

A S R - THERMODYNAMICS

RESULTS OF A NUMERICAL SIMULATION AND SURFACE TEMPERATURE MEASUREMENTS

by

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1. NUMERICAL SIMULATION

The computer code HOTREC was used to calculate the thermodynamic behavior of the ASR-Receiver. The code is briefly described in Ref.1. Based on the partial differential equations describing the energy balance for the tube wall, the heat carrier sodium and the ceramic backwall the simulation code has the following characteristics

- 1. Heat conduction in tube wall in radial and in the direction of the circumference.
- 2. Heat transfer to sodium using heat transfer coefficient.
- 3. Radiation exchange between tube surface, ceramic backwall and environment calculated separately in the visible and infrared wavelength. Application of the 'enclosure method' (Ref.2).
- 4. Losses by convection (using correlations of Ref.3).
- 5. Spatial angle dependent heat flux distribution (HEL-IOS) serves as input parameter.

To compare the code with other calculations concerning Ask-Thermodynamics (Ref.3 or Ref.4) steady state conditions has been calculated. The ASR is described in detail elsewhere (Ref.3 and Ref.5). At design point the following results were obtained:

Incident	Power	2760	KW
Absorbed	Power	2486	KW

Fig.1 and Fig.2 represents the corresponding flux density distribution.

Losses

Reflection	116	KW
Convection	80	KW
Emission	78	KW

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Sodium

Inlet Temperature	270	С
Outlet Temperature	530	С
Flow Rate	7.3	kg/sec

The losses by reflection were determined using an effective Emissivity of $\varepsilon_{eff} = 0.9576$. A structured surface like a tube panel produces an effective emissivity which is larger than that of a flat plate. The exact correlation for a tube panel with no space between the tubes would be the solution of a Fredholm-Integral, which analytically is difficult to get. But there is a range in between the effective emissivity has to be (see Ref.10).

$$\varepsilon(1 + (1-\varepsilon)(1-2/\pi)) < \varepsilon_{off} < \varepsilon / (1 - (1-\varepsilon)(1-2/\pi))$$

Assuming $\epsilon = 0.935$ yields $\epsilon_{eff} = 0.957$. This value approximately corresponds to the measurements of R. Carmona (Ref.6). Since the measurement port of the emissivity measurement device is larger than the diameter of one tube, the measured datas are effective emissivities. The losses by emission are based on calculations using an effective emissivity in the infrared wavelenth of $\epsilon_{eff} = 0.9$.

The optical properties of the Pyromark coating are responsible for the amount of absorption and emission. Its high temperature resistance and excellent optical behavior favours Pyromark for solar application. But there is one disadvantage of Pyromark. Its thermal conductivity is very bad compared to metal. As reported in Ref.7 Pyromark 2500 consists of 100 percent silicone resin. The addition of refractory pigments provides the flat black color. By vitrification the silicone resins are converted to inorganic silica producing a thin refractory coating. For silica one finds thermal conductivities reaching from $\lambda = 0.6 - 1.8 \text{ W/m/K}$. Even if the thickness of the coating is very small compared to the tube wall there may be the same temperature gradient through Pyromark as through the tube wall. For the ASR the original thickness of the Pyromark layer was measured, and had an average value of 45 Microns (Ref.8). This yields a higher front surface temperature. As a consequence the losses may be increased a bit (for design conditions approximately 15 KW additional losses). But this doesn't affect the temperature distribution in the tube wall significantly.

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The results of the numerical simulation with HOTREC for design condition are presented in Fig.3 - Fig.8 . Fig.3 -Fig.7 show the heat flux and the temperature profiles along the tube length. Sodium inlet is on the right side sodium outlet on the left. Fig.8 represents the temperature profile in the tube wall of tube no. 98 at 1.7m above the lower aperture rim. Arcus 0 corresponds to the front side of the tube, arcus π to the back side of the tube facing the ceramic backwall. For steady state at design condition a maximum outer metal temperature of T = 597. °C is reached. The results agree essentially with calculations of other simulation codes (Ref.3, Ref.4).

<u>2 MEASSUREMENT OF SURFACE TEMPERATURE BY USING AN</u> INFRARED IMAGING SYSTEM

As a part of the HERMES-System the infrared camera was applied to measure the front surface temperature distribution during the measurement campaign in autumn 1984. The specifications of the camera are described in Ref.1. The thermodynamic and optical properties of the surface affects strongly the surface temperature. Since the measurement is physcally based on infrared radiation a variation in the emissivity results in measurement errors. If the variation of the emissivity is less than 1.5% this yields an error of ± 8 K As there are some more sources of errors (see Ref.1) the sum of them (applying the Gauss-Correlation) yields a total error of ± 10 K.

The intention of the temperature measurements was to get datas about typical operating conditions as there are steady state, transient behaviour, start up, shut down and partial load. In the following some results concerning steady state are presented. The datas were measured on December 12th, 1984. Due to heliostat failures (89 of 93 heliostats were in operation), increased shading and blocking, reduced mirror reflectivity (r=0.8) and insolation (I=800 W/m/m) the power to the receiver is about 40% smaller than for design conditions. Fig.9 shows the isothermal lines of the front surface of the tubes at 9:42:00h solar time. At that time we had steady state conditions. The thermodynamic parameters of the ASR taken from the Class Summery Report of the DAS are listed below: Receiver inlet temperature262.0 CReceiver outlet temperature530.6 CSodium Flow20.9 m**3/h

The surface temperature exceeds 600 °C on the 5th panel. But one has to keep in mind that this is the surface temperature of the Pyromark coating. As mentioned in chapter 1 there is an increased surface temperature of the Pyromark compared to the metal temperature.

The 3D-presentation of the temperature distribution (Fig.10) gives an impression about the shape of the distribution. Fig.11 - Fig.15 show some vertical temperature profiles of the front surface along the tube length. The top of the receiver tubes corresponds to 0.635m the bottom to 3.365m.

Fig. 16 and Fig. 17 represents horizontal temperature profiles. Especially Fig. 16 points out the panel design of th ASR. Panel 1 is on the very left side and has the lowest temperature which approximately is equal to the sodium inlet temperature since the flux density is very small in the lower left edge of the receiver. Panel 5 is characterized by the highest inlet temperature of about 440. C. Fig. 17 is a horizontal cross section of the temperature distribution where the highest surface temperatures occur at 1.86m above the lower aperture rim. There the maximum surface temperature of 626. C was measured on the 5th panel.

Knowing the measured surface temperature distribution the HERMES-Software calculates the losses by infrared emission of the whole receiver and of each panel. Assuming an emissivity in the infrared wavelength range of $\varepsilon_{eff}=0.9$ the losses are:

total em:	ission		102	KW
emission	panel	1	9	KW
	panel	2	9	KW
	panel	3	17	KW
	panel	4	28	KW
	panel	5	39	KW

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3. COMPARISON CALCULATION-MEASUREMENT

To compare the measurements shown in chapter 2 with calculations by HOTREC the meteo, heliostat field and thermodynamic datas belonging to this conditions are used. The calculation provides:

Incident power	1766 KW
Losses	
reflection	75 KW
emission	77 KW
convection	77 KW

The thickness of Pyromark layer was assumed to be 45 Microns the thermal conductivity 0.6 W/m/K. The isothermal lines of the front surface temperature for this calculation is shown in Fig.18 and as a 3D-Presentation in Fig.19. The shape has to be compared with Fig.9 and Fig.10. Obviously the shape of the measurement and the calculation are very similar. A more detailed comparison is presented by Fig.20. Measured and calculated temperature profiles of tube 98 are plotted versus the tube length. Its the calculated and measured Pyromark surface temperature which has to be compared to judge the agreement between calculation and measurement. The maximum value of th measurement is higher than the calculated one. There may be two reasons to explain the difference:

- 1. The thermal conductivity of Pyromark used for the calculation may be smaller than assumed.
- 2. After the refilling incident (September 1983) and the following repair of the distorted tubes some tubes were repainted with Pyromark by brushing and the thickness of the layer might have been increased.

That means both the thickness of the coating and the correct value of the thermal conductivity are necessary and has to be measured.

Regarding the shape of the measured temperature profile there is a dip just above the half of the tube length. This observation fits very well with the emissivity measurements of R.Carmona and M.Geyer (Ref.9). They detected on the 5th panel an emissivity degradation in the same region where the temperature dip occurs. As written above variation of the emissivity is the main error for infrared measurements. But nevertheless there is still a good agreement between calculation and measurement. As a consequence the code HOTREC seems to be a tool to simulate the thermodynamic behavior correctly.

4. HIGH FLUX EXPERIMENT

To achieve flux densities of about 2.5MW/sqm at the SSPS/CRS it is necessary to change the aiming strategy for the ASR. If there is only one aim point at (0.,0.) one gets the flux distribution shown in Fig.21 and Fig.22. Here only Martin-Marietta heliostats are used to concentrate solar radiation on ASR. A maximum flux of 2.48 MW/sqm is reached. This distribution served as input for the simulation code HOTREC to calculate the temperature distribution and efficiency. As a consom quence of the high flux the losses will be reduced a bit. The values are listed below:

Incident power

2868 KW

Losses

reflection	121	KW
emission	77	KW
convection	79	KW

Fig.23 and Fig.24 are showing the temperature profiles of the outer tubes of panel 4. The average metal temperature difference of those two tubes is responsible for the distortion of the panel. For design conditions they were limited to 40 C. Fig.25 represents the expected heat flux and temperature profile along tub 98 where the highest temperature occurs and the focus point is situated. There one has to expect a maximum metal temperature of 685 C and a maximum temperature gradient along the circumference of the tube of 165 C.

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Fig.3: Temperature and Heat Flux vs. Tube Length (Tube 19); Design Conditions; Steady state



Fig.4: Temperature and heat flux vs. tube length (tube 59); Design conditions; steady state.

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Fig.5: Temperature and heat flux vs. tube length (tube 98); design conditions; steady state





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Fig.7: Temperature and heat flux vs. tube length (tube 176); design conditions; steady state.





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680.

Temperature, (Centigrade)

220

12-Dec-84 10:44:43

Weather

Windvel. 4.90 m/s Winddir. 79.92 Degs Humidity 59.26 % Tempert. 12.00 C-Dg

Radiance

Dir.-1 808.20 W/m2 Dir.-2 788.06 W/m2 Diffuse 51.84 W/m2 G1b.Hrz. 367.08 W/m2 G1b.Gdd. 947.14 W/m2

Circumsolar Factor 0.00 %

Sun Location Sol.time 9.69 hrs Elevat. 21.54 Degs Azimuth 325.84 Degs Declin. -23.11 Degs Ascens. 259.75 Degs Longit. 260.58 Degs

(20)





Fig.12: Vertical surface temp. profile (measured); in region of tube 56





lower aperture rim (panel 1 on left side).



Fig.17: Horizontal surface temperature profile (measured by Infrared Camera, HERMES); at 1.86m above lower aperture rim; panel 1 on left side.

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700 Heat Flux (calculated) .8E6 650 W/m/m Centigrade Pyromarl: Surface Temp. (measured by Infrared Camera) Pyromarl Surface Temp. (calculated by HOTREC) 600 .6E6 Distribution Δ 550 Metal Surface Temp. .4E6 (calculated) Temperature Sodium Temp. (calculated) 500 сx С .2E6 Ш 450 400 .0E0 -.5 -1.5.0 .5 1.0 -1.01.5 Tube Length, m

A. M. Constant of March

En That State State Barrier &



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Fig.21: Flux distribution for High Flux Experiment; one aim point (0.,0.) only Martin Marietta heliostats.



Fig.22: Flux distribution for High Flux Experiment; one aim point.

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Isolines of Flux Distribution



Fig.23: Temperature and heat flux profiles vs. tube length (tube 78) for High Flux Experiment; calculated by HOTREC.



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Fig.25: Temperature and heat flux profiles vs. tube length (tube 98) for High Flux Experiment; calculated by HOTREC.

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