in the steam tables. Thus for boiling water and steam in contact, 14.7 psi abs and 212 F, 50 psi abs and 281 F, 100 psi abs and 328 F, etc. are saturation pairs.

ENTHALPY ("HEAT") DEFINED

For reasons too long to explain here the term "heat content" is in bad repute with the steam experts. The quantities formerly known as the "heat" of liquid, "heat" of evaporation and "total heat" of steam are now technically known as the enthalpy of the (saturated) liquid, enthalpy of evaporation, enthalpy of saturated vapor and enthalpy of the superheated vapor.

The enthalpy of water or steam is the heat that must be added, Btu per lb, to bring it from liquid at 32 F to its present temperaisre, pressure and condition. Enthalpy of evaporation is the enthalpy difference between saturated liquid and dry saturated vapor.

In Table 1, for example, turn to the line for atmospheric pressure, 14.7 psi abs, corresponding to a saturation temperature of 212 F. Enthalpy of the

liquid is given as 180.0 Btu. This means that if you hold t lb of water at a constant pressure of 14.7 psi abs and heat it from 32 F to 212 F the heat supplied will be 180 Btu.

For low pressures and temperatures, enthalpy of water can be estimated by subtracting 32 from water temperature. (To reduce error at higher pressures, use saturation tables like those on p 91, or complete ones. For maximum accuracy, use compressed-liquid table. For example, take water at 300 F and 1000 psis. Rule of thumb shows 300 — 32 = 268 Btu, saturation table 269.6. Applying correction from compressed-liquid table gives true 271.4 Btu.)

The same line tabulates the enthalpy of evaporation as 970.4 Btu. This means that (at 14.7 pai abs and 212 F) it takes 970.4 Btu to convert one pound

of boiling water into dry saturated steam. If the flow of heat is reversed, as when this same steam condenses at atmospheric pressure, 970.4 Btu will flow out as each pound of dry saturated steam at 212 F is reconverted to a pound of liquid at 212 F.

Next add 180.0 and 970.4 to give 1150.4 Btu, the total heat that must be supplied to convert one pound of water at 32 F into dry saturated steam. The table lists this figure as the enthalpy of the saturated vapor.

If, now, the steam is taken away from the presence of the boiling water and is then heated in a superheater, its temperature will rise above the saturation temperature, and its enthalpy will increase by the amount of heat supplied per pound. Total enthalpy of superheated steam is given in Table 3.

HELPFUL HINTS.

THROTTLING. When steam expands without doing mechanical work, its enthalpy does not change. This type of expansion is called throttling, and occurs
whenever flowing steam encounters
fixed resistances such as orifices, throttling valves, pip. friction or cramped
fittings. Examples of how to figure what
happens when steam is throttled are
shown on the next/two pages, along
with examples of how to use the following practical hints.

MEATING OR COOLING WATER. Amount of heat supplied or removed to heat or cool one pound of water is simply the

change in enthalpy. For all cases within range of everyday operation in lowand medium-pressure steam plants take enthalpy change in the water as equal to the temperature change.

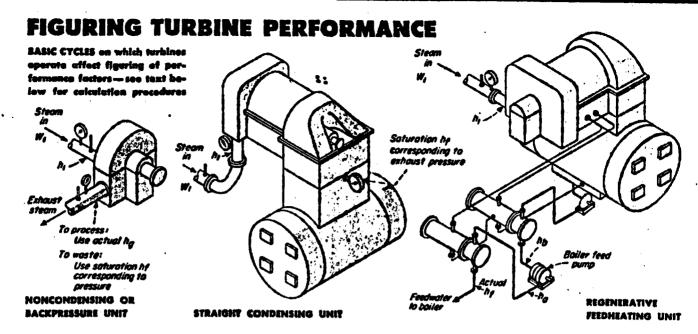
STEAM GENERATION, CONDENSATION. Heat supplied by a steam generator to convert feedwater into steam is merely the enthalpy of the final steam minus the enthalpy of the feedwater.

Heat removed from a pound of exhaust steam by a condenser is the enthalpy of the exhaust steam minus the enthalpy of water entering the hot well. Note, however, that the exhaust steam

is almost always wet, so its enthalpy cannot be taken directly from the table.

The enthalpy of wet steam is the enthalpy of the liquid plus the dryness percent multiplied by the enthalpy of the evaporation. It can also be figured as the enthalpy of the saturated vapor minus the percent moisture multiplied by the enthalpy of evaporation.

EFFICIENCY. The thermal efficiency of any device is its output divided by its input. In the case of a steam generator the output is the heat required to convert the feedwater into the delivered steam. The input is the heat in the fuel.



Turbines convert energy in steam to shaft energy. In selecting and operating them, we're always interested in how effectively this is done. Turbine performance is measured in various ways. Here are common ones:

STEAM RATE is amount of steam required by a turbine to produce a given unit output - usually expressed in 1b per kwhr. It is of direct practical concern in figuring boiler steam needs and performance changes of individual turbines. It has only limited value for comparing different turbines because it doesn't reflect changes in throttle pressure, as does heat rate.

HEAT RATE is amount of energy to produce a given unit output - usually expressed as Btu per kwhr. Because it deals with basic heat units, it is better than steam rate for comparing turbines. THERMAL EFFICIENCY is ratio of energy output to energy input. It is directly related to heat rate: thermal efficiency

=3413/heat rate. See chart.

ENGINE EFFICIENCY is measure of how well an actual turbine compares with an ideal one. Expanding from given throttle to exhaust conditions, a lb of steam does maximum work if expansion is at constant entropy. This ideal condition is never obtained. When actual work done by a lb of expanding steam is divided by ideal expansion

work, the resulting ratio is engine efficiency. It serves as a measure of design effectiveness.

FOR ALL TYPES OF TURBINES.

Steam rate, ib per hwhr steam flow, ib per he (W1)

generator or shaft output, kwhr (P)

FOR BACKPRESSURE TURBINES:

Heat rate, Btu per kwhr

Wi (hi-h')

P ht = steam enthalpy entering turbine, Btu per lb (see diagram)

m steam exhausts to pi = actual exhaust enthalpy, Btu per lb when steam exhausts to waste: =saturated-water enthalpy at exhaust pressure, Btu per lb (see diagram)

Engine efficiency 3413 P

We-We) (he-he) +We (ht-hee)
We steam leaving turbine system from
glands and leaks, ib per hr
he=exhaust-steam enthalpy at entropy of

initial steam, Btu per lb

hes = leakoff steam enthalpy at entropy of initial steam, Btu per lb

FOR STRAIGHT-CONDENSING TURBINES

Heat rate, Btu per kwhr $= \frac{(W_1-W_0) (h_1-h_1) + W_0 (h_1-h_{10})}{m}$ P

he = saturated-water enthalpy at exhaust pressure, Btu per lb (see diagram)

vaporization enthalpy of leakoff steam at discharge press, Btu per lb Engine efficiency

3413 P

(W1-We) (h1-ha) + We (h1-hoe)

FOR REGENERATIVE TURBINES:

Heat rate, Btu per kwhr

_ W1 (ht-ht)+(Wt ha-ha)

he = enthalpy of feedwater leaving last

hr = enthalpy or return to reaving me-heater, Btu per lb hs = enthalpy of feedwater leaving boiler-feed pump, Btu per lb hs = enthalpy of feedwater entering boiler-feed pump, Btu per lb (see diagram) Engine efficiency
3413 P

= W_{b1} (h₁ -h_{sb1})+W_{b2} (h₁ -h_{sb2})+... +W_{b0} (h₁ - h_{sb0})+W₀ (h₁ - h_{sc}) +W₀ (h₁ - h_{sc})

Wes, Wes = bleed steam flows, ib per hr

hose hose hom = enthalpies of bleed steam at initial steam

atram at initial steam
entropy, Btu per lb
Wo =exhaust steam flow, lb per hr
hes =exhaust steam enthalpy at initial
steam entropy, Btu per lb

FOR ALL TYPES OF TURBINES.

Thermal efficiency = Heat rate, Btu per kwhr PERFORMANCE VARIATIONS, Steam rate, heat rate, thermal efficiency and engine efficiency plotted against shaft or generator output in kw show turbine-performance variation with load. Common method for showing performance for automatic-extraction and mixed-pressure turbines plots total hourly steam flow against output for a range of extraction flows.

Turbine performance changes with variations in steam pressure, and temperature, exhaust pressure, makeupwater flow, etc. For methods of figuring corrections for these factors see Test Code for Steam Turbines, PTC 6-1949, published by ASME, 29 West 39th St., New York 18, N. Y.

Thermal lefficiency, percentil 42 40 38 36 34 32 30 21 20: 9,000 2 10,000 11,000 / 12,000 13,000 19,000%, 20,000%, 21,000%, 22,000%, 23,000 14,000 15,000 16,000 77,000 18,000 Heat rate, Blu per kwhr Φ.

CONVERSION SCALE permits quick transfer from thormal officiency (percent) to heat rate (8te per kwhr) for usual range

SECTION 6 MODES OF OPERATION AND TRANSITIONS

The operating modes and transitions for each subsystem are described below:

Receiver Operating Modes

RS1	Receiver cold and drained
RS2	Receiver drained with trace heat on
RS3	Receiver drained with trace heat on and warm-up heliostats
RS4	Receiver cold flow with trace heat on and warm-up heliostats
RS5	Receiver cold flow with trace heat on, no warm-up heliostats
	and receiver door closed
RS6	Receiver operation, manual with flow control
RS7	Receiver operation, temperature control

Receiver Transitions

	. –			
Start-up	RS1	to	RS2 -	Turn on trace heaters
	RS2	to	RS3 -	Drained and warm to warm-up heliostats
	RS3	to	RS4 -	Warm-up heliostats to cold flow through
				receiver
	RS4	to	RS5 -	Cold flow through receiver with receiver door
				closed
		to	RS6 -	To salt flow through receiver with flow
				control
		to	RS7 -	To salt flow through receiver with
				temperature control
	RS6	to	RS7 -	Salt flow with flow control to temperature
				control
			•	
Shutdown	RS7	to	RS6 -	Salt flow with temperature control to flow
				control
		to	RS5 -	Salt flow with temperature control to cold
		RS2 RS3 RS4	RS2 to RS3 to RS4 to to to RS6 to Shutdown RS7 to	RS2 to RS3 - RS3 to RS4 - RS4 to RS5 - to RS6 - to RS7 - RS6 to RS7 - Shutdown RS7 to RS6 -

flow with door closed

with trace heat on

to RS2 - Salt flow with temperature control to drained

RS6 to RS5 - Salt flow with flow control to cold flow with door closed

to RS2 - Salt flow with flow control to drained with trace heat on

RS5 to RS2 - Cold flow with door closed to drained with trace heat on

RS4 to RS2 - Cold flow with warm-up heliostats to drained with trace heat on

RS3 to RS2 - Drained with warm-up heliostats to drained with trace heat

RS2 to RS1 - Turn off trace heaters

Thermal Storage Operating Modes

TSS1 Hot tank drained and cold

TSS2 Hot and cold salt tanks warm and ready for operation

TSS3 Charging with propane heater

Thermal Storage Transitions

o Start-up TSS1 to TSS2 - Pre-test check lists to pre-conditioning hot salt tank

TSS2 to TSS3 - Pre-test check lists to charging hot salt tank

o Shutdown TSS3 to TSS2 - Charging hot salt tank to shutdown, salt in both tanks

TSS2 to TSS1 - Drain hot tank

Steam Generator Subsystem Operating Modes

SGS1 SGS cold and drained
SGS2 SGS warm and salt drained (diurnal shutdown)
SGS3 SGS warm standby (cold salt flow)
SGS4 SGS operating in boiler following mode
SGS5 SGS operating in turbine following mode

Steam Generator Transitions

o Start-up SGS1 to SGS2 - Pre-test check lists, pre-heat to diurnal shutdown

SGS2 to SGS3 - Diurnal shutdown to cold salt flow

SGS3 to SGS4 - Cold salt flow to boiler following mode

SGS4 to SGS5 - Boiler following to turbine following mode

o Shutdown SGS5 to SGS4 - Turbine following to boiler following mode

SGS4 to SGS3 - Boiler following mode to cold salt flow

SGS3 to SGS2 - Cold salt flow to diurnal shutdown

SGS2 to SGS1 - Diurnal shutdown to drained and cold

Electic Power Generation Subsystem Operating Modes

EPGS1 Shutdown

EPGS2 (Turbine standby) EPGS pumps on

EPGS3 EPGS standby (operating - offline)

EPGS 4 EPGS on-line (operating - synchronized)

Electric Power Generation Subsystem Transitions

o Start-up EPGS 1 to EPGS 2 - Pre-test check lists, pre-op and start-up pumps

EPGS 2 to EPGS 3 - Turbine standby to EPGS standby

EPGS 3 to EPGS 4 - EPGS standby to on-line

o Shutdown EPGS 4 to EPGS 3 - On-line to standby

EPGS 3 to EPGS 2 - EPGS standby to turbine standby

EPGS 2 to EPGS 1 - Turbine standby to shutdown

Valve alignments for remote-operated valves are given in Table 6.1 for pretest, operating, and post-test modes.

FIGURE 6.1 MSEE REMOTE OPERATED VALVE ALIGNMENT

		005	T. C. T.	· · · · · · · · · · · · · · · · · · ·	ADE D	TION	Docat		
		PRE	TEST		OPERA	TION	POST		
VALVE	FUNCTION	BASIC FULL SYSTEM	MODIFICATION TO OPERATE 1. W/O RECUR	TO OPERATE	BASIC FULL SYSTEM	MODIFICATION TO OPERATE 1. W/O RECVR	TEST		
			2. W/ OR W/O PROPANE HTR	2. PROPANE HTR ONLY		1. W/O RECVR -AND- 2. W/PROPANE HTR			
FCV-101	RECUR FLOW CTRL	O MAN			C CASC SR SALT	O MAN	O MAN		
FCV-102	RECVR FLOW CTRL	O MAH			© CASC SP.SALT	O MAN	O MAN		
FCV-151	CST LEVEL CTRL	MAN	OL MAN	OL MAN (W/HTR)	© CASC LT-151	OL MAN	O MAN		
FC V-161	HST LEVEL CTRL	Auto SP 75*	OL MAN	L MAN (W/ HTR)	C AUTO	OL MAN	O MAN		
FCV-162	HST LEVEL CTRL	Aυτο SP 20"	O MAN	O MAN (W/ HTR)	AUTO SP 20"	O MAN	O MAN		1
FCV-180-189	RECUR PRAIN	0			•		•		1
FCV-190-198	RECUR PURGE	0			•		•		
FCV-199	RECUR DRAIN & FILL	0			•		0		
	and the state of t								1
	and the section of th		<u> </u>						+
FCY-201	COLD SUMP LEVEL CTRL	AUTO SP 23"			© AUTO SP 23"		MAN	 	†
FCV-211	COLD SUMP ISOLATE	⊕ L			0		O L		
FCV-221	HOT SUMP LEVEL CTRL	AUTO	der en	المراجعة ال	© AUTO 5P 20"		MAN		<u> </u>
FCV-231	HOT SUMP ISOLATE	⊕ L			0	1	O L		-
FCY-241	PROPANE HTR FLOW CTRL	● L			O L	Ox8 MAN	•		
FCV-242	PROPANE HTR ISOLATE	⊕ L	() _A ((UTB)	(w/ura)	O L	0	•		+
			(W/HTR)	(W/HTR)					
					,				
FCV-301	EVAP SALT TEMP CTRL	MAN ON		MAN ON	MAN OFF		MANON		+
FCV-321	SGS SALT FLOW CTRL	O MAN ON			MAN OFF		O MAN ON		 -
FCV-331	STEAM TEMP CTRL	010% MAN ON			MAN OFF		Q10%MAN ON		
FCV-341	SGS COLD SALT FILL CTRL	MAN OH		L MAN ON	1110 0430		MAN ON		
FCV-351	SGS HOTSALT FILL CTRL	MAN ON			O MAN ON		MAN ON		
FCV-381	EVAP SALT DRAIN	MANON			MAN ON		MAN ON		+
FCV-382	SUPHTR SALT DRAIN	0					•		
FCV-383	START-UP HTR BYPASS	MAN ON			O MAN ON		MANON		-
FCV-384	START-UP HTR ISOLATE	O MAN ON			MANON		O MAN ON		

									+
FCV-401	FWP PRESSURE CTRL	AUTO SP 1250			© AUTO SP 1250		AUTO		
FCV-411	FEEDWTR FLOW CTRL	MAN ON			MAN OFF		SP 1250 MAN ON		
FCV-421	FWH TEMP CTRL	O AUTO SP 520°F			AUTO .		O AUTO		
FCV-431	DA OR STEAM PRESS CTRL	CASC PT-431			© SP \$20°F © CASC PT-432 SP 233		CASC PT-431		
FCV-432	DA PRESSURE CTRL	O SP 233			© AUTO SP 240		O SP 1080		
FCY-471	DA LEVEL CTRL	AUTO SP O"			© AUTO SP 15"		AUTO		
FCV-483	DA VENT NO. 1	O LOCAL		:	O LOCAL		SP O"		-
FCV-484	DA VENT NO. 2	LOCAL			LOCAL		LOCAL		
FCV-485	DEMIN WATER TANK FILL	6 LOCAL		-	6 LOCAL		LOCAL		
FCV-491	START-UP STEAM CTRL	AUTO 57 1900			O AUTO SP 1000		AUTO SP 1000		
•		J. 1-00			_ SF 1000		- 3r 1000		
FCV- 501	TURBINE STOP	•			0		•		
FCV-511	HOT WELL OVERFLOW	•			©		•		
FCV- 512	HOTWELL MAKE-UP	EN.HLC OFF (LOCAL CNTRL)			EN,HLC ON (AUTOCHTEL)		EN.HLC OFF		
FCV-521	OIL COOLANT FLOW CTRL	AUTO SP 120° F			© AUTO SPIZO F		MAN		
FCV-541	CNST MAKE-UP	O LOCAL CHTEL			LOCAL CHTRL		COCAL CHTRL		
FCV-551	CONDENSATE RECIRC	•			•		•		
FCV-561	TURBINE TRIP	ET OFF			ET OFF		● ET OFF		<u> </u>
TVM	TURBINE THROTTLE	•			<u>©</u>		•		1
							-		
									
		⊕ L	0	©	·				
		LOCKED	OPEN	CONTROLL	NG				-
		CLOSED							
				·			· · · · · · · · · · · · · · · · · · ·		
									<u> </u>

7.1 CONSOLE OPERATING PROCEDURES

COP #1 CONTROL ROOM PRETEST CHECKLIS	COP	#1	CONTROL	ROOM	PRETEST	CHECKL	IST
--------------------------------------	-----	----	---------	------	---------	--------	-----

TE	ST	DAT	Ē
9	/1	B/84	

This Console operating procedure will be utilized to verify process control integrity prior to all tests. It is unnecessary to verify control integrity of subsystems not used (not applicable). This checklist shall be completed by the control room process console operator.

1.	Test Description		
		è	Start Time
II.	Responsible operating personnel	Primary	Backup
	Test Conductor (MDAC)	Stan Saloff	
	Heliostat Operator	Arleen Vance	-
	Console Operator	Evans/Nelson	1
	Operation/Safety Engineer	John Holmes	
	Subsystem Technicians		· ·
	RS	Jerome Griego	
	TSS	Matt Matthews	
	SGS	Matt Matthews	· · · · · · · · · · · · · · · · · · ·
	HRFS	Jay Holton	
	EPGS	Jay Holton	-

	A :		
•		Verify that all test personnel have been briefed on the scheduled test description, objectives, individual responsibilities, and expected response to emergencies	
	в.	Communications established to all manned control points	
(c.	Safety equipment in place:	
		1. OSHA protective gloves	
		2. Fire retardant coveralls	
		3. Hard hats/Face shields	
		4. Approved fire extinguishers	
•	•	9	ì
2.	So	lar only	
	Α.	"Test In Progress" lights on in the tower	
1	В.	Non-Test personnel informed and in secure location	
1	С.	Diesel-Generator on and frequency OK	
	D.	Field monitor on call after solar start-up	
	Ε.	Communications established	
1	F.	Tower top barricade up	
1	G.	Gates closed and posted with red lights or signs	
	н.	Field clear and ready for start-up	
		ontrol Room locked	

DESCRIPTION

VERIFICATION

Notice

Four items that impact system start-up significantly and should be verified and/or corrected first are:

- a. Emcon operation
- b. Acurex temperatures
- c. D/D level and temp.
- d. Steam drum level and temp.

DID - Death in

IV. MASTER CONTROL SUBSYSTEM

- A. EMCON D/2 HOST START UP CHECKLIST Complete this checklist for all operations.
 - 1. Equipment powered up:
 - a) Host cabinet
 - b) Operator Console 1
 - c) Operator Console 2
 - d) (2) LA-120 Terminals
 - e) VT-100 Terminal
 - f) Tri-log printer

Disk Packs (2)			
drives running	with "READY"	lamp lit.	

- 3. EMCON system booted and "START-UP" command file executed:
 - a) Correct date and time
 - b) Disk unit DLI mounted
 - c) CCM, PCMs loaded (optional)
 - d) EMCON host programs running
 - 1. SPNCOL 5. CONSL2
 2. POWER 6. CONSL1
 3. ALRMMX 7. SYSMON
 - 4. ALARMS 8. TRACKR
- 4. MSSND program executing when data logging display is required on the Auxiliary Data Logging/Display System.
- 5. Unlock Console to allow activation of operational alarms and Receiver Control Algorithm.
- 6. Enable general alarms by turning GAL on.

6. Label file used:__

7. Data file used:__

UP #I	CONTROL ROOM PRETEST CHECKLIST	
STEP	DESCRIPTION	VERIFICATION
В.	ACUREX START-UP CHECKLIST Complete this checklist for all operations using sal	t.
	1. Equipment powered up:	
	a) Host chassis - Autodate Ten/50 b) Electrohome monitor c) GT-100 Terminal d) Texas Instruments 820 RO Terminal	•
	2. Tape Cassette loaded in host drive.	
	3. Recent (within 60 minutes) logout of temperatures available on Tl printer.	Last Print Tim
	4. Set scan rate to every 60 minutes.	
c.	AUXILIARY DATA LOGGING/DISPLAY SYSTEM Data acquisition checklist completion optional as re	quired.
	1. Equipment powered up:	
	a) H-P 1000 Cabinet b) H-P 2645 Terminal c) H-P 2621 Terminal d) Tektronix 4014 Terminal e) Tektronix 463 hard-copy unit f) (6) Display CRTs g) Versatec Video Copier h) Versatec Printer i) H-P 7925 Disc Drive	
	 Disk pack installed in drive, disc drive running with "READY" lamp lit. 	
	3. System booted:	
	a) Correct date and timeb) Transfer file IMSRP executed	
	4. MSPAS program executing when data logging/ display is required and MSSN2 has been started on the EMCON host.	
	5. Following support programs available for execut:	
	a) MSRTP b) MSPSU c) MSDSD d) MSSL1 through MSSL6 e) MSCDT	4

7. Align/verify the following valve alignment; confirm valve temps are acceptable before moving. (to avoid bellows damage) Coordinate with Receiver technician. RCK 'ON' may be used to auto align these, turning itself off when complete.

	<u>Valve</u>	<u>Description</u>	Position		
	FCV-101	Salt flow control	Man/Open/N√	Spen 6% crepor	
01	FCV-102	Salt flow control	Man/Open/N	CPAR CON OCTIFICA	
	FCV-180-189	Drain valves	On/Open/N	(ZSH180-189 On)	80
	FCV-190-198	Purge valves	On/Open/N	(ZSH190-198 On)	09
04	CSP.EN	Enable CSP control	On./	•	
04	BP.EN	Enable BP control "	ON		

03

DESCRIPTION

VERIFICATION

VI. TSS - THERMAL STORAGE SUBSYSTEM

Complete this checklist for all operations using salt.

. .

1. Verify that the Acurex TSS trace heaters are operating and the temperatures are above 480°F (Table B). NOTE EXCEPTIONS. If req'd heat tracing control can be controlled locally at salt storage control building.

11:00

Time

2. If operating Propane Heater without SGS, verify that these Acurex SGS inlet trace heaters are above 480°F (Ref. Table C):

Channe1	Channel	Local Temp, Verific.
204	255	FCV-241
205	256	Hot Tank inlet line
206	257	•
	258	,

3. Verify salt levels in storage tanks and sumps are commensurate with test requirements:

LT-201 Cold Sump 47.3 in. (60" max)**@ 37.2 F (Acurex Chan 124,125)

LT-281 Cold Tank 5.3 in. (40" min)* 05627 °F (Acurex Chan 110-112)

LT-221 Hot Sump 4.4 in. (45" max)**@ 7276 °F (Acurex Chan 126,127)

LT-291 Hot Tank 984 in. 0000 °F (Acurex Chan 134-136)

*Minimum level req'd to maintain cold sump level during fill operations.

**Maximum levels require vent checks; advise technician.

4. Align/verify the following valves for operation with RS, with SGS, & without Propane Heater.
Confirm valve temps are accept. before moving.
Coordinate with thermal storage technician.
TCK 'ON" may be used to auto align these, turning itself off when complete.

	itsei	I OII Milett Combiere.	
	Valve	Description	Position
	*FCV-151	CST Level Control	Man/Closed/N√
02	FCV-161	HST Level Control(Hot)	Man/Closed/N✓
	FCY-162	HST Level Control(Cold)	Man/Closed/N✓
	FCV-199	Bypass valve	Off/Open /N / (ZSH199 on)-
	FCV-201	Cold Sump Level Control	Auto/Closed/N SP 23"/
04	FCV-211	Cold Sump Isol. (OPN/CLS.211)	Closed/Locked Y (ZSLZII on).
V -	FCV-221	Hot Sump Level Control	Auto/Closed/N SP 20%
	FCV-231	Hot Sump Isol. (OPN/CLS.231)	Closed/Locked√ (ZSL231 on)
	FCV-241	Propane Heater Inlet	Man/Closed/Locked√,
05	FCV-242	Propane Heater Isolation	Off/Closed/Locked ✓ (ZSL242 on)
	FCV-301	Bypass Salt Flow	Closed/N/ (MAN on, SP Auto U%
13	FCV-341	Cold Salt Isol.	Closed/N√ (MAN on. SP Auto 0%
13	FCV-351	Hot Salt Isol.	Closed/N / (MAN on, SP Auto 0%
757	CSD FM	Enable CSP Control	On 🗸
04	that signal (b)	ual can indicate EDS closure.	Clear trips and reset EPS1 & EPS3 to

*Bad signal (blue) can indicate EPS closure. Clear trips and reset EPS1 & EPS3 tregain control.

7-1

•	STEP	DESCRIPT	ION	VERIFICATION
	5.	For operation with Propane of Receiver OR for SGS alovalve alignment of step 4	ne, Modify the	
		<u> Valve</u>	Position	
02 <u>05</u>		FCV-151 FCV-161 FCV-162 FCV-242	Locked Locked Man/Open/N Nuetral	
	6.	For operation without SGS, alignment of step 4 as follows:		<u> </u>
	•	<u>Valve</u>	Position	
13		FCV-301 FCV-341	Locked Locked	
04	7.	Verify pump bearing temp's (TE 180, 286, & 387 on EMCO		
VI		S - STEAM GENERATION SUBSYS mplete this checklist for o		
	1.	Verify that the Acurex SGS are operating and the temperature above 480°F (Table C). NOT If required, heat tracing of taken over locally at the scontrol building Acurex calls	eratures are TE EXCEPTIONS. Control can be Salt storage	
	2.	Align/verify the following Confirm valve temps are accordinate with thermal sto All SGS control valve MAN (Emcon commands not applica SCK 'ON' may be used to auturning itself off when commands the story of the sto	cept. before moving. brage technician. signals should be On. able from Net 90) to align these,	Time
		Emcon Command	Valve Description	Position
	MAN	.321 On/ SP-321 Auto 100% .331 On/ SP-331 Auto 10%	Main Salt Flow Steam Attemp.	Open 10% Open
13	*MAN	.38182 On/FCV-38182 On .384 On/ FCV-384 On .383 On/ FCV-383 Off	Salt Drain Circ Htr Supply Circ Htr Bypass	Open Open Closed
04	HSP		Enable HSP Control	On

^{*}Open FCV-384 before closing FCV-383 to avoid SGS Pump and Heater Shut-off

DESCRIPTION

VERIFICATION

Complete the following steps after completing HRFS startup. (Presuming SGS is in Diurnal Shutdown).

3. If SGS F.W. inlet pipe temp. (Acurex Channel 132) is below 200°F, increase bridge pipe feedwater temperature: Yerify D/D TE-451 is above 250°F Advise the SGS technician to open the **b**) bridge feedwater drain HV-370, then open FCV-411 to 20% (Emcon MAN.411 on/SP Auto 20%) Verify Acurex channel 132 increases above 200°F (Approx 5 min after opening FCY-411) Reclose HV-370 and FCV-411 Verify drum level LT-311 is at 0.0 inches. If drum level is below 0.0 inches; open HV-488, then open FCV-411 to 20% and fill to 0.0". Close FCV-411 and HV-488 to avoid FW leakage into drum. 5. Verify that the boiler water circulation pump (BWCP) is running (ZSHBCP). If it is not running: a) Review overnight data to determine reason and correct. b) Start BWCP c) Start circulation heater (pulse EHAC.ON)

If freezing ambient temperatures have been experienced, resolve any suspicious instr. transmitter readings with the SGS technician. Be skeptical of all readings until proven.

DESCRIPTION

VERIFICATION

VIII. HRFS - HEAT REJECTION AND FEEDWATER SUBSYSTEM Complete this checklist for all water system operations.

1. Set/Verify the following control devices in the listed positions: HCK 'ON' may be used to auto align these, turning itself off when complete.

	İ	to auto aing	yn tnese, turning i	tseir off when complete.	
	Id	entifier	Description	Command	Position
call			D Press Enable	Off	N/A
	EN.	DTC451 D/	/D Heater 1 Enable	Off	N/A
ш р	EN.		/D Heater 2 Enable	0ff	N/A
	D	TC-451 D/	/D Heater 1	Auto SP 390 or 400°F	Not Enabled
	<i>≥</i> D	TC-452 D/	/D Heater 2	Auto SP 390 or 400°F	Not Enabled
7	J.F	CV-401"" FW	MP Press Recirc	Auto SP 1250 psi	Closed
2	J F	CV-411 Fe	edwater Delivery	MAN.411 On/SP-411 AUTO 0%	Closed
. 3 3	ş <u>F</u>	CV-421 FW	WH Steam Supply	Man	Closed
18 🐧	· F	CV-431 D/	D Steam Inlet	Auto/Casc to PT-431	Closed
. J. S.			team Line Press		N/A
		PT-432 D/	/D Press NHX Divert	Auto SP 233 psi	N/A
· · · · · · · · · · · · · · · · · · ·		CV-432 -SW CV-471 T-	NHX UIVERT	Auto SP 240 psi	Open to Bypass
	г	∪1-4/1 I− FV_479 CM	-G Condensate Retur 4UP Stroke Position		Closed
	F		GS Steam Delivery		Closed Closed
	*F	CV-501 Ma	in Steam Ston	######################################	Closed
	•	*TVM Tu	irbine Steam	Off/ZSL-501 On TVM.OPN Off/ZT-581 O% Oper	Closed
19720	FW	P.EN/SWP.EN/C	WP.EN/CMP.EN/CFP.F	N/CF1.EN thru CF6.EN	On
				ves is disabled if TCPMS is	
				,	,
	EP		IC POWER GENERATION		
19	1.	PP.EN SIGNAL	S ON-CTP.EN, CTF.EN	,EOP:.EN,AEP.EN,	
20		CWP.EN,FCV-5	521 Auto SP 12 0, FC	Ý-501 off, EN. HLC off,	
21				o auto align these,	
		turning itse	elf off when comple	te.	
	3 1	Vand C. DOD O	Nama (Nama (Na	\ 9. 1	
	1.1	verity kup u	Gen Breaker gr <mark>een (</mark>	open) light is on.	
21	2.	Confirm corr	ect selection of F	PGS operating mode,	
		Remote (TCPM	(S On) or Local (TC	PMS Off).	
		•			
	3.	Verify Gener	ator operator has	procured	
		the Sync swi	tch handle from the	e MSEE key box.	
					,,-,-,-
	4.		hotwell level con	trol by	
		turning EN.H	ILC off.	: _ 	
	_			• •	
	5.	Uverride EPS	vibration trips by	y turning	
		VIB.OVR on.			

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6. Momentarily enable EPS3.RST and EPS2.RST.

7. Verify FCV-521 Oil Cooler C.W. is in Auto with a SP of 120°F Closed. (Emcon control disabled if TCPMS is in local (off)).

•	•						ACUREX
	T/C	DESCRIPTION		CUREX ANNEL	T/C	DESCRIPTION	CHANNEL
	TEH-190	Purge Valve	#1	000 /	TEH-157	Receiver Outlet-Heater R	027~
	TEH-191	Purge Valve	#2	001	TEH-158	Receiver Outlet-Heater R	028 /
	TEH-192	Purge Valve	#3	002 /	TEH-153	Hot Surge Tank Inlet-Heater N	029/
a.	TEH-193	Purge Valve	#4	003	TEH-159	Hot Surge Tank Outlet-Heater	N 030 /
	TEH-194	Purge Valve	#5	004	TEH-152	Cold Surge Tank Inlet-Heater	0 031 /
	TEH-195	Purge Valve	#6	005 /	TEH-156	Cold Surge Tank-Heater O	032 /
	TEH-196	Purge Valve	#7	006	TEH-150	Receiver Inlet-Heater P	033 /
_	TEH-197	Purge Valve	#8	007 /	TEH-151	Receiver Inlet-Heater P	034 /
	TEH-198	Purge Valve	#9	008 /	TEH-162	FCV-101-Heater Q	035 ~
	TEH-180	Drain Valve	#1	009 /	TEH-163	FCV-102-Heater Q	036 🗸
	TEH-181	Drain Valve	#2	010	TEH-154	Drain Line-Heater T	037
	TEH-182	Drain Valve	: #3	011	TEH-155	Drain Line-Heater T	038
	TEH-183	Drain Valve	#4	012	TEH-166	Hot Surge-Heater U	039
	TEH-184	Drain Valve	. #5	013 👵	TEH-167	Hot Surge-Heater U	040 <
	TEH-185	Drain Valve	#6	014	TEH-164	Cold Surge-Heaster V	041
	TEH-186	Drain Valve	e #7	015 (Bad)	TEH-165	Cold Surge-Heater V	042
	TEH-187	Drain Valve	÷ #8	016	TEH-131	Riser-Heater H	300 <
	TEH-188	Drain Valve	# 9	017	TEH-133	Riser-Heater I	301
	TEH-189	Drain Valve	e #10	018	TEH-134	Riser-Heater I	302
	TEH-160	Purge Line	-Heater S	019	TEH-135	Riser-Heater J	303 🐇
	TEH-161	Purge Line	-Heater S	020	TEH-136	Riser-Heater J	304
	TEH-176	Drain Line		021 (66 is	TEH-130	Downcomer-Heater K	305
	TEH-177	Drain Line		022	TEH-132	Downcomer-Heater L	306
	TEH-172		Pass #1	023	TEH-137	Downcomer-Heater M	307
	TEH-173	(Header) Pass #10		024	TEH-138		308
	TEH-174	Pass #11		025	TEH-139	Downcomer-Heater L (Ski	p) 309
	TEH-175	Pass #18		026 J			

TSS Heat Trace Instrumentation

		ACUREX				ACUREX
T/C	DESCRIPTION	CHANNEL		T/C	DESCRIPTION	CHANNEL
TEH-218	Hot Tank Outlet	(B)100		TEH-207	Boost Pump Outlet - Heater A	122 450.
TEH-216	FCV-211, Line X	(B)101		TEH-208	Boost Pump Outlet - Heater A	123
TEH-219	Hot Sump Outlet	(B)102		TEH-227	Cold Sump	*124
TEH-222	Hot Sump	(B)103		TEH-228	Cold Sump	*125
TEH-225	Cold Sump Outlet	104		TEH-220	Hot Sump	(B)*126
TEH-230	Cold Tank Inlet	105		TEH-221	Hot Sump	(B)*127
TEH-201	Boost Sump Drain - Heater D	106 (نەس))	TEH-211	Riser - Storage End - Heater H	128
TEH-202	Cold Pump Outlet - Heater C	107 (LOW)		TEH-241	FCV-151, Heater H	(A) 129
ГЕН-265	Cold Sump Outlet	108		TEH-212	Downcomer - Storage - Heater K	130
TEH-229	Cold Sump Inlet	109		TEH-240	FCV-161, Heaters A-Y, K	131
TEH-233	Cold Tank #1, CT-1 thru 7	*110		TEH-213	Hot Tank #1	*134
EH-234	Cold Tank #2, CT1 thru 7	*111		TEH-214	Hot Tank #2	*135
TEH-235	Cold Tank #3, CT-1 thru 7	*112		TEH-215	Hot Tank #3	*136
EH-231	FCV-201	113		TEH-217	Cold/Hot Tank Bypass-Heater AA	(A,B)137
TEH-232	Cold Tank Outlet	114		TEH-223	Propane Heater	(A)138 472
TEH-205	Boost Suump - Heater W	. 115 (skip))	TEH-224	Propane Heater	(A) 139 47
TEH-206	Boost Sump - Herater W	116		TEH-236	Cold/Hot Tank Bypass, Heater A/	
TEH-203	Boost Pump Bypass - Heater E	117		TEH-238	FCY-242	141 +32
TEH-204	Boost Pump Outlet - Heater B	(بيما) 118		TEH-239	Propane Heater Outlet	(A) 142
TEH-209	Cold Tank Inlet - Heater F	(B)119				
TEH-210	Cold Tank Bypass - Heater G	120	*	Record 1	or TSS Step 2, stored salt temp	o's
EH-237	FCV-162, Heater F	(B)121	(A)	Normally	not operating during system of	peration
					ired for Propane Heater operati	

Table B TSS Heat Trace Instrumentation

<u>T/C</u>	DESCRIPTION	ACUREX CHANNEL	6.0
TEH-305, 306	Hot Salt Inlet Lines	200, 201	
TEH-307, 308	Salt Piping Between SH and EV	202, 203	
TEH-309 thru 311	Cold Salt Inlet Lines	204 thru 206	
TEH-312 thru 314	EV Salt Outlet	207 thru 209	
TEH-315 thru 317	Salt Drain Lines	210 thru 212	_
TEH-318, 319	SH and EV Outlet Overpressure	**213, 214	
TEH-320, 321	Superheater	215, 216	
TEH-322. 323	Evaporator	217, 218	_
6005 thru 6009	Misc. Salt Lines (info.)	230 thru 234	233 (Skfp)
6011 thru 6016	Superheater (info.)	##236 thru 241	234 (O.R.)
	FCV-351 Body, Bonnet	242,/243	
6020 thru 6025	Evaporator (info.)	# #245 thru 250	
6026 thru 6029	Hot Salt Inlet (info.)	251 thru 254	
6030, 6031	FCY-341 Body, Bonnet	255,/256	
6032, 6033	FCV-301 Body, Bonnet	257, 258	
6034, 6035	FCV-321 Body, Bonnet	259, 260	
6036, 6037	FCV-381 Body, Bonnet	261, 262	
6038, 6039	FCV-382 Body, Bonnet	263, 264	
6040 thru 6042	Salt Drain Lines (info.)	##265 thru 267	
6043	SH Drain (info.)	**268	
6044 thru 6053	Misc. Lines (info.)	269 thru 278	275 (Skip) 277 (O.R.)
**************************************	.99119	•	4// (U.K.)

^{**}These will normally be below salt freezing temperature (no problem).

TABLE C SGS HEAT TRACE INSTRUMENTATION

^{##}These may be below 480°F - But they should be above 400°F prior to salt flow.

	į	1		•		1 St.	• •	
T	ABL	.E D	6	ROUP ALAI	M LIST		:	
				- 4 -		i.		
G AL		GE	NERAL	ALARM	r :			
			;	,, ,, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	, !	•		
		T-20		TE-180	TE - 383	TE- 50	8 LS-541	LV- 28
	<u> </u>	T- 22). 	TE- 181	387		_	LV-43
	ļ., Ļ	T+281	<u> </u>	TE-184	388		•	LV- N9
	Ļ	T-241		TE-211	TE - 481		TS-501	N90-AL
		T-3)		TE-231	484		T8-502	
		T-47)		TF-281	484			
		T-511		TE-286		-1-	المؤلم منتشق المداء المراديات	
					: : • • •			1
RAL		RECE	VER C	PERATIC	WAL ALA	ams		,
	-				· i -	ie !	4 s	
FT-101	ļ	T-151		TE-101	PT-181	,		
	į	T-161	1	TE-102	PT-182			
				E-161				
				RS TE'S				
SAL	9	STEAM	GEN	erator c	PERATION	AL ALARA	2	
		* •	•	TE-301	TE- 384	PT-321	PT-431	
				TE-331	386	382	432	
				777	uni	707	: 407	

* - v · · • ·	1E-331	386	382	432
•	732	421	383	483
	TE-382	483	384	
ļ	•		38 <i>6</i>	

PAL ELECT. POWER OPERATIONAL ALARMS

ET-581	77-501	7E-505	77-521	PT-501	PT-531
ST-581	TT-502	7E-506	TT-5'87	502	581
ZSH-AEP	7E-503	11-507			.583

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TABLE E MSEE REMOTE OPERATED VALVE ALIGNMENT

			PRE	TEST		OPER	ATION	POST		
	VALVE	FUNCTION	BASIC FULL SYSTEM	MODIFICATION TO OPERATE 1. W/O RECUR 2. W/OR W/O PROPANE HTR	TO OPERATE 1. RECVRONLY -OR- 2. PROPANE	Basic Full System	MODIFICATION TO OPERATE 1. W/O RECVR: -AND- 2. W/PROPANE HTR	TEST		·
	FCV-101	RECVE FLOW CTEL	O MAN			© CASC SREAL	OMAN	O MAN		
-	FCV-102	RECVE FLOW CTEL	O MAN			© CASE SP.SALT	MAN	O MAN		
	FCV-151	CST LEVEL CTRL	MAN MAN	@ L MAN	OL MAN (W/HTA)	© CASC LT-151	OL MAN	O MAN		
	FCV-161	HST LEVEL CTRL	0 20%·	OL MAN	OL (W/ HTR)	AUTO	OL MAN	O MAN		
	FCV-162	HST LEVEL CTRL	0	O MAN	O MAN (W/ HTR)	AUTO .	O MAN	O MAN		
	FCV-180-189	RECUR PRAIN	0			•		•		
.v.	FCV-190-198	RECUR PURGE	0			•		•		
7-/2	FCV-501	TURBINE STOP	8			0				
. <i>\tilde{</i>	FCV-511	HOT WELL OVERFLOW				©				
	FCV-512	HOTWELL MAKE-UP	ENTRICIDEE			EN,HLC ON	·	-EMMES DEF		
	FCV-521	OIL COOLANT FLOW CTRL	ANTO SP 120 F			© AUTO F		• MAN		
	FCV-541	CNST MAKE-UP	O LOCAL CATEL			LOCAL CHTRL		LOCALCHTRL		
	FCV-551	CONDENSATE RECIRC	0			•		•		
	FCV-561	TURBINE TRIP	ET OFF			• ET OFF		● ET OFF		
	TVM	TURBINE THROTTLE	©			<u>©</u>		•		
										_
			⊕ L	0	©					
			-rocked	-OPEN	-CONTROLL!	NG				
			L-C'LOSED				•			
2							1			

Test	Date
9/22	/84

COP #2 CONTROL ROOM POST-TEST CHECKLIST

This Console operating procedure will be utilized to secure the process controls following all tests. This checklist shall be completed by the Control Room process console operator.

STE	P	DESCRIPTION								<u>N</u>
I.	HEL	IOSTAT	SUBSYST	<u>EM</u>						
	1.		system ststs,			-				
II.	RS	RECEIV	ER SUBS	ì						
	1.	Verify	the fol	llowing v	alve al	ignment:				
01					Man/Op Man/Op Off/C1 Off/C1	en osed	(ZSL's		08 09	
02	2.		the rec		vity do	or is ful	1 y			_
	3.			red from		cian - po: #4).	st		······································	_
III.	TSS	THERM	AL STORA	GE SUBSY	STEM					
	1.	Verify	the fol	lowing va	alve al	ignment i	n MAN:			
02		FCV-16 FCV-16 FCV-19 FCV-20	2 Open 9 Open 1 Closed	04 i	FCV-221 FCV-231 FCV-241 FCV-242	Closed/Lo Closed Closed				_
	2.	Record	d the fo	ollowing s	salt le	vels & ter	mp's:			
	LT-	-201 Co	ld sump		_in.	0	•F	(Acurex	Chan	124,125)
03	LT-	-281 Co	d tank	475	_in.	e	b _F	(Acurex	Chan	110-112)
)3	LT-	-221 H	ot sump		_in.	0		Ŷ.		
	LT-	-291 Ho	t tank		_in.	0	°F	(Acurex	Chan	134-136)
	3.			cured from t complet		nician - p P #4).	oost	 		

(Lock-up)

4. Net-90

STEP	<u> </u> 	DESCRIPTION		VERIFICATION
	i i			
i i	FM	CON System Shutdown		
	a)	Terminate MSSND execution		!
	b)	Execute "SHUT UP" command file	1 .	s.
	:	1) No device modifications		-
I .	c)	Spin down disk drives		
	d)	Turn off power to equipment		
2.	Ac	urex System Shutdown	i	4
	a)	Terminate host operation via key switch control		
	b)	Turn off power to equipment		
3.	Dat	ta System Shutdown		
	a)	Terminate programs		
	b)	Spin down disc drive		
	c)	Turn off power to equipment		· · · · · · · · · · · · · · · · · · ·

7.2 RE	PETACK O	PEKATING P	PROCEDURES	

• • •		Tool Bala
ROP	#1 RECEIVER PRETEST CHECKLIST	Test Date 6/7/84
	This Receiver operating procedure will be utilized to verify RS intregrity prior to all tests that use the Receiver. This checklist shall be completed by the RS technician.	
STEP	DESCRIPTION	VERIFICATION
1.	Turn on the Tower Air Compressor in continuous duty. Verify pneumatic air is available at 80 psig min. Note it may already be on for HRFS or Facility.	
2.	Verify air is being supplied to the Cold Surge Tank and backup air supply for the Drain/Purge Valves (separate manifolds) as follows:	
	 a. Open valves on supply bottles. b. Verify supply bottles at 300 psig minimum. c. Adjust HPCV-171 to read 200 psig on the Cold Surge Tank regulator. d. Adjust the backup air supply regulator to 65 psig 	
	Verify the EPS and 2 each control panel power supplies are ON with each set to 24 volts.	
4.	Verify the receiver uninterruptible power supply (UPS) is ready and operational (battery gage greater than 90V).	
5.	Set up remote camera.	
	Verify/adjust the pneumatic activated valve air set on the Drain and Purge valves (FCV 180 - 198) to 30 psig outlet pressure (should be done with valves open).	
	CAUTION	
	Verify valve temp's with control room prior to cycling.	
	Align/verify valve positions as specified - coordinate with EMCON operator; verify pneumatic pressure to the valves (FCVs)	
	FCV 101 Salt Flow Control Open/N FCV 102 Salt Flow Control Open/N FCV 180-189 Drain Valves Open/N FCV 190-198 Purge Valves Open/N	
	Using a probe, verify the Hot Surge Tank Vent is free of frozen salt (not blocked).	

9. Check Flux Gage Coolant Pump, and radiator for leaks. Verify level in radiator is within 2" of top.

ROP #1 RECEIVER PRETEST CHECKLIST

STEP	DESCRIPTION	VERIFICATION
10.	Verify coolant flow through Flux Gages.(indication on flowmeter.)	
11.	Visually check the Receiver Cavity Door, Cavity Walls, and the door supports for evidence of scorching. Coordinate RS cavity door operation with Emcon operator.	
12.	Check for visual evidence of blown fuses, burned relays or burned electrical components in the power junction box and generally through out the receiver subsystem.	
13.	Inspect the salt system for evidence of leaks and insulation damage. This is a general inspection for any condition that appears abnormal. If a problem is detected (i.e. salt leak, etc.), a more thorough inspection will be required.	
	o RS tower piping o Surge Tanks (2 ea) o Valves (21 ea) o Receiver Assembly (Panel)	,
14.	Advise the control room that the RS pre-test checklist has been completed.	

THE RECEIVER SUBSYSTEM IS READY FOR STARTUP

This Receiver operating procedure shall be performed by the Emcon operator. Periodically advise the RS technician of status.

STEP DESCRIPTION

VERIFICATION

- 1. Verify completion of the following checklists:
 - o CS Pretest Activity (Heliostats to Line Bottom)
 - o COP #1 Control Room Pretest Checklist
 - o ROP #1 RS Pretest Checklist /
 - o TOP #1 TSS Pretest Checklist

WARNING

Only operating personnel are allowed in the salt storage and receiver areas while system is operating. Access is to be controlled by the test conductor. Protective clothing must be worn by personnel working in these areas during operation. All other personnel are to keep clear of these areas.

- 2. Advise the Heliostat operator to Bring the Heliostat Field up to Far Standby.
- Open the Receiver Cavity Door (DR.OPN).

 Verify visually and by micro indications (ZSHDR on).
- 26 4. Reset EPS Racks 1 and 3 (turn EPS1.RST and EPS3.RST on then off). Verify Emcon SCRAM disable signal is On.
 - 5. Advise the Heliostat operator to
 Direct Warmup A Heliostat Group at the receiver.
 (Use CRTF's OP-78-03 for specific steps.)

NOTE

Graphic 990

Receiver panel temperatures
(TE-131 thru TE-148) must be greater than 450°F
prior to opening FCV 151 (step 19) during manual
startup or starting RS.Fill automatic sequence
(step 11) during automatic startup.

CAUTION

o Receiver maximum temperature: 1050°F

If any receiver temperatures remain below 450°F, heliostats may need to be added to increase the temperature of that portion of the panel. Conversely, if any temperatures start approaching 1000°F, heliostats will have to be removed to limit the flux to that portion of the panel.

	STEP	DESCRIPTION	VERIFICATION
	6.	Advise the salt storage tech. to unlock FCV-211.	
04	7.	When unlocked, open FCV 211, verify micros. (If Cold Sump level LT-201 is equal to or greater then 50 inches, this step should be delayed until just prior to starting the CSP to avoid leakage and possible sump overflow.	
	8.	Enable cold sump level control and fill; sump as follows to prime CSP for starting and provide an adequate salt reservoir for fill operations:	
04		 a. Activate FCV-201 with a SP of 48° b. Verify sump level is 50° min. (60° max.) c. Reset FCV-201 SP to 45° 	
	9.	Reverify salt path temperatures are acceptable:	
06 10 07		Receiver Panel TE-131 thru 148 Receiver Pass Outlet TE-101 thru 120 Receiver Header TE-182 thru 198 Acurex RS (COP #1 Table A) COP #1 Table B)	<u>\</u>
		NOTE	
12		The auto fill sequence starts here. Start-up	
GR 992		can be accomplished using the auto start sequence (RS.FILL On) or manually from the Emcon console. For auto fill verify RS.MAN OFF	MAN (AUTO 1.24 1)
	10.	Activate the FCV 161 Hot Surge Tank Level Control with a set point of 75 inches.	
	11.	Activate the FCV 162 Hot Surge Tank Level Control with a set point of 56 inches. In manual fill RS.MAN must be enabled to permit a SP change different than 20".	

NOTE

RS.MAN is available to override FCV-161/162's transfer control.

14

STEP	DESCRIPTION	VERIFICATION
12.	Start the Cold Salt Pump (CSP).	
13.	Start the Boost Pump (BP).	
14.	Enable pump pressure alarm PT180.	
15.	When the PT-180 Pump Outlet pressure is greater than 310 psi, incrementally open FCV 151 to 50% in 10% steps.	
	NOTE	
	Monitor the Receiver sequential fill. Pipes fill (TE-161), CST level rises (LT-151), Flow starts (FT-101), HST level rises (LT-161).	
16.	Close FCY-199 (FCY-199 on) when HST level LT-161 reaches 10" (after 50" CST level). Yerify micro ZSL199 on.	
17.	When the LT-161 Hot Surge Tank level approaches 55 inches, Verify FCV-162 is in auto and maintaining 56 inches.	
18.	Close drain valves FCV-180 thru 189 (off). Verify closure.	
19.	Sequentially close the following Purge Valves at 10 sec. intervals (off) to establish serpentine flow. Verify closure.	Jan
	FCV-190 FCV-193 FCV-196 FCV-191 FCV-194 FCV-197 FCV-195 FCV-198	
20.	Reset the FCV-162 Hot Surge Tank Level set point to 20".	
21.	Reset the FCV-201 Cold Sump Level set point to 23".	
22.	Establish Receiver manual salt flow control:	
	a. Take RCA off scan. b. Activate FCV-101/102 CASC control (from FD-101) c. Verify FD-101 is in auto and adjust SP to 30 Klb/hr. Verify flow below 35Klb/hr.(1984 (1984))	
23.	Activate the FCV 151 casc. Cold Surge Tank Level Control, then update auto. LT 151 level control with a set point of 87 inches.	

<u>s</u>	TEP	DESCRIPTION	VERIFICATION
	24.	Activate the Receiver Temperature Control by putting RCA on scan. (Temperature set point SP.SALT will automatically come up at 750°F. This will maintain a low salt flow rate through the receiver with only the warm-up Heliostats on target. FD-101 is automatically controlled from RCA.)	
	25.)	Enable Receiver operational alarms by turning RAL on.	
	26.	Verify/Turn off RS.FILL if it was used. (Turns itself off when auto fill is complete).	
•	THIS	IS THE END OF THE AUTOMATIC SEQUENCE. THE R.S. IS NOW OPE (WARM STANDBY) AWAITING START OF SOLAR CHARGING ACTIVITY.	RATIONAL
		NOTE	
		Receiver minimum flow rate is auto limited to 30 klb/hr.	
;	27.	To maintain the Warm Standby condition (cold flow) for an extended period of time:	
01		 a. Deactivate the Receiver Control Algorithm by taking RCA off scan. b. Reset the FD-101 Salt Flow Control set point to 30 klb/hr or to desired flow rate. c. Remove the warmup heliostats from the receiver. d. Close the receiver cavity door amd verify. 	t ended Warm St dby
:	28.	 a. Receiver cavity door is open. b. Warm-up Heliostats are on Receiver. c. RCA Receiver temperature control algorithm is activated - scan on. d. SP.SALT setpoint is initially set to 750°F. 	
2	29.	Conduct solar charging by advising the Heliostat operator to direct incremental Heliostat groups onto the Receiver per operating condition requirements. (Eighth of the field increments are standard). Adjust/Step-up SP.SALT accordingly (1050°F max.) and be alert for cloud and process transients.	Solar Charging

STEP | DESCRIPTION

VERIFICATION

30. When individual heat trace thermocouple temperatures exceed 750°F, verify the following Acurex channels indicate CLSD (circuit automatically turned off):

Channe1	Area
*063	Upper and Lower Headers * *
* 064	Secondary Headers
065	Header East End
066	Receiver outlet
069	Hot Surge Tank
451	Downcomer and Hot Tank inlet

*The switch on the Module Control Room local control panel must be in REMOTE to allow Acurex automatic control to turn these off.

THE RS IS NOW ON LINE IN SOLAR CHARGING CONFIGURATION.

NOTE

During RS Solar operations, intermittantly monitor these parameters:

- -- Solar Insolation (CF) Control Room Weather Monitor Panel above 600 W/M² (TSS) Emcon 'SUN'
- -- Cavity Door Temperatures Acurex channels 45,46, & 47

This Receiver operating procedure shall be performed by the Emcon operator. Periodically advise the RS and TSS technicians of status.

		į į	
	STEP	DESCRIPTION	<u>VERIFICATION</u>
	1.	Defocus the heliostats.	
01	2.	Verify/Adjust SP.SALT to 750°F, FCY-201 SP to 23".	
02	3.	When FT-101 drops to less than 30 Klb/hr, close the receiver cavity door and verify micros.	
01 02	4.	Deactivate the Receiver Control Algorithm (by taking RCA off scan) and set the FD-101 set point to 60 Klb/hr. Wait 3 minutes minimum and continue when TE-161 is less than 700°F. Verify FCV-162 is open and maintaining level in HST.	***************************************
02	5.	Deactivate FCY-161 control and close.	
	6.	Check Acurex Ch 000-018, if below 480°F advise RS technician to turn heat trace to local 'ON' until accept When individual heat trace thermocouple temperatures drop below 700°F, verify the following Acurex channels indicate OPEN (circuit automatically turns on):	cable.
		*063 Upper and Lower Headers *064 SecondaryHeaders 065 Header East End 066 Receiver Outlet 069 Hot Surge Tank Inlet	
		*The switch on the Module Control Room local control panel must be in REMOTE to allow Acurex automatic control to turn these on.	
		THE RS IS NOW IN WARM STANDBY. SALT FLOW MAY BE VARIED TO PROVIDE DESIRED TEMPERATURE/FLOW THROUGH THE RECEIVER	. .
		NOTE	
12 GR 9	992	The RS.DRAIN Auto Drain Sequence starts here. Shutdown can be accomplished using the Auto sequence or manually from the EMCON console. Note Auto seq. steps are not performed in the exact order that follows.	MAN AUTO
01	7.	Set FD-101 setpoint to 30 Klb/hr. Wait for flowmeter FT-101 to stabilize at 30 Klb/hr + 3 Klb/hr, then cont.	

STEP	DESCRIPTION	VERIFICATION
8.	Open the following purge and drain valves (on). Verify open micros ZSH 180 thru 198 on .	
d.	FCV-180-189 FCV-194 FCV-190 FCV-195 FCV-191 FCV-196 FCV-192 FCV-197 FCV-193 FCV-198	
9.	Disable RAL by turning it off.	
10.	Deactivate FCV-101 & 102 auto control. Close FCY-101 & 102. Verify closed micros. Wait 30 seconds before continuing. (Note Auto sequence leaves these in Auto).	*************
11.	Change LT-151 set point to zero. Verify FCV-151 closed.	
12.	Deactivate FCV-151 auto control.	
13.	Verify FCV-162 closed (in Auto). The RS is now bottled up and stagnant.	(
	CAUTION	
	The next three steps initiate salt drain back to the Cold Salt Tank and must be accomplished following the sequence described. An early response could cause an overflow of the hot surge tank. A late response could cause damage to the receiver piping.	
	WARNING	
	Only operating personnel are allowed in the salt storage and receiver areas while system is draining. Access is to be controlled by the test conductor. All other personnel are to keep clear of these areas.	
14.	To drain HST and downcomer, Deactivate FCV-162 auto control, ramp open FCV-162 to 100% in 20% increments 5 seconds apart, verify open micro, continue when LT-161 reaches 0" or stops decreasing.	
15.	Open FCV-199 to drain CST and riser, observe LT-151 at 15 inches, then wait 5 seconds.	
16.	Open FCV-101 & 102 5% to drain Receiver residual salt, Record time. (Ref. step 24).	TIME
	· · · · · · · · · · · · · · · · · · ·	

02

01

STEP	DESCRIPTION	VERIFICATION
17.	Deleted. NOTE	
	If SGS is operating (ZSH.HSP ON), go to Step 24.	
18.	Dicable PT_180 numn pressure alarm	
19.	Turn off boost pump.	
20.	Turn off cold salt pump.	
21.	Change FCV-201 set point to zero, wait 15 seconds.	
22.	Put FCV-201 into manual.	,
23.	Close FCV-211 and manually lock it closed.	
24.	Open FCV-101 & 102 100%, approximately 2 minutes after completing Step 16.	TIME
25.	Verify/Turn off RS.DRAIN. (Turns itself off when Auto Drain is complete)	IIME
	THIS IS THE END OF THE AUTOMATIC DRAIN SEQUENCE. THE RS IS AWAITING RESIDUAL SALT DRAINBACK.	
26.	If the SGS is not in operation, 15 minutes after completing Step 24, open:	· }
	FCV-151 FCV-161 (only if hot tank has salt leve	1)
27.	If the SGS is not in operation, 20 minutes after completing Step 24, close the following valves:	
	FCV-180-189 FCV-194 FCV-190 FCV-195 FCV-191 FCV-196 FCV-192 FCV-197 FCV-193 FCV-198	
28.	Advise RS tech to turn trace heat back to remote, if turned on locally in step 6.	and the second second second second
29.	Advise the RS and TSS technicans to complete their post test checklists (ROP #4 & TOP #4). if no further RS or TSS operation planned.	

THE RS IS NOW SHUTDOWN AND DRAINED.

This Receiver operating procedure will be utilized to verify RS integrity following all tests that use the Receiver. This checklist shall be completed by the RS technician.

STEP	DESCRIPTION	VERIFICATION
1.	Inspect the salt system for evidence of leaks and insulation damage. This is a general inspection for any condition that appears abnormal. If a problem is detected (i.e. salt leak, etc.), a more thorough inspection will be required.	!
	o RS tower piping o Surge Tanks (2 ea) o Valves (21 ea)	
2.	Verify the following valve alignment. Coordinate with Emcon operator.	
	FCY-101 OPEN FCY-102 OPEN FCY-180 thru 189 CLOSED FCY-190 thru 198 CLOSED	
3.	Open the Receiver Cavity Door and inspect Receiver Assembly for evidence of leaks (white on black surface) and general condition. Close the door when the inspection is complete. Coordinate with Control Room.	
4.	Secure remote camera.	
5.	Close the Cold Surge Tank and Receiver pneumatic backup supply bottles handvalves. Record values, CST = p/Air =	
6.	Turn off the Tower Air Compressor only after obtaining clearance from Control Room. (It may still be in use for HRFS or Facility).	
7.	Note any items or abnormalities encountered during test activities.	
8.	Advise the control room that RS post-test checklist has been completed and the RS is secure.	

7.3	THE	RMAL	STORAGE	OPERATING	PROCEDURES
TNP	#1	22T	PRETEST	CHECKLIST	

Test Date 6/20/84

This Thermal Storage operating procedure will be utilized to verify TSS integrity prior to all tests that use Molten Salt. It shall be performed by the TSS tech.

STEP	DESCRIPTION	VERIFICATION
1.	Inspect the salt system for evidence of leaks and insulation damage. This is a general inspection for any condition that appears abnormal. If a problem is detected, a more thorough inspection will be required.	
	 TSS salt piping Hot, Cold, and Booster Pumps and Sumps Vents Valves 	
2.	Check for visual evidence of blown fuses, burned relays or burned electrical components in the power junction boxes and generally throughout the TSS.	
3.	Verify that the EPS Power Supply (lower part of rack) is set to 24 VDC and is ON.	
4.	Start/verify the air compressors are ON with a 80 psig supply pressure. Drain water from old compress tank.	
5.	Inspect the fan and louvers in the pump house for proper operation. Verify that the fan thermostat is set to 70°F.	
6.	Open the hand valve HV-284 at the old air compressor	
7.	Verify coolant flow through the HSP and BP bearings (piping will be cold with indication on the flow meter).	
8.	Verify the HSP, CSP and BP circuit breakers are off and the shafts of all three pumps are free. (Bump BP to verify freedom with C.B. On in local).	
9.	Turn on the HSP, CSP and BP circuit breakers and place the controls for the pumps in Auto. and verify air flow through the Cold Salt Pump bearings.	
10.	Using a probe, verify the C.S., C.T., H.S., H.T., and Booster Pump Sump vents are free of frozen salt. During routine operation, only intermittant verification is required. Particularly verify prior to restart after a shutdown or if pluggage is suspected from high salt levels (CS 60", HS 45").	

STEP	DESCRIPTION		VERIFICATION
11.	Turn ON the TSS/SGS back	y as follows:	
	 a) Verify supply bottles b) Open the valves on the isolation valve c) Adjust the regulator 	e supply bottles and m	um ain
12.	Check coolant pumps and operation. Verify that open. At the beginning in the radiators and fil	293 are	
13.	Align/verify the valve po Coordinate with Emcon ope		
	<u>Valve</u> <u>Description</u>	Positi	on Air Press.
14.	FCV-151 Cold Surge Lever FCV-161 Hot Tank Inlet FCV-162 Cold Tank Inlet FCV-199 Bypass FCV-201 Cold Sump Lever FCV-211 Cold Sump Lever FCV-221 Hot Sump Lever FCV-221 Hot Sump Isolat FCV-241 Propane Heater FCV-242 Propane Heater FCV-301 Bypass Salt Flor FCV-341 Cold Salt Isolat FCV-351 Hot Salt Isolat FCV-351 Hot Salt Isolat FCV-352 Hot Salt Isolat FCV-353 Hot Salt Isolat FCV-353 Hot Salt Isolat FCV-354 Hot Salt Isolat FCV-355 Hot Salt Isolat FCV-356 Hot Salt Isolat FCV-357 Hot Salt Isolat FCV-358 Hot Salt Isolat FCV-359 Hot Salt	Closed/ Closed/ Open/N Closed/	N 30 psi N 40 psi N 40 psi N 40 psi Locked 40 psi Locked 30 psi N N N
	FCV-151 FCV-161	.ocked .ocked open/N	
	FCV-242	luetral	
15.	For operation without SGS of step 13 as follows:	, Modify the valve al	ignment ——————
		.ocked .ocked	

STEP	DESCRIPTION	VERIFICATION
16.	Align/Verify the hand valve positions listed below:	
	HV-280 HS/CS Tie Closed HV-281 HT/CT Tie Closed	
17.	Determine if the OLIN Salt Test Loop is to be used. If it is, align these HV's accordingly (with SGS only):	
	HV-282 Salt Inlet Open HV-283 Salt Outlet Open	
18.	Set up the Eppley sun meter insolation instrument. It is located on a post south of the TSS. (Emcon 'SUN').	
	 a) Rotate platform of tracker (by hand) to acquire sun Fine adjust using azimuth and elev. screw adjust. (Sun dot should be in center of target on rear of i 	
	 b) Open door of timer box located on post. Rotate timer (turn on) to appropriate run time. (Adjust to approx. one half hour past shut-down). Close timer door 	
	c) Verify operation. Listen for tracker motor running. Recheck sun target on Eppley, readjust using thumb screws. Tighten lock screws.	
19.	Advise the Control Room that the TSS Pretest checklist has been completed.	

NOTE

Complete the SGS pretest checklist (SOP #1) and/or Local Propane Heater startup (TOP #2A) as required.

PROPANE HEATER PROCESS START-UP TOP #2

The Propane Heater is used to charge hot salt when weather conditions do not allow adequate solar charging or when the Receiver or Collector subsystems are not on line.

This Thermal Storage operating procedure shall be performed by the Emcon operator. Periodically advise the TSS technician of status.

Turn on propane inlet and outlet lines trace heater circuits (TEH 223, TEH 224, and TEH 239 for temperature readings) a minimum of 10 hours prior to intended usage of the Propane Heater. Ch 138, 139, 142

STEP	DESCRIPTION	VERIFICATION
1.	Verify completion of the following checklists:	
	 COP #1 Control Room pretest checklist √ TOP #1 TSS pretest checklist 	
2.	Instruct/Confirm TOP #2A Local Propane Heater Start-up.	
3.	Record the time upon notification from the TSS technician that the Propane Heater is on Main Flame with 700°F stack outlet temperature. (Ref. steps 10 and 12).	12:03 TIME
05 4.	Verify Cold Tank level LT-281 is greater than 30 inches. If the SGS is operating (on-line) continue at step 11.	
5.	Verify Cold Sump Level LT-201 is less than 60 inches.	1
6.	Place FCV-211 in neutral and fully open; verify micros.	
7.	Verify/increase the Cold Sump Level to 50 inches.	
8.	Activate the FCV-201 Cold Sump Level Control with a set point of 23 inches.	
9.	Verify LT-201 alarm is activated.	/
04 10.	14 minutes after MAIN FLAME (step 3) start Cold Pump.	
11.	Verify Cold Pump outlet pressure PT-180 increases to greater than 170 psi.	
	NOTE	

NUIL

The Hot Tank must be precharged to 750°F prior to introduction of any high temp. salt. During precharge, leave FCV-221/231 open until the Hot Sump level increases (40" max.), then quickly close FCV-221/231.

DESCRIPTION VERIFICATION STEP Initiate salt flow through the Propane Heater 05 12. 15 minutes after completing step 3; Unlock and open FCV-241 to to 50% open. 13. Open FCV-242. Record Time. NOTE . It will take approximately 10 minutes for the salt to flow through the Propane Heater. Monitor Acurex channel 142 and LT-291 for verifing flow through the heater. Advise the TSS technician to turn off the trace heater 14. L6-1 and inlet to Hot Tank if TEH-239 salt temperature will be exceeding 750°F. Verify. Adjust the Propane Heater for a 1050°F (or desired tem-15. perature) salt outlet temperature by accomplishing the following after salt flow into hot tank verified (LT-291 10 minutes later): Advise the TSS technician to set the Burner Temperature a. control to 1100-1200°F stack temperature. Use TEH-239 (Acurex channel 142) as the actual salt salt outlet temperature indication (1040°F max.).

c. Adjust FCV 241 to TBD% (approximately 40 to 55% for 750-900 F salt and 35-40% for 900-1050 salt). If 1050 salt is desired place stack tempature at 1250 and start with FCV 241 at 50% and adjust accordingly.

Actual temperature approximately 50°F higher than channel 142 read-out at high (1000 °F) temperatures; approximately 20°F higher at low (700°F) temperatures.

d. Monitor Acurex channels 134/136 as hot tank salt temperature and EMCON TE-291.

THE PROPANE HEATER IS NOW ON-LINE AND CHARGING SALT

This Thermal Storage operating procedure will be utilized to locally operate the Propane Heater in conjunction with Emcon (Propane Heater) process operation. This procedure shall be performed by the TSS technician.

STEP		DESCRIPTION	VERIFICATION
1.	Pla tem		
2.	Check level of the Propane Tank and verify sufficient propane for present test - 15% or 900 gallons minimum.		
3.	Che	ck/ignite pilot lights of propane evaporators:	
	Α.	If vaporizers are not lit, then remove small square cover on south side. Turn knob to pilot.	
	В.	Open center cover (west side) to get to pilot. Pilot is located between metal cylinders at the bottom.	
	c.	While holding knob on south side in full C.C.W. position, light pilot.	
	D.	Hold in this position for 30 to 60 seconds, then turn to on position. Replace covers slowly or flame may go out.	
4.	(to	n all three evaporator outlet hand valves p east side of evaporators) fully. ssure guage at Heater inlet should read 55 to 60 psi.	
5.	Che The	ck pressure gauge bottom north side of heater. reading should be about 8 oz.	
6.	Pla	ce Burner switch on local console to preheat.	
7.		n on power switch - red power and timer light ould come on.	
8.	Timer light will remain on for about 2 min. as system is purged prior to introduction of pilot flame gas. Timer light will then go off and about 20 sec. later both timer and pilot light will come on to ignite the pilot flame. If IR scanner does not datect a pilot flame within 6 sec., the start sequence will be stopped and the timer will reset and start over. When the pilot flame is achieved, the PILOT LIGHT will come on.		

STEP

DESCRIPTION

VERIFICATION

WARNING

If pilot flame does not light after two tries, close valve on vaporizer and troubleshoot system.

	0.000 14.70 0 14.50 14.00 0 0 0	
9.	After pilot is lit for about 1 minute, switch to main flame, set temperature control to 250°F and allow to soak for three minutes minimum.	
10.	Slowly advance temperature control to 700°F - do this slowly to avoid screeching of heater. Main flame light should stay lit.	
11.	Notify Control Room that the Propane Heater is on Main Flame with a 700°F stack outlet temperature (awaiting 15 min. heat soak prior to process operation).	

TROUBLE SHOOTING GUIDE

Signs of trouble are:

- 1. Low or very high reading at pressure gauge.
- 2. Stack temperature varies or stays low.
- 3. Unit will not start, no pilot.

All the above can be caused by the vaporizers not being lit. Any vaporizer that is out can cause these troubles.

If the heater is running and frost can be noted on the fuel lines, DO NOT TURN HEATER OFF. Relight the vaporizer(s) that are out and continue to run at reduced temperature until the frost is gone.

If you cannot get the vaporizer to light, turn off the hand valve and let the heater run until frost has left the lines. Heater will run on one vaporizer at reduced output. Try to get at least one lit to help remove the liquid propane from the lines.

If the heater will not light, check to see if the ignition wire on bottom of the heater is on the plug.

TOP #3 PROPANE HEATER PROCESS SHUT-DOWN

This Thermal Storage operating procedure shall be completed by the Emcon operator. Periodically advise the TSS technician of status.

STEP	DESCRIPTION

VERIFICATION

NOTE

When shutting down the Propane Heater in conjunction with the SGS (both in operation), perform SOP #5 - not this procedure.

		not this procedure.	
05	1.	Advise the TSS technician to adjust the burner temperature Control to 600°F stack temperature when the Hot Tank level LT-291 is within 12 inches of the desired level (or within 7 inches of desired level in the Cold Tank).	
	2.	Open FCV-241 to 60%.	
	3.	When 2 inches from desired level, or when channel 142 reads 800°F, deactivate FCV-201 Cold Sump Level Control.	<u> </u>
	4.	Close FCV-201 and FCV-211 (manually lock closed).	
04	5.	Turn off the Cold Pump when it cavitates. (PT-180 drops below 165 psig, LT-201 approx. 11.5"). Record Time. (Ref. steps 7 and 8).	13:45 TIME
05	6.	Open FCV-241 to 100% open.	
02	7.	Wait 2 minutes to allow salt drainage, then unlock and open FCV-151 and FCV 161.	
		NOTE	
		LT-201 will increase to approximately 58 inches during propane heater draining.	
	8.	Advise the TSS technician to shutdown the Propane Heater 30 minutes after Cold Pump shutoff (step 5) with TOP #3A.	
05	9.	Close FCV-241, FCV-242.	
	10.	Advise the TSS technician of the following days operating requirements for heat trace actuation.	
	11.	Verify Propane Heater shutdown from TSS technician.	
	12	Advise the TSS tech to complete TOP #4 as required.	

This Thermal Storage operating procedure will be utilized to locally shut down the Propane Heater after Emcon (Propane Heater) process operation. This procedure shall be performed by the TSS technician.

STEP	DESCRIPTION	VERIFICATION
1.	Turn stack temperature control to 600°F when directed to do so by Emcon operator.	
2.	After cold salt pump has been turned off, allow a minimum of 30 minutes to drain.	
	NOTE	
	If shutdown includes SGS, the Cold Pump may be restarted to deplete the cold sump. Allow full 30 minutes drain time.	
3.	Turn main flame/preheat switch to preheat.	
4.	Turn temperature to 200°F.	
5.	Turn power off.	
6.	Close the 3 evaporator outlet hand valves to avoid the collection of liquid propane in the line.	
7.	Adjust the Propane Heater heat tracing as follows:	
	a. For Propane Heater use the following day, Turn on the Propane Heater outlet line LG-1 and Hot Tank inlet heat trace.	
	b. If Propane Heater is not to be used the following day, turn off the Propane Heater inlet line heat trace (TEH-223, 224).	
8.	Advise the Control Room that the Propane Heater is shutdown.	

TOP #4 TSS POST TEST CHECKLIST

This Thermal Storage Operating procedure will be utilized to verify TSS integrity following all tests that use the TSS. This checklist shall be completed by the TSS technician.

STEP	DESCRIPTION	VERIFICATION
1.	Complete the SGS post test checklist SOP #4 (first) if no further SGS operation planned.	
2.	Inspoect the salt system for evidence of leaks and insulation damage. This is a general inspection for any condition that appears abnormal. If a problem is detected, a more thorough inspection will be required. Particularly inspect:	
	 TSS salt piping Hot, Cold, and Booster Pumps and Sumps Vents Valves 	
3.	Check for visible evidence of blown fuses, burned relays, or burned electrical components in the power junction boxes and generally throughout the TSS.	
4.	Close and Lock these valves, Verify.	
	FCV-211 Close/Lock FCV-231 Close/Lock	
5.	If the Olin test loop was used, close HV-282 and HV-283.	
6.	Turn off the CSP,BP, and HSP local starter circuit breakers.	
7.	Turn off the CSP bearing cooling air HV-284.	
8.	Secure the TSS/SGS back-up pneumatic air by closing the supply bottles HV's.	
9.	Leave both Air Compressors On.	
10.	Leave TSS coolant pump and radiator On.	
11.	Advise the Control Room that the TSS post test checklist is complete and the TSS is secure.	

Test	Date
8/02	/84

TOP	#5	SALT	TRANSFER
101	<i>11</i> •	~ · · ·	

Α.	HOT	TANK	T0	COLD	TANK
----	-----	------	----	------	------

I.	Gravity	Transfer	(700	F	maximum))
----	---------	----------	------	---	----------	---

- Verify completion of the following checklists. Particularly verify TSS heat trace temp's and valve align.
 - COP #1 Control Room pretest checklist
 - o TOP #1 TSS pretest checklist
- 2. Verify FCV-211 and 231 manually closed and locked.
- 3. Open HV-281.
- Open FCV-201 and 221.

(Salt flow rate starts to lessen when LT-291 passes 50". Gravity transfer can take the Hot Tank down to approx. 30".)

II. C.S. Pumped Transfer to C.T.

- 1. Verify RS heat trace temps are OK (COP #1 Table A).
- 2. Start off with Gravity Transfer to ensure proper flow
- Close FCV-101/102. (For safety not really required)
- Open FCV-162 and FCV-199 (verify micro's).
- Unlock and place FCV 211-in neutral.
- 6. Ensure LT-201 is greater than 50" (Open/close FCV-211).
- 7. Start the CSP and BP verify PT-180 increases to over 300 psi.
- 8. Close FCV-201.
- 9. Open FCV-211.
- 10. Incrementally open FCV-151 to approximately 40%.

NOTE

Maintain Cold Sump level at 25" by varying FCV-151 setting. (Setting will need to decrease as LT-291 decreases.)

III. Shutdown

- 11. When reaching desired LT-291 level, perform the next steps expeditiously:
 - a. Close FCV-151
 - b. Turn off the CSP and BP
 - c. Close FCV-221 and FCV-201
 - d. Close FCY-211 (and manually lock it).
 - e. Close HV-281.
- 12. After 2 minutes, Open FCV-151, 101, 102, (and FCV-161 if elbow is above 480°F) to drain back residual salt.
 - 13. After 5 minutes, close FCV-151, 161, and 162.

Tes	t	Da	te
8/	02	/8	4

1	UD.	#5	SALT	TR	ANSI	FFR
	UF	πJ	JALI	11134	71121	-11

)P #5	SALT TRANSFER	8/02/84
В	HOT SUMP TO COLD TANK	
I.	C.S. Pumped Transfer to C.T.	
1.	Valve Configuration per COP #1 Part VI TSS.	
2.	Verify transfer line and HV-280 are greater than 450°F by local T/C check.	
3.	Close FCV 101/102 (for safety not really required.)	
4.	Verify FCV-221 and 231 manual closed and lock FCV-231.	·
5.	Open FCV-162 and FCV-199 (verify micros).	
6.	Place FCY-201 in Automatic Control with a set point of 50 inches.	
7.	Unlock and place FCV-211 in neutral.	
8.	Open FCV-211.	
9.	Ensure LT-201 is approximately 50 inches and change FCV-201 set point to 25 inches.	
10.	Start the CSP and BP and verify PT-180 increases to over 300 psi.	
11.	In 10% increments open FCV-151 to approximately 40%.	
	NOTE Circulation of salt must stabilize at a sump level (LT-201) of approximately 25 inches. Monitor LT-151 and LT-161 levels.	
II.	H.S. Pumped Transfer to C.S.	
12.	Open HV-280.	
13.	Turn on Hot Salt Pump.	
III.	Shutdown	
14.	When reaching desired LT-221 level:	
	a) Turn off Hot Salt Pumpb) Close HV-280	
15.	When LT-201 stabilizes at approximately 25 inches:	
	 a) Close FCV-151 b) Turn off BP and CSP c) Close FCV-211 (and manually lock it) d) Deactivate and manually close FCV-201 	
16.	After 2 min., open FCV-151, 101, 102 (and FCV-161 if elbow is above 480°F) to drain back residual salt.	

After 5 min., close FCV-151, 161 and 162. 7-38

17.

Test	: Da	te
6/2	25/8	4

SOP #1 SGS PRETEST CHECKLIST

This Steam Generation operating procedure will be utilized to verify SGS integrity prior to all tests that use the SGS. This checklist shall be completed by the SGS technician. This checklist presumes SGS is in Diurnal Shutdown.

STEP	DESCRIPTION	VERIFICATION
1.	Verify completion of TOP #1 TSS pretest checklist.	
2.	Inspect the salt system for evidence of leaks or damage. This is a general inspection for any condition that appears abnormal. If a problem is detected, a more thorough inspection will be required.	
	All SGS salt pipingValvesSuperheater and Evaporator	
3.	Inspect the water/steam system similarly:	
	 SGS piping Valves, traps BWCP Flange Connestions Drain Plugs Superheater Evaporator Steam Drum Attemperator Drain and Blowdown Tank 	
4.	Check for visual evidence of blown fuses, burned relays or burned electrical components in the power junction box and generally throughout the SGS.	
5.	Intermittantly verify these amperages with a clamp-on Ammeter. Caution - 480V.	
	A. Circ. Heater EH-1 28A EH-2 28A EH-3 16A EH-4 16A EH-5 16A	
	B. BWCP Each Phase 7.8A	
6.	If freezing ambient temperatures have been experienced, Verify operability - Unthaw the following:	
	A. Instrument Transmitters - particularly LT-311 - open xmtr piping drain valves for 10-15 sec. intervals - work with system temp. increases.	
	B. Steam Traps - T-481/HV-491 and T-482/HV-487 - open 1/4 turn and listen for flow. Externally heat as necessary. Open fully after 10 minutes.	

STEP		DESCRIPTION	<u> </u>	VERIFICATION
7.	SGS water	chemistry sampling -		
	flus	in a drum water sample by hing the sample station l filling a one liter samp	ines for 10 minutes,	
	B. Anal	yze and Evaluate the samp	le per HOP #6.	
	for be a	uct a Millipore filter sam suspended iron. Results of dded to the HOP #6 dissol rmination for comparison	of this must ved iron	
	Open to d prot	e HV-386 upon completion of the vent HV-384 located of rain the sample line, part ect against freezing. Clo r totally draining the lin	adjacent to HV-386 ticularly to ose the vent HV-384	
8.	SGS Phosp	hate injection -		
	phos chem	etermined by water chemist phates can be added to the ical feed station on the s ction should be started as	e SGS with the SGS skid (HV-387/388).	
	175 50 a	phosphate injection mixtur grams of granular Trisodio rams of powdery Disodium (2 and 1/2 gallons of dem	um Phosphate and Phosphate mixed	
9.		ify the valve positions lewith Emcon operator.	isted below.	
	<u>Valve</u>	Description	Position	
	FCV-321 FCV-331 FCV-381 FCV-382 FCV-383 FCV-384	Steam Attemperator Evap. Salt Drain Superhtr. Salt Drain Circ. Htr. Bypass Circ. Htr. Supply	Open 10% Open Open Open Closed Open Closed	

STEP

DESCRIPTION

VERIFICATION

10. Align/Verify the following valve positions.

<u>Valve</u>	Description	Position
HV-370	Bridge Feedwater Drain	Closed
HV-371	Circ. Heater Drain	Closed
HV-372	BWCP Volute Drain	Closed
HV-373	BWCP Bearing Cavity	Closed
HV-375	SGS Air Supply	Open
HV-381	Drain	Closed
HV-382	Blowdown Control	Closed
HV-383	Blowdown Isolation	Closed
HV-384	Pump Isolation	Open/Locked
HV-385	Steam Drum Vent	Closed
HV-386	Sample Line Isolation	Closed
HV-387	Chemical Feed Metering	As needed
HV-388	Chemical Feed Isol.	As needed
HV-389	Chemical Feed Drain	Closed
HV-390	Drum No Inlet	
HV-481	Steam Delivery Isol.	Closed
HV-485		Closed
HV-486	Steam Delivery Drain	Closed
	Steam Delivery Drain	Closed
HV-487	Trap Isolation	0pen
HV-488	Feedwater Supply Isol.	Closed
HV-491	Steam Trap Isol.	Open

- 11. After HRFS start-up, coordinate with the Control Room to replenish SGS water. Particularly operate HV-370 and HV-488 as needed. Leave HV-370 closed and HV-488 Open.
- 12. Advise the Control Room operator that the SGS pretest checklist has been completed.

NOTE

After operation is established and consent obtained from the Control Room, Blowdown the steam drum to reduce high Iron and TDS concentrations found by the water chemistry analysis. The blowdown period using HV-382 and HV-383 shall be as follows:

Iron (ppm)	TDS (ppm)	Blowdown Time
200	50	0 Minute
200 to 300	50 to 100	1 Minute
300 to 500	100	2 Minute

Blowdown will only help remove dissolved solids Periodically drain certain dead legs in the SGS using HV-371 and HV-372 to remove suspended solids. This Steam Generation Operating Procedure shall be performed by the Emcon operator. Periodically advise the SGS technician of status. This procedure assumes SGS is in Diurnal Shutdown.

	STEP	DESCRIPTION	VERIFICATION
	Α.	DIURNAL SHUTDOWN TO WARM STANDBY MODE	
	1.	Verify completion of the following checklists:	
		 COP #1 Control Room pretest checklist TOP #1 TSS pretest checklist SOP #1 SGS pretest checklist HOP #1 HRFS pretest checklist and local startup HOP #2 HRFS startup 	
		CAUTION	
		If freezing temperatures have been experienced, be aware of possible bad SGS instrument readings.	
18	2.	Verify D/D temp TE-451 (DTC PV) is above 250°F, then position FCV-431 to Manual Open to start steam pipe heat-up with D/D steam.	
02	3.	If R.S. is not operational, check Acurex channels 121, 129, and 131 are above 480°F and reverify FCV-151 and 161 are closed and locked, FCV-162 is open.	
16	4.	Place/verify MAN.EHAC and EHAC are ON. This places the Circulation Heater in Automatic Pressure Control. Also, verify MAN.ESH-1 thru MAN.ESH-5 are off.	
13	5.	Verify that SP.DL is set at 0.0", that MAN.411 is off, FCV-411 is in cascade at Net 90, and that drum level is being maintained at 0.0 inches + or5 inches.	
	6.	Place/verify SDC and MAN.SDC are both OFF. (These may have to be on to override Hi steam drum levels)	
	7.	Place/verify FCV-321, and 331 are in cascade, at the N90 console Groups H & F, (COT/C). (Ready for N90 control after EMCON deact)	
	8.	Verify the following set points:	
13		SP.EST 850°F Evaporator Salt Temperature (FCV-301) SP.SP 1100 psi Steam Delivery Pressure (FCV-321) SP.ST 950°F Steam Delivery Temperature (FCV-331)	

	STEP	DESCRIPTION	VERIFICATION	
18	9.	Verify D/D Feedwater Temperature at TE451 is above 250°F Change DTC-451 and DTC-452 set points to 300°F.	•	
	10.	Note the Steam Drum Temperature at TE-383. The temperature must be above 500°F to initiate salt flow. If the temperature is below 500°F, wait for circulation heaters to increase the temperature above 500°F prior to proceeding.		
	11.	Verify cold sump temp. Accurex channel 124 and 125 are within 100°F of TE-383 to prevent shocking the superheat If difference is over 100°F, continue to heat SGS to within 100°F with circulation heaters.	er. 	
	12.	Reverify salt path temperatures are acceptable Ref. COP #1 Table B & C.		
	13.	Reset FCY-201 SP to 45" and stabilize.		
	14.	Advise the SGS technician to open HV-481 (ahead of FCV-49 and Verify HV-488 is Open.	91)	
	15.	Have field technician unlock FCV-211.		
	16.	Activate FCV-431 casc. control via PT-431 SP 1080 psi.		
	17.	Activate FCV-491 automatic control with SP 1000 psi.		
	18.	Monitor PT-321 and reduce set point of FCV-491 as require to maintain a constant level during auto SGS.CF sequence	ed •	
	19.	During auto SGS.CF sequence when LT-311 reaches 6" turn on MAN.SDC and SDC.		
	20.	Close salt drain valves after verifying Acurex channel 265 is above 480°F by turning FCV-38182 and MAN.38182 off. Verify closure.		
		The SGS cold flow auto sequence starts here. Monitor 'Control Room' Notes during auto sequence and perform as required.		
cn o	21.	Activate SGS.CF 'ON' to start auto sequence.		
GR 9	22.			
	23.	Start the cold pump; PT-180 greater than 150 PSI before continuing.		
	24.	Activate the following alarms:		
		LT-311 PT-180 TE-301 TE-384 PT-383 TE-383		

STEP DESCRIPTION

VERIFICATION

25. Set SP.341 to 100% to fully open FCV-341 and verify the position. This fills the SGS with cold salt in approx. 12 minutes.

NOTE (CONTROL ROOM)

TIME (REF STEP 25)

- 1. Monitor LT-201 to maintain sump level above 17 inches Do not cavitate pumps.
- 2. If salt temps are low (550°F) turn on Net 90 heater 1 to protect against freezing. Heater 1 will turn off upon FCV-383/384 switchover.

NOTE (CONTROL ROOM)

After opening FCV-341 monitor the SGS temperatures on Acurex and EMCON as listed below to verify that salt is flowing thru the SGS. Each Acurex chanel or EMCON Thermocouple read the same as the Cold Salt Temperature in the order listed:

204 255	*F
270 254	°F
TE382 (EMCON) 216 215 241 203	COLD SALT TEMP (ACUREX CH 124/125)
TE301 (EMCON) 250	
TE384 (EMCON) 208	

If these channels do not appear to be consistent with the Cold Salt Temperature, a blockage may exist. If so, OPEN FCV-301 fully to improve flow temporarily then CLOSE FCV-301 and monitor FT-321 to determine if the blockage has cleared.

NOTE (CONTROL ROOM)
When auto ramp is complete and LT-311 is below 7" turn off
MAN.SDC and SDC.

- 26. Once superheater is filled with salt, TE-301 should read cold salt temp (approx. 5 minutes after step 24). Open FCV-301 with SP.301 to 100% and verify position.
- 27. When FT-321 flow is greater than 10 Klb/hr., set SP.301 to 0% and turn MAN.301 OFF. Verify that FCV-301 closes.

The SGS.CF cold flow auto sequence stops here. The next few steps will be performed manually.

	STEP	DESCRIPTION	VERIFICATION
	28.	Place FCY-301 in Cascade at the Network 90 to control Evaporator salt temperature at SP.EST. NOTE	
		Reactivate FCV-301 at Net 90 after any trip. SGS IS NOW IN WARM STANDBY AWAITING INTRODUCTION OF RESERVED IN TRANSPORTED IN TRANSPORTED IN TRODUCTION OF RESERVED IN TRANSPORTED IN TRANS	HOT SALT
В.	WAR	M STANDBY TO THE ON-LINE CONDITION	
	1.	Verify FCV-221 is closed.	
		Verify the Hot Sump level (LT-221) is less than 48 inches.	
13		Set MAN.331 to OFF to activate the FCV-331 Steam Delivery Temperature Control at SP.ST. Verify that FCV-331 closes and is in Casc. at Net. 90.	
	4.	Yerify/place FCY-231 in neutral.	
		The SGS.ON auto ramp sequence starts here.	
	5.	Activate SGS.ON 'ON' to start auto ramp sequence.	
	6.	Set MAN.383 to ON and FCV-383 ON (Open) and verify Micro.	
		Set MAN.384 to ON and FCV.384 to OFF (Closed) and verify micro; verify that all circulation heater circuits are off.	
	8.	Verify the CSP is operating and FCV-341 is open 100%	
	9.	Activate the FCV-221 Hot Sump Level Control with a set point of 40 inches.	
	10.	Open FCV-231 by turning OPN.231 on, then off. Verify open micro.	
	11.	When Hot Sump level reaches 40 inches, reset FCV-221 set point to 20 inches.	
	12.	Close FCY-231 (CLS.231 ON, then off).	
		NOTE (CONTROL ROOM) When LT-221 reaches 30" open FCV-231 to allow hot salt to enter the hot sump. Operate as required to maintain level.	
	13.	Turn on the Hot Salt Pump.	

STEP

DESCRIPTION

VERIFICATION

NOTE

During the following activity of increasing salt temperature, verify the operation of FCY-432 so that deaerator pressure is held constant at 233 psi and all excess energy is being rejected by the cooling water circuit.

CAUTION

Monitor PT-382. If PT-382 pressure goes above 85 psig, close FCV-351.

14. Open FCV-351 then close FCV-341 in series using the following incremental steps to increase superheater inlet temperature (TE-382). The Operator shall monitor TE-382 to assure that TE-382 does not increase more than 100°F in any 6-minute period.

```
FCV-351 to 2% for 2 minutes
                                      TE-382 TEMP
        to 3%
                . 11
         to 4%
   Ħ
         to 5%
                                     Hot Salt Temp
         to 6%
                н
                          H
                                  (Acurex Ch 126/127)
         to 7%
                п
         to 8%
                 11
   11
         to 9%
                             ; maintains 10% position
         to 10%
FCV-341 to 80% for 1 minute
         to 60%
                          u
   11
         to 40%
   Ħ
         to 20%
   11
         to 10%
         to 05%
   11
         to 2.5% "
   IJ
         to 1.0% "
         to 0%
                            : maintain closed
```

- 15. Close FCV-321 to 50% by setting SP.321, wait 5 sec. then set SP.321 to 10%. Wait 5 sec., then set SP.351 to 50%. Wait 5 sec., then set SP.351 to 100%.
- 16. Set the TSS, SGS, and HRFS operational alarms and wait 30 seconds.

PT-431	LT-221
PT-432	LT-281
	LT-291
TE-483	LT-471

SOP #2 SGS START-UP (EMCON)

STE	DESCRIPTION	VERIFICATION
17.	Set SP.321 to 20%, wait 20 seconds.	•
18.	Set SP.321 to 30%, wait 20 seconds.	····
19.	Set SP.321 to 40%, wait 20 seconds.	· · · · · · · · · · · · · · · · · · ·
	NOTE	
	The SGS.ON auto ramp sequence stops here	
20.	Verify/Turn off SGS.ON if it was used.	
	THE SGS IS NOW ON-LINE IN SALT FLOW CONTROL (FCV-321 manually controlling SGS salt flow and FCV-431 auto controlling HRFS steam pressure via PT-431 SP normally 1080 psi.)	
21.	Advise the SGS technician that drum blowdown may now be performed if required. (As determined by his SGS pretest checklist water chemistry analysis.)	
	NOTE	
	The Turbine/Generator will be brought on line at this point in later testing(POP#2). To simulate the Turbine loading, complete the transfer from HRFS pressure control to SGS pressure control (steps 22 & 23) and manually position FCV-431 to change the steam dump to the deaerator.	
22.	Set MAN.321 to OFF to activate SGS Steam Press. control. (FCV-321 auto controlling steam pressure at SP.SP 1100 psi.	
23.	Deactivate the FCV-431 HRFS Steam Pressure Control and manually position valve to establish minimum steam flow (approx. 3 Klb/Hr.) and simulate steam loading.	
	THE SCS IS NOW ON LINE IN AUTOMATIC ROLLER FOLLOWING MODE.	

REFERENCE INFORMATION

	<u>S</u>	team Load I	FCV-431-% Open	FCV-321-%
	30%	3.45K1b/Hr	55%	
	60%	7 K1b/Hr	7 4%	
FW	Temp	400°F 100% 9.8K1b/	lr 85%	102%

This Steam Generation operating procedure shall be performed by the Emcon operator. Periodically advise the SGS technician of status.

STEP DESCRIPTION

VERIFICATION

- 1. When steam demand has dropped to less than 3500 lbs/hr, switchover from SGS pressure control to flow control:
 - a) Set SP.321 value to the same value as shown on ZT321, or 50%.
 - b) Activate the FCV-431 HRFS Steam Pressure Control (using PT-431) with a set point of 1080 psig. Turn off GSTAT, Reset FCV-432 SP to 233 psi.
 - c. Deactivate the SGS Steam Pressure Control by turning MAN.321 ON.
- 2. Close FCV-351 to 10% and open FCV-321 to 100% in the following steps. Set SP.351 to 50% wait 5 seconds, then set SP.351 to 10%. After 5 seconds, set SP.321 to 50%, wait 5 seconds then set SP.321 to 100%.

NOTE

The SGS.OFF auto ramp may be used to complete step 3.

MAN AUTO

3. Open FCV-341 then close FCV-351 in series using the following incremental steps to decrease superheater inlet temperature (TE-382). The operator shall monitor TE-382 to assure that it does not decrease more than 100F° in any six minute period. Record start time.

Time

```
SP.341 to 10% for 1 minute
       to 20%
       to 30%
 Ħ
                                               TE-382
       to 40%
       to 50%
       to 60%
       to 70%
 Ħ
       to 80%
 11
                11
       to 90%
       to 100%
                        "; maintain open
```

	STEP	DESCRIPTION	VERIFICATION
	3.	Hot salt ramp down (cont'd).	
		SP.351 to 6% for 1 minute " " to 4% " 3 " " to 2% " " " " to 1.5% " " " " to 1% " " " " to 0.5% " " " " to 0% " " "; maintain closed	
		Verify/Turn off SGS.OFF if it was used. (USEDNOT USED)	
04	4.	Turn off the Hot Salt Pump. N90 will hold FCY-351 closed if the Hot Salt Pump is not running.	
	5.	Deactivate automatic control and close FCV-221. Verify closed.	
	6.	Close FCV-231. If sump level (LT-221) shows indication of leakage (slow rise), manually lock FCV-231 closed.	
13	7.	Deactivate the FCV-331 Steam Delivery Temperature Controby setting SP.331 to 10% and turning MAN.331 to ON.	1
	8.	Set FCV-384 to ON (Open) and verify the position on the micros.	
	9.	Set FCV-383 to OFF (Close) and verify the position on the micros.	
	10.	Verify MAN.EHAC ON, EHAC OFF and then back ON (pulse signal). TE-383 must be below 500°F.	

THE SGS IS NOW IN WARM STANDBY

NOTE

To maintain the Warm Standby condition accomplish the following:

- a) Verify salt system temperatures (COP #1 Tables A & B) are 480°F minimum.
- b) To maintain water/steam pressure at 1100 psig, reduce salt flow thru FCV-341 to lowest compatible with stable flow (still maintaining PT-383 at 1100 psig).

Extended Warm Stdby

SOP #3 SGS SHUTDOWN (EMCON)

•	STEP	DESCRIPTION	VERIFICATION
13	11.	Deactivate the FCY-301 Evaporator Salt Inlet Temperature Control by setting SP.301 at 0% and turning MAN.301 ON.	
15 18	12.	Deactivate the following Alarms:	
10		TE-301 LT-221 PT-383 TE-383 LT-281 PT-432 TE-384 LT-291 PT-483 TE-483 LT-311 LT-471	
04	13.	Turn off the boost pump and cold salt pump. Verify FCV-341 closed. N-90 will hold FCV-341 and FCY-301 closed if the Cold Salt Pump is not running.	
13	14.	Place/verify the following setpoints: SP.301 0% SP.341 0% SP.351 0%	
04	15.	Deactivate automatic control and close FCV-201.	
	16.	Close FCV-211. If sump level shows indication of leakage (slow rise), manually lock FCV-211 closed.	
	17.	Turn MAN.SDC and SDC ON. This MUST be accomplished to allow opening of the Salt Valves for drainage.	
	18.	Record sump levels and time prior to SGS drainback.	
		LT-201 Cold sump, LT-221 Hot sump	Time
13	19.	Open the Cold Salt and Salt Drain Valves by setting the following controls and verify correct valve position.	Time
		SP.301 100% SP.341 100% MAN.38182 On FCV-38182 On	
	20.	Wait 5 minutes from step 18 to allow drainage of salt to the Cold Sump prior to proceeding to step 21. Cold sump level should increase 6 to 10" during drainback.	

	STEP	DESCRIPTION	<u>VERIFICATION</u>
	21.	Open the Hot Salt Valve by setting SP.351 to100%. Verify the valve postion and expect a hot sump level change of approximately 16 inches.	
	22.	Verify FCV-491 is closed in auto with a SP of 980 psi.	
	23.	Fill the drum with Feedwater to a level of +15 inches by setting SP.411 to 20% and turning Man.411 ON. When the level has reached +15 inches, set SP.411 to 0%.	
		NOTE	
		HRFS is no longer needed to support SGS and may be shutdown now if not seperately required.	
13	24.	20 minutes after step 18, set the controls in the following postions and verify the correct valve position:	
		SP.341 0%	
		SP.301 0% SP.351 0%	
		FCV-38182 OFF	
	25.	Turn SDC and MAN.SDC OFF.	
		NOTE	
		If ambient temperature conditions either are or expected to be less than 32F°, assure that water side freeze protection circuits are operational and that no water/steam transmitter signals (particularly LT-311) are frozen prior to leaving the system unattended. If there is any indication that LT-311 may not provide a valid signal during unattended diurnal shutdown, due to freezing or any other reason, the circulation heater should be de-energized.	
02	26.	If FCV-151, FCV-161, and FCV-162 have not been manually locked closed during the SGS salt flow activity, an acumulation of salt will leak by and stagnate. Open FCV-151, FCV-161, and FCV-162 and allow the salt to drain.	
	27.	Advise the SGS technician to complete the SGS posttest checklist (SOP #4) if no further SGS operation is planned, and the TSS posttest checklist (TOP #4) if no further TSS operation is on-going or planned.	
	27.	checklist (SOP #4) if no further SGS operation is planned, and the TSS posttest checklist (TOP #4)	

NOTE
This procedure will not detail the steps to take the SGS from Diurnal Shutdown to the Empty Condition because it is not a planned part of the SGS testing.
Refer to the SGS Manual Section 3.10 (Operating Procedures) for these detailed steps.

7-51

SOP #4 SGS POST TEST CHECKLIST

This Steam Generation operating procedure will be utilized to verify SGS integrity following all tests that use the SGS. It shall be performed by the SGS technician.

STEP DESCRIPTION

VERIFICATION

CAUTION

Salt and water/steam temperatures will normally be maintained above 500°F. If repairs are required, a shut down to the Empty condition may be required.

1. Close the following isolation valves:

HV-481 St. Deliv. HV-488 Feedwater HV-487 T-482 HV-491 T-481

- Inspect the salt system for evidence of leaks and insulation damage. This is a general inspection for any condition that appears abnormal. If a problem is detected, a more thorough inspection will be required.
 - o All SGS salt piping
 - o Valves
 - o Superheater and Evaporator
- Inspect the water/steam system for evidence of leaks and insulation damage. This is a general inspection for any condition that appears abnormal. If a problem is detected, a more thorough inspection will be required.
 - o SGS piping
- o Superheater
- o Valves, traps
- o Evaporator

o BWCP

- o Steam Drum
- o Flange connections
- o Attemperator
- o Drain Plugs
- o Drain & Blowdown Tank
- 4. Check for visual evidence of blown fuses, burned relays or burned electrical components in the power junction box and generally throughout the SGS/TSS.
- 5. Verify operation of the SGS skid coolant pump and radiator.
- 6. Secure the boiler water sample station (HV-386).
- 7. Turn off/verify the chemical feed pump and close HV-387.
- 8. Note any abnormalities encountered during test activities.
- 9. Advise the Control Room that the SGS post test has been completed and the SGS is secure.
- 10. Complete the TSS post test checklist (TOP #4) if no further TSS operation is planned.

SOP #5 SGS and Propane Heater Shutdown

This procedure will only be used for shutdown when the SGS and Propane Heater are in simultaneous operation. Due to the volume of salt that must be drained into the Cold Sump from the Propane Heater, salt will be bottled up in the SGS for approximately 20 minutes prior to drain. Perform steps 16 through 27 expeditiously.

	STEP	DESCRIPTION	VERIFICATION
	1.	Advise the TSS technician to adjust the Propane Heater stack temperature control to 600°F. Propane Heater salt outlet temperature (Acurex channel 142) will decrease over a period of time.	
13	2.	When steam demand has dropped to less than 3500 lbs/hr, switchover from SGS pressure control to flow control.	
		a) Set SP.321 value to the same value as shown on ZT321.	
		b) Activate the FCV 431 HRFS Steam Pressure Control (using PT-431) with a set point of 1100 psig.	
		c) Deactivate the Steam Pressure Control by turning MAN.321 on.	
	3.	Close FCV 351 to 10% and open FCV 321 to 100% in the following steps: Set SP.351 to 50%, wait 5 seconds; then set SP.351 to 10%; after 5 seconds, set SP.321 to 50%; wait 5 seconds, then set SP.321 to 100%.	
	4.	Open FCV 341; then close FCV 351 in series using the following incremental steps to decrease superheater inlet temperature (TE382). The operator will monitor TE382 to assure that TE382 does not decrease more than 100°F in any 6-minute period. Record start time.	
		SP.341 to 10% for 1 minute " " to 20% for " "	Time
		" " to 30% for " "	
		" " to 40% for " "	
		" " to 50% for " "	
		" " to 60% for 1 minute	
		" " to 70% for " "	
		" " to 80% for " " " " to 90% for " "	
		" " to 100% for " "; maintain full open	
		to took for a marriagin farr open	

	STE	<u>P</u> <u>DESCRIPTION</u>	VERIFICATION
		SP.351 to 6% for 1 minute " " to 4% for 3 minutes " " to 2% for 3 minutes " " to 1.5% for 3 minutes " " to 1% for 3 minutes " " to 0.5% for 3 minutes " " to 0.5% for 3 minutes " " to 0% for 3 minutes; maintain closed	
04	5.	Turn off the Hot Salt Pump. N90 will hold FCV351 closed if the Hot Salt Pump is not running.	
	6.	Deactivate hot sump level control and close FCV 221. Verify closed.	
	7.	Close FCV231. If sump level (LT-221) shows indication of leakage (slow rise), manually lock FCV231 closed.	
13	8.	Deactivate the FCV331 Steam Delivery Temperature Control by setting SP.331 to 10% and turning MAN.331 On.	
14	9.	Set FCY384 to ON (open) and verify the position on the micros.	
13	10.	Set FCV383 to OFF (closed) and verify the position on the micros.	
	11.	Verify MAN.EHAC ON. Turn EHAC off and then back on (pulse signal)	

SGS IS NOW IN WARM STANDBY

NOTE

To maintain the Warm Standby condition accomplish the following:

- a) Verify salt system temperatures (COP #1 Table A & B) are 480 F minimum.
- b) To maintain water/steam pressure at 1100 psig, reduce salt flow thru FCV341 to lowest compatible with stable flow (still maintaining PT-383 at 1100 psig).

Extended Warm Stdby

and verify PT-180 increases to greater

Incrementally open FCV 151 to 40%.

than 170 psig.

20.

SOP #5 SGS AND PROPANE HEATER SHUTDOWN		
STEP	DESCRIPTION	VERIFICATION
21.	If SGS is used to deplete cold sump, Open FCV-301 and FCV-341.	
22.	Turn off the Cold Salt Pump and Boost Pump when LT-201 reaches approx. 25".	
23.	Close FCV 151, if used.	
24.	Turn MAN.SDC and SDC ON. This MUST BE accomplished to allow opening of the Salt Valves for drainage.	
25.	Open the Salt and Salt Drain Valves by setting the following controls. Verify correct valve position.	
	MAN.301 On/SP.301 100% MAN.38182 On MAN.341 On/SP.341 100% FCV.38182 On	
	NOTE	
	Monitor LT201 Cold Sump level during salt drainage. The level should increase by approx 6 inches.	
26.	Open the Hot Salt Valve by setting SP.351 to 100%. Verify the valve position and expect a hot sump level change of approximately 16 inches. Do not exceed 40" on LT-221.	
27.	Verify FCY491 is closed in auto with a SP of 1050 psi.	
28.	Fill the drum with Feedwater to a level of +15 inches, set SP.411 to 20% and turning MAN.411 ON. When the level has reached +15 inches, set SP.411 to 0%.	
	STEP 21. 22. 23. 24. 25. 26.	21. If SGS is used to deplete cold sump, Open FCV-301 and FCV-341. 22. Turn off the Cold Salt Pump and Boost Pump when LT-201 reaches approx. 25". 23. Close FCV 151, if used. 24. Turn MAN.SDC and SDC ON. This MUST BE accomplished to allow opening of the Salt Valves for drainage. 25. Open the Salt and Salt Drain Valves by setting the following controls. Verify correct valve position. MAN.301 On/SP.301 100% MAN.38182 On MAN.341 On/SP.341 100% FCV.38182 On NOTE Monitor LT201 Cold Sump level during salt drainage. The level should increase by approx 6 inches. 26. Open the Hot Salt Valve by setting SP.351 to 100%. Verify the valve position and expect a hot sump level change of approximately 16 inches. Do not exceed 40" on LT-221. 27. Verify FCV491 is closed in auto with a SP of 1050 psi. 28. Fill the drum with Feedwater to a level of +15 inches, set SP.411 to 20% and turning MAN.411 ON. When the level has reached

NOTE

HRFS is no longer needed to support SGS and may be shutdown now if not seperately required.

	SUP #	5 SGS AND PROPANE HEATER SHUTDOWN	
	STE	P DESCRIPTION	VERIFICATION
	29.	Advise the TSS technician to complete TOP #3A Local Propane Heater Shutdown.	
13	30.	Close the following valves as follows:	
02 05		SP.341 0% FCV 151 Closed SP.301 0% FCV 162 Closed SP.351 0% FCV 241 Closed FCV.38182 OFF FCV 242 Closed	
	31.	Lock the following valves closed:	
		FCV 301 FCV 341 FCV 241 FCV 242	
	32.	Turn SDC and MAN.SDC OFF.	
		NOTE	
		If ambient temperature conditions either are or are expected to be less than 32 F, assure that water side freeze protection circuits are operational and that no water/steam transmitter signals (particularly LT-311) are frozen prior to leaving the system unattended. If there is any indication that LT-311 may not provide a valid signal during unattended dirnal shutdown, due to freezing or any other reason, the circ. heater should be deenergized.	·
02	33.	If FCV-151, FCV-161, & FCV-162 have not been manually locked closed during the SGS salt flow activity, an accumulation of salt will leak by and stagnate. Open FCV-151, 161, & 162 to allow the salt to drain.	
	34.	Advise the TSS/SGS technicians to complete the SGS and TSS posttest checklists (SOP #4 & TOP #4) if no further TSS/SGS operation planned.	
	~	NO TO HOW THE DELIGHBLE CHUTDOWN WITH THE CALT CYCTEM DRAINER	1

SGS IS NOW IN DIURNAL SHUTDOWN WITH THE SALT SYSTEM DRAINED

NOTE

This procedure will not detail the steps to take the SGS from Diurnal Shutdown to the Empty Codition because it is not a planned part of the SGS testing. Refer to the SGS Manual Section 3.10 (Operating Procedures) for these detailed steps.

7.5 ELECTRIC POWER GENERATION OPERATING PROCEDURES

Te	st	Dat	e
6	/19	/84	

EPGS PRETEST CHECKLIST POP #1

6.

closed.

This electric Power generation operating procedure will be utilized

to verify EPGS integrity prior to all tests that use the EPGS. This checklist shall be completed by the EPGS technician. **VERIFICATION** DESCRIPTION **STEP** Be advised that these valve positions are NOTE 1. verified correct in HRFS check-lists: Main Steam Isolation (Open) HV-501 (As Rea'd) HV-577A & B FWP Cooling Water (Closed from EMCON) FCV-471 Condensate Return Inspect for evidence of water and oil leaks NOTE 2. or other abnormalities as you complete this checklist. (Verify none found in Setp 34). Condenser Platform - 60' Level These valves remain closed. 1. Check only if you suspect they have been opened. HV-593 Condenser inlet waterbox vent Condenser inlet waterbox drain HV-594 b. Condenser blind waterbox drain HV-597 c. Condenser blind waterbox vent HV-598 d. 2. Verify these valves are open: HV-584 Hotwell outlet/CNP suction HV-581 CNP discharge b. CNP discharge orifice recirculation HV-582 c. Condenser vacuum exhaust isolation HV-583 d. Turbine steam seal exhaust isolation HV-586 Record hotwell level from sight glass LI-581, 3. Lv1. leave isolation HV-595 & 596 open. 60' Level В. 4. Verify these valves are open: AEP seperator tank make-up HV-578 a. AEP cooler cooling water supply HV-588A b. AEP cooler cooling water return HV-588B Verify AEP separator tank level is between 4 & 6" 5. at sight glass LI-583 (auto LV-581 M-U)

Verify CNP and AEP local disconnect switches are

STEP	DESCRIP	TION	VERIFICATION
c.	<u>Control</u>	Area - 80' Level	
	7.	Verify EPGS UPS has 2 Green lights on.	
-	8.	Turn on exciter cabinets vent fans with switch on side of VRP. Verify vent fan operation at VRP, rectifier cabinet, resistor cabinet, and at isolation transformer enclosure (L4 Bkr. 12).	
	9.	Verify generator breaker is racked in, charged, and open.	
	10.	Verify electrical power is (always) on:	
		 a. TCP - Timer display on (L4 bkr 9) b. GCP - Generator Breaker green light on (L4 c. Generator heater - Local starter on/TCP sw d. Oil heater - Local starter on/TCP sw in Aut 	in Auto
	11.	Close TCP sw.'s for FCV-501, 511, 512, 541, & 551	
	12.	Determine where the EPGS will be operated from - 'local' at T-G or 'remote' at Emcon Console. Reposition mode select switch, if required, in the next step.	ocal Remote
	13.	Determine if CTP is operating for HRFS/FWP (TCP red light) a. CTP off - Position TCP mode select switch in the control mode determined in Step 12.	ocal Remote
		b. CTP on - Verify TCP mode select sitch is positioned in agreement with Step 12. Correct switch position, if necessary, only with Emcon operator permission (to avoid FWP trip).	,
	14.	Turn on all local starters except Exciter disc., 8 total, and verify 5 TCP indicating lights on.	CTP on
	15.	Verify compressed air is available and controls functional by stroking FCV-521 from oper. mode cont'l location. Verify local air venting or valve motion and Emcon ZT-521 operation. Close FCV-521 and confirm after function check.	
	16.	Assure turbine oil temperature is above 60°F. Conduct POP #1A Part A - Turbine oil temp. ck., if necessary, to determine oil temperature and/or warm oil.	

STEP	DESCRIPTION		VERIFICATION
D.	T-G Plat		
	17.	Verify HV-592 steam line drain valve is closed.	
	18.	Verify these valves are open:	
		a. HV-575 Steam line trap b. HV-576 Steam seal (1/4 turn open) c. HV-587 Generator cooling water supply d. HV-521 Lube oil cooler oil diverting (open to cool.)	
		e. HV-574 Throttle Valve trap	
	19.	Verify OST mechanism is reset.	
	20.	Verify Throttle Valve is reset closed by inspection no un-threaded rod showing on cylinder screw.	on –
	21.	Verify FCV-501 is closed by inspection.	
	22.	Verify EOP local disconnect switch is closed.	
	23.	Verify turbine oil reservoir level is 2 1/2", + 1/2", above normal operating level mark at dipstick LI-582; or if EOP is on for oil heating, verify dipstick LI-582 normal operating level is maintained.	
	24.	Verify excitor bearing oil reservoir is full by removing wing-nut reservoir plug & inspecting.	
	25.	Verify duplex oil strainers are operational. Alternate strainer selection weekly.	
E.	Tank Are	<u>ea</u> - 80' Level	
	26.	Verify CTP local disconnect switch is closed.	
	27.	These valves remain closed. Check only if you suspect they have been opened.	
		a. HV-580 CNST drain b. HV-590 CTDT make-up c. HV-591 CTDT drain d. HV-599 CNST make-up isolation	
	28.	Open these valves:	
		a. HV-579 Hotwell make-up b. HV-585 Hotwell dump c. HV-589 CTP suction	

STEP	DESCRIP	VERIFICATION	
	29.	Verify CTDT is full by overflow when M-U water is added thru HV-590; or if CTP is on for HRFS/FWP, verify CTDT maintains normal operating level of 18 between 16 and 20" at sight glass LI-585.	3 ^{II}
	30.	Assure hotwell water quality is acceptable. Conduct (HRFS) water chemistry analysis as necessary to insure iron is less than 500 ppb. Record, if measured. Drain and refill hotwell if required to correct, Ref. POP #1A Parts B & C.	ppb. Iron
	31.	 Verify hotwell and CNST levels are correct. Conduct POP #1A Parts B & C, Hotwell and CNST level adjustment, if necessary, to correct. 	epas an an
		a. Hotwell level 12" (betw. 9 & 14") at condens sight glass LI-581, initially recorded in Step 3.	er
		 b. CNST level between 12 & 30" at tank sight glass LI-584. 	
		c. Verify agreement between TCP meter LT-511 and LI-581 sight glass hotwell level.	
F.	CMUP Ro	om - 80' Level	
	32.	Verify FCV-471 is closed by inspection.	
	33.	Open HV-406 condensate return to HRFS.	
	34.	Verify no water or oil leaks or other abnormalities found.	
	35.	Advise control room that EPGS Pre-test checklist has been completed. (Turbine oil temperature & hotwell are okay).	

"EPGS PRE-TEST CHECKLIST COMPLETE"

Test Date

Disable OH.ON

POP #1A EPGS FLUID ADJUSTMENT

	STEP	DESCRIPTION	VERIFICATION			
В.	Hotwell Level Adjust, as Required					
	1.	Complete pretest checklist (Steps 1 - 30)				
	2.	Transfer record of hotwell level here from POP #1 EPGS Pretest checklist Step 3.	Lv1. "			
	3.	Verify remote Emcon EN.HLC auto hotwell level control is off.				
	4.	Make up Hotwell if less than 9"				
		 a. Attempt to determine cause of level loss (leaky pipes, improperly opened valves, shutdown). Correct as required. b. From TCP control location selected, open make-up FCV-512. c. Fill till hotwell level sight glass LI-581 is 12". d. If CNST did not have enough water to complete fill, close FCV-512, conduct CNST make-up (POP #1A Part C), then resume fill. e. Close FCV-512. 				
	5.	 Dump Hotwell if above 14". a. Attempt to determine cause of level increase (improperly opened valves). Correct as required. b. Start CNP. c. Open FCV-511. d. Dump till hotwell level sight glass LT-581 is 12" e. Close FCV-511. f. Stop CNP. 				
	6.	Alternate dump if above 14" or to correct water quality (wastes condensate). Open CNP inlet strainer S-581 HV till LI-581 is 12", or if draining, Zero".				
	7.	Verify agreement between LT-511 TCP meter and LI-581 sight glass hotwell level. Record level as left.	Lv1.			

VERIFICATION

- C. CNST Level Adjustment, as Required
 - 1. Verify CNST level is between 12 and 30" at sight glass LI-584.
 - 2. Dump if above 30" by draining through HV-580 into floor drain. The preferred dump is into the hotwell (POP #1A Part B, Step 4), but it is assumed here that the hotwell level is already properly adjusted.
 - 3. Fill if lower than 12".

NOTE

This fill procedure will deplete the CMUP stand pipe. If CMUP is operating, do not allow this to happen by reducing the stand pipe air overpressure, either by relief valve manual blow-off or regulator adjustment.

- a. Verify HRFS/Cycle Fill Pump is on.
- b. Open CNST M-U FCV-541 with TCP switch.
- c. Open M-U HV-599.
- d. When filled, close HV-599 and FCV-541.
- e. Readjust CMŮP stand pipe level.

NOTE

Hydrazine can be added to the CNST as determined from a Water Quality Analysis by filling a beaker at the HRFS Hydrazine Feed Tank drain and pouring it into the CNST LS-541 flange opening.

POP	#2A	LOCAL EPGS START-UP	Test Date 10/04/84
	STEP	DESCRIPTION DESCRIPTION PUMP S/U Verify:	VERIFICATION
Α.	EPGS	PUMP S/U	
	1.	Verify:	
		 Synch sw. handle has been procured as required. POP #1 EPGS Pretest Checklist is complete. EPGS control is in local (Do not disrupt CNP oper.)).
	2.	Start CTP, if not already on. Verify on.	
	3.	Start CTF if ambient temp. is above freezing. Verify.	
	4.	Confirm LT-511 hotwell level is 12" (or between 9 & 14")	
	5.	Open FCV-551 for CNP recirculation.	
	6.	Start CNP. Verify on, LT-511 hotwell level will drop 1". Note EPS will lock this out upon prior SGS BCP shutdown. Advise the Emcon operator to reset EPS 3 and 2 to clear.	
	7.	Start AEP. Verify on, PT-502 condenser pressure should decrease to less than 15" Hg.	
	8.	Confirm oil cooling FCV-521 closed (Emcon ZT-521).	
	9.	Place EOP select. sw. in auto. Start EOP. Verify on. PT-501 oil bearing pressure should increase above 8 psi.	
1	10.	Wait 1 minute, then verify TT-521 oil temperature is above 60°F.	
1	11.	Reset Emerg. trip ETR (FCV-561) and verify PT-531 Hydraulic oil pressure is above 50 psig.	

'EPGS PUMPS ON'

	STEP	DESCRIPTION	VERIFICATION
В.	T-G S	ET-UP	
	1.	Verify from Emcon operator that condenser cooling water temp. TE-486 is below 100°F.	
	2.	Verify SGS steam production from Emcon operator.	-
		a. PT-431 Steam pressure above 1000 psib. TE-483 Steam temperature above 600°F and rising	
	3.	Verify from Emcon operator that SGS is in manual salt flow control (5 klb/hr min. steam flow) and FCV-431 is controlling steam pressure.	
•	4.	Advise the Emcon operator to transfer primary D/D level control from CMUP to CNP by activating FCV-471 with a SP of 15" and resetting the SP of FY-472 to 14".	
	5.	Close CNP recirc. FCY-551.	
	6.	Verify EPGS turbine start-up readiness	
		a. (sight windows) FI-501 & 502 brg. oil flow b. TT-521 oil temperature above 60°F c. PT-501 brg. oil press above 8 psig d. PT-502 condenser vacuum below 15" Hg. e. LT-511 hotwell level at 12" (betw 9 & 14") f. PT-531 hydraulic oil press above 50 psig	
	7.	Drain steam pipe condensate by opening HV-592A & B until dry steam emerges. Reclose. Open Traps.	
	8.	Verify TT-583 turb. steam temp. is above 550°F.	
	9.	Open FCV-501 to allow steam up to throttle valve.	
1	0.	Verify PT-581 turb. steam press. increases above 850 PSI.	
1	1.	Record time of day and wait 2 min. to warm pipe before starting turbine.	71
1	2.	Establish LT-511 12" hotwell lvl. control betw. 9 & 14"	Time
		1. Continuously monitor LT-511 hotwell lvl.	
		 Dump if LT-511 above 14" by opening FCV-511 until level drops to 12". 	
		 Make-up if LT-511 below 9" by opening FCV-512 until level rises to 11". 	(Continuous)
1	3.	Establish FCV-521 120°F cool. oil temp. cont'l.	
		1. Continuously monitor TT-521 oil temp.	
		 Adjust FCV-521 position to maintain TT-521 oil temp. at 120°F (betw. 110-130°) 	(Continuous)

VERIFICATION

WARNING

Clear non-involved personnel away from the T-G for safety.

CAUTION

Trip Turbine if operation abnormal with ET - Emerg. Trip

NOTES

- 1. Maintain coordination between T-G and Steam operations.
- 2. Verify proper turbine operation as follows:
 - a. Field monitor
 - 1. Turbine rolling
 - 2. No abnormal rubbing or noise (rod ck)
 - 3. No unusually excessive vibration (5 G Trip)
 - 4. FI-501 & 502 bearing oil flowing (sight windows)

b. Instruments

- 1. ST-582 generator speed below 1250 rpm
- 2. AZT-581 turbine vibration not abnormal (Emcon VIB.OVR override available)
- 3. TT-501, 502, 507 (also TE-503, 505, 506 at Emcon). Bearing oil temp.'s equalize within 20° of each other, within 50° of TT-521, and betw. 60 170°F limits.
- 4. PT-502 cond'r vacuum below 15" Hg.
- 5. PT-582 steam seal press. above PSI.
- 6. TT-583 steam temperature above 700°F
- 7. PT-581 steam pressure above 850 PSI

c. Controls

- 1. LT-511 hotwell level between 9 & 14"
- 2. TT-521 cooling oil temp. between 60 & 130°F.
- 3. EOP controlling hydraulic oil press. at 120 psi. (On at 10 pressures, Off when shaft pump operating).
- 3. Verify ET/OST Turbine trips as follows:
 - a. PT-531 hydraulic oil press drops to '0' PSI
 - b. ST-582 generator speed decreasing
 - c. Turbine physically slowing down
 - d. FCV-501 closed (ZSL-501 on)
- 4. Conduct the following 3 test trips to verify their functional operation & preheat the Turbine.

VERIFICATION

C. T-G START-UP

- 1. Start the 1st Turbine roll to half speed, after 2 minute pipe warming, by opening throttle valve to 25% with motor. Continue opening throttle valve manually untill roll starts, then close slightly to roll-out very slowly and smoothly. Progressively and very slowly increase speed to 600 RPM. Verify proper Turbine operation (Note 2).
- Conduct test trip 1 Lo speed MOST (Man. Overspeed Trip):
 - a. Hit OST trip button on turbine
 - b. Verify turbine tripped (Note 3)
 - c. Reset OST mechanism
 - d. Reset throttle valve closed TVM.CLS, ZT-581 0% open
 - e. Reset EPS2.RST
 - f. Verify trip reset by PT-531 hydraulic oil pressure above 50 psi
- 3. Restart Turbine a 2nd time to half speed, if trip functioned properly and before turbine stops, by reopening FCY-501 and throttle valve until generator again slowly reaches 600 RPM. Reverify proper Turbine operation (Note 2).
- 4 Conduct test trip 2 Lo speed ET (Emerg. Trip):
 - a. Actuate ET Emerg. Trip
 - b. Verify Turbine tripped (Note 3)
 - c. Reset ETR FCV-561 (ET off)
 - d. Reset throttle valve closed TVM.CLS, ZT-581 0% open
 - e. Reset EPS2.RST
 - e. Verify trip reset by PT-531 hydraulic oil pressure above 50 psi
- 5. Restart Turbine a 3rd time to full speed, if trip functioned properly and before turbine stops, by reopening FCV-501 and throttle valve until generator slowly reaches 1200 RPM. Locally guarantee ST-582 gen. speed does not exceed 1200 rpm and that govern. control holds it at 1200 rpm. Reverify proper turb. operation (Note 2). Do not prolong full speed operation unless TT-521 above 100°F
- 6. Conduct test trip 3 Full speed trip.
 On alternate day start-ups, repeat either the MOST, the ET, or the EPS T-G trip (Control Room PB).

MOST ET PB

7. Restart Turbine a 4th time to full speed by reopening FCV-501 and throttle valve 100%. Locally guarantee ST-582 gen. speed holds at 1200 rpm.

VERIFICATION

8. Reverify proper turbine operation (Note 2).
Continue manually controlling LT-511 and FCY-521.
Confirm CTF is on and EOP is off.

CAUTION

Do not continue full speed oper. unless TT-521 oil temperature quickly increases above 110°F (within 5 minutes)

- 9. Locally turn on Exciter Disc. Sw. to start Generator voltage build-up.
- 10. Verify generator no-load operation:
 - a. 460V at GCP meter or Emcon ET-581
 - b. 'O'A at GCP meter or Emcon IT-581
 - c. Generator air temperature below 120°F (Emcon TE-508)
 - d. Emcon gen. stator temp.'s equalize within 5°F below 180°F. (Emcon TT-510 thru 515)

CAUTION

Synchronize the generator ASAP after achieving turbine full speed and generator voltage to minimize high turbine exhaust temperatures. TI-581 or TE-581 should be kept below 150°F.

NOTE

During the turbine heat soak, SGS salt flow can be reduced to the minimum required to maintain 1100 psi steam (controlled by HRFS FCV-431) to conserve hot salt.

VERIFICATION

D. GENERATOR SYNCHRONIZING / LOCAL OR EMCON

1. Verify that T-G operation is established and then continue to complete this synch. procedure ASAP. A control transfer from local to Emcon may be done at this point.

Local Emcon

Time

NOTE

Synchronizing control location coincides with turbine control location (i.e., Local - GCP or Remote - RGP) as determined by TCPMS.

- 2. Advise the steam operator to prepare for Gen. Sync. by increasing SGS salt flow to 10 klbs/hr, (FCV-321 in flow control), and insuring that HRFS FCV-431 is in steam press. control. Verify that he has done so before proceeding.
- 3. Verify gen. speed above 1150 rpm and adjust to rated speed of 1200 rpm and freq. of 60 HZ with the governor control sw.
- 4. Adjust the generator sync voltage using the voltage control switch until the running volts equals incoming volts at approximately 120 v. + 2 V.
- 5. Install the sync sw handle and place the sync sw in the ON position. Verify sync LT's and synchroscope operation.
- 6. Adjust the generator speed with the governor control switch until the pointer on the synchroscope slowly rotates in a clockwise (fast) direct.

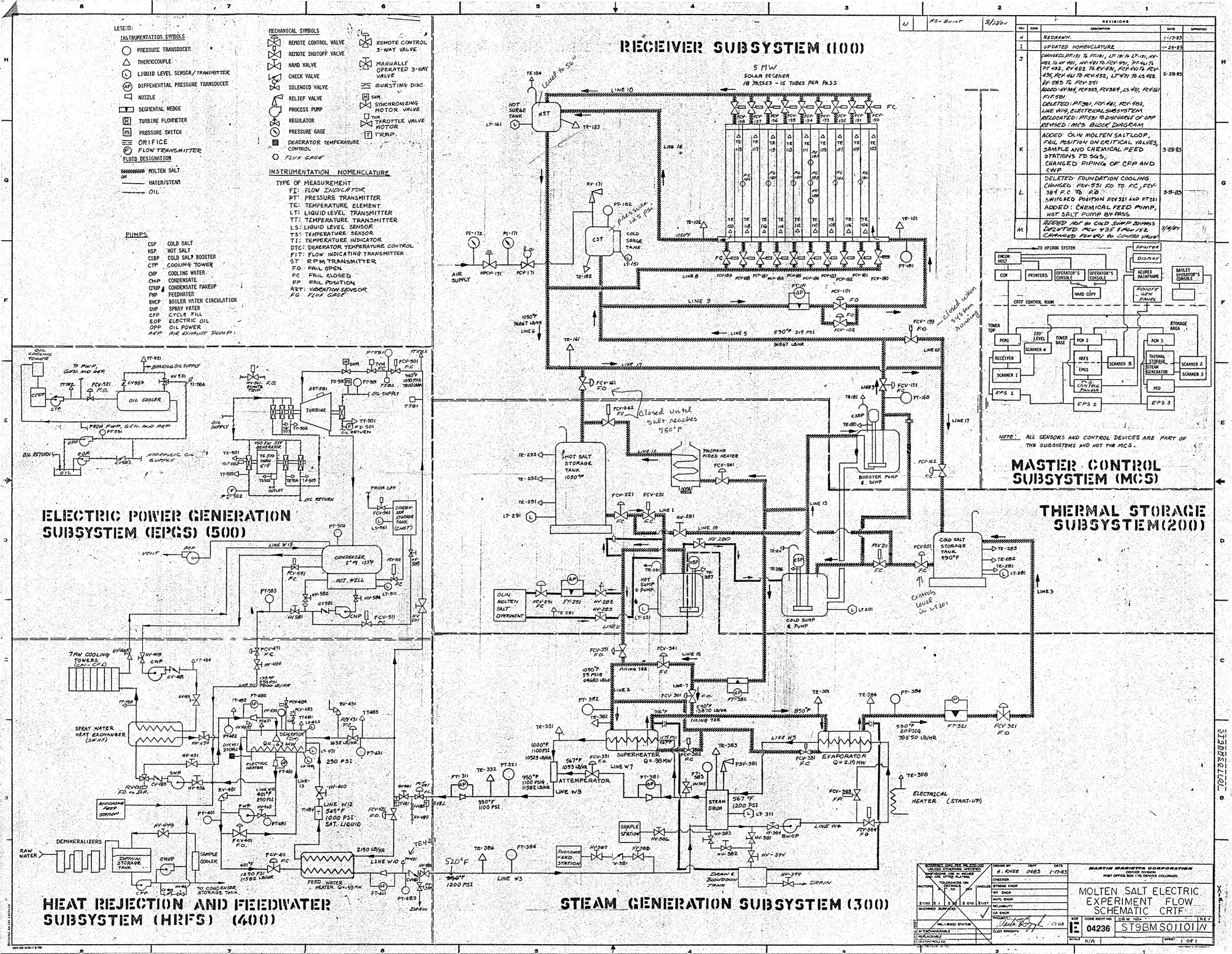
CAUTION

The generator must be in sync prior to closing the generator circuit breaker.

- 7. When the pointer is just before 12 o'clock with the sync lights out, close the generator circuit breaker.
- 8. Verify the generator C/B closes by red light on.
- 9. Partially load the generator to about 25 KW by raising the turb. gov. setting with the governor control switch.
- 10. Adjust the power factor between 1 and .8 lag with the voltage control switch (5 10 KVARS at VT-581).
- 11. Turn off the sync switch, record time and heat soak the Turbine for 15 minutes at this load. A control transfer from local to Emcon may be done at this point.
- 12. Start conducting T-G hourly checks.

CAUTION

On-line generator breaker trips automatically initiate a turbine trip by FCV-501 closure.



POP # ZA EPGS HOURLY OPERATING CHECK-LIST UPDATED 6/20/84

Verify all Parameters 1/2 Hourly or Hourly as shown.

Record Values for Parameters indicated R.

Primarily Monitor Guage Values,

Compare & Confirm TCP & Encon values

	Comp	pare y Co	patirm T	CP 4 EMCC	M ANINCZ				/^`.			/^ <i>/</i>
AREA	PARAMETER	LOCAL	TCP/EMC	EMCON	VALUE	<u> v</u>		ZHR	3	4	5	6
CONDIR	COND'R	PI-584	PT-50Z		∠ 15" Hg.	R						
	COND'R (STEAM) TEMP.	TI-581				R						
	HOTWELL (CONDENSATE) TEMP.	TI-582	1		100-150°F	R					in the state of th	
	HOTWELL LVL.	LI-581	LT-511		9-14"		Ž.		ĺ		Page (1)	
	COND'R IN	TI-584			< 120°F	R	h -					
	GLYCOL OUT	i .	<u>.</u>		< 120°F	R	! " - !	, ,				
	c.w.	PI-586			16 PSI	R			:		l	
60' LVL	AEP SEP. TK LVL.	L1-583	1		4-6"			The state of the s			A providing the second	
	AEP C.W. TEMP	TI-590	i		< 120°F	R						
	CNP SUCT.	PI-585				R			i		**************************************	
	Hosid			PT-583		R					1	
ZANKS	CNST LVL.	LI-584	;		12-30"				4.00			
	CTOT LVL	LI-585			16-20"	1						-
	SUCT	PI-588			1" Hg. Vac.	,				-		:
	CTP DISCH	PI-587			30-35 PU	R	-	; ;				
	C.W.			TE-SBZ	,	R			ess Avent Polyso 1 1	The contract of		

AREA	PARAMETER	LOCAL	TCP/EMC	EMCON	VALUE	v		2	3	4	5	6
TURB	OJL LVL	DIPSTICK LI-582			oper. LVL Mark							
	OIL	FI-501		,	FLOW							
	FLOW	FI-502	,		FLOW				1			ļ
	OIL BRG.	PI-581	PT-501		>6 PSI							
	PRESS HYD.	PI-582	PT-531	1	>50 PSI							
			TT-501		110-170°F	R						
	BRG		TT-50Z		110-1704	R						
	OIL			TE-503	110-1707	R						
	TEMP.			TE-505	110-170°F	R						
				TE-506	110-170°F	R		i j				
			TT-507		110-170°F	R						
	COOLER DIL TEMP.	TI-586	T-521		80- 130°F	R					on the state of th	
•		TI-588			<120°F	R		**!				
	TEMP OUT	TI-587			∠ 120°F	R				1		
	MAIN		PT-581		85019	R						
	ST.		TT-583	<u> </u>	750°F	R						
	ET. CEAL	PI-583		4		R		appendig to the control of the contr				
		,	PT-582			R				<u> </u>		
GEN	AIR TEMP	TI-580		TE-508	< 100°F < 40°C	R		1		:		
	C.W. TEMP	TI-589	ı		< 120°F	R				•	,	
					L 260	R			;			
				• •	∠ 260°F	R				,		
	STATOR				4260°F	R				:		
	TEMP			† · · · · · · · · · · · · · · · · · · ·	2260°F	R				;		
			<u>_</u>		7 500 E	R						
					1260° F	R						
GEN	WATTS		JT-581		∠750 kW			-	1			
ELECT.	VARS		VT-581		< 100 KVAR		##= U5	·	ļ			
X	VOLT		ET-581		460V					9		
	CURRENT		IT-581		C IZOO A				 			
	POWER FACTOR		PFT-58)	 	1 To .8 Lag							
	FREQ.		ST-581		60 Hz			<u> </u>	1	1	!	

A Instr's Listed are at GCP/EMC. 8

POP	#2	EPGS OPERATION			Test Date 10/04/84
<u>s</u>	TEP	DESCRIPTION			VERIFICATION
A.	<u>L0</u>	CAL START-UP COORI	DINATION		
	Com	plete these items	at the request of	the local EPGS operator.	
	1.	Momentarily enabl	le EPS3.RST and EPS	RST if required.	
	2.	Verify Condenser	C.W. temperature Ti	E-486 is below 100°F.	
	3.	Transfer primary by activating FCV the SP of FY-472	D/D level control in 4-471 with a SP of 1 to 14".	from CMUP to CNP 15" and resetting	
•	4.	Verify PT-431 abo	ove 1000 psi and TE-	-483 above 600°F.	
	5.			ow control (5 klb/hr ted and MAN.321 on.	
В.	EP	GS CONTROL TRANSFE	ER CHECKLIST		
	(TC	PMS 'OFF' to 'ON')	after T-G operation	ring EPGS control from Lo on is locally established rning itself off when com	(POP #2A).
	1.	Turn on FCY-501.			
	2.	Enable the auto.	hotwell level contr	ol EN.HLC.	
	3.	Verify that lube	ofl cooling FCV-521	is in auto S.P. 120°F.	
,	4.	Turn on the follo	owing enable and cor	trol signals:	
		(19)	(20)	(21)	
		CTP CTP.EN	CTF CTF.EN	CNP CNP.EN AEP AEP.EN EOP EOP.EN	
	5.	Enable EPGS opera	itional alarms PAL.		
			NOTE		
			fer may be complete j. Follow POP #2A g	d before or after uidelines to synch.	
	6.	Coordinate transf him switching TCF	er with EPGS techni key switch from lo	cian, accomplished by cal to remote.	

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*ELECTRIC POWER PRODUCTION"

Verify the local T-G hourly checklist is being completed.

Monitor the attached list of T-G operating parameters.

2.

Monitor these parameters intermittantly during T-G operation from Emcon:

GROUP	PARAMETER	DESCRIPTION	VALUE	PARTICULARLY
23	J T- 581 VT-581	KW generation KVAR generation	0 - 750 KW 10 - 20 KVAR	Watch for creep Adjust with load
22	TT-501 TT-502 TE-503 TE-505 TE-506 TT-507	Brg. oil temps	110 - 160 °F	Establish stability
23	TT-510 TT-511 TT-512 TT-513 TT-514 TT-515	Gen. stator temps	150 - 200 °F	Establish stability
22	PT-581 TT-583	Steam pressure Steam temp.	above 750 psi above 750 °F	Trip parameter Trip parameter
call-up	TT-509	Gen. air temp	below 110 °F	Trip parameter
2 2	PT-502	Condenser vacuum	below 15 "Hg.	Affects KW generation
22 21	LT-511 FCV-521	Hotwell level Oil temp. control	9 - 14 " 120 °F	Controls check Controls check
call-up	TE-581	Turb. exh. temp	130 -150 °F	Minimize overtemp.

YERIFICATION

A. T-G Manual Emerg. trip

NOTE

Initiate emerg shutdown only if necessary, but do not hesitate if emerg. conditions exist. Advise all operators of actions ASAP. If possible, try to reduce generator load before trip with governor control switch.

1. Open generator breaker with breaker CS
or Actuate ET
or Actuate EPS T-G trip button from control room.
(Operate all 3 for safety)

C.S. ET. EPSTGT

CAUTION

Stay clear of T-G/generator breaker for safety. Expect HRFS & SGS safety relief valves to open. SGS salt flow will stop and HRFS will attempt to desuperheat steam.

- Verify trip; turbine speed decreasing, gen. breaker open.
- 3. When safe and orderly, proceed with manual shutdown Step 6.

B. T-G Normal Shutdown

- 1. Establish communications with Emcon operator to coordinate generator load shedding with steam reduction operations.
- 2. Reduce generator load by lowering governor contol switch and voltage control switch. Do not reduce load faster than 75 kw/min. (Do not exceed an SGS steam flow reduction rate of 10%/min.)

NOTE

Opening the gen. bkr CS automatically initiates a turb. trip by FCY-501 closure.

- 3. Shutdown the T-G by opening the generator breaker with the breaker control switch as generator load is reduced to zero with the governor control switch.
- 4. Verify generator breaker open by green light on.

	POP #3	EPGS SHUTDOWN	
	STEP	DESCRIPTION	VERIFICATION
	5.	Yerify turbine trip by FCY-501 closure (Emcon ZSL501 on), turbine steam press PT-581 decrease to zero and generator speed ST-582 decreasing. Manually close FCY-501 control switches also.	
	8.		
	7.	Verify T-G speed ST-582 decreases to zero.	
	8.	Verify throttle valve reset closed by ZT-581 0% open.	
18	9 .	Emcon operator deactivate FCV-471 and change FY-472 SP to 15"	
	10.	Record time of day to allow 20 min. turbine/condensor vapor extraction before AEP shutdown (Step 16). As req'd, continue with shutdown up to that step.	Time
	11.	Emcon operator turn off GSTAT and deactivate alarms (PAL off). A control transfer may be done at this point.	
c.	EPGS S	' <u>T-G SHUTDOWN</u> '	
21	12.	Turn off EOP.	
	13.	Close cooling oil temp control FCV-521	
		a. TCP local control mode - Use FCV-521 dfal.	
		 TCP remote control mode - Emcon operator place FCV-521 in manual close. 	
22	14.	If operating remotely, Verify LT-511 hotwell level is between 9& 14", then disable EN.HLC.	
	15.	If operating locally, adjust LT-511 hotwell level to 12", then close TCP switches for FCV-501, 511, 512, 541, & 551.	
21	16.	Turn off CNP.	
	17.	Insure 20 min. have elapsed after T-G shutdown (Step 10) before proceeding.	
	18.	Turn off AEP.	
20	19.	Turn off CTF.	
19	20.	Turn off CTP, unless still required for HRFS/FWP.	
	21.	Complete the EPGS post test check-list.	As req'd

'EPGS SHUTDOWN'

This electric Power generation operating procedure will be utilized to verify EPGS integrity following all tests that use the EPGS. This checklist shall be completed by the EPGS technician.

STEP	DESCRIPTION	VERIFICATION
1.	If used, remove the GCP synchronizing switch handle and return it to the MSEE key box.	
2.	Turn off local starters. Do <u>not</u> turn off CTP if being used for HRFS/FWP.	
	a. CTF b. CTP c. AEP d. EOP e. CNP f. Exciter Disconnect g. Throttle Valve Disconnect	
3.	Verify oil heater and generator heater local starters are on, TCP switches are in auto, and Emcon 'OH.ON' is off.	
4.	Turn off Exciter cabinet vent fans.	
5.	Verify EPGS UPS has 2 green lights on.	
6.	Record, then Reset any trip functions.	
7.	Yerify throttle valve is reset closed by inspection. No unthreaded rod showing on cylinder screw.	
8.	Verify FCY-501 is closed by inspection.	
9.	Close these valves:	
	a. HV-579 Hotwell make-up Tanks at 80' Level b. HV-585 Hotwell dump Tank at 80' Level c. HV-406 Condensate to HRFS CMUP room at 80'	
10.	Drain hotwell through CNP S-581 HV if extended shutdown planned (longer than 1 week).	
11.	Verify no evidence of leaks or other abnormalities found.	
12.	Notify control room that the EPGS post-test has been completed.	

'EPGS SECURED"

Section 8

EMCON Graphics and Groups

This section contains reproductions of the EMCON graphic displays and the pre-defined groups in the 22 line format. This material is arranged as follows:

Graphic Displays

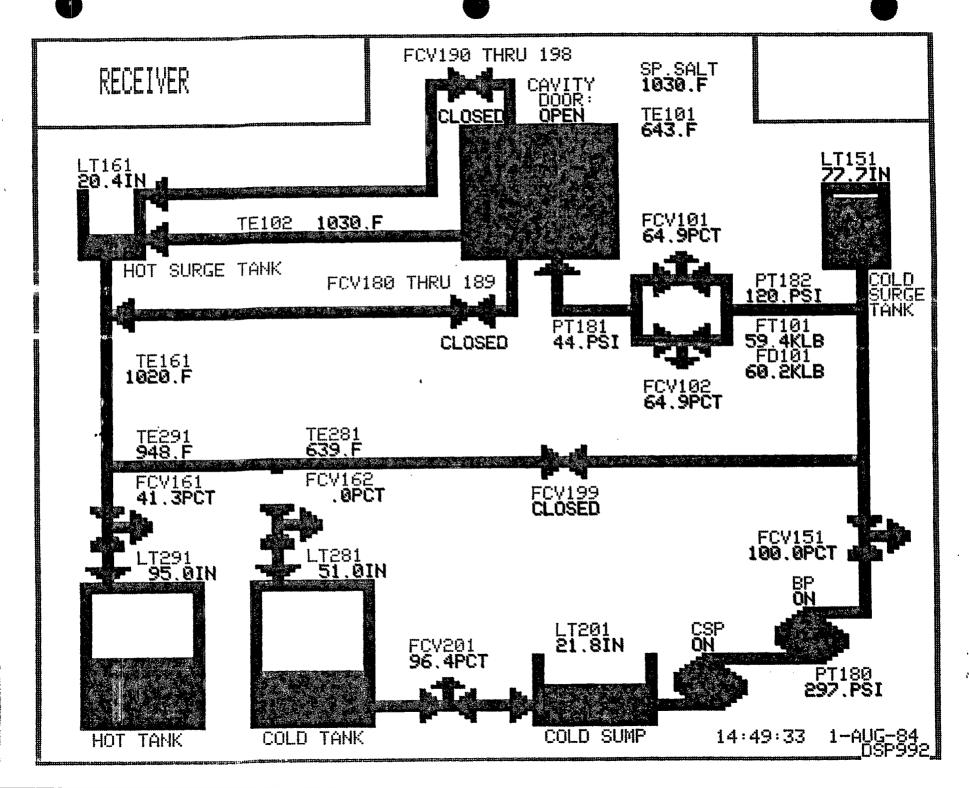
Graphic Name	<u>Page</u>
Receiver Panel Warm-up Temperatures	8-2
MSEE Overall	8-3
Receiver Subsystem	8-4
	8-5
	8-6
· · · · · · · · · · · · · · · · · · ·	8-7
Electric Power Generation Subsystem	8-8
	Receiver Panel Warm-up Temperatures MSEE Overall Receiver Subsystem Thermal Storage Subsystem Steam Generator Subsystem Heat Rejection and Feedwater Subsystem

Pre-defined Groups

Group <u>Number</u>	Group Name	Page
10	RS controls with drain and purge valves	8-9
02	RS and TSS controls	8-10
03	RS and TSS instrumentation	8-11
04	TSS pump house	8-12
05	TSS storage tanks for propane heater operations	8-13
06	RS back tube temp	8-14
07	RS header temp	8-15
08	RS drain micros	8-16
09	RS purge micros	8-17
10	RS pass temp	8-18
11	Critical instrument readings	8-19
12	RS fill and drain sequence	8-20
13	SGS operation	8-21
14	SGS operations	8-22
15	SGS instrumentation	8-23
16	SGS heater control	8-24
17	SGS valve micros	8-25
18	HRFS controls	8-26
19	HRFS pump controls	8-27
20	HRFS cooling fan controls	8-28
21	Turbine operations	8-29
22	Turbine operations	8-30
23	Generator operations	8-31
26	EPS trips	8-32
27	EPS trips	8-33
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	PECEIVER PANEL			848.F MII	N T: 486.F		
EAST							WEST
	TE136	TE135	TE134	TE133	TE132	TE131	
	850.F	696.F	675.F	5 59.F	566.F	498.F	
用	1E14c	TELHI	TE140	TE139	TE138	TE137	
	837.F	792.F	528.F	644.F	688.F	641.F	
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	TE148	TE147	TE146	TE145	TE144	TE143	
	600.F	819.F	613.F	649.F	730.F	487.F	_
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01 FCW 01 02 FCV102 03 FT101 04 FD101	. IPCT XXX RCVR . OKLB XXX RCVR . OKLB XXX FLOW	SALT FLOW CONTRL SALT FLOW DEMAND	H 100.0 L 20.0 PCM 1 H 100.0 L .0 PCM 1
05 RCA	.0KLB OFF RCVR	CONTRL ALGORM SALT TEMP SETPT BOOST PUMP DSCHGE INLET PRESS INLET HEADER	H 100.0 L .0 PCM 1
06 SP.SALT	750.F XXX RCVR		H 1060. L 700. PCM 1
07 PT180	0.PSI XXX RCVR		H 400. L 275. PCM 3
08 PT181	0.PSI XXX RCVR		H 125. L 10. PCM 1
09 TE101	632.F XXX RCVR		H 650. L 500. PCM 1
10 TE102	531.F XXX RCVR	OUTLET HEADER	H 1060. L 500. PCM 1
11 FCV180T89	0.0FF RCVR	DRAIN VALVES	PCM 1
12 FCV190	0.0FF PURGE	VALVE PANELS 01.02	PCM 1
13 FCV191	0.0FF PURGE	VALVE PANELS 03.04	PCM 1
14 FCV192	0.0FF PURGE	VALVE PANELS 05.06 VALVE PANELS 07.08 VALVE PANELS 09.10 VALVE PANELS 11.12 VALVE PANELS 13.14	PCM 1
15 FCV193	0.0FF PURGE		PCM 1
16 FCV194	0.0FF PURGE		PCM 1
17 FCV195	0.0FF PURGE		PCM 1
18 FCV196	0.0FF PURGE		PCM 1
19 FCV197 20 FCV198 21 LT151 22 LT161 COPY	0.0FF PURGE 0.0FF PURGE .0IN XXX RCVR 1.0IN XXX RCVR	VALVE PANELS 15.16 VALVE PANELS 17.18 COLD SURGE TANK HOT SURGE TANK	PCN 1 PCN 1 H 90.0 L 10.0 PCM 1 H 70.0 L 15.0 PCM 3 GROUP 01 S7-JUL-84 15:41:54

01 P/188 02 FCV101 03 FCV102 04 FCV161 05 FCV162 07 FCV179 10 ZSH199 11 ZSH199 12 CLS 211 13 CLS 211 14 ZSH211 15 ZSH211	98.4PCT XXX RCVR 98.6PCT XXX RCVR 1.4IN XXX RCVR 1.4IN XXX RCVR 1.4IN XXX RCVR 26.4IN XXX RCVR 0.0FF RCVR 0.0FF RCVR 0.0FF XXX RCVR	SALT FLOW CONSTRUCT FLOW COLD SURGE TO DWNCMR COLD TO DWNCMR COLD TO DRAIN FILL IN COLD SUMP IN	ONTRL H 100.0 ONTRL H 100.0 ONTRL H 100.0 ONTRL H 100.0 ONTRL H 70.0 ONTRL H 100.0 ONT	PCN 3-133333333333333333333333333333333333
16 DR OPN 17 DR CLS 18 ZSHDR 19 ZSLDR 20 LT281 21 LT291 22 PS281 COPY	0.0FF RCVR 0.0FF XXX RCVR 1.0N XXX RCVR 124.9IN TSS .9IN LOA TSS 1.0N TSS	CAVITY DOOR CL CAVITY DOOR CL CAVITY DOOR CL COLD TANK LI HOT TANK LI	PEN LOSE PEN LOSED EVEL H 134.0 EVEL H 190.0 UPPLY GROUP 02	PCM 1 PCM 1 PCM 1 PCM 1 L 15.0 PCM 3 L 10.0 PCM 3 PCM 3

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01 1161 02 LT161 03 LT201 04 LT221 05 LT291 07 PT180 08 PT181 09 PT182 10 FT101 11 TE102 13 TE180 14 TE181 15 TE182 16 TE183 17 TE184	.7IN XXX RCVI 29.8IN XXX TSS 39.8IN XXX TSS 50.2IN XXX TSS 108.2IN XXX RCVI 0.PSI XXX RCVI 0.PSI XXX RCVI 0.PSI XXX RCVI 108.5F XXX RCVI 178.F XXX B000 178.F XXX RCVI	COLD SUMP HOT SUMP COLD TANK HOT TANK HOT PRESS NILET PRESS COLD SURGE SALT FLOW SURGE TOWN TOWN TOWN TOWN TOWN TOWN TOWN TOWN	TANK LEVEL LEVEL LEVEL LEVEL TANK TANK TANK TANK YENT	70.0 L 70.0 L 134.0 L 134.0 L 1390.0 L 125.1 L 100.0 L	15.0 PCM 3 15.0 PCM 3 15.0 PCM 3 15.0 PCM 3 15.0 PCM 1 10.0 PCM 1 20.0 PCM 1 20.0 PCM 1 20.0 PCM 1 500. PCM 1 500. PCM 1 500. PCM 1 -99. PCM 1 -99. PCM 1
		HUI SURGE HOT SURGE COLD SUMP HOT SUMP CTANK RAKE CTANK RAKE		1070. L 400. L 400. L 400. L 750. L 750. L	

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GROUP 03 27-JUL-84 15:47:45

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01	0.0FF XXX T T	COLD SS COLD S	SUMP ISOLAT PUMP ENABLE PUMP ENABLE SALT	H 190. L	PCM
	94.F XXX 8	300ST PUMP ISS COLD			-99. PCM 3 -99. PCM 3

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01 FCV242 02 FCV242 03 FCV201 04 FCV221 05 PT180 06 OPN.211 09 LT201 10 LT201 10 LT201 11 TE201 12 TE201 13 TE201 14 LT201 15 TE201 15 TE201 16 TE201 17 TE201 17 TE201 18 ZSH242 20 ZSL242 21 ZSH211	0.0FF XXX TSS 29.9IN XXX TSS 39.8IN XXX TSS 39.9IN XXX TSS 39.9IN XXX TSS 39.9IN XXX TSS 58.2IN XXX TSS 594.2PCT XXX TSS 594.2PC	PRPANE HEATER ISULAT COLD SUMP LEVEL H 60.0 L 15.0 PCM 3 HOT SUMP LEVEL H 100.0 L .0 PCM 3 BOOST PUMP DSCHGE H 400. L 275. PCM 3 COLD SUMP ISOLAT PCM 3 COLD SUMP ISOLAT PCM 3 COLD SUMP LEVEL H 60.0 L 15.0 PCM 3 HOT SUMP LEVEL H 60.0 L 15.0 PCM 3 COLD SUMP LEVEL H 41.0 L 15.0 PCM 3 COLD TANK LEVEL H 134.0 L 15.0 PCM 3 CTANK RAKE LOWER H 750. L 500. PCM 3 CTANK RAKE UPPER H 750. L 500. PCM 3 CTANK RAKE UPPER H 750. L 500. PCM 3 HTANK RAKE UPPER H 1070. L 500. PCM 3 HTANK RAKE LOWER H 1070. L 500. PCM 3 HTANK RAKE UPPER H 1070. L 500. PCM 3 HTANK RAKE UPPER H 1070. L 500. PCM 3 HTANK RAKE UPPER H 1070. L 500. PCM 3 PRPANE HEATER ISOLAT PCM 3 PRPANE HEATER ISOLAT PCM 3	
	1.UN XXX 155 0.OFF XXX TSS 1.ON XXX TSS	COLD SUMP ISOLAT PCM 3 COLD SUMP ISOLAT PCM 3 COLD SUMP ISOLAT PCM 3 GROUP 05 27-JUL-84 15:56:17	

01 TE132 02 TE132 03 TE133 04 TE134 05 TE135 06 TE137 08 TE138 09 TE149 10 TE149 11 TE144 12 TE144 13 TE144 15 TE144 15 TE144 16 TE148	98.F 1	XXX RCVR XXX RCVR	PANEL BACK	UPPER H UPPER H UPPER H UPPER H UPPER H MIDDLE H MIDDLE H MIDDLE H MIDDLE H LOWER H	745. L 915. L 915. L 980. L 1045. L 985. L 995. L 1045. L 1035. L	500. PCM 1 500. PCM 1

ØI NEISE		RUNR	COLO SURGE	TANK		500 F COM
02 TE183	473.F	XXX RCVR	HOT SURGE	TANK H	1070. L	500. PCM 1
03 TE185	311.F	XXX RCVR	PASS02 OUTLET	TEMP H	665. L	500. PCM 1
04 TE186	598.F	XXX RCVR	PASS03 OUTLET		690. L	500. PCM 1
05 TE187	237.F	XXX RCVR	PASS04 OUTLET		720. L	500. PCM 1
06 TE188	177.F	XXX RČVR	PASSOS OUTLET		750. E	500. PCM 1
07 TE189	406.F	XXX RČVR	PASSO6 OUTLET		780. L	500. PCM 1
08 TE190	642.F	XXX RČVR	PASS07 OUTLET		810. L	500. PCM 1
09 TE191	337.F	XXX RCVR	PASSOS OUTLET		835. L	500. PCM 1
10 TE192	615.F	XXX RCVR	PASS09 OUTLET		865. L	500: PCM 1
			PASS12 OUTLET		950. L	500. PCM 1
11 TE193	361.F	XXX RCVR				
12 TE194	672.F	XXX RCVR	PASS13 OUTLET		975. L	500. PCM 1
13 TE195	<u>443.F</u>	XXX RCVR	PASS14 OUTLET		990. L	500. PCM 1
14 <u>TE196</u>	655.F	XXX RCVR	PASS15 OUTLE		1010. L	500. PCM 1
15 TE197	343.F	XXX RCVR	PASS16 OUTLE		10 <u>3</u> 0. L	500. PCM 1
16 TE198	566.F	XXX RCVR	PASS17 OUTLE	r temp h	l 1050. L	500. PCM 1

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01 ZSH189 02 ZSH181 03 ZSH182 04 ZSH183 05 ZSH184 06 ZSH185 07 ZSH186 09 ZSH188 10 ZSH189 11 ZSL189 11 ZSL189 12 ZSL181 13 ZSL181 14 ZSL182 14 ZSL183 15 ZSL184 16 ZSL185	0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 0.0FF XXX RCVR 1.0N XXX RCVR 1.0N XXX RCVR 1.0N XXX RCVR 1.0N XXX RCVR 1.0N XXX RCVR	DRAIN NO.2 DRAIN NO.3 DRAIN NO.4 DRAIN NO.5 DRAIN NO.5 DRAIN NO.7 DRAIN NO.9 DRAIN NO.9 DRAIN NO.1 DRAIN NO.1 DRAIN NO.2 DRAIN NO.3 DRAIN NO.3 DRAIN NO.3 DRAIN NO.4 DRAIN NO.5 DRAIN NO.6	OPEN OPEN OPEN OPEN OPEN OPEN OPEN OPEN	PCN 1
14 ZSL183	1.0N XXX RCVR	DRAIN NO.4	CLOSED	PCM 1
15 ZSL184	1.0N XXX RCVR	DRAIN NO.5	CLOSED	PCM 1

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01 25H191 0.0FF XXX RCVR PURGE NO.2 02 ZSH191 0.0FF XXX RCVR PURGE NO.3 04 ZSH192 0.0FF XXX RCVR PURGE NO.4 05 ZSH193 0.0FF XXX RCVR PURGE NO.5 06 ZSH195 0.0FF XXX RCVR PURGE NO.6 07 ZSH196 0.0FF XXX RCVR PURGE NO.7 08 ZSH197 0.0FF XXX RCVR PURGE NO.9 10 ZSL198 1.0N XXX RCVR PURGE NO.9 12 ZSL191 1.0N XXX RCVR PURGE NO.2 12 ZSL192 1.0N XXX RCVR PURGE NO.3 13 ZSL193 1.0N XXX RCVR PURGE NO.5 15 ZSL195 1.0N XXX RCVR PURG	OPEN OPEN OPEN OPEN OPEN OPEN OPEN OPEN
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01 TE103 02 TE103 03 TE104 04 TE105 06 TE109 07 TE109 09 TE110 10 TE113 11 TE115 15 TE116 17 TE118	214.F.F.F.F.F.F.F.F.F.F.F.F.F.F.F.F.F.F.F	RCVR RCVR RCVR RCVR RCVR RCVR RCVR RCVR	PASSOS OUTLET TEMP	640. L 640. L 665. L 720. L 750. L 780. L 835. L 950. L 975. L 975. L 1010. L	500. PCM 1 500. PCM 1
	261.F 282.F 242.F 515.F				

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01 PS281 02 PS281 03 ZSHDR 04 ZSLDR 05 TE286 06 TE180 07 TE101 08 TE102 09 RMAXT 10 RMINT 11 TE140 12 PT181 13 TE211 14 TE181 15 TE184 16 ZSHCSP 17 ZSHCSP 18 ZSHCLP	1.0N TSS 0.0FF XXX RCVR 1.0N XXX RCVR 1.0N XXX RCVR 158.F XXX BOOST 517.F XXX RCVR 249.F XXX RCVR 89.F XXX RCVR 90.F XXX RCVR 205.F XXX RCVR 205.F XXX RCVR 205.F XXX RCVR 205.F XXX RCVR 205.F XXX RCVR 207.F XXX RCVR	SGS AIR SUPPLY CAVITY DOOR OPEN CAVITY DOOR CLOSED COLD PUMP BEARNO PUMP BEARNG TEMP INLET HEADER OUTLET HEADER PANEL MAX TEMP PANEL MAX TEMP PANEL MAX TEMP PANEL BACK MIDDLE INLET PRESS COLD SUMP VENT PUMP SUMP VENT PUMP SUMP VENT SALT BOOST PUMP COLD SALT PUMP COOLNT PUMP	Y 190. L -99. P 190. L -99. P 190. L 500. P 1080. L 500. P 1080. L 500. P 1080. L -99. P 1080. L	
19 LV181 20 LV281 21 FT101 22 TE161 COPY	1.0N XXX 24VDC 1.0N XXX 24VDC .0KLB XXX RCVR 417.F XXX TSS	CONTRL POWER SUPPL' CONTRL POWER SUPPL' SALT FLOW DWNCMR OUTLET TEMP	Ϋ́P	PCM 1 PCM 3 PCM 1 PCM 3

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01 65	F0V201	6.0FF XXX TSS		ALT			15 0 FON 3 PCN 3
02 03	ZSHCSP ZSHBP	0.0FF XXX RCVR	SALT B	300ST	PUNP	400 1	PCM 3
04 05	PT180 FCV151	0.PSI XXX RCVR .0PCT XXX RCVR		PUMP SURGE	DSCHGE H TANK H	400. L 1 <u>00</u> .0 L	275. PCM 3 0 PCM 1
06 07	FCV162 FCV161	.0IN XXX RCVR .0IN XXX RCVR		COLD HOT	Tank H Tank H	70.0 L 70.0 L	15.0 PCM 3 15.0 PCM 3
Ø8 Ø9	FCV199 DRCLSD	0.OFF RCVR 1.ON XXX RS		FILL VALVES	ISOLAT CLOSED		PCM 3 PCM 1
	PÜČLSD PT182	I ÖN XXX RS Ø.PSI XXX RCVR	PURGE V	VALVES BURGE	CLOSED TANK H	180. L	PCN I 10. PCM I
12	LT151	.0IN XXX RCVR	COLD S	SURGE	TANK H	90.0 L	10.0 PCM 1
13	FT101	0.PSI XXX RCVR .0KLB XXX RCVR	SALT F	PRESS FLOW	AUDDI II	125. L 100.0 L	10. PCM 1 20.0 PCM 1
15 16	RS.DRAIN	0.OFF RCVR 0.OFF XXX RCVR	CTANK A DRAIN	AIR	SUPPLY	this is on your the to be west to not the personal to the pers	PCN 1
17 18	RS.FILL RS.MAN	0.OFF XXX RCVR 0.OFF XXX RCVR	FILL UNDER M	MANUAL	CONTRL when	this is on a fect to be were to be	PCM 3
19		750.F XXX RCVR		TEMP	SETPT H	1060. L	700. PČN I

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82 SP. DL .0IN XXX SGS DRUN LEVEL SETPT H 4.0 L -4.0 PCM 3 83 SP. SP 1100 PSI XXX SGS STEAM PRESS SETPT H 1130 L 1070 PCM 3 84 SP. ST 950 F XXX SGS STEAM TEMP SETPT H 1130 L 1070 PCM 3 85 MAN. 301 0.0FF REQUEST MANUAL CONTRL FCV301 PCM 3 96 SP. 381 .0FF REQUEST MANUAL CONTRL FCV321 PCM 3 98 SP. 321 .0FF REQUEST MANUAL SETPT H 100.0 L .0 PCM 3 10 MAN. 331 .0FF REQUEST MANUAL SETPT H 100.0 L .0 PCM 3 11 MAN. 341 .0FF REQUEST MANUAL CONTRL FCV341 PCM 3 12 <th>01 831-81</th> <th>850.F</th> <th>EVAR SALT</th> <th></th> <th>H 870 L</th> <th>788. FCN 3</th>	01 831-81	850.F	EVAR SALT		H 870 L	788. FCN 3
04 SP.ST 950.F XXX SGS STEAM TEMP SETPT H 980. L 920. PCM 3 05 MAN.301 0.0FF REQEST MANUAL CONTRL FCV301 PCM 3 06 SP.301 .0PCT XXX SGS FCV301 MANUAL SETPT H 100.0 L .0 PCM 3 07 MAN.321 90.0FF REQEST MANUAL CONTRL FCV321 PCM 3 09 MAN.331 0.0FF REQEST MANUAL CONTRL FCV331 PCM 3 10 SP.331 9.9PCT XXX SGS FCV331 MANUAL SETPT H 100.0 L .0 PCM 3 11 MAN.341 0.0FF REQEST MANUAL CONTRL FCV341 PCM 3 12 SP.341 .0PCT XXX SGS FCV341 MANUAL SETPT H 100.0 L .0 PCM 3 13 MAN.351 0.0FF REQEST MANUAL SETPT H	02 SP.OL	XXX NIO.	SGS DRUM	LEVEL SETPT	H 4.0 L	-4.0 PCN 3
05 MAN.301 0.0FF REQEST MANUAL CONTRL FCV301 PCM 3 06 SP.301 .0PCT XXX SGS FCV301 MANUAL SETPT H 100.0 L .0 PCM 3 07 MAN.321 0.0FF REQEST MANUAL CONTRL FCV321 PCM 3 08 SP.321 99.7PCT XXX SGS FCV321 MANUAL SETPT H 100.0 L .0 PCM 3 09 MAN.331 0.0FF REQEST MANUAL CONTRL FCV331 PCM 3 10 SP.331 9.9PCT XXX SGS FCV331 MANUAL SETPT H 100.0 L .0 PCM 3 11 MAN.341 0.0FF REQEST MANUAL CONTRL FCV341 PCM 3 12 SP.341 .0PCT XXX SGS FCV341 MANUAL SETPT H 100.0 L .0 PCM 3 13 MAN.351 0.0FF REQEST MANUAL CONTRL FCV351 PCM 3 14 SP.351 .0PCT XXX SGS FCV351 MANUAL SETPT H 100.0 L .0 PCM 3 15 MAN.411 0.0FF REQEST MANUAL CONTRL FCV411 PCM 3 16 SP.411 .0PCT XXX SGS FCV411 MANUAL SETPT H 100.0 L .0 PCM 3 17 MAN.38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 19 MAN.383 0.0FF SGS ELECT HEATER BYPASS </td <td>03 SP.SP AA SP ST</td> <td>1100.PSI XXX 950 E XXX</td> <td>SGS SILAM</td> <td>PRESS SEIPI TEMP CETPT</td> <td>H 1130. L H 900 I</td> <td></td>	03 SP.SP AA SP ST	1100.PSI XXX 950 E XXX	SGS SILAM	PRESS SEIPI TEMP CETPT	H 1130. L H 900 I	
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08 SP.321 99.7PCT XXX SGS FCV321 MANUAL SETPT H 100.0 L .0 PCM 3 09 MAN.331 0.0FF REQEST MANUAL CONTRL FCV331 PCM 3 10 SP.331 9.9PCT XXX SGS FCV331 MANUAL SETPT H 100.0 L .0 PCM 3 11 MAN.341 0.0FF REQEST MANUAL CONTRL FCV341 PCM 3 12 SP.341 .0PCT XXX SGS FCV341 MANUAL SETPT H 100.0 L .0 PCM 3 13 MAN.351 0.0FF REQEST MANUAL CONTRL FCV351 PCM 3 14 SP.351 .0PCT XXX SGS FCV351 MANUAL SETPT H 100.0 L .0 PCM 3 15 MAN.411 0.0FF REQEST MANUAL CONTRL FCV411 PCM 3 16 SP.411 .0PCT XXX SGS FCV411 MANUAL SETPT H 100.0 L .0 PCM 3 17 MAN.38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF	06 SP.301	.0PCT XXX	SGS FCV30:	MANUAL SETPT	H 100.0 L	.0 PCM 3
09 MAN.331 0.0FF REQEST MANUAL CONTRL FCV331 PCM 3 10 SP.331 9.9PCT XXX SGS FCV331 MANUAL SETPT H 100.0 L .0 PCM 3 11 MAN.341 0.0FF REQEST MANUAL CONTRL FCV341 PCM 3 12 SP.341 .0PCT XXX SGS FCV341 MANUAL SETPT H 100.0 L .0 PCM 3 13 MAN.351 0.0FF REQEST MANUAL CONTRL FCV351 PCM 3 14 SP.351 .0PCT XXX SGS FCV351 MANUAL SETPT H 100.0 L .0 PCM 3 15 MAN.411 0.0FF REQEST MANUAL CONTRL FCV411 PCM 3 16 SP.411 .0PCT XXX SGS FCV411 MANUAL SETPT H 100.0 L .0 PCM 3 17 MAN.38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 19 MAN.383 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3		U.UFF 99 JPCT VVV			H 100 0 I	PUN 3 0 PCN 3
11 MAN.341 0.0FF REQEST MANUAL CONTRL FCV341 PCM 3 12 SP.341 .0PCT XXX SGS FCV341 MANUAL SETPT H 100.0 L .0 PCM 3 13 MAN.351 0.0FF REQEST MANUAL CONTRL FCV351 PCM 3 14 SP.351 .0PCT XXX SGS FCV351 MANUAL SETPT H 100.0 L .0 PCM 3 15 MAN.411 0.0FF REQEST MANUAL CONTRL FCV411 PCM 3 16 SP.411 .0PCT XXX SGS FCV411 MANUAL SETPT H 100.0 L .0 PCM 3 17 MAN.38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 19 MAN.383 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3	09 MAN.331	0.OFF	reqest Manuai	CONTRL FCV331		PCM 3
12 SP.341 .0PCT XXX SGS FCV341 MANUAL SETPT H 100.0 L .0 PCM 3 13 MAN.351 0.0FF REQEST MANUAL CONTRL FCV351 PCM 3 14 SP.351 .0PCT XXX SGS FCV351 MANUAL SETPT H 100.0 L .0 PCM 3 15 MAN.411 0.0FF REQEST MANUAL CONTRL FCV411 PCM 3 16 SP.411 .0PCT XXX SGS FCV411 MANUAL SETPT H 100.0 L .0 PCM 3 17 MAN.38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 19 MAN.383 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3			SGS FCV33:	MANUAL SETPT	H 100.0 L	
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15 MAN.411	13 MAN.351	0.0FF	REQEST MANUAI	CONTRL FCV351		PCM 3
16 SP.411 .0PCT XXX SGS FCV411 MANUAL SETPT H 100.0 L .0 PCM 3 17 MAN.38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS EVAP SUPHTR DRAIN PCM 3 19 MAN.383 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3	14 SP.351		SGS FCY35	I MANUAL SETPT	H 100.0 L	
17 MAN.38182 0.0FF SGS EYAP SUPHTR DRAIN PCM 3 18 FCV38182 0.0FF SGS EYAP SUPHTR DRAIN PCM 3 19 MAN.383 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3	16 SP.411				H 100.0 L	
19 MAN.383 0.0FF SGS ELECT HEATER BYPASS PCM 3 20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3	17 MAN.38182	0.OFF	SGS EVAP	SUPHTR DRAIN		PCM 3
20 FCV383 0.0FF SGS ELECT HEATER BYPASS PCM 3 21 MAN.384 0.0FF SGS ELECT HEATER STRTUP PCM 3 22 FCV384 0.0FF SGS ELECT HEATER STRTUP PCM 3		Ø.UFF Ø.OFF	SGS EVAP	SUPHIK UKHIN HEATER RYPACC		PUN 3 PUN 3
22 FCV384 0.OFF SGS ELECT HEATER STRTUP PCM 3	20 FCV 383	0.0FF	SGS ELECT	HEATER BYPASS		PCM 3
CC FLY384 0.0FF 363 ELECT MEHIER STRIUF FLY3	21 MAN.384	0.OFF	SGS ELECT	HEATER STRTUP		PCM 3
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105.F XXX HRFS HIGH PRESS STEAM H 990. L 03 PT383 62.PSI XXX SGS STEAM DRUM PRESS H 1250. L 04 FT411 00KLB XXX HRFS FEED WATER FLOW H 16.00 L 05 FT311 01KLB XXX SGS MAIN STEAM FLOW H 12.60 L 06 FT381 0.LB XXX SGS ATTEMP STEAM FLOW H 2500. L 07 TE332 102.F XXX SGS ATTEMP STEAM FLOW H 2500. L 08 TE331 302.F XXX SGS TURBIN THROTIL TEMP H 990. L 09 PT321 63.PSI XXX SGS SPRHTR STEAM OUTLET H 1200. L 10 PT386 0.PSI XXX SGS STEAM DLIVRY PRESS H 1500. L 11 TE386 97.F XXX SGS STEAM DLIVRY PRESS H 1500. L 12 TE388 304.F XXX SGS FEED WATER TEMP H 1100. L 13 ZT411 .0PCT XXX HRS FEED WATER TEMP H 1100. L 14 ZT331 .0PCT XXX SGS EVAPTR WATER TEMP H 1100. L 15 ZSL384 1.ON XXX SGS ELECT HEATER STRTUP 16 ZSL384 0.OFF XXX SGS ELECT HEATER STRTUP 17 FCV401 18.PSI XXX HRFS FDWATR PUMP PRESS H 1500. L 18 FCV421 140.F XXX HRFS FDWATR TEMP CONTRL H 2500. L 19 FCV432 1.PSI XXX DEATOR OPRING PRESS CONTRL H 400. L 20 FCV432 1.PSI XXX SGS STEAM DLIVRY PRESS H 1150. L 21 FCV491 63.PSI XXX SGS STEAM DLIVRY PRESS H 1150. L 22 LT471 14.71N XXX HRFS DEATOR LEVEL CONTRL H 200. L	850. PCM 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3
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02 TE382 457.F XXX SGS SPRHTR SALT 03 TE301 521.F XXX SGS EVAPTR SALT 04 TE384 511.F XXX SGS EVAPTR SALT 05 PT384 3.PSI XXX SGS EVAPTR SALT 06 FT382 3.13KLB XXX SGS COLD BYPA 07 FT321 4.5KLB XXX SGS TOTAL SALT 08 ZT301 62.6PCT XXX SGS FCV301 VALV 09 ZT321 100.0PCT XXX SGS FCV321 VALV 10 ZT341 .0PCT XXX SGS FCV351 VALV 11 ZT351 .0PCT XXX SGS FCV351 VALV 12 FCV221 39.9IN XXX TSS HOT SUMP 13 FCV201 29.9IN XXX TSS COLD SUMP 14 PT180 0.PSI XXX RCVR BOOST PUMP 15 LT281 49.9IN XXX TSS COLD TANK 17 PT383 58.PSI XXX SGS STEAM DRUM 18 FT311 .0IKLB XXX HRFS FEED WATE 20 LT311 -14.2IN XXX SGS STEAM DRUM 21 TE386 154.F XXX TSS COLD PUMP 22 TE286 <th>FLON H 100.0 L .0 PCM 3 POS H 100.0 L .0 PCM 3 POS H 100.0 L .0 PCM 3 POS H 100.0 L .0 PCM 3 LEVEL H 100.0 L .0 PCM 3 LEVEL H 100.0 L .0 PCM 3 LEVEL H 60.0 L 15.0 PCM 3 LEVEL H 134.0 L 15.0 PCM 3 LEVEL H 190.0 L 10.0 PCM 3 PRESS H 1250. L 950. PCM 3 PRESS H 1250. L 3.20 PCM 3</th>	FLON H 100.0 L .0 PCM 3 POS H 100.0 L .0 PCM 3 POS H 100.0 L .0 PCM 3 POS H 100.0 L .0 PCM 3 LEVEL H 100.0 L .0 PCM 3 LEVEL H 100.0 L .0 PCM 3 LEVEL H 60.0 L 15.0 PCM 3 LEVEL H 134.0 L 15.0 PCM 3 LEVEL H 190.0 L 10.0 PCM 3 PRESS H 1250. L 950. PCM 3 PRESS H 1250. L 3.20 PCM 3
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01 ESH2 02 ESH2 03 ESH3 04 ESH3 05 ESH5 06 MAN. ESH3 07 MAN. ESH3 08 MAN. ESH4 10 EH2. ON 11 EH2. ON 12 EH3. ON 13 EH4. ON 14 EH5. ON 15 MAN. BMCP 18 MAN. 384 17 EH5. ON 18 MAN. 384 19 MAN. 384 20 MAN. 384 21 ECV384 22 ECV384	0.0FF SGS SGS SGS SGS SGS SGS SGS SGS SGS S	ELECT HEATER NO.3 ELECT HEATER NO.4 ELECT HEATER NO.1 ELECT HEATER NO.1 ELECT HEATER NO.2 ELECT HEATER NO.3 ELECT HEATER NO.3 ELECT HEATER NO.4 ELECT HEATER NO.1 ELECT HEATER NO.1 ELECT HEATER NO.2 ELECT HEATER NO.3 ELECT HEATER NO.3 ELECT HEATER NO.4 ELECT HEATER NO.4 ELECT HEATER NO.4 ELECT HEATER NO.5 WATER CIRC PUMP WATER CIRC PUMP BOILER CIRC PUMP BOILER CIRC PUMP ELECT HEATER STRTUP PCMMMMMMMMMMMMMMMMMMMMMMMMMMMMMMMMMMMM	
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01 28-381		EVAP DRAIN	PEN 3
02 ZSL38 1	0.OFF XXX SGS	EVAP DRAIN	PCN 3
03 ZSH382	1.ON XXX SGS	SUPER HEATER DRAIN	PCM 3
04 ZSL382	0.OFF XXX SGS	SUPER HEATER DRAIN	PCM 3
05 ZSH383	0.OFF XXX SGS	ELECT HEATER BYPASS	PCM 3
06 ZSL383	1.ON XXX SGS	ELECT HEATER BYPASS	PCM 3
07 ZSH384	1.ON XXX SGS	ELECT HEATER STRTUP	PCM 3
08 ZSL384	0.OFF XXX SGS	ELECT HEATER STRTUP	PCM 3
09 ZSL491	1.ON XXX HRFS	STEAM SHUT OFF	PCM 3
10 ZT301	62.7PCT XXX SGS	FCV301 VALVE POS H	100.0 L :0 PCN 3
11 ZT321	100.0PCT XXX SGS	FCV321 VALVE POS H	100.0 L .0 PCM 3
12 ZT341	.0PCT XXX SGS	FCV341 VALVE POS H	100.0 L .0 PCM 3
13 21351	. ØPCT XXX SGS	FCV351 VALVE POS H	100.0 L .0 PCM 3

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01	198. F XXX HRFS 198. F XXX HRFS 18. PSI XXX HRFS 140. F XXX HRFS 140. F XXX HRFS 140. F XXX HRFS 140. F XXX HRFS 1. PSI XXX DEATO	DEATUR HEATER DEATUR HEATER DEATUR HEATER FOUNTE PUMP FOUNTE TEMP FOUNTE TEMP STEAM CONTRL R OPRING PRESS	CONTRL H CONTRL H CONTRL H CONTRL H	750. L 750. L 1500. L 2500. L 1200. L 100.0 L 400. L	-300. PCM 2 -300. PCM 2 -300. PCM 2 -300. PCM 2 -300. PCM 2 -300. PCM 2 0 PCM 2 0, PCM 2 PCM 2
10 FCV483 11 FCV484 12 PT401 13 PT432 14 PT482 15 PT481 17 TE481 18 TE482 20 FT482 21 FCV471 22 FCV471	0.0FF HRFS 18.PSI XXX HRFS 1.PSI XXX HRFS 4.PSI XXX HRFS 0.PSI XXX HRFS 16.PSI XXX HRFS 197.F XXX HRFS 196.F XXX HRFS	DEATOR VENT DEATOR VENT FDWATR PUMP DEATOR PRESS SPRAY WATER FDWATR PUMP DEATOR STEAM HIGH PRESS SPRAY WATER SPRAY WATER SPRAY WATER FEED SPRAY DEATOR LEVEL	NO.1 NO.2 PRESS H CONTRL H PRESS H SUPPLY H TEMP H STEAM H TEMP H NATER H CONTRL H	1400. L 250. L 300. L 1230. L 400. L 990. L 160. L 160. L	PCM 2 900. PCM 2 200. PCM 2 100. PCM 2 170. PCM 2 300. PCM 2 850. PCM 2 9. PCM 2

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01 FUP. EN 02 FUP. EN 03 SUP. EN 04 CUP. EN 05 CUP. EN 06 CFP. EN 10 CFP. EN 11 CFP. EN 12 ZSHCWP 14 ZSHCWP 15 ZSHCWP 16 ZSHCWP 16 ZSHCFP 17 ZSHCFP 18 ZSHCFP 19 LT471		HRFS COND HRFS CICL EPGS COOL HRFS DEAT	ENABLE LE WARRENDE LA	PUMP PUMP PUMP PUMP PUMP PUMP	30.0 L	PONTARIA PON
18 ZSHCIP 19 LT471 20 TE582	14.6IN XXX	EPGS COOL HRFS DEAT EPGS COOL	OR LEVEL		30.0 L 100. L	

GROUP 19

01 CF2 02 CF3 04 CF4 05 CF6 EN 05 CF2 EN 10 CF5 EN 11 CF5 EN 12 CF6 EN 12 TE484 14 TE482 15 FT482 16 CFF EN 17 TE451 18 CFF EN 18 CFF EN 19 CFF EN 20 CFF EN 20 CFF EN 21 CFF EN 21 CFF EN 22 CFF EN 22 CFF EN 23 CFF EN 24 CFF EN 25 CFF EN 26 CFF EN 27 CFF EN 27 CFF EN 28 CFF EN 29 CFF EN 20 CFF EN 20 CFF EN 20 CFF EN 21 CFF EN 21 CFF EN 22 CFF EN 23 CFF EN 24 CFF EN 25 CFF EN 26 CFF EN 27 CFF EN 28 CFF EN 28 CFF EN 29 CFF EN 20 CFF EN 20 CFF EN 20 CFF EN 20 CFF EN 21 CFF EN 21 CFF EN 22 CFF EN 23 CFF EN 24 CFF EN 25 CFF EN 26 CFF EN 27 CFF EN 27 CFF EN 28 CFF EN	0.0FF	COOLING TOWER FAINS CF1 ENABLE CF2 ENABLE CF3 ENABLE CF4 ENABLE CF5 ENABLE CF6 ENABLE CF6 ENABLE COOLING TOWER OUTLET H SPRAY WATER FLOW H DEATOR LEVEL CONTRL H DEATOR HEATER CONTRL H SPRAY WATER TEMP H COOLING TOWER FAINS CTF ENABLE COOLING TOWER FAINS	130. L 110. L 160. L 30.0 L 445. L	PCM

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01 (CHIS 02 FCV471	11.9IN XXX HRFS	SENDIES NOTE: SEL DEATOR LEVEL <u>C</u> ON	TRL H 30	.0 L 10	O PCM 2
03 FCV521 04 OH.ON 05 EOP	77.F XXX EPGS 0.0FF EPGS 1.0N EPGS 1.0N EPGS	OIL COOLER TEM OIL HEATER ELECT OIL PUM		7. L	0. PCM 2 PCM 2 PCM 2 PCM 2 PCM 2
06 EOP.EN 07 ZSHEOP 08 PT50!	0.OFF XXX EPGS 0.PSI XXX EPGS	EOP ENABLE ELECT OIL PUN OIL SUPPLY PRE	SS H 41	0. L <u>1</u> 1	0. PCM 2
09 PT531 10 TT521 11 TE582	77.F XXX EPGS 75.F XXX EPGS	HYDRO OIL PRE OIL COOLER TEM COOLNG TOWER DSC	P H 141 HGE H 101	0.L 10	5. PCM 2 0. PCM 2 0. PCM 2
12 AEP 13 AEP.EN 14 ZSHAEP	1.0N EPGS 1.0N EPGS 0.0FF XXX EPGS	AIR XHAUST PUM AEP ENABLE AIR XHAUST PUM	P		Ø. PCM 2 PCM 2 PCM 2 PCM 2
15 PT502 16 CNP 17 CNP.EN	23.9IN XXX EPGS 1.0N EPGS 1.0N EPGS	CONDSR PRESS COND PUMP CNP ENABLE	H 15	.0 L	.0 PCM 2 PCM 2 PCM 2
18 ZSHCNP 19 PT583 20 FCV551	0.0FF XXX EPGS 0.PSI XXX HRFS 0.0FF EPGS	COND PUMP ON COND PUMP OUT COND RECIRC	PUT H 30	0, L 24	PCM 2 0. PCM 2 PCM 2
21 LT511 22 EPS2.RST COPY	18.4IN XXX EPGS 0.0FF EPS	HOT WELL LEV RESET FROM PCM	12	21 84 07:25:4	1.0 PCM 2 PCM 2

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01 ETR 02 ETR 03 PT581 04 TT583 05 ST582 06 FCV501 07 ZSH501 08 ZSL501 09 TVM.OPN	0.0FF EPGS 92.F XXX EPGS 92.F XXX EPGS 9.0FF EPGS 0.0FF XXX EPGS 1.0N XXX EPGS 1.0N XXX EPGS 0.0FF EPGS	EMER TRIP RESTURBIN STEAM PRETURBIN STEAM GEN SPEED TURBIN STOP TURBIN STOP VALUE MOTTURBIN S	SS H H VE VE OR	1500. L 990. L 1270. L	PCM 2 PCM 2 PCM 2 PCM 2 PCM 2 PCM 2 PCM 2 PCM 2
10 TVM.CLS 11 ZT581 12 PT582 13 PT502 14 LT511 15 PT501 16 PT531 17 TT501 18 TE503 20 TE505 21 AZT581 COPY	0.0FF EPGS .0PCT XXX EPGS 2.PSI XXX EPGS 23.9IN XXX EPGS 13.9IN XXX EPGS 1.PSI XXX EPGS 1.PSI XXX EPGS 78.F XXX EPGS 78.F XXX EPGS 78.F XXX EPGS 78.F XXX EPGS .1PCT XXX EPGS .1PCT XXX EPGS	CONDSR PRESS HOT WELL LEY OIL SUPPLY PRE HYDRO OIL PRE TURBIN OUTBD BEA TURBIN OUTBD GEA TURBIN OUTBD GEA GEN OUTBD GEA GEN INBD GEA	SS H SS H SS H SS H SS H SS H SS H SS H	100.0 L 15.0 L 15.0 L 16.0 L 100. L 170. L 170. L 170. L 170. L	PCM 22 9 PCM 22 9 PCM 22 10 PCM 22 110 PCM 22 110 PCM 22 110 PCM 22 110 PCM 22 110 PCM 22

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01 1158 02 E1581 03 ST582 04 ST581 05 IT581 06 PFT581 07 VT581 08 TT507 09 TE508 10 TT510 11 TT511 12 TT512 13 TT513	0. VAC XXX EPGS 0. VAC XXX EPGS 0. RPM XXX EPGS 0. ANP XXX EPGS 1.00LAG XXX EPGS 1.00LAG XXX EPGS 79. F XXX EPGS 78. F XXX EPGS 96. F XXX EPGS 96. F XXX EPGS 97. F XXX EPGS 97. F XXX EPGS	VOLTS GEN SPEED FREQ 5565 HERTZ CURRNT POWER FACTOR VARS 0960 KYARS GEN OUTBD BEARNG GEN AIR TEMP STATOR WINDNG 1 STATOR WINDNG 3 STATOR WINDNG 3 STATOR WINDNG 4	H 480. L H 1270. L H 1200. L H 1200. L H 170. L H 260. L H 260. L H 260. L H 260. L	450. PCM 2 450. PCM 2 0. PCM 2 40.0 PCM 2 0. PCM 2 0. PCM 2 110. PCM 2 -300. PCM 2 0. PCM 2 0. PCM 2
	92.F XXX EPGS 94.F XXX EPGS 93.F XXX EPGS	STATOR WINDNG 4 STATOR WINDNG 5	H 260. L H 260. L H 260. L	

COPY

GROUP 23 27-JUL-84 16:25:31

01	0.0FF EPS EPS EPS EPS 0.0FF XXX RCVR RCVR RCVR RCVR RCVR RCVR RCVR	PUMP SUMP LEVEL SUMP HIGH LEVEL SUMP HIGH LEVEL DRUM LEVEL LO.LO WATER RECIRC PUMP DRUM LEVEL HI.HI MANUAL TRBGEN TRIP OIL PRESS LOW GEN BEARNG TEMP GEN AIR TEMP GEN BRKR TRIP VIBRAT HIGH	PCM 2 PCM 3 PCM 1 PCM 1 PCM 1 PCM 1 PCM 2 PCM 3 PCM 3 PCM 2 PCM 2 PCM 2 PCM 2 PCM 2 PCM 2
2ĭ TR588	0.0FF XXX EPGS	STEAM ENERGY LOW	PČN B

8-32

COPY

GROUP 26 27-JUL-84 16:27:28

01 17.181 0.017 XXX BOOST 0.075 XXX BOOST 0.075 XXX RCVR 0.075 XXX BOOST 0.075 XXX BOOST 0.075 XXX BOOST 0.075 XXX BOOST 0.075 XXX COLD 0.075 XXX XX	PUMP LOW PRESS INLET PRESS LOW TUBE HIGH TEMP HTANK HIGH LEVEL PUMP SUMP LEVEL CONTRL POWER SUPPLY SUMP HIGH LEVEL CONTRL POWER SUPPLY DRUM LEVEL LO.LO WATER RECIRC PUMP K 90 ALARM	PCM 3 PCM 1 PCM 1 PCM 3 PCM 2
--	--	---

This Console operating procedure will be utilized to verify process control integrity prior to all tests. It is unnecessary to verify control integrity of subsystems not used (not applicable). This checklist shall be completed by the control room process console operator.

I.	Test Description		
			Start Time
II.	Responsible operating personnel	Primary	Backup
	Test Conductor (MDAC)	Stan Saloff	
	Heliostat Operator	Arleen Vance	
	Console Operator	Evans/Nelson	
	Operation/Safety Engineer	John Holmes	
	Subsystem Technicians		
	RS	Jerome Griego	
	TSS	Matt Matthews	•
	SGS	Matt Matthews	
	HRFS	Jay Holton	
:	EPGS	Jay Holton	

III.		fety Checklist mplete this checklist for all operations.	0/5
1.	Sf	te occupants	
	Α.	***	
	В.	Communications established to all manned control points	
	c.	Safety equipment in place:	
		1. OSHA protective gloves	
		2. Fire retardant coveralls	
		3. Hard hats/Face shields	
		4. Approved fire extinguishers	
2.	٥2	lar only	
٤.		·	
	A.	"Test In Progress" lights on in the tower	
	В.	Non-Test personnel informed and in secure location	
	c.	Diesel-Generator on and frequency OK	
	D.	Field monitor on call after solar start-up	
	Ε.	Communications established	
	F.	Tower top barricade up	
	G.	Gates closed and posted with red lights or signs	
	н.	Field clear and ready for start-up	
3.	C	ontrol Room locked	
4.		eam up command shall be given only after above hecklist is completed by O/S Engineer	

DESCRIPTION

VERIFICATION

Notice

Four items that impact system start-up significantly and should be verified and/or corrected first are:

- a. Emcon operation
- b. Acurex temperatures
- c. D/D level and temp.
- d. Steam drum level and temp.

IV. MASTER CONTROL SUBSYSTEM

- A. EMCON D/2 HOST START UP CHECKLIST Complete this checklist for all operations.
 - 1. Equipment powered up:
 - a) Host cabinet
 - b) Operator Console 1
 - c) Operator Console 2
 - d) (2) LA-120 Terminals
 - e) VT-100 Terminal
 - f) Tri-log printer
 - 2. Disk Packs (2) installed in drives, disk drives running with "READY" lamp lit.
 - 3. EMCON system booted and "START-UP" command file executed:
 - a) Correct date and time
 - b) Disk unit DLI mounted
 - c) CCM, PCMs loaded (optional)
 - d) EMCON host programs running
 - 1. SPNCOL 5. CONSL2
 2. POWER 6. CONSL1
 - 3. ALRMMX 7. SYSMON
 - 4. ALARMS 8. TRACKR
 - 4. MSSND program executing when data logging display is required on the Auxiliary Data Logging/Display System.
 - 5. Unlock Console to allow activation of operational alarms and Receiver Control Algorithm.
 - 6. Enable general alarms by turning GAL on.

DESCRIPTION

VERIFICATION

В.	ACUREX START-UP CHECKLIST Complete this checklist for all operations using sale	t.
	1. Equipment powered up:	
	a) Host chassis - Autodate Ten/50 b) Electrohome monitor c) GT-100 Terminal d) Texas Instruments 820 RO Terminal	
	2. Tape Cassette loaded in host drive.	
	3. Recent (within 60 minutes) logout of temperatures available on T1 printer.	Last Print Time
	4. Set scan rate to every 60 minutes.	
c.	AUXILIARY DATA LOGGING/DISPLAY SYSTEM Data acquisition checklist completion optional as rec	uired.
	1. Equipment powered up:	
	a) H-P 1000 Cabinet b) H-P 2645 Terminal c) H-P 2621 Terminal d) Tektronix 4014 Terminal e) Tektronix 463 hard-copy unit f) (6) Display CRTs g) Versatec Video Copier h) Versatec Printer i) H-P 7925 Disc Drive	
	 Disk pack installed in drive, disc drive running with "READY" lamp lit. 	
	3. System booted:	
	a) Correct date and timeb) Transfer file IMSRP executed	·
	4. MSPAS program executing when data logging/ display is required and MSSN2 has been started on the EMCON host.	
	5. Following support programs available for execut:	
	a) MSRTP b) MSPSU c) MSDSD d) MSSL1 through MSSL6 e) MSCDT	
	6. Label file used:	
	7. Data file used:	—

	STEP		DESCRIPTION	VERIFICATIO	<u>N</u>
	Ī). NE	TWORK 90 SETUP CHECKLIST operation with SGS.		
		1.	Verify equipment powered up and operational.		
ļ			 a) Bailey PCU b) Operator Interface Drive Unit *c) Keyboard Console *d) Printer 		
		*The	se components may be turned off when not in use.		_
i	٧.	RS +	RECEIVER SUBSYSTEM lete this checklist for operation with Receiver.		
		7.	Verify acceptable limits on winds (less than 30 MPH), solar insolation (above 600 W/m²) and cloud condition (partly cloudy or clear).		_
İ		2.	Verify TV cameras are on and operational.		-
i		3.	Verify the Control Room SCRAM and EPS power supplies behind Weather Monitor Panel are On and set at 24VDC.		
02		4.	Open the Receiver cavity door upon the request of the RS technician for the RS pretest check. Reclose or leave open as required. (DR.OPN/CLS).		
07		5.	Verify Emcon RS header temperatures are above 480°F. (TE-188 inoperable).		
		6.	Verify the Acurex RS trace heaters are operating and the temperatures are above 480°F (Table A). NOTE EXCEPTIONS. If required, heat tracing control can be taken over locally at the module control room.		
		7.	Align/verify the following valve alignment; confirm valve temps are acceptable before moving. (to avoid bellows damage) Coordinate with Receive technician. RCK 'ON' may be used to auto align these, turning itself off when complete.	er	Time
			<u>Valve</u> <u>Description</u> <u>Position</u>	•	
01				SH180-189 Or	
04			FCV-190-198 Purge valves On/Open/N (ZCSP.EN Enable CSP control On BP.EN Enable BP control ON	/SH190-198 Or	1) 09

03

DESCRIPTION

VERIFICATION

- VI. TSS THERMAL STORAGE SUBSYSTEM
 - Complete this checklist for all operations using salt.
 - 1. Verify that the Acurex TSS trace heaters are operating and the temperatures are above 480°F (Table B). NOTE EXCEPTIONS.

 If req'd, heat tracing control can be controlled locally at salt storage control building.

8:55

Time

2. If operating Propane Heater without SGS, verify that these Acurex SGS inlet trace heaters are above 480°F (Ref. Table C):

Channe1	Channel	Local Temp. Verific.
204	255	FCV-241
205	256	Hot Tank inlet line
206	257	
	258	

3. Verify salt levels in storage tanks and sumps are commensurate with test requirements

LT-201 Cold Sump 29,5 in. (60" max)**@ 606 °F (Acurex Chan 124,125)

LT-281 Cold Tank 39.8 in. (40" min)* @ 580 °F (Acurex Chan 110-112)

LT-221 Hot Sump 25.8 in. (43" max)**@ 725 °F (Acurex Chan 126,127)

- LT-291 Hot Tank 32.9 in. @ 32.7 °F (Acurex Chan 134-136)

 *Minimum level req'd to maintain cold sump level during fill operations

 **Maximum levels automatically close FCV-211 and 231 thru Emcon and lockout may overridden by turning OVR3 on. Maximum levels require vent checks; advise technician.
 - 4. Align/verify the following valves for operation with RS, with SGS, & without Propane Heater. Confirm valve temps are accept. before moving. Coordinate with thermal storage technician. TCK 'ON" may be used to auto align these, turning itself off when complete.

Description Valve Position & minute specto 4. 513 6 100 *FCV-151 CST Level Control Man/Closed/怀 Lecked 6. 5.11 6.00 13 02 FCV-161 HST Level Control(Hot) Man/Closed/Nucceed FCV-162 HST Level Control(Cold) Man/Closed/N C -FCV-199 Bypass valve Off/Open /N (ZSH199 on) FCY-201 Cold Sump Level Control Auto/Closed/N SP 23" 04 FCV-211 Cold Sump Isol. (OPN/CLS.211) Closed/Locked (ZSL211 on) Auto/Closed/N SP 20" FCV-221 Hot Sump Level Control FCY-231 Hot Sump Isol. (OPN/CLS.231) Closed/Locked (ZSL231 on) FCV-241 Propane Heater Inlet Man/Closed/Locked 05 FCY-242 Propane Heater Isolation Off/Closed/Locked ~ (ZSL242 on) (MAN on, SP Auto O' FCV-301 Bypass Salt Flow Closed/N 13 FCV-341 Cold Salt Isol. (MAN on, SP Auto O Closed/N FCV-351 Hot Salt Isol. Closed/N (MAN on, SP Auto Of 04 Enable CSP Control CSP.EN On

*Bad signal (blue) can indicate EPS closure. Clear trips and reset EPS1 & EPS3 to regain control.

	·			
STEP	DESCRIPTION	<u>ON</u>	VERIFICATION	
5.	For operation with Propane I of Receiver OR for SGS alone valve alignment of step 4 as	Modify the	·	
	<u>Valve</u>	Position		
02	FCV-151 FCV-161 FCV-162	Locked Locked Man/Open/N		
<u>05</u>	FCY-242	Nuetral		
6.	For operation without SGS, Malignment of step 4 as follows:		N/A	
	<u> Valve</u>	Position		
13	FCV-301 FCV-341	Locked Locked		
04 7.	Verify pump bearing temp's ar (TE 180, 286, & 387 on EMCON)			
	GS - STEAM GENERATION SUBSYSTE omplete this checklist for ope			
1.	Verify that the Acurex SGS tare operating and the temperabove 480°F (Table C). NOTE If required, heat tracing cotaken over locally at the sacontrol building Acurex cabi	atures are EXCEPTIONS. Introl can be It storage		91.30
2.	Align/verify the following veron confirm valve temps are acces coordinate with thermal stores All SGS control valve MAN si (Emcon commands not applicate SCK 'ON' may be used to auto turning itself off when compared to the	pt. before moving. age technician. gnals should be On. le from Net 90) align these,		Time
	Emcon Command	Valve Description	Position	
MAI 13 MAI *MAI	N.321 On/ SP-321 Auto 100% N.331 On/ SP-331 Auto 10% N.38182 On/FCV-38182 On N.384 On/ FCV-384 On N.383 On/ FCV-383 Off	Main Salt Flow Steam Attemp. Salt Drain Circ Htr Supply Circ Htr Bypass	Open 10% Open Open Open Closed	
	P.EN	Enable HSP Control	On	

DESCRIPTION

VERIFICATION

Complete the following steps after completing HRFS startup. (Presuming SGS is in Diurnal Shutdown).

3.	If is	SGS be1	F.W. inlet pipe temp. (Acurex Channel 132) ow 200°F, increase bridge pipe feedwater temperatu	re:
		a)	Verify D/D TE-451 is above 250°F	
		b)	Advise the SGS technician to open the bridge feedwater drain HV-370, then open FCV-411 to 20% (Emcon MAN.411 on/SP Auto 20%)	
		c)	Verify Acurex channel 132 increases above 200°F (Approx 5 min after opening FCY-411)	
		d.	Reclose HV-370 and FCV-411	
4.	If the	drui en o	drum level LT-311 is at 0.0 inches. m level is below 0.0 inches; open HV-488, pen FCV-411 to 20% and fill to 0.0". Close 1 and HV-488 to avoid FW leakage into drum.	
5.	Ver (BV	rify √CP)	that the boiler water circulation pump is running (ZSHBCP). If it is not running:	
	a)	Rev	iew overnight data to determine son and correct.	
	ь)	Star	rt BWCP	
	c)	Stai	rt circulation heater (pulse EHAC.ON)	
6.	exp	eri Insmi	ezing ambient temperatures have been enced, resolve any suspicious instr. itter readings with the SGS technician. otical of all readings until proven.	

DESCRIPTION

VERIFICATION

- VIII. HRFS HEAT REJECTION AND FEEDWATER SUBSYSTEM
 Complete this checklist for all water system operations.
 - Set/Verify the following control devices in the listed positions: HCK 'ON' may be used to auto align these, turning itself off when complete.

	<u>Identifier</u>	Description D/D Press Enable	Command Off (PT-431 control)	Position N/A
call	EN.DTC451	D/D Heater 1 Enable	Off	N/A
up	EN.DTC452	D/D Heater 2 Enable	Off	N/A
	DTC-451	D/D Heater 1	Auto SP 390 or 400°F	Not Enabled
	DTC-452	D/D Heater 2	Auto SP 390 or 400°F	Not Enabled
	FCV-401	FWP Press Recirc	Auto SP 1250 psi	Closed
	FCV-411	· · · · · · · · · · · · · · · · · · ·	MAN.411 On/SP-411 AUTO 0%	Closed
	FCV-421	FWH Steam Supply	Man	Closed
18	FCV-431	D/D Steam Inlet	Auto/Casc to PT-431	Closed
••	PT-431	Steam Line Press	Auto SP 1080 psi	N/A
	PT-432	D/D Press	Auto SP 225 psi	N/A
	FCV-432	SWHX Divert	Auto SP 233 psi	Open to Bypass
	FCV-471	T-G Condensate Return	Auto SP 0%	Closed
	FY-472	CMUP Stroke Positioner		Closed
	FCV-491	SGS Steam Delivery	Auto SP 900 psi	Closed
21	ZSL-501	Main Steam Stop micro	On '	Closed
	TCPMS	EPGS Control Mode	Off (local)	N/A
	CF1.EN	Cooling Fan 1 Enable	On	N/A
	CF2.EN	1 2	On	N/A
20	CF3.EN	3 4 5	On	N/A
	CF4.EN	\ \ 4 \	On	N/A
	CF5.EN	1 15 1	On	N/A
	CF6.EN	A 4 6 4	On	N/A
				
	CFP.EN	•	able On	N/A
	CMP.EN	Cond. Make-up Pump	On On	N/A
19	CWP.EN	Cooling Water Pump	On	N/A
	SWP.EN	Spray Water Pump	∖ On	N/A
	FWP.EN	Feed Water Pump	∳ On	N/A

- IX. EPGS ELECTRIC POWER GENERATION SUBSYSTEM

 Complete this checklist for all turbine-generator operations.
 - 1. Verify RGP Gen Breaker green (open) light is on.
 - 2. Verify that the Sync switch handle has been procured from the MSEE key box if synch is to be completed or observed from the control room.

T/C	DESCRIPTION	ACUREX CHANNEL	T/C	DESCRIPTION	ACUREX CHANNEL
TEH-190	Purge Valve #1	000	TEH-157	Receiver Outlet-Heater R	027
TEH-191	Purge Valve #2	001	TEH-158	Receiver Outlet-Heater R	028
TEH-192	Purge Valve #3	002	TEH-153	Hot Surge Tank Inlet-Heater	N 029
TEH-193	Purge Valve #4	003	TEH-159	Hot Surge Tank Outlet-Heater	N 030
TEH-194	Purge Valve #5	004	TEH-152	Cold Surge Tank Inlet-Heater	0 031
TEH-195	Purge Valve #6	005	TEH-156	Cold Surge Tank-Heater O	032
TEH-196	Purge Valve #7	006	TEH-150	Receiver Inlet-Heater P	033
TEH-197	Purge Valve #8	007	TEH-151	Receiver Inlet-Heater P	034
TEH-198	Purge Valve #9	800	TEH-162	FCY-101-Heater Q	035
TEH-180	Drain Valve #1	009	TEH-163	FCV-102-Heater Q	036
TEH-181	Drain Valve #2	010	TEH-154	Drain Line-Heater T	037
TEH-182	Drain Valve #3	011	TEH-155	Drain Line-Heater T	038
TEH-183	Drain Valve #4	012	TEH-166	Hot Surge-Heater U	039
TEH-184	Drain Valve #5	013	TEH-167	Hot Surge-Heater U	040
TEH-185	Drain Valve #6	014	TEH-164	Cold Surge-Heaster V	041
TEH-186	Drain Valve #7	015 (Bad)	TEH-165	Cold Surge-Heater V	042
TEH-187	Drain Valve #8	016	TEH-131	Riser-Heater H	300
TEH-188	Drain Valve #9	017	TEH-133	Riser-Heater I	301
TEH-189	Drain Valve #10	018	TEH-134	Riser-Heater I	302
TEH-160	Purge Line-Heater S	019	TEH-135	Riser-Heater J	303
TEH-161	Purge Line-Heater S	020	TEH-136	Riser-Heater J	304
TEH-176	Drain Line	021	TEH-130	Downcomer-Heater K	305
TEH-177	Drain Line	022	TEH-132	Downcomer-Heater L	306
TEH-172	Outlet of Pass #1 (Header)	023	TEH-137	Downcomer-Heater M	307
TEH-173	Pass #10	024	TEH-138	Downcomer-Heater M	308
TEH-174	Pass #11	025	TEH-139	Downcomer-Heater L (Skip	309
TEH-175	Pass #18	026			

TABLE A RS HEAT TRACE INSTRUMENTATION

T/C	DESCRIPTION	ACUREX CHANNE		DESCRIPTION	ACURE CHANN
TEH-218	Hot Tank Outlet	(B)100	TEH-207	Boost Pump Outlet - Heater A	122
TEH-216	FCY-211, Line X	(B)101	TEH-208	Boost Pump Outlet - Heater A	123
TEH-219	Hot Sump Outlet	(B)102	TEH-227	Cold Sump	*124
TEH-222	Hot Sump	(B)103	TEH-228	Cold Sump	*125
EH-225	Cold Sump Outlet	104	TEH-220	Hot Sump	(B)*126
TEH-230	Cold Tank Inlet	105	TEH-221	Hot Sump	(B)*127
TEH-201	Boost Sump Drain - Heater D	106	TEH-211	Riser - Storage End - Heater H	128
TEH-202	Cold Pump Outlet - Heater C	107	TEH-241	FCV-151, Heater H	(A)129
TEH-265	Cold Sump Outlet	108	TEH-212	Downcomer - Storage - Heater K	130
TEH-229	Cold Sump Inlet	109	TEH-240	FCV-161, Heaters A-Y, K	131
TEH-233	Cold Tank #1, CT-1 thru 7	*110	TEH-213	Hot Tank #1	*134
EH-234	Cold Tank #2, CT1 thru 7	*111	TEH-214	Hot Tank #2	*135
TEH-235	Cold Tank #3, CT-1 thru 7	*112	TEH-215	Hot Tank #3	*136
TEH-231	FCY-201	113	TEH-217	Cold/Hot Tank Bypass-Heater AA	(A,B)137
TEH-232	Cold Tank Outlet	114	TEH-223	Propane Heater	(A)138
TEH-205	Boost Suump - Heater W	115	TEH-224	Propane Heater	(A)139
TEH-206	Boost Sump - Herater W	116	TEH-236	Cold/Hot Tank Bypass, Heater AA	(A,B)14C
TEH-203	Boost Pump Bypass - Heater E	117	TEH-238	FCV-242	141
PEH-204	Boost Pump Outlet - Heater B	118	TEH-239	Propane Heater Outlet	(A)142
TEH-209	Cold Tank Inlet - Heater F	(B)119			
TEH-210	Cold Tank Bypass - Heater G	120	* Record	for TSS Step 2, stored salt ter	mp's
TEH-237	FCV-162, Heater F	(B)121	(A) Normal	ly not operating during system	operation
		((B) Not re	equired for Propane Heater opera	tion 🖁

TABLE B TSS HEAT TRACE INSTRUMENTATION

233 (Skip) 234 (O.R.)
134 (0.8.)
•
275 (Skip) 277 (O.R.)

^{**}These will normally be below salt freezing temperature (no problem).

TABLE C SGS HEAT TRACE INSTRUMENTATION

^{##}These may be below 480°F - But they should be above
400°F prior to salt flow.

TABLE D GROUP ALARM LIST

					•	
<u>G AL</u>	_ GENER	LAL ALARM	v			
. N M	LT-201	TE-180	TE - 383	TE- \$08	LS-541	LV-28
	LT- 221	TE- 181	387	- 509	PS-281	LV-481
-	LT-281	TE-184	388	- 581	28y-29	LV-N9t
1.5	LT-291	TE-211	TE - 481		TS-501	N90-AL!
	LT-311	TE-231	484		T8-502	
	LT-471	TE-281	486			
	LT-511	TE-286	*··~		aga ang ang	:
			1			;
RAL	RECEIVER	- OPERATIO	WAL ALARI	~		
1					v = 4	
FT-101	LT-151	TE-101	PT-181	RMINT		
	LT-161	TE-102	PT-182	RMAXT		
		TE-161				
SAL	STEAM C	SENERATOR (OPERATIONA	L ALARMS		
		TE-301	TE- 384	PT-321	PT-431	
		TE-331	386	<i>382</i>	432	
		<i>3</i> 32	421	3 83	483	
		TE-382	483	384	•	
				3 86		
PAL	ELECT. POW	er openat	TOUAL ALA	nns		
	ET-581	77-501	7E-505	TT-521	PT-501	PT-531

7E-506

11-507

TT-502

TE-503

TT-587

ST-581

ZSH-AEP

581

583

502

TABLE E MSEE REMOTE OPERATED VALVE ALIGNMENT

		PRETEST			OPERA	ATION	POST	
VALVE	FUNCTION	BASIC FULL SYSTEM	MODIFICATION TO OPERATE I. W/O RECUR 2. W/OR W/O PROPANE HTR	TO OPERATE 1. RECVRONLY -OR- 2. PROPANE	BASIC FULL SYSTEM	MODIFICATION TO OPERATE 1. W/O RECVR -AND- 2. W/PROPANE HTR	TEST	
FCV-101	RECUR FLOW CTRL	O MAN			C CASC SP. SAL	O MAN	O MAN	
FCV-102	RECVR FLOW CTRL	O MAN			© CASE SP.SALT		O MAN	
FCV-151	CST LEVEL CTRL		OL MAN	L MAN (W/HTR)	© CASC LT-151	OL MAN	O MAN	
FCV-161	HST LEVEL CTAL	• MAN	OL MAN	OL MAN	C AUTO	&L MAN	O MAN	
FCV-162	HST LEVEL CTRL	· MAN	O MAN	O MAN (W/ HTR)	9 AUTO .	O MAN	O MAN	
FCV-180-189	RECUR DRAIN	0			•		•	
FCY-190-198	RECUR PURGE	0			•		•	
FCV-501	TURBINE STOP	•		, to the same section	0		6	
FCV-511	HOT WELL OVERFLOW	8			©			
FCV-512	HOTWELL MAKE-UP	ENJALCIOFF (LOCALCHTEL)			ENHLE ON		(LOCAL CHTAL)	
FCV-521	OIL COOLANT FLOW CTRL	AUTO SP 120 F			© AUTO		@ MAN	
FCV-541	CNST MAKE-UP	LOCAL CHTEL			LOCAL CHTRL		LOCAL CHTRL	
FCV-551	CONDENSATE RECIRC	•			8			
FCV-561	TURBINE TRIP	ET OFF			● ETOFF		● ET OFF	
TVM	TURBINE THROTTLE	0		· · · · · · · · · · · · · · · · · · ·	©		•	
						·		
		O L	0	©			-	
		LOCKED	OPEN	CONTROLL	NG			
		CLOSED						
								

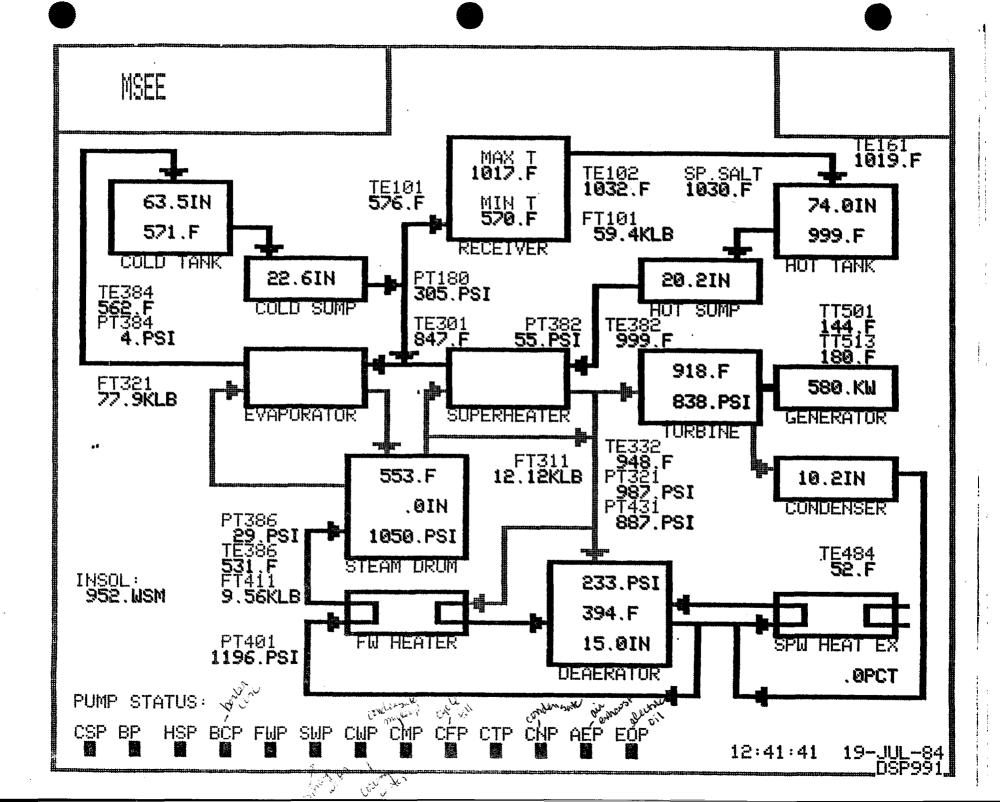
COP	#2	CONTROL	ROOM	POST-TEST	CHECKLIST
.	<i>"</i>	CONTINUE	110011	1001-1601	CHECKE

Test Date 9/22/84

This Console operating procedure will be utilized to secure the process controls following all tests. This checklist shall be completed by the Control Room process console operator.

SIE	SIEP		<u>D</u>	DESCRIPTION					VERIFICATION		
I.	HEL	IOST	AT SI	JBSY ST E	<u>M</u>						
	1.				returned alt, ste		afe conditer)	tion;		 	
II.	RS	RECI	EIVEF	SUBSY	STEM					•	
	1.	Ver	ify t	he fol	lowing v	alve al	ignment:				_
01		FCV-		thru 19		Man/Ope Man/Ope Off/Clo	en osed	(ZSL's		08 09	
02	2.	Veri clos	ify t	he rec	eiver ca on).	vity do	or is full	ly	varaposago esperadoral		- -
	3.				red from complet		cian – pos #4).	st	4- 4		_
III.	TSS	THE	ERMAL	. STORA	GE SUBSY	STEM					
	1.	Veri	ify t	he fol	lowing v	alve al	ignment ir	n MAN:			
02		FCY- FCY- FCY-	-161 -162 -199 -201	Open Open Open Closed	04 04 05 05	FCV-221 FCV-231 FCV-241 FCV-242	Closed/Lo Closed Closed/Lo Closed Closed	ocked v			•
		, CSP .	EN O	ITT, BP	EN UTT,	HSP.EN	Uff				-
	2.				llowing :	salt lev	/els & tem	•			
- _	LT.	-201	Cold	sump_		_in.	0	°F	(Acurex	Chan	124,125)
03	LT	-281	Co1d	tank		fn.	0	°F	(Acurex	Chan	110-112
- -	LT-	-221	Hot	sump _		_in.	0	•F	(Acurex	Chan	126,127)
	LT.	-291	Hot	tank		_in.	@	°F	(Acurex	Chan	134-136)
	3.				cured fro		nician - p 9 #4).	ost			

(Lock-up)



This Console operating procedure will be utilized to verify process control integrity prior to all tests. It is unnecessary to verify control integrity of subsystems not used (not applicable). This checklist shall be completed by the control room process console operator.

I.	Test Description		
			Start Time
11.	Responsible operating personnel	Primary	Backup
	Test Conductor (MDAC)	Stan Saloff	
	Heliostat Operator	Arleen Vance	
	Console Operator	Evans/Nelson	
	Operation/Safety Engineer	John Holmes	
	Subsystem Technicians		
	RS	Jerome Griego	
	TSS	Matt Matthews	
	SGS	Matt Matthews	
	HRFS	Jay Holton	
	EPGS	Jay Holton	

DESCRIPTION

VERIFICATION

- VIII. HRFS HEAT REJECTION AND FEEDWATER SUBSYSTEM

 Complete this checklist for all water system operations.
 - 1. Set/Verify the following control devices in the listed positions: HCK 'ON' may be used to auto align these, turning itself off when complete.

call up —	Identifier GSTAT EN.DTC451 EN.DTC452 DTC-451 DTC-452	Description D/D Press Enable D/D Heater 1 Enable D/D Heater 2 Enable D/D Heater 1 D/D Heater 2	Command Off (PT-431 control) Off Off Auto SP 390 or 400°F Auto SP 390 or 400°F	Position N/A N/A N/A N/A Not Enabled Not Enabled
	FCY-401 FCY-411 FCY-421	FWH Steam Supply	Auto SP 1250 psi MAN.411 On/SP-411 AUTO 0% Man	Closed Closed Closed
18	FCV-431 PT-431 PT-432 FCV-432 FCV-471	D/D Steam Inlet Steam Line Press D/D Press SWHX Divert T-G Condensate Return	Auto/Casc to PT-431 Auto SP 1080 psi Auto SP 225 psi Auto SP 233 psi Auto SP 0%	Closed N/A N/A Open to Bypass Closed
	FY-472 FCV-491	CMUP Stroke Positioner SGS Steam Delivery	Auto SP 0% Auto SP 900 psi	Closed Closed
21	ZSL-501	Main Steam Stop micro	On	Closed
	TCPMS	EPGS Control Mode	Off (local)	N/A
20	CF1.EN CF2.EN CF3.EN CF4.EN CF5.EN CF6.EN	Cooling Fan 1 Enable 2 3 4 5 6	On On On On On On	N/A N/A N/A N/A N/A N/A
19	CFP.EN CMP.EN CWP.EN SWP.EN FWP.EN	Cycle Fill Pump End Cond. Make-up Pump Cooling Water Pump Spray Water Pump Feed Water Pump	able On On On On On	N/A N/A N/A N/A N/A

- IX. EPGS ELECTRIC POWER GENERATION SUBSYSTEM

 Complete this checklist for all turbine-generator operations.
 - 1. Verify RGP Gen Breaker green (open) light is on.
 - 2. Verify that the Sync switch handle has been procured from the MSEE key box if synch is to be completed or observed from the control room.

Telephone numbers for maintenance calls:

MOD COMP

1-800-327-8928 give site number found on sticker on cabinet front panel.

HEWLETT - PACKARD

9-842-1283 give model, serial, and ADP information on attacked sheet.

RAMTEK

on-site spares first, no existing maintenance contract.

DIGITAL (DEC)

9-345-4471 give following information: CPU 11/34A, Serial of No. AG 25174, identify faulty item.

EMC (EMCON)

8-7/3-665-99// give nature of problem to Bob Marian or Jerry Kulbeck

BAILEY (N90)

8-303-757-5408 give nature of problem to Denver office makoney

VERSATEC PRINTER VERSATEC VIDEO COPIER 292-1212 (BFA) give P.O. number 47-4080 and nature of problem.

TECKTRONIX 4014 TEXAS INST TERMINALS

4-3091 (Org. 2617) give nature of problem, terminal type, 5'#, serial number.

dr Hden:

842-1283

the HDP numbers for the equipment that you requested is to put on maintenance are:

Model		Serial number	ADP No.	Prop. No
2113B	DSP	2015A06179	288-45	5263101
2112A	MCS	1611A00666	284-54A	524497
21138	DEV	1737A00225	284-69	524861
21138	L. CYCLE	2020A06523	289-53	52729
Z117F	Bcs	18 10 A 00 132	284-78	52540
Z117F	FCS	2012 A01467	288-45	Sz631

DSP and MCS are covered for 4 hour response, all others are covered for next day response. Systems met listed will be sovered win T&M contracts.

:

TE161 3 -99, \rightarrow 2500.

TE281 3 -99, \rightarrow 2500.

TE291 3 -99, \rightarrow 2500.

TE101 0 -99, \rightarrow 2500.

TE102 0 -99, \rightarrow 2500.

SP.SALT 0 -99, \rightarrow 2500.

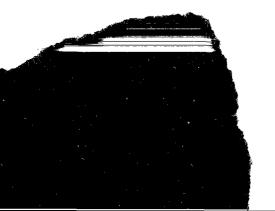
Bob Marion or Jerry

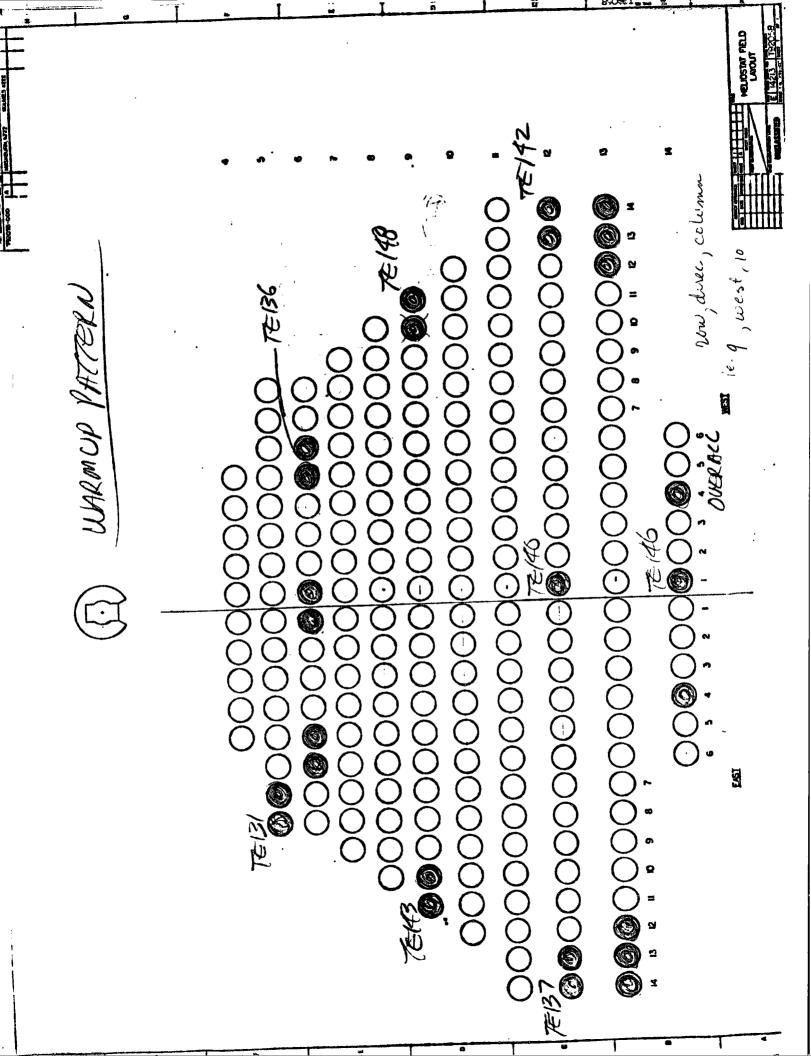
A/B converter card into PCM 1

if it has to be calibrated in place they have to come q do it

4-6360 & leave message

[Exchange cards 15 in Pen 2 3 Pen 2]





Follon this sequence when you get to step #10 of ROP #2

RECEIVER AUTO FILL SEQUENCE CHECKLIST

Step	Description	Verification
1.	Cold Salt Pump ON	
2.	Boost Pump ON	
3.	Boost Pump Discharge Pressure PT-180 to 310 PSI	
4.	FCV-151 OPEN 50%	
5.	TE-161 Responds to Salt	
6.	Salt in Cold Surge Tank	
7.	TE-101 Responds to Salt FT-101 Starts Indicating Flow	
8.	Salt in Hot Surge Tank (when cold surge tank level LT-151 reaches 40-50 inches).	
9.	FCV-199 CLOSED (when hot surge tank level LT-161 reaches 10"	
10.	Drain Valves CLOSED (when hot surge tank level LT-161 reaches 56"	
11.	Purge Valves Sequentially Close (EMCON Group 09)	
12.	Hot Surge Tank Level LT-161 Decrease to 20" With FCV-162 Controlling	
13.	Cold Sump Level Controlling at 20"	
14.	FCV-101/102 Controlling Receiver Salt Flow at 30 Klb/hr	
15.	FCV-151 100% OPEN Increasing Cold Surge Tank Level LT-151 to 80-85"	
16.	Return to Step 26 of Receiver Startup Procedure ROP #2	

- Confirm receiver technician is completing receiver pretest checklist (ROP #1)
- 4. Confirm thermal storage technician is completing TSS pretest checklist (TOP #1)
- 5. Complete control room pretest checklist (COP ♣) Sections I VI #1
- 6. Fill receiver, establish serpentine flow, and transition to extended warm standby mode (ROP #2 Sections 1 35)
 %7
- 7. Increase salt flow to 45 KLB/hr, stabilize and confirm level controls of hot and cold surge tanks and cold sump. \(\) Link at Faller
- 8. Increase salt flow to 60 KLB/hr, restabilize and reconfirm level controls. $(c_5 + r_{col})$
- 9. Increase salt flow to 85 KLB/hr, monitor cold sump level and compare to low alarm level. Reduce flow if necessary and restabilize at a flow rate which allows the sump level to be maintained. Determine the maximum steady state flow rate as limited by the sump supply line.

FT-101 Max steady state flow
LT-281 Cold storage tank level ______

- 10. Reduce flow demand to 30 KLB/hr
- 11. Shut down receiver (ROP#3)

5.2 OPERATIONAL EXERCISES

5.2.1 Receiver Cold Flow

Description

- o Fill receiver
- o Circulate the cold salt through the receiver and back to the cold storage tank
- o Drain receiver

Objectives

- o Introduce the operator to receiver start-up and shutdown operations
- o Familiarize the operator with the receiver loop equipment and controls

Initial System Conditions

- o RS2 Receiver drained with trace heat on
- o TSS2- Hot and cold salt tanks warm and ready for operation
- o SGS not applicable
- o EPGS not applicable

<u>Procedure</u>	<u>Completed</u>
 Advise data system operator to load system data package. 	
2. Advise data system operator to display the	

LT-281	Cold storage tank level
FT-101	Receiver salt flow rate
TE-101	Receiver inlet salt temp
TE-102	Receiver outlet salt temp
LT-151	Cold salt surge tank level
LT-161	Hot salt surge tank level

following on the data display screens:

MCDONNELL DOUGLAS